

## Incompressible substance model

- Liquids and solids are often approximated as being incompressible
- $v=$ constant
- $u=u(T)$
- $\quad c(T)=c_{v}(T)=c_{p}(T)$
- Textbooks often have tables of specific heat values for solids and liquids.
- From the definition of the specific heats,

$$
\begin{aligned}
& u\left(T_{2}\right)-u\left(T_{1}\right)=\int_{T_{1}}^{T_{2}} c(T) d T \\
& h\left(T_{2}, p_{2}\right)-h\left(T_{1}, p_{1}\right)=u\left(T_{2}\right)-u\left(T_{1}\right)+\left(p_{2}-p_{1}\right) v
\end{aligned}
$$

If $c$ doesn't vary much with temperature (as a rule of thumb, when temperature changes are less than a few hundred Kelvin), then $c \approx$ constant and,

$$
\begin{aligned}
& u\left(T_{2}\right)-u\left(T_{1}\right) \approx c\left(T_{2}-T_{1}\right) \\
& h\left(T_{2}, p_{2}\right)-h\left(T_{1}, p_{1}\right) \approx c\left(T_{2}-T_{1}\right)+\left(p_{2}-p_{1}\right) v
\end{aligned}
$$

For example, for liquid water at 1 bar (abs):


| TABLE A-19 |  |  |  |
| :---: | :---: | :---: | :---: |
| Properties of Selected Solids and Liquids: $\boldsymbol{c}_{p}, \rho$, and $\kappa$ |  |  |  |
| Substance | Specific <br> Heat, $c_{p}$ <br> (kJ/kg $\cdot \mathrm{K}$ ) | Density, $\left(\mathrm{kg} / \mathrm{m}^{3}\right)$ | Thermal Conductivity, $\kappa$ (W/m $\cdot \mathrm{K}$ ) |
| Selected Solids, 300K |  |  |  |
| Aluminum | 0.903 | 2700 | 237 |
| Coal, anthracite | 1.260 | 1350 | 0.26 |
| Copper | 0.385 | 8930 | 401 |
| Granite | 0.775 | 2630 | 2.79 |
| Iron | 0.447 | 7870 | 80.2 |
| Lead | 0.129 | 11300 | 35.3 |
| Sand | 0.800 | 1520 | 0.27 |
| Silver | 0.235 | 10500 | 429 |
| Soil | 1.840 | 2050 | 0.52 |
| Steel (AISI 302) | 0.480 | 8060 | 15.1 |
| Tin | 0.227 | 7310 | 66.6 |
| Building Materials, 300K |  |  |  |
| Brick, common | 0.835 | 1920 | 0.72 |
| Concrete (stone mix) | 0.880 | 2300 | 1.4 |
| Glass, plate | 0.750 | 2500 | 1.4 |
| Hardboard, siding | 1.170 | 640 | 0.094 |
| Limestone | 0.810 | 2320 | 2.15 |
| Plywood | 1.220 | 545 | 0.12 |
| Softwoods (fir, pine) | 1.380 | 510 | 0.12 |
| Insulating Materials, 300K |  |  |  |
| Blanket (glass fiber) | - | 16 | 0.046 |
| Cork | 1.800 | 120 | 0.039 |
| Duct liner (glass fiber, coated) | 0.835 | 32 | 0.038 |
| Polystyrene (extruded) | 1.210 | 55 | 0.027 |
| Vermiculite fill (flakes) | 0.835 | 80 | 0.068 |
| Saturated Liquids |  |  |  |
| Ammonia, 300K | 4.818 | 599.8 | 0.465 |
| Mercury, 300K | 0.139 | 13529 | 8.540 |
| Refrigerant 22, 300K | 1.267 | 1183.1 | 0.085 |
| Refrigerant 134a, 300K | 1.434 | 1199.7 | 0.081 |
| Unused Engine Oil, 300K | 1.909 | 884.1 | 0.145 |
| Water, 275K | 4.211 | 999.9 | 0.574 |
| 300K | 4.179 | 996.5 | 0.613 |
| 325K | 4.182 | 987.1 | 0.645 |
| 350K | 4.195 | 973.5 | 0.668 |
| 375K | 4.220 | 956.8 | 0.681 |
| 400K | 4.256 | 937.4 | 0.688 |

Sources: Drawn from several sources, these data are only representative. Values can vary depending on temperature, purity, moisture content, and other factors.
Table A-19 from Moran et al., Fundamentals of Engineering Thermodynamics, $8^{\text {th }}$ ed., Wiley.

