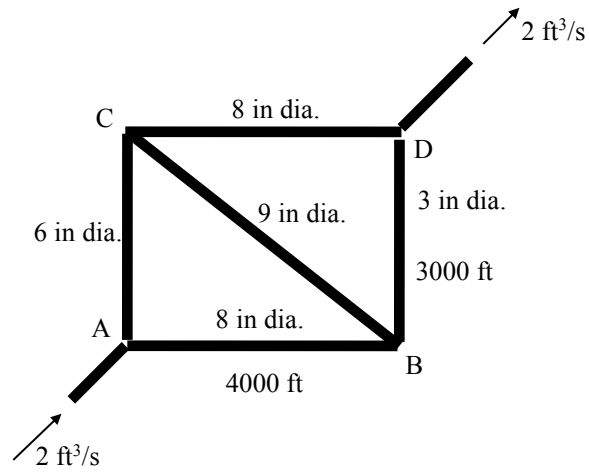


In the five-pipe horizontal network shown in the figure, assume that all pipes have a friction factor  $f=0.025$ . For the given inlet and exit flow rate of  $2 \text{ ft}^3/\text{s}$  of water at  $20^\circ\text{C}$ , determine the flow rate and direction in all pipes. If  $p_A=120 \text{ lb}/\text{in}^2$  (gage), determine the pressures at points B, C, and D.



SOLUTION:

Apply the Extended Bernoulli Equation around the loops ABCA and DBCD.

$$\left( \frac{p}{\rho g} + \alpha \frac{\bar{v}^2}{2g} + z \right)_A = \left( \frac{p}{\rho g} + \alpha \frac{\bar{v}^2}{2g} + z \right)_A - H_{L,ABCA} + H_{S,ABCA} \quad (1)$$

$$\left( \frac{p}{\rho g} + \alpha \frac{\bar{v}^2}{2g} + z \right)_D = \left( \frac{p}{\rho g} + \alpha \frac{\bar{v}^2}{2g} + z \right)_D - H_{L,DBCD} + H_{S,DBCD} \quad (2)$$

Note that the shaft head terms ( $H_{S,ABCA}$  and  $H_{S,DBCD}$ ) are zero since there are no fluid machines in the loops. Simplifying Eqns. (1) and (2) gives:

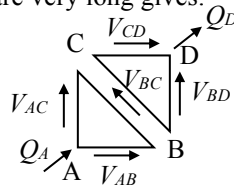
$$H_{L,ABCA} = 0 \quad (3)$$

$$H_{L,DBCD} = 0 \quad (4)$$

Expanding the head loss term and neglecting minor losses since the pipes are very long gives:

$$H_{L,ABCA} = f_{AB} \left( \frac{L_{AB}}{D_{AB}} \right) \frac{\bar{v}_{AB}^2}{2g} + f_{BC} \left( \frac{L_{BC}}{D_{BC}} \right) \frac{\bar{v}_{BC}^2}{2g} - f_{AC} \left( \frac{L_{AC}}{D_{AC}} \right) \frac{\bar{v}_{AC}^2}{2g} = 0 \quad (5)$$

$$H_{L,DBCD} = -f_{BD} \left( \frac{L_{BD}}{D_{BD}} \right) \frac{\bar{v}_{BD}^2}{2g} + f_{BC} \left( \frac{L_{BC}}{D_{BC}} \right) \frac{\bar{v}_{BC}^2}{2g} + f_{CD} \left( \frac{L_{CD}}{D_{CD}} \right) \frac{\bar{v}_{CD}^2}{2g} = 0 \quad (6)$$



Note that particular velocity directions have been assumed in the head loss expressions.

