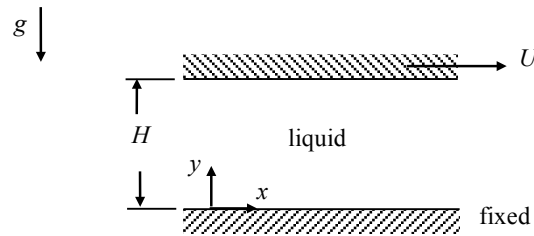


A viscous, incompressible, Newtonian liquid is contained between two infinitely long plates that are separated by a distance,  $H$ . There are no pressure gradients in the horizontal direction. The top plate moves at constant velocity,  $U$ , and the bottom plate is fixed. No pressure gradients are applied in the  $x$ -direction. For a laminar flow, determine:

1. Determine the velocity distribution for this flow. Clearly state all assumptions and boundary conditions.
2. Determine the shear stress acting on the upper wall due to the fluid.



**SOLUTION:**

Make the following assumptions:

1. steady flow  $\Rightarrow \frac{\partial}{\partial t}(\dots) = 0$
2. gravity acts in the  $y$ -direction  $\Rightarrow f_{B,y} = -g, f_{B,x} = 0, f_{B,z} = 0$
3. fully-developed flow in the  $x$ -direction  $\Rightarrow \frac{\partial u_x}{\partial x} = \frac{\partial u_y}{\partial x} = \frac{\partial u_z}{\partial x} = 0$
4. the flow is planar  $\Rightarrow u_z = 0, \frac{\partial}{\partial z}(\dots) = 0$
5. no pressure gradients in the horizontal direction  $\Rightarrow \frac{\partial p}{\partial x} = \frac{\partial p}{\partial z} = 0$

Write the continuity and Navier-Stokes equations in Cartesian coordinates for an incompressible fluid with constant viscosity.

$$\underbrace{\frac{\partial u_x}{\partial x}}_{=0(3)} + \frac{\partial u_y}{\partial y} + \underbrace{\frac{\partial u_z}{\partial z}}_{=0(4)} = 0 \Rightarrow \frac{\partial u_y}{\partial y} = 0$$

From (3) and (4),  $\frac{\partial u_y}{\partial x} = \frac{\partial u_y}{\partial z} = 0 \Rightarrow u_y = \text{constant}$

Since there is no flow through the wall boundaries:  $u_y = 0$  (condition 6)

$$\rho \left( \underbrace{\frac{\partial u_x}{\partial t}}_{=0(1)} + u_x \underbrace{\frac{\partial u_x}{\partial x}}_{=0(3)} + \underbrace{u_y}_{=0(6)} \frac{\partial u_x}{\partial y} + \underbrace{u_z}_{=0(4)} \frac{\partial u_x}{\partial z} \right) = \rho \underbrace{f_{B,x}}_{=0(2)} - \underbrace{\frac{\partial p}{\partial x}}_{=0(5)} + \mu \left( \underbrace{\frac{\partial^2 u_x}{\partial x^2}}_{=0(3)} + \frac{\partial^2 u_x}{\partial y^2} + \underbrace{\frac{\partial^2 u_x}{\partial z^2}}_{=0(4)} \right)$$

$$\rho \left( \underbrace{\frac{\partial u_y}{\partial t}}_{=0(1)} + u_x \underbrace{\frac{\partial u_y}{\partial x}}_{=0(3)} + \underbrace{u_y}_{=0(6)} \frac{\partial u_y}{\partial y} + \underbrace{u_z}_{=0(4)} \frac{\partial u_y}{\partial z} \right) = \rho \underbrace{f_{B,y}}_{=-g(2)} - \frac{\partial p}{\partial y} + \mu \left( \underbrace{\frac{\partial^2 u_y}{\partial x^2}}_{=0(3)} + \underbrace{\frac{\partial^2 u_y}{\partial y^2}}_{=0(6)} + \underbrace{\frac{\partial^2 u_y}{\partial z^2}}_{=0(4)} \right)$$

$$\rho \left( \underbrace{\frac{\partial u_z}{\partial t}}_{=0(1)} + u_x \underbrace{\frac{\partial u_z}{\partial x}}_{=0(3)} + \underbrace{u_y}_{=0(6)} \frac{\partial u_z}{\partial y} + \underbrace{u_z}_{=0(4)} \frac{\partial u_z}{\partial z} \right) = \rho \underbrace{f_{B,z}}_{=0(2)} - \underbrace{\frac{\partial p}{\partial z}}_{=0(5)} + \mu \left( \underbrace{\frac{\partial^2 u_z}{\partial x^2}}_{=0(3)} + \underbrace{\frac{\partial^2 u_z}{\partial y^2}}_{=0(4)} + \underbrace{\frac{\partial^2 u_z}{\partial z^2}}_{=0(4)} \right)$$

Rewriting the momentum equations:

$$\text{x-direction:} \quad \frac{d^2 u_x}{dy^2} = 0$$

$$\text{z-direction:} \quad 0 = 0$$

$$\text{y-direction:} \quad \frac{dp}{dy} = -\rho g$$

Note: Since  $u_x$  is not a fcn of  $x$  or  $z$ , we use a  $d/dy$  instead of  $\partial/\partial y$ .

Integrating the x-direction momentum equation twice:

$$\frac{d^2 u_x}{dy^2} = 0$$

$$\frac{du_x}{dy} = c_1$$

$$u_x = c_1 y + c_2$$

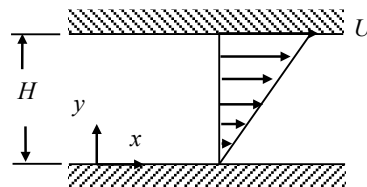
Apply boundary conditions:

no-slip at  $y = 0$ :  $u_x(y=0) = 0 \Rightarrow c_2 = 0$

no-slip at  $y = H$ :  $u_x(y=H) = U \Rightarrow c_1 = \frac{U}{H}$

Thus, the velocity profile is:

$$u_x(y) = U \left( \frac{y}{H} \right)$$



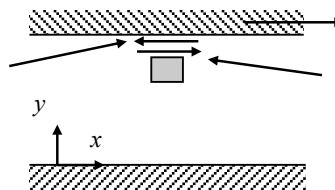
The shear stress that the top wall exerts on the fluid is:

$$\sigma_{yx}(y=H) = \mu \left( \frac{\partial u_x}{\partial y} + \frac{\partial u_y}{\partial x} \right)_{y=H} = \frac{\mu U}{H}$$

From Newton's Third Law, the shear stress the fluid exerts on the wall is:

$$\tau_{\text{on top wall}} = -\frac{\mu U}{H}$$

shear stress acting on wall,  $|\tau_{\text{on top wall}}|$



shear stress acting on fluid element,  $\sigma_{yx}$