## Ideal Gas Model

- Used to describe the behavior of real gases in the limit of zero pressure and infinite temperature (i.e., zero density). The model does not account for the interaction between molecules of the gas, e.g., inter-molecular forces.
- Equations of state:
$p v=R T$
where $R=\bar{R}_{u} / M$ and $\bar{R}_{u}=8.314 \mathrm{~kJ} /(\mathrm{kmol} . \mathrm{K})$ and $M$ is the molecular weight

$$
M_{\mathrm{air}}=28.98 \mathrm{~kg} / \mathrm{kmol} \Rightarrow R_{\mathrm{air}}=0.287 \mathrm{~kJ} /(\mathrm{kg} . \mathrm{K})
$$

$u=u(T)$ and $h=h(T)$
$\Rightarrow u\left(T_{2}\right)-u\left(T_{1}\right)=\int_{T_{1}}^{T_{2}} c_{v}(T) d T$ and $h\left(T_{2}\right)-h\left(T_{1}\right)=\int_{T_{1}}^{T_{2}} c_{p}(T) d T$
$c_{p}=c_{v}+R$

- $\quad c_{p}(T), c_{v}(T)$, and $k(T)$ for common gases are often given in tables.
- If $c_{v}$ and $c_{p}$ don't vary much with temperature (as a rule of thumb, when temperature changes are less than a few hundred Kelvin at temperatures above $0^{\circ} \mathrm{C}$ ), then $c_{v}$ and $c_{p}$ may be treated as constants and,

$$
\begin{aligned}
& u\left(T_{2}\right)-u\left(T_{1}\right) \approx c_{v}\left(T_{2}-T_{1}\right) \\
& h\left(T_{2}\right)-h\left(T_{1}\right) \approx c_{p}\left(T_{2}-T_{1}\right)
\end{aligned}
$$

An ideal gas with constant specific heats is known as a "perfect gas".
For example, for air:


- Specific heat values for air and other ideal gases are often given in textbook tables.
- Property values for air, taking into account the temperature dependence of the specific heats, are frequently available in tabular form in textbooks.

