

Survey III – Preventative Measures to Address Dust Explosivity Hazards and Powder Handling in the Pharmaceutical Industry

Ayman Allian- Senior Director, Engineering Technology and Process Safety

# Agenda

- Who are we?
- Dust explosivity hazards in the chemical Industry
- Dust explosivity hazards in the pharmaceutical industry
- Survey format and objectives
- Survey format and highlights
- What's in the pipeline?

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### Who are we?

- Pre-competitive group under the-International Consortium for Innovation and Quality in Pharmaceutical
   Development- IQ Consortium is a not-forprofit organization of pharmaceutical and biotechnology companies
- IQ Thermal Hazard Group: Founded 5 years ago to share best practices

#### https://iqconsortium.org/

Eisai, Inc.



#### Current IQ Consortium members include:

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- Information discussed in this presentation were generated from the IQ
   Thermal Hazards WG.

### Who are we?

- Initial focus was on thermal hazards
- Dust explosivity in the pharmaceutical industry
- Driving force
- Dust explosivity hazard is real
- Safety is first, but across the pharmaceutical industry
  - Development timelines are shrinking
  - Low material availability for testing in early phases of development



#### Process Safety in the Pharmaceutical Industry—Part I: Thermal and Reaction Hazard Evaluation Processes and Techniques

Ayman D. Allian,\* Nisha P. Shah, Antonio C. Ferretti, Derek B. Brown, Stanley P. Kolis, and Jeffrey B. Sperry

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- Won ACS Editor award, due to its impact was granted free access around the globe even for non ACS members
- Article is on the list of "Most Read", >30,000 views

Link to the paper

https://pubs.acs.org/doi/10.1021/acs.oprd.0c00226

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# Dust explosivity in the chemical industry

- Metal dust can be a fire and explosion hazard, titanium, copper, and brass particles.
- In the chemical industry 2019, 87% of the global fatalities recorded occurred because of dust explosions
  - Out of these accidents, up to 65% were due to organic dusts.

In the chemical industry Q1 2020, 26 dust explosions occurred worldwide, and 80% of them were caused by organic dusts.

Cloney, C. 2019, Dust Safety Science–Combustible Dust Incident Report, 2019. Cloney, C. 2020, Dust Safety Science–Mid Year Combustible Dust Incident Report, 2020.

# Dust explosivity in the chemical industry

February 2008, Imperial Sugar manufacturing facility in Port Wentworth, Georgia, USA.

14 workers were killed and 36 injured.



Image adopted from: U.S. CHEMICAL SAFETY AND HAZARD INVESTIGATION BOARD, Report No. 2008-05-I-GA, September 2009, SUGAR DUST EXPLOSION and FIRE

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## Solid Handling in the pharmaceutical industry

- 1. Milling in Pharmaceutical industry
  - Control the particle size of APIs
- 2. Charging operations
- 3. Formulation, excipients and blending operations
  - Optimize a drug's delivery and performance
- 4. Packaging

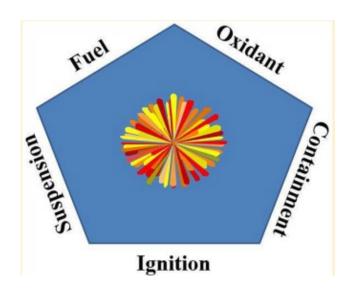


Image adopted from: Nicholas S. Reding and Mark B. Shiflett, *Industrial & Engineering Chemistry Research* **2018** *57* (34), 11473-11482

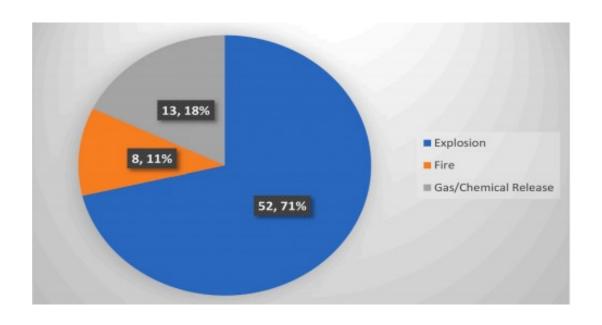
Ralph Zhao, Theodore R. Furman, and Megan Roth, Organic Process Research & Development 2021 25 (11), 2566-2577

## **Explosions in the pharmaceutical industry**

On January 29, 2003, an explosion and fire destroyed the West Pharmaceutical Services plant in Kinston, North Carolina, causing six deaths, dozens of injuries, and hundreds of job losses.