At each pipe node the volumetric flow rate must be conserved (conservation of mass). Hence:

$$\text{at node A: } Q_A = Q_{AB} + Q_{AC} \quad \Rightarrow \quad Q_A = \bar{v}_{AB} \frac{\pi D_{AB}^2}{4} + \bar{v}_{AC} \frac{\pi D_{AC}^2}{4} \quad (7)$$

$$\text{at node B: } Q_{AB} = Q_{BC} + Q_{BD} \quad \Rightarrow \quad \bar{v}_{AB} \frac{\pi D_{AB}^2}{4} = \bar{v}_{BC} \frac{\pi D_{BC}^2}{4} + \bar{v}_{BD} \frac{\pi D_{BD}^2}{4} \quad (8)$$

$$\text{at node C: } Q_{CD} = Q_{AC} + Q_{BC} \quad \Rightarrow \quad \bar{v}_{CD} \frac{\pi D_{CD}^2}{4} = \bar{v}_{AC} \frac{\pi D_{AC}^2}{4} + \bar{v}_{BC} \frac{\pi D_{BC}^2}{4} \quad (9)$$

$$\text{at node D: } Q_D = Q_{BD} + Q_{CD} \quad \Rightarrow \quad Q_D = \bar{v}_{BD} \frac{\pi D_{BD}^2}{4} + \bar{v}_{CD} \frac{\pi D_{CD}^2}{4} \quad (10)$$

Simplify and summarize Eqns. (5) - (10).

$$f_{AB} \left( \frac{L_{AB}}{D_{AB}} \right) \bar{V}_{AB}^2 + f_{BC} \left( \frac{L_{BC}}{D_{BC}} \right) \bar{V}_{BC}^2 - f_{AC} \left( \frac{L_{AC}}{D_{AC}} \right) \bar{V}_{AC}^2 = 0 \quad (11)$$

$$-f_{BD} \left( \frac{L_{BD}}{D_{BD}} \right) \bar{V}_{BD}^2 + f_{BC} \left( \frac{L_{BC}}{D_{BC}} \right) \bar{V}_{BC}^2 + f_{CD} \left( \frac{L_{CD}}{D_{CD}} \right) \bar{V}_{CD}^2 = 0 \quad (12)$$

$$\left( \frac{\pi D_{AB}^2}{4} \right) \bar{V}_{AB} + \left( \frac{\pi D_{AC}^2}{4} \right) \bar{V}_{AC} = Q_A \quad (13)$$

$$\left( \frac{\pi D_{BC}^2}{4} \right) \bar{V}_{BC} + \left( \frac{\pi D_{BD}^2}{4} \right) \bar{V}_{BD} - \left( \frac{\pi D_{AB}^2}{4} \right) \bar{V}_{AB} = 0 \quad (14)$$

$$\left( \frac{\pi D_{AC}^2}{4} \right) \bar{V}_{AC} + \left( \frac{\pi D_{BC}^2}{4} \right) \bar{V}_{BC} - \left( \frac{\pi D_{CD}^2}{4} \right) \bar{V}_{CD} = 0 \quad (15)$$

$$\left( \frac{\pi D_{BD}^2}{4} \right) \bar{V}_{BD} + \left( \frac{\pi D_{CD}^2}{4} \right) \bar{V}_{CD} = Q_D \quad (16)$$

Note that Eqn. (16) is not independent since it can be formed by adding Eqns. (13) and (14), subtracting Eqn. (15) and noting that  $Q_D = Q_A$ . Hence, Eqns. (11) - (15) represent five equations with five unknowns ( $\bar{V}_{AB}$ ,  $\bar{V}_{BC}$ ,  $\bar{V}_{AC}$ ,  $\bar{V}_{BD}$ , and  $\bar{V}_{CD}$ ). Note that  $f_{AB}$ ,  $f_{BC}$ ,  $f_{AC}$ ,  $f_{BD}$ , and  $f_{CD}$  are given in the problem statement along with each pipe's length and diameter and the volumetric flowrate  $Q_A$ .

