

Programmable Valves Enable
Both Precision Motion Control
and Energy Saving

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[Outline]

- Development of Programmable Valves
- Control of Programmable Valves
- On-board Modeling of Valve Flow Mapping
- Programmable Valves Bypass Sandwiched Deadband Problem
- Summary

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[E/H precision motion control system]

Objective:

- Performance
- Energy efficiency
- Cost

Energy usage:

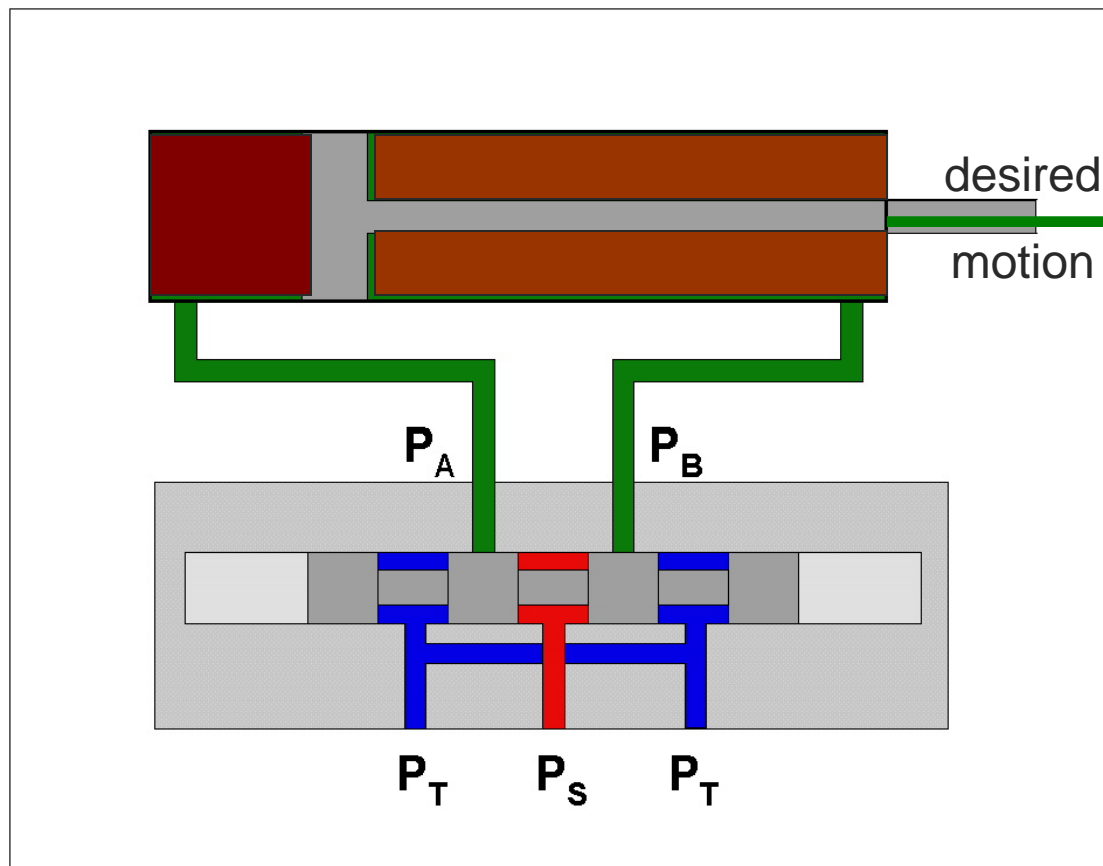
$$E = \int_{t_0}^{t_1} P_s(\tau) Q_s(\tau) d\tau$$

To reduce energy usage:

- Reduce the supply pressure $P_s(t)$
- Reduce the pump flow rate $Q_s(t)$

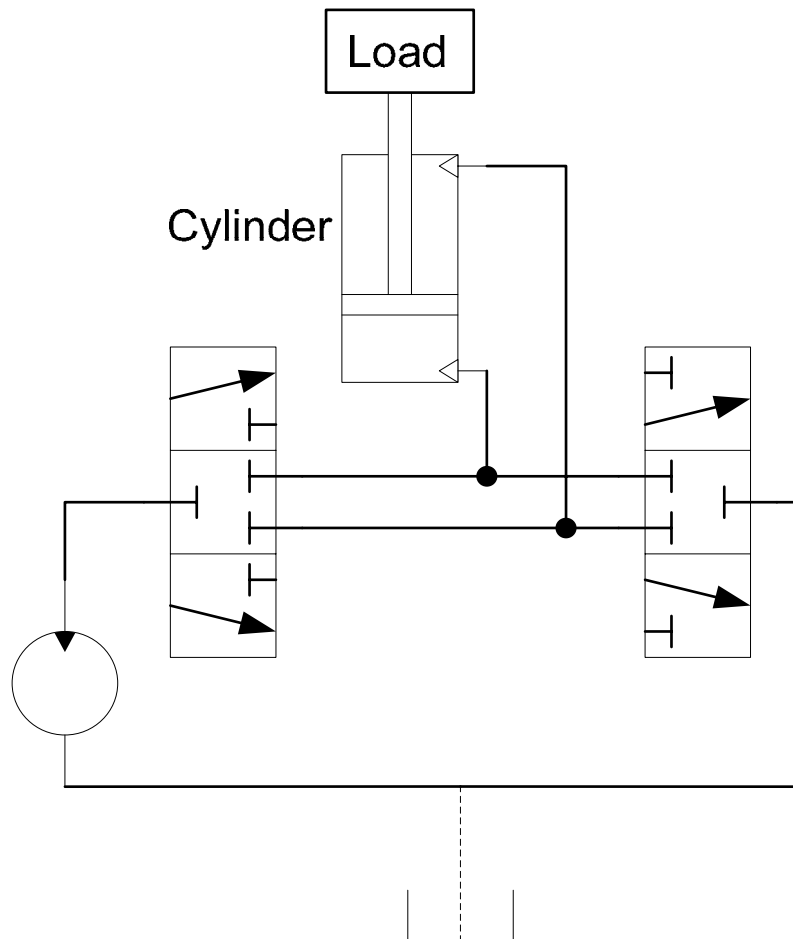
To reduce supply pressure ...

Must break the mechanical linkage between the meter-in and meter-out orifices



- Meter-in and meter-out orifice areas are coupled in 4-way directional control valves
- Cannot control all cylinder states (pressures of both chambers)
- Deadband for PDC valves
- Leakage for servo valves

Dual-Valve Meter-in and Meter-out



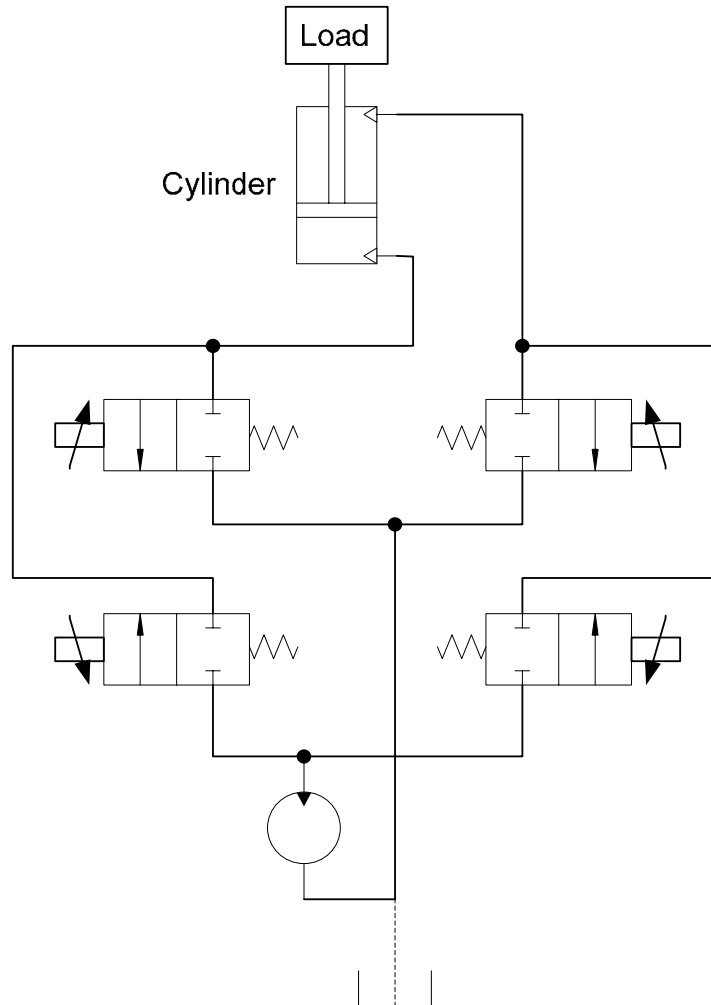
- **Two valves:**

Patented by:

J. Ardema, 1996

Uses two directional control valves to meter flows

Four-Valve Meter-in and Meter-out



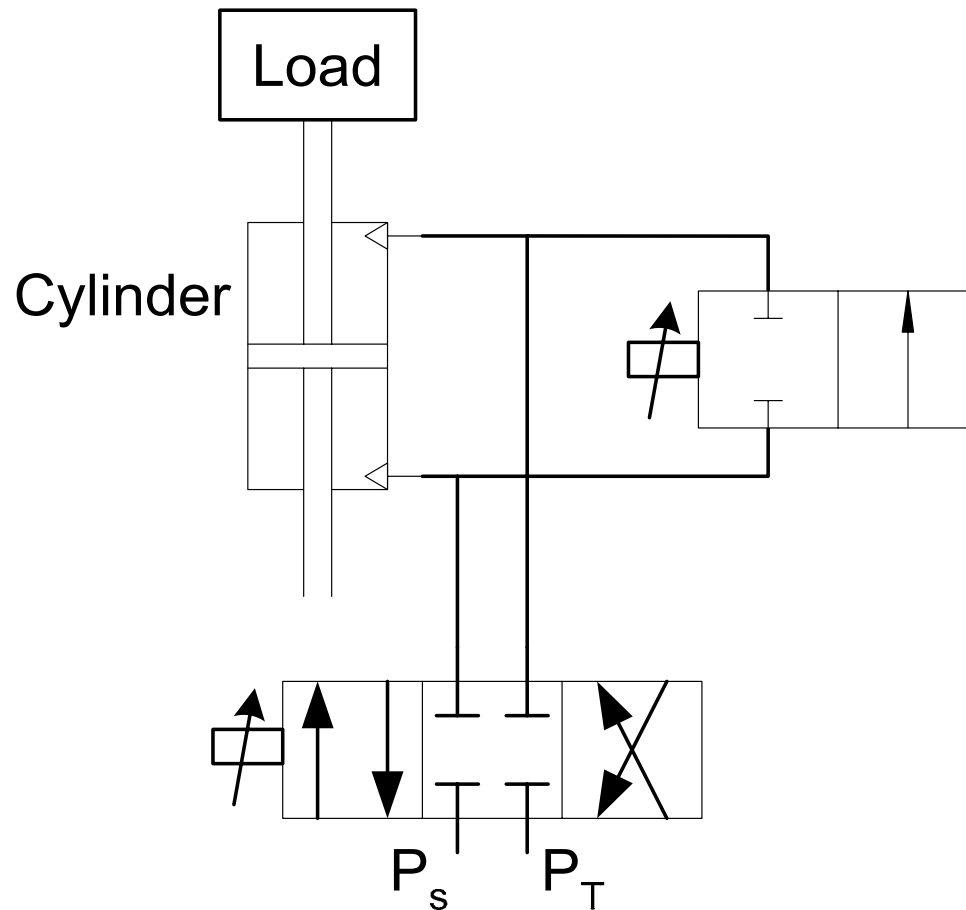
- Four valves

J. Ardema and D. Koehler

Uses four poppet valves to independently control meter-in and meter-out flows

Ardema and Koehler, Caterpillar Inc., "System and method for controlling an independent metering valve", United States Patent 5,947,140, 1999