## Process safety incidents in the pharmaceutical industry



- 73 process safety incidents leading to 108 fatalities found between 1985 and 2019
- >70% of the incidents were explosions.

Maaz S. Maniar, Apoorv Kumar, Ray A. Mentzer, Global process safety incidents in the pharmaceutical industry, Journal of Loss Prevention in the Process Industries, Volume 68, 2020.

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# Stages of the drug development process

10,000

250

5

# Stages of the drug development process

10,000

250

5

### **Consensus on definitions**

- Early Stage: Programs conducted in a lab environment, at discovery/MedChem scale.
- Mid-Stage: Progressed from discovery to process research and development, (First In Human) and/or are in process characterization in the development lab, kilo lab and/or pilot plant.

 Late Stage: Progressed from Mid-stage to tech transfer to production facility internally or at a CMO, engineering runs, validation and commercial delivery.

## **Objectives**

- Understanding how pharmaceutical industry addressed dust explosion hazard and understand if approaches and testing are impacted by the phase of development and/or scale of operations.
- There are plethora of tests (MIE, MIT, LIT, Kst, Pmax, volume resistivity, charge decay):
  - Understand how development/manufacturing decisions are made based on test results
  - The survey want to dive into the decision made based on the results.
  - Implication on operation, inertion is required, grounding personnel and equipment
  - The apparatus used and method deployed ASTM, EU and UN.
  - What tests are done internally and what tests are outsourced?
- Sharing best practices and bringing the learning to our own companies.
- Not just helping our own companies, but also the industry at large as we did with the first paper.

## The Survey

- Survey questions were discussed and formulated in the working group
- We have good participation, 11 companies participated. Answers were blinded before analysis
- 18 main questions, but all were somewhat nested resulting in 56 questions total
- Team members from Lilly and Abbvie (Ayman and Zhe) lead the writing, analysis of the data - Zhe retired
  - Team members (Han, Mike, Onkar and Nisha) started to craft a paper
- Target end of Q3/2023 for publication

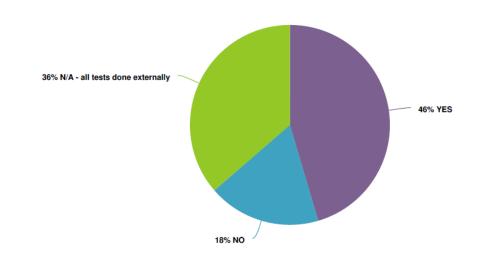
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# If you do testing internally, can your company handle potent compounds? What is a potent compound?

- 5 companies said yes.
- Occupational exposure limits (OELs)
   are regulatory values which indicate
   levels of exposure that are considered
   to be safe (health-based) for a
   chemical substance in the air of a
   workplace
- What is considered potent?
  - OEL<10 μg/m<sup>3</sup>
  - OEL $<5 \mu g/m^3$
  - Two companies indicated that if OEL>1
     μg/m³ testing can be handled

3. If you do testing internally, can your company handle potent compound?



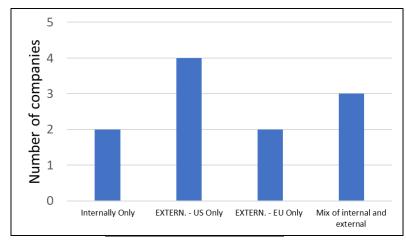
Value	Percent	Responses
YES	45.5%	5
NO	18.2%	2
N/A - all tests done externally	36.4%	4