| TABLE A-20 |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Ideal Gas Specific Heats of Some Common Gases (kJ/kg - K) |  |  |  |  |  |  |  |  |  |  |
| Temp. K | $c_{p}$ | $c_{v}$ | $k$ | $c_{p}$ | $c_{v}$ | $k$ | $c_{p}$ | $c_{v}$ | $k$ | Temp. K |
|  | Air |  |  | Nitrogen, $\mathrm{N}_{2}$ |  |  | Oxygen, $\mathrm{O}_{2}$ |  |  |  |
| 250 | 1.003 | 0.716 | 1.401 | 1.039 | 0.742 | 1.400 | 0.913 | 0.653 | 1.398 | 250 |
| 300 | 1.005 | 0.718 | 1.400 | 1.039 | 0.743 | 1.400 | 0.918 | 0.658 | 1.395 | 300 |
| 350 | 1.008 | 0.721 | 1.398 | 1.041 | 0.744 | 1.399 | 0.928 | 0.668 | 1.389 | 350 |
| 400 | 1.013 | 0.726 | 1.395 | 1.044 | 0.747 | 1.397 | 0.941 | 0.681 | 1.382 | 400 |
| 450 | 1.020 | 0.733 | 1.391 | 1.049 | 0.752 | 1.395 | 0.956 | 0.696 | 1.373 | 450 |
| 500 | 1.029 | 0.742 | 1.387 | 1.056 | 0.759 | 1.391 | 0.972 | 0.712 | 1.365 | 500 |
| 550 | 1.040 | 0.753 | 1.381 | 1.065 | 0.768 | 1.387 | 0.988 | 0.728 | 1.358 | 550 |
| 600 | 1.051 | 0.764 | 1.376 | 1.075 | 0.778 | 1.382 | 1.003 | 0.743 | 1.350 | 600 |
| 650 | 1.063 | 0.776 | 1.370 | 1.086 | 0.789 | 1.376 | 1.017 | 0.758 | 1.343 | 650 |
| 700 | 1.075 | 0.788 | 1.364 | 1.098 | 0.801 | 1.371 | 1.031 | 0.771 | 1.337 | 700 |
| 750 | 1.087 | 0.800 | 1.359 | 1.110 | 0.813 | 1.365 | 1.043 | 0.783 | 1.332 | 750 |
| 800 | 1.099 | 0.812 | 1.354 | 1.121 | 0.825 | 1.360 | 1.054 | 0.794 | 1.327 | 800 |
| 900 | 1.121 | 0.834 | 1.344 | 1.145 | 0.849 | 1.349 | 1.074 | 0.814 | 1.319 | 900 |
| 1000 | 1.142 | 0.855 | 1.336 | 1.167 | 0.870 | 1.341 | 1.090 | 0.830 | 1.313 | 1000 |
| Temp. K | Carbon <br> Dioxide, $\mathrm{CO}_{2}$ |  |  | Carbon Monoxide, CO |  |  | Hydrogen, $\mathrm{H}_{2}$ |  |  | Temp. K |
| 250 | 0.791 | 0.602 | 1.314 | 1.039 | 0.743 | 1.400 | 14.051 | 9.927 | 1.416 | 250 |
| 300 | 0.846 | 0.657 | 1.288 | 1.040 | 0.744 | 1.399 | 14.307 | 10.183 | 1.405 | 300 |
| 350 | 0.895 | 0.706 | 1.268 | 1.043 | 0.746 | 1.398 | 14.427 | 10.302 | 1.400 | 350 |
| 400 | 0.939 | 0.750 | 1.252 | 1.047 | 0.751 | 1.395 | 14.476 | 10.352 | 1.398 | 400 |
| 450 | 0.978 | 0.790 | 1.239 | 1.054 | 0.757 | 1.392 | 14.501 | 10.377 | 1.398 | 450 |
| 500 | 1.014 | 0.825 | 1.229 | 1.063 | 0.767 | 1.387 | 14.513 | 10.389 | 1.397 | 500 |
| 550 | 1.046 | 0.857 | 1.220 | 1.075 | 0.778 | 1.382 | 14.530 | 10.405 | 1.396 | 550 |
| 600 | 1.075 | 0.886 | 1.213 | 1.087 | 0.790 | 1.376 | 14.546 | 10.422 | 1.396 | 600 |
| 650 | 1.102 | 0.913 | 1.207 | 1.100 | 0.803 | 1.370 | 14.571 | 10.447 | 1.395 | 650 |
| 700 | 1.126 | 0.937 | 1.202 | 1.113 | 0.816 | 1.364 | 14.604 | 10.480 | 1.394 | 700 |
| 750 | 1.148 | 0.959 | 1.197 | 1.126 | 0.829 | 1.358 | 14.645 | 10.521 | 1.392 | 750 |
| 800 | 1.169 | 0.980 | 1.193 | 1.139 | 0.842 | 1.353 | 14.695 | 10.570 | 1.390 | 800 |
| 900 | 1.204 | 1.015 | 1.186 | 1.163 | 0.866 | 1.343 | 14.822 | 10.698 | 1.385 | 900 |
| 1000 | 1.234 | 1.045 | 1.181 | 1.185 | 0.888 | 1.335 | 14.983 | 10.859 | 1.380 | 1000 |

Source: Adapted from K. Wark, Thermodynamics, 4th ed., McGraw-Hill, New York, 1983, as based on "Tables of Thermal Properties of Gases," NBS Circular 564, 1955.
Table A-20 from Moran et al., Fundamentals of Engineering Thermodynamics, $8^{\text {th }}$ ed., Wiley.