Use Regeneration Flow



- Regeneration Valve

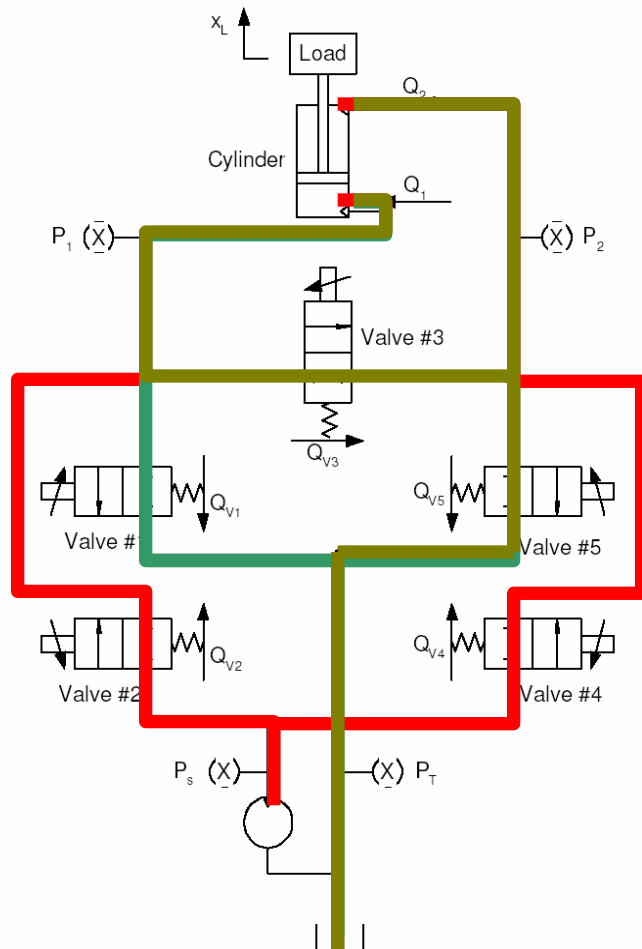
Patented by:

K. Garnjost, 1989.

Uses one additional valve to provide regenerative flow for energy saving but cannot control both chambers independently

Garnjost, K. D., "Energy-conserving regenerative-flow valves for hydraulic servomotors", United States Patent 4,840,111, 1989

Energy Saving Programmable Valves



Purdue Energy Saving Programmable Valves

Developed by:
Bin Yao, 2000

- Take advantages of four valve configuration to control meter-in/meter-out flows independently for precise cylinder positioning
- Use an additional valve to precisely control cross-port flow (or regenerative flow) for energy saving
- Overcome the sandwiched deadband control problem of conventional PDC valves through the use of cheap but fast acting cartridge valves

Programmable Valves Advantages

- Fully decoupled meter-in and meter-out flow
- Fully controlled true cross port regeneration flow
- More flexibility and controllability
- Completely solve/bypass the sandwiched deadband problem of EH systems controlled by closed-center valves
- Virtually eliminate leakage
- Faster response than PDC valves
- Low cost
- Low maintenance cost

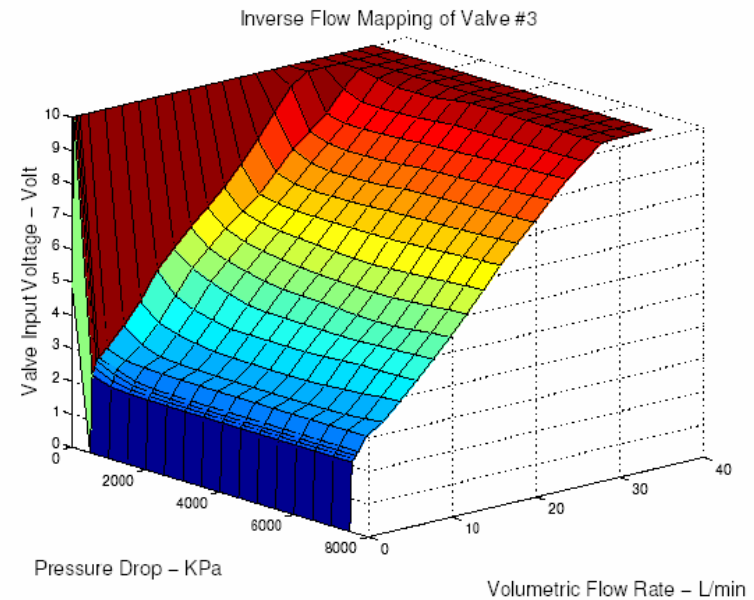
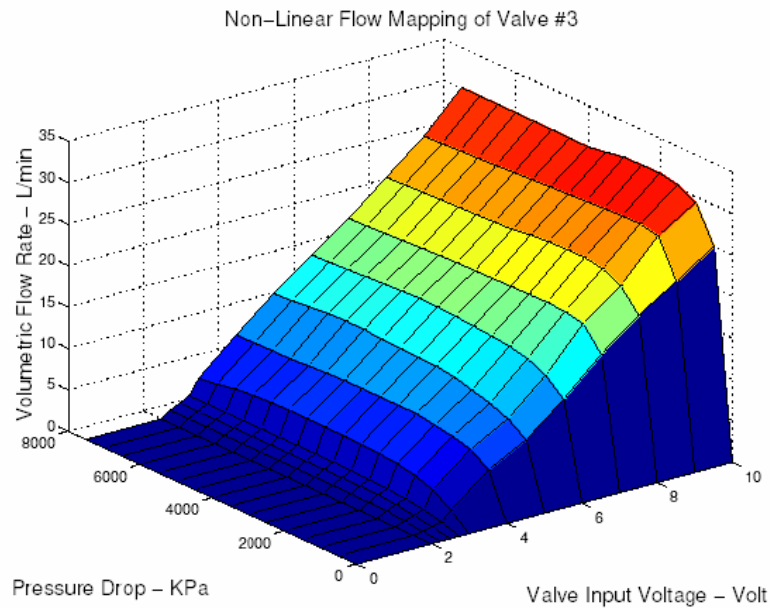
[Outline]