Totals: 11

## **Minimum Ignition Energy**

Extremely important test: Minimum ignition energy (MIE) can be interpreted as the probability of the occurrence of a combustible dust explosion

- All survey respondents indicate they routinely use the results of the MIE test
- Where they do it
  - Two companies do it internally only
  - Four companies outsource these tests but within the US
  - Two companies outsource it to firms in the EU
  - Remaining pharma companies utilize a host of these options



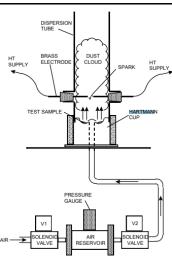
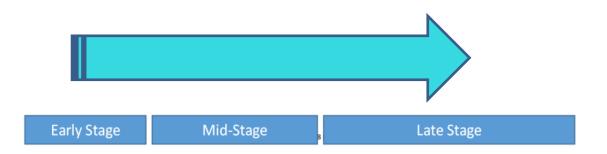


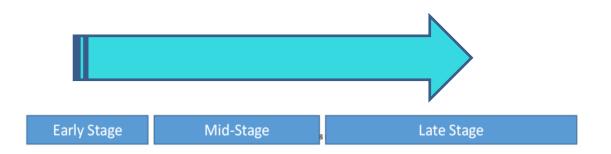
Image adapted from Dust explosion hazards, The United Nations Economic Commission for Europe

## Minimum Ignition Energy- Double Click on it



- Does the stage of development impact when this testing is triggered?
  - Two companies said No
  - No companies do it in the early phase of development
  - 3 in the Mid-Stage
- Is there a mass threshold that your company uses to trigger this test?
  - Eight companies said No
  - Two said yes >5 Kg, 100 Kg

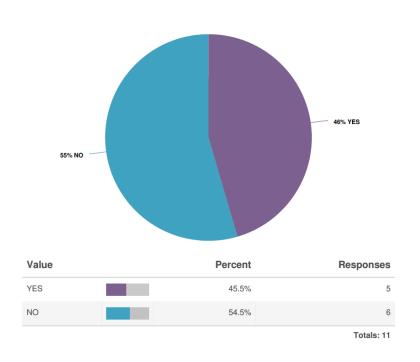
## Minimum Ignition Energy- Double Click on it



- Test apparatus and Standard used
  - 1.2 L Vertical tube (Hartman tube)
  - ASTME2019
  - EN ISO/IEC 80079-20-2:2016 (Clause 8)
- What are the red flags and/or impact of this study?
  - >10 mJ (grounding personnel)
  - >30 mJ would require inertion and grounding

## **Combustible Dust Determination (Initial Screening)**

- Combustible Dust Determination (Initial Screening) –
   Similar to MIE but powerful ignition source is used ~ 5 K
  - Not widely utilized.
  - More than half don't carry out these tests.
  - Done in the Mid-Stage.
- Type of apparatus and method
  - 1.2 L Vertical tube (Hartman tube)
  - ASTME2019
  - EN ISO/IEC 80079-20-2:2016 (Clause 8)
- Red flags: If initial screening test is positive:
  - Consider running full test with more sample.
  - Default to precautions needed for highly ignition sensitive powders.

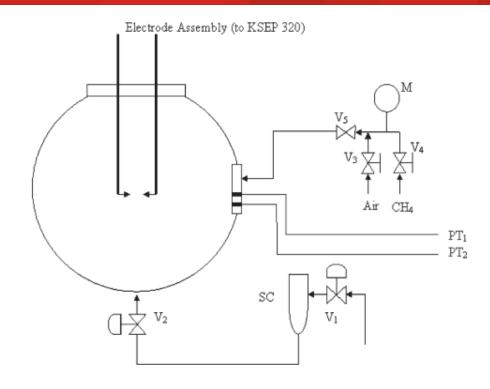


**Dust Explosivity Testing** 

# **Dust Explosibility Characteristics (Kst, Pmax) of Organic Chemical Dusts**

#### **Pmax**

- Maximum explosion overpressure (Pmax)
  - Difference between pressure at the time of ignition (normal pressure) and pressure at the highest point from a dust explosion in the testing chamber
- Provide understanding of the damaging pressures that may be generated during a dust explosion
- Tests conducted typically in 20 L sphere