Using the given data:

$$\begin{aligned} f_{\text{all pipes}} &= 0.025 \\ L_{AB} = L_{CD} &= 4000 \text{ ft} \\ L_{AC} = L_{BD} &= 3000 \text{ ft} \\ L_{BC} &= 5000 \text{ ft (from the Pythagorean theorem)} \\ D_{AB} = D_{CD} &= 8/12 \text{ ft} \\ D_{AC} &= 6/12 \text{ ft} \\ D_{BD} &= 3/12 \text{ ft} \\ D_{BC} &= 9/12 \text{ ft} \\ Q_A &= 2 \text{ ft}^3/\text{s} \end{aligned}$$

The system of non-linear algebraic equations (Eqns. (11) - (15)) can be solved iteratively. One approach is given below.

1. Assume a value of  $\bar{V}_{AB}$ .
2. Solve for  $\bar{V}_{AC}$  using Eqn. (13).
3. Solve for  $\bar{V}_{BC}$  using Eqn. (11).
4. Solve for  $\bar{V}_{CD}$  using Eqn. (15).
5. Solve for  $\bar{V}_{BD}$  using Eqn. (12).
6. Solve for  $\bar{V}_{AB}$  using Eqn. (14).
7. Are the  $\bar{V}_{AB}$  s from step 6 and step 1 equal? If so, then the iterations are finished. If not, then choose a new value for  $\bar{V}_{AB}$  and go to step 2.

After some iteration.

$\bar{V}_{AB} = 3.40 \cdot 10^0 \text{ ft/s}$	$\Rightarrow Q_{AB} = 1.19 \cdot 10^0 \text{ ft}^3/\text{s}$
$\bar{V}_{AC} = 4.14 \cdot 10^0 \text{ ft/s}$	$\Rightarrow Q_{AC} = 8.13 \cdot 10^{-1} \text{ ft}^3/\text{s}$
$\bar{V}_{BC} = 2.24 \cdot 10^0 \text{ ft/s}$	$\Rightarrow Q_{BC} = 9.90 \cdot 10^{-1} \text{ ft}^3/\text{s}$
$\bar{V}_{CD} = 5.17 \cdot 10^0 \text{ ft/s}$	$\Rightarrow Q_{CD} = 1.80 \cdot 10^0 \text{ ft}^3/\text{s}$
$\bar{V}_{BD} = 4.02 \cdot 10^0 \text{ ft/s}$	$\Rightarrow Q_{BD} = 1.97 \cdot 10^{-1} \text{ ft}^3/\text{s}$

To find the pressure at the various nodes, apply the Extended Bernoulli Equation between the nodes.

$$\left( \frac{p}{\rho g} + \alpha \frac{\bar{V}^2}{2g} + z \right)_B = \left( \frac{p}{\rho g} + \alpha \frac{\bar{V}^2}{2g} + z \right)_A - H_{L,AB} + H_{S,AB}$$

where

$$p_A = 120 \text{ psig}$$

$$p_B = ?$$

$$V_A = V_B \text{ (the velocity just upstream of point B is equal to the velocity just downstream of point A)}$$

$$z_A = z_B$$

$$H_{S,AB} = 0$$

$$\rho_{\text{H}_2\text{O}} @ 20^\circ\text{C} = 1.94 \text{ slug/ft}^3 \text{ (Note: } 1 \text{ lbf} = 1 \text{ slug}\cdot\text{ft/s}^2\text{)}$$

$$H_{L,AB} = f_{AB} \left( \frac{L_{AB}}{D_{AB}} \right) \frac{\bar{V}_{AB}^2}{2g}$$

$$\Rightarrow p_B = p_A - \frac{1}{2} \rho \bar{V}_{AB}^2 f_{AB} \left( \frac{L_{AB}}{D_{AB}} \right)$$

$$\boxed{p_B = 1.08 \cdot 10^2 \text{ psig}}$$

Using a similar approach from A to C (or from B to C):

$$\boxed{p_C = 1.03 \cdot 10^2 \text{ psig}}$$

Using a similar approach from B to D (or from C to D):

$$\boxed{p_D = 7.57 \cdot 10^1 \text{ psig}}$$