- Development of Programmable Valves
- Control of Programmable Valves
 - Challenges
 - Two-level control system
 - Comparative experimental results
- On-board Modeling of Valve Flow Mapping
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[Challenges]

- Multi-input dual-objective system
- Lack for accurate mathematical model of cartridge valves
- Coordination of the five cartridge valves
- Highly nonlinear hydraulic dynamics
- Large parameter variations
- Uncertain nonlinearities such as external disturbances, flow leakage and seal frictions

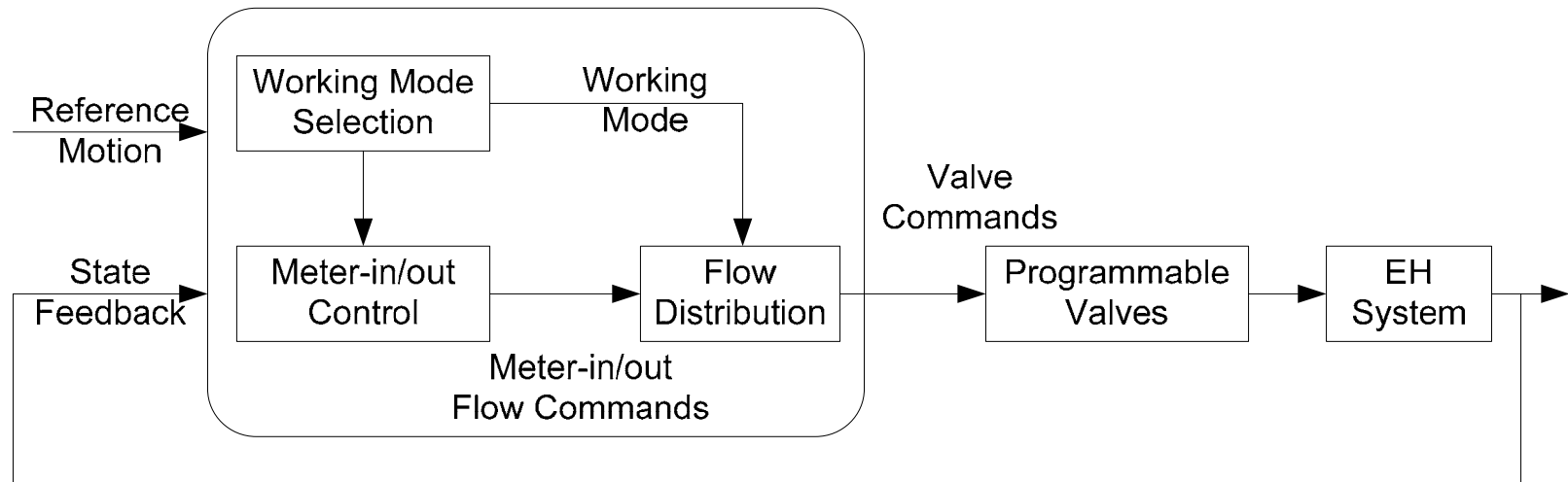
Nonlinear Valve Flow Mapping



$$Q_{vi} = f_{vi}(\Delta P_{vi}, u_{vi})$$

$$u_{vi} = f_{vi}^{-1}(\Delta P_{vi}, Q_{vi})$$

Control of Programmable Valves



Schematic of the two-level Control System

[Two-level Control System]