**Figure 1.** Schematic view of the Siwek 20-L spherical vessels for the determination of dust explosion parameters.

Image adopted from -Combined Effect of Ignition Energy and Initial Turbulence on the Explosion Behavior of Lean Gas/Dust-Air Mixtures Almerinda Di Benedetto, Anita Garcia-Agreda, Paola Russo, and Roberto Sanchirico Industrial & Engineering Chemistry Research 2012 51 (22), 7663-7670

# **Dust Explosibility Characteristics (Kst, Pmax) of Organic Chemical Dusts**

#### Kst

- The dust deflagration index, Kst, is a rates of pressure rise normalized in 1 m<sup>3</sup> vessel
  - St-0, no explosion
  - St-1, 0 < Kst < 200, weak explosion (dust explosion class 1)
  - St-2, 200 < Kst < 300, strong explosion (dust explosion class 2)
  - 300 < Kst, very strong explosion (dust explosion class 3)
- Used to design containment, isolation, explosion protection (e.g., explosion relief venting, explosion suppression .

## **Dust Explosion Severity (Kst, Pmax)**

- Dust Explosion Severity (Kst, Pmax)
  - 10 Companies conduct this test
  - 3 companies have the capability
  - 2 companies do internal testing only
     Available sites for outsourcing
  - 6 US sites are available
  - 4 EU available sites for testing
  - 1 testing center in Asia
- Does the stage of development impact when this testing is triggered?
  - 1 Mid-Stage
  - 9 Late Stage

- Is the test triggered by Mass?
  - 8 No
  - 2 Yes, (>1 Kg, 5 Kg, 10 Kg)
- Type of apparatus and method
  - 20 L sphere
  - EN ISO/IEC 80079-20-2:2016 & EN 14034-2, 14034-1
  - ASTM E1226
- Red flags: Kst = 3 or Pmax > 10 bar:
   Milling not allowed in our plants without technical modifications.

# Minimum Explosivity Concentration (MEC) and Limiting Oxygen Concentration (LOC) of Combustible Dust Clouds

#### **MEC**

- Only half of companies carry out this test
- Two companies have this internal capabilities
- Availability in US (4 companies are utilizing them)

#### LOC

- More than 80% of companies conduct this test
- Only one company has this capabilities internally
- Where are these tests are done
  - 6 firms in the US
  - 3 in EU
  - 1 in Asia

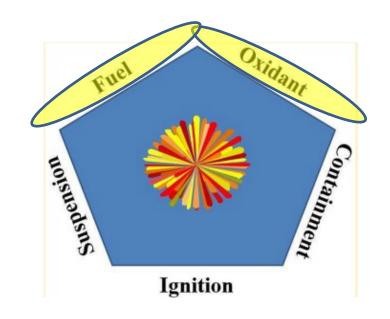


Image adopted from: Nicholas S. Reding and Mark B. Shiflett, *Industrial & Engineering Chemistry*Research **2018** 57 (34), 11473-11482

# Minimum Explosivity Concentration (MEC), Limiting Oxygen Concentration (LOC)

#### **MEC**

- Test triggered by mass
  - No
  - Rarely done unless specifically using as basis of safety. We normally assume a worst case MEC of 20g/m3. In most cases we are well below the worst case MEC
- Type of tests and standard used
  - 20 L Sphere
  - EN 14034-3, ASTM E1515
- Red flags: operation close or above MEC require further action.

