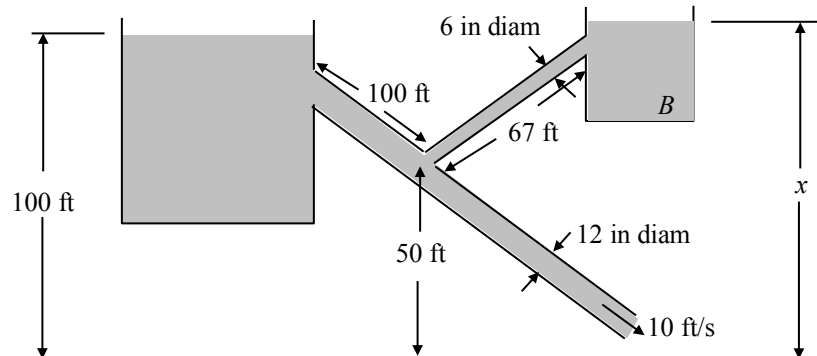
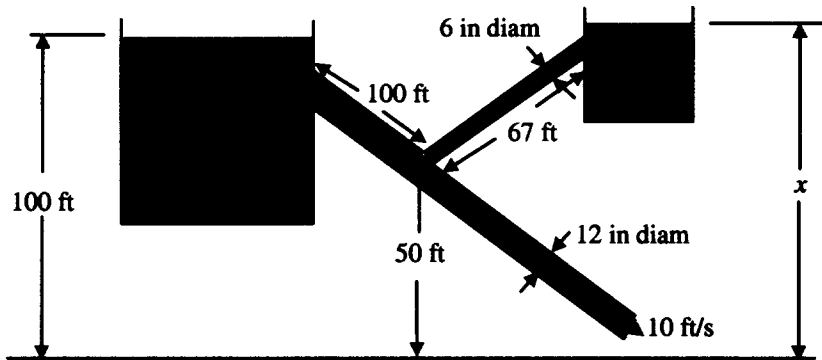


In the water flow system shown, reservoir  $B$  has variable elevation,  $x$ . Determine the water level in reservoir  $B$  so that no water flows into or out of that reservoir. The speed in the 12 in diameter pipe is 10 ft/sec. Assume the pipes are constructed of cast iron and that the entrances are sharp-edged.

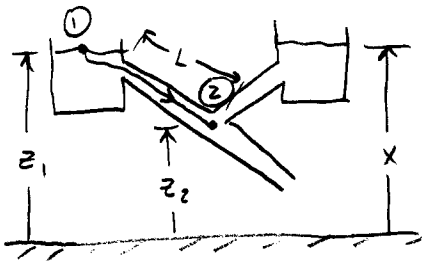


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SOLUTION:

Apply the Extended Bernoulli Eqn from ① to ②:



$$\left( \frac{p}{\rho g} + \alpha \frac{\bar{V}^2}{2g} + z \right)_2 = \left( \frac{p}{\rho g} + \alpha \frac{\bar{V}^2}{2g} + z \right)_1 - H_{L_{1 \rightarrow 2}} + H_{S_{1 \rightarrow 2}}$$

where  $p_1 = 0$  (gage)  
 $p_2 = \rho g(x - z_2)$  (gage) (from hydrostatics)  
 $\bar{V}_2 = 10 \text{ ft/s}$  (assume turbulent flow  $\Rightarrow \alpha_2 \approx 1$ )  
 $\bar{V}_1 \approx 0$   
 $z_1 = 100 \text{ ft}$   
 $z_2 = 50 \text{ ft}$   
 $H_{S_{1 \rightarrow 2}} = 0$

$$H_{L_{1 \rightarrow 2}} = K_{\text{viscous}} \frac{\bar{V}_2^2}{2g} + K_{\text{entrance}} \frac{\bar{V}_2^2}{2g}$$

from tables  $K_{\text{sharp edged entrance}} = 0.5$

where  $K_{\text{viscous}} = f \left( \frac{L}{D} \right)$

with  $f = 0.0195$  (from Moody chart)

$$Re_D = \frac{\bar{V}_2 D}{\nu} = \frac{(10 \text{ ft/s})(1 \text{ ft})}{(1.08 \times 10^{-5} \text{ ft}^2/\text{s})} = 924,000$$

(turbulent flow!)

$$\frac{\epsilon}{D} = \frac{0.00085 \text{ ft}}{1 \text{ ft}} = 0.00085$$

$L = 100 \text{ ft}$   
 $D = 1 \text{ ft}$   
 $\Rightarrow K_{\text{viscous}} = 1.95$

SOLUTION...

• Substitute and simplify:

$$(x - z_2) + \frac{\bar{V}_2^2}{2g} + z_2 = z_1 - (K_{\text{viscous}} + K_{\text{entrance}}) \frac{\bar{V}_2^2}{2g}$$

$$\Rightarrow \underline{x = z_1 - (K_{\text{viscous}} + K_{\text{entrance}} - 1) \frac{\bar{V}_2^2}{2g}}$$

For  $z_1 = 100 \text{ ft}$

$K_{\text{viscous}} = 1.95$

$K_{\text{entrance}} = 0.5$

$\bar{V}_2 = 10 \text{ ft/s}$

$g = 32.2 \text{ ft/s}^2$

NOTE:  
Entrance loss  
is not negligible  
compared to viscous  
loss.

$\Rightarrow \boxed{x = 97.7 \text{ ft}}$