Ideal Gas Table for air.

| Temp. $[\mathrm{K}]$ | $\mathrm{h}[\mathrm{kJ} / \mathrm{kg}]$ | $\mathrm{u}[\mathrm{k} / \mathrm{kg}]$ | $\mathrm{s}^{\bullet}[\mathrm{kJ} / \mathrm{kg} / \mathrm{K}]$ | pr | vr |
| :---: | :---: | :---: | :---: | :---: | :---: |
| 200 | 200.0 | 142.5 | 1.309 | 0.3363 | 1707.0 |
| 210 | 210.0 | 149.7 | 1.352 | 0.3987 | 1512.0 |
| 220 | 220.0 | 156.8 | 1.395 | 0.4690 | 1346.0 |
| 230 | 230.0 | 164.0 | 1.437 | 0.5477 | 1205.0 |
| 240 | 240.0 | 171.1 | 1.479 | 0.6355 | 1084.0 |
| 250 | 250.0 | 178.3 | 1.520 | 0.7329 | 979.0 |
| 260 | 260.0 | 185.4 | 1.559 | 0.8405 | 887.8 |
| 270 | 270.0 | 192.6 | 1.597 | 0.9590 | 808.0 |
| 280 | 280.1 | 199.8 | 1.633 | 1.0889 | 738.0 |
| 285 | 285.1 | 203.3 | 1.651 | 1.1584 | 706.1 |
| 290 | 290.1 | 206.9 | 1.669 | 1.2311 | 676.1 |
| 295 | 295.1 | 210.5 | 1.686 | 1.3068 | 647.9 |
| 300 | 300.1 | 214.1 | 1.703 | 1.3860 | 621.2 |
| 305 | 305.2 | 217.7 | 1.719 | 1.4686 | 596.0 |
| 310 | 310.2 | 221.2 | 1.736 | 1.5546 | 572.3 |
| 315 | 315.2 | 224.8 | 1.752 | 1.6442 | 549.8 |
| 320 | 320.2 | 228.4 | 1.768 | 1.7375 | 528.6 |
| 325 | 325.3 | 232.0 | 1.783 | 1.8345 | 508.4 |
| 330 | 330.3 | 235.6 | 1.799 | 1.9352 | 489.4 |

Carbon Dioxide ( $\mathrm{CO}_{2}$ )

| Temp. [ K$]$ | $\mathrm{h}[\mathrm{k} / \mathrm{kmol}]$ | $\mathrm{u}[\mathrm{kJ} / \mathrm{kmol}]$ | $\mathrm{s}^{*}[\mathrm{~kJ} / \mathrm{kmol} / \mathrm{K}]$ |
| :---: | :---: | :---: | :---: |
| 0 | 0.0 | 0.0 | 0.000 |
| 220 | 6601.0 | 4772.0 | 203.100 |
| 230 | 6937.0 | 5026.0 | 204.600 |
| 240 | 7278.0 | 5284.0 | 206.000 |
| 250 | 7625.0 | 5547.0 | 207.400 |
| 260 | 7976.0 | 5815.0 | 208.800 |
| 270 | 8332.0 | 6088.0 | 210.200 |
| 280 | 8693.0 | 6366.0 | 211.500 |
| 285 | 8875.0 | 6506.0 | 212.100 |
| 290 | 9058.0 | 6648.0 | 212.800 |
| 295 | 9242.0 | 6791.0 | 213.400 |
| 300 | 9428.0 | 6935.0 | 214.000 |
| 305 | 9615.0 | 7080.0 | 214.600 |
| 310 | 9802.0 | 7226.0 | 215.200 |
| 315 | 9991.0 | 7373.0 | 215.800 |

Note: To convert from $\mathrm{kJ} / \mathrm{kmol}$ to $\mathrm{kJ} / \mathrm{kg}$, divide by the molecular mass of the gas, e.g., $M_{\mathrm{C}}=12.0107$ $\mathrm{kg} / \mathrm{kmol}$ and $M_{\mathrm{O}}=15.999 \mathrm{~kg} / \mathrm{kmol}=>M_{\mathrm{CO} 2}=12.0107+2 * 15.999 \mathrm{~kg} / \mathrm{kmol}=44.01 \mathrm{~kg} / \mathrm{kmol}$,

$$
h_{@ 220 K}=\frac{6601.0 \frac{\mathrm{~kJ}}{\mathrm{kmol}}}{44.01 \frac{\mathrm{~kg}}{\mathrm{kmol}}}=149.99 \frac{\mathrm{~kJ}}{\mathrm{~kg}}
$$