#### **LOC**

- Stage triggered, When it is used
  - 0 early stage
  - 0 mid-stage
  - 6 late stage
- Test triggered by mass
  - 8 No
  - Test is triggered when we are required to use inertion based on MIE or other factors.
- Type of tests
  - 20 L Sphere
  - EN 14034-4
- Red flags: If a particularly low LOC was observed (< or = to 5% v/v)</li>

# Minimum Ignition Temperature (MIT) of a Dust Cloud and Layer, Hot Surface, Ignition Temperature of Dust Layer (LIT)

#### MIT

- Widely used, 10 companies, execute these tests
- 4 companies have this internal capability, and two companies rely exclusively on their internal capabilities.
- 6 companies use US based safety labs, 4 Europe and 1 in Asia

#### LIT

- Seven companies conduct this test
- 3 companies have this internal capability and those companies don't outsource these tests.
- Available sites for outsourcing
  - 3 firms in the US
  - 3 in EU
  - 1 in Asia

# Minimum Ignition Temperature (MIT) of a Dust Cloud, Layer, Surface Ignition Temperature (LIT)

### **MIT**

- Stage triggered, When it is used
  - 0 Early Stage, 3 mid-stage, 6 late stage
- Test triggered by mass
  - 8 No, 2 yeses
    - 5 Kg, Milling >1 kg
    - When MIE is triggered, MIT is done (does not take a lot of material)
- Type of tests
  - BAM Oven, Godbert-Greenwald Furnace
  - EN 50281-2-1 & EN ISO/IEC 80079-20-2:2016 (Clause 8.1), ASTM E1491
- Red flags: (1) MIT less than 340°C (2) Less than 300°C "Must be inerted"

#### <u>LIT</u>

- Stage triggered, When it is used
  - 0 early stage, 2 mid-stage, 5 late stage
- Test triggered by mass
  - 6 No, 1 Yes
  - Equipment required.
- Type of tests
  - Hot plate
  - EN 50281-2-1 & EN ISO/IEC 80079-20-2:2016
     (Clause 8.2) and ASTM E2021
- Red flags: LIT is above maximum temp. of equipment in the plant (with safety margin) then it would raise obvious concerns. Less than 300°C must be inerted

## **Static Electricity**

- Walking on the carpet, touching a doorknob (30 mJ)
  - Metal Scope

Materials rub against each other; they may become electrically charged.

Flowing of non-conductive fluid



Lab Scale Model of AFD

Lab AFD: Charles D. Papageorgiou, Christopher Mitchell, Justin L. Quon, Marianne Langston, Suzanna Borg, Frederick Hicks, David am Ende, and Mark Breault, Organic Process Research & Development 2020 24 (2), 242-254

## **Volume Resistivity and Charge Relaxation**

#### Volume Resistivity

- Measures the conductivity of a dust/powder sample.
- 9 companies conduct this tests (Internally and/or externally) with 4 companies having this important capability internally.
- 5 companies use US based safety labs, 2 Europe.

#### Charge Relaxation

- Identifies the electrostatic charge decay time of a dust sample.
- 6 companies conduct this test with 3 companies having this internal capability.
- Companies outsource these tests to 4 US based safety labs.

# Minimum Explosivity Concentration (MEC), Limiting Oxygen Concentration (LOC)

#### **Volume Resistivity**

- Stage triggered
  - 0 Early Stage
  - 1 mid-stage
  - 5 late stage
- Test triggered by mass
  - No
  - Yes, 5 Kg or If MIE < 10 mJ
- Type of tests and standard used
  - High Resistance (Teraohm)
  - EN IEC 60079-32-2 & also EN ISO/IEC 80079-20-2:2016 (Clause 8.4)
- Red flags: The grounding requirements will be stressed for Products with high resistivity.

#### **Charge Relaxation**

- Stage triggered, When it is used
  - 0 early stage
  - 1 mid-stage
  - 3 late stage
- Type of tests
  - Charge Decay Apparatus
  - BS7506 Part 2
- Red flags: After having gone through final processing (filtration, drying and isolation) charged powder must be allowed to relax its charge before further handling.

# Impact Sensitivity and Friction test Red flags from screening tools i.e. DSC or ARC

Impact Sensitivity: <a href="https://www.youtube.com/watch?v=31875ma8k50">https://www.youtube.com/watch?v=31875ma8k50</a>

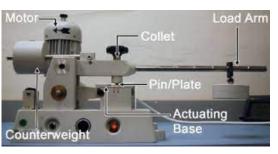
Los Alamos National Lab for explosive understanding

- All 11 companies deploy this test
- 9 companies have this important capability.
- 3 companies use US based safety labs, 2 Europe and 1 in Asia.

#### Friction Sensitivity

- Determine the sensitivity to friction of solid
- 6 companies conduct this test
- 4 companies have this internal capability.





Phillips, J. J., and M. L. Ching. 2020. A comparative study of two BAM designs for friction sensitivity testing of explosives. Propellants, Explosives, Pyrotechnics 45 (4):628–36. doi:10.1002/prep.201900361 SMALL-SCALE IMPACT SENSITIVITY TESTING ON EDC37, Peter C. Hsu and Gary A. Hust and Jon L. Maienschein, 2008.

## **Impact Sensitivity**

- Stage triggered
  - 6 Early Stage
  - 2 mid-stage
  - 1 late stage
- Test triggered by mass
  - No (if triggered, it will be done regardless of mass)
- Type of tests and standard used
  - MP-3 falling hammer Bureau of Mines Impact Apparatus
  - ASTM E680, EN 13631-4
- Red flags: If an audible pop or flame is present material may be removed from process/site orderings if below 30J
- If positive at 10J then material is considered unsafe for isolation at any scale.
- If screening test is positive (40 J energy), external testing required to obtain more precise impact energy

## **Friction Sensitivity**

- Stage triggered
  - 2 Early Stage
  - 3 mid-stage
  - 1 late stage
- Test triggered by mass
  - No (if triggered, it will be done regardless of mass)
- Type of tests and standard used
  - BAM, friction apparatus, Rotary Friction test, Friction sensitivity test
  - EN13631-3 and NATO STANAG 4487 (Explosives), UN Manual of Tests and Criteria for Transportation of Dangerous Goods Test 3(b)(i).
- Red flags: Solids showing a high degree of friction sensitivity must not be scraped or ground, and must be weighed out with a non-metal spatula. Milling must be completely inerted.

## Flash point and Burn rate

#### Flash Point

- Flash point is the lowest temperature at which application of a test flame causes the vapor of a specimen to ignite
- 7 companies conduct these tests
- 3 US sites are available, 1 EU is also utilized.

The Burn Rate UN 4.1: Used to evaluate if solids at hand is flammable Solids. This information is important when for characterizing your material when it comes to transportation.

- 9 companies conduct these tests
- 5 companies have the capability and 4 of those companies conduct the test internally
- 4 US safety firms are available, 2 EU and 1 Asian site

## Flash point and Burn rate

#### **Flash Point**

- Stage triggered
  - 0 Early Stage
  - 4 mid-stage
  - 2 late stage
- Test triggered by mass, mostly No
  - 1 yes, For shipment of potentially flammable liquids or are handling > 5L solutions.
  - For solids containing flammable solvents similar to timing of MIE testing.
- Type of tests and standard used
  - Closed Cup, ASTM D92, EN ISO 2719 (CC)
- Red flags: if material is classified as flammable liquid requires special storage and shipping

#### **Burn Rate**

- Stage triggered, When it is used
  - 0 early stage
  - 4 mid-stage
  - 5 late stage
- Type of tests
  - UN N1
  - EU A.10 Test
- Red flags: If material is classified as flammable solid requires special storage and shipping.

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Transportation and Shipment

### Conclusion

Pharmaceutical industry is very conscious of the dust hazard

Conduct battery of tests internally or at an external sites

- Several tests are not conduct at the early phase
- Engineering control
- Computational and risk assessment tools

## **Thermal Hazard IQ Forum**







**MERCK** 





















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