- Task level (Working Mode Selection)
 - Proper hydraulic circuitry
 - Optimal valve configuration for maximal energy saving
- Valve level (ARC Control)
 - Nonlinear model based design to take the system nonlinearities into account explicitly
 - Adaptive model compensation to reduce the effects of parametric uncertainties and disturbances
 - Robust feedback to guarantee stability

Working Mode Selection --- Tracking Task

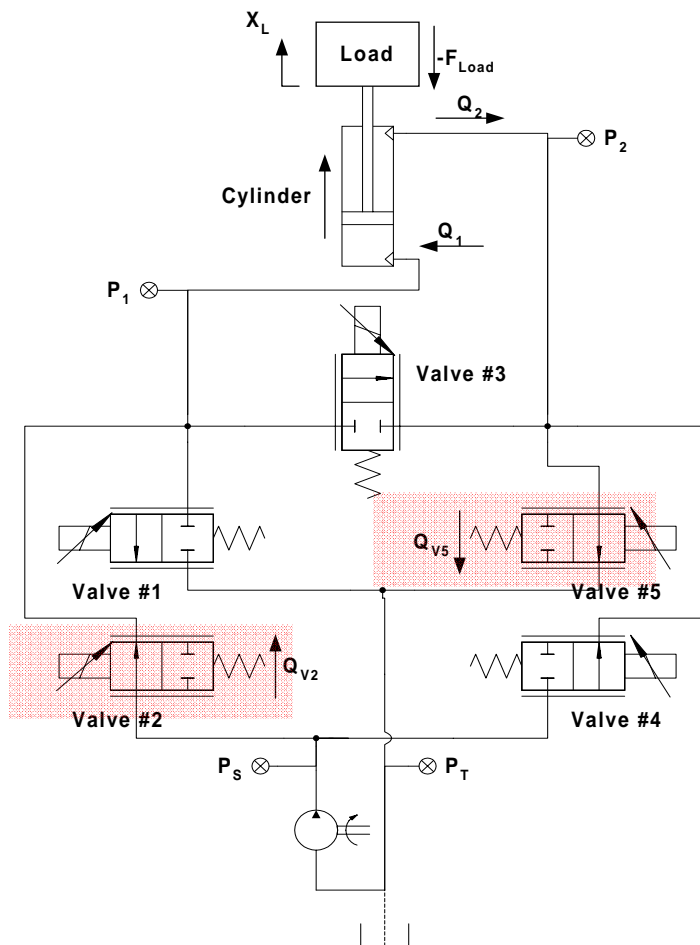
Table 3.1 Programmable valves tracking mode selection

\dot{x}_d	P_{lda}	Valve Configuration	Off-side	Mode
> 0	> 0	$Q_1 = Q_{v2}$ $Q_2 = Q_{v5}$	P_2	T1
> 0	< 0	$Q_1 = Q_{v2} - Q_{v3}$ $Q_2 = -Q_{v3}$	P_1	T2
< 0	> 0 $P_1 > P_2$	$Q_1 = -Q_{v3}$ $Q_2 = Q_{v5} - Q_{v3}$	P_2	T3
< 0	> 0 $P_1 \leq P_2$	$Q_1 = -Q_{v1}$ $Q_2 = -Q_{v4}$	P_2	T4
< 0	< 0	$Q_1 = -Q_{v1}$ $Q_2 = -Q_{v4}$	P_1	T5

Working Mode Selection --- Regulation Task

Table 3.2 Programmable valves regulation mode selection

\dot{x}_d	$x - x_d$	Valve Configuration	Off-side	Mode
$= 0$	$> \varepsilon$	$Q_1 = -Q_{v3}$ $Q_2 = Q_{v5} - Q_{v3}$	P_2	R1
$= 0$	$< -\varepsilon$	$Q_1 = Q_{v2}$ $Q_2 = Q_{v5}$	P_2	R2
$= 0$	<i>otherwise</i>	$Q_1 = 0$ $Q_2 = 0$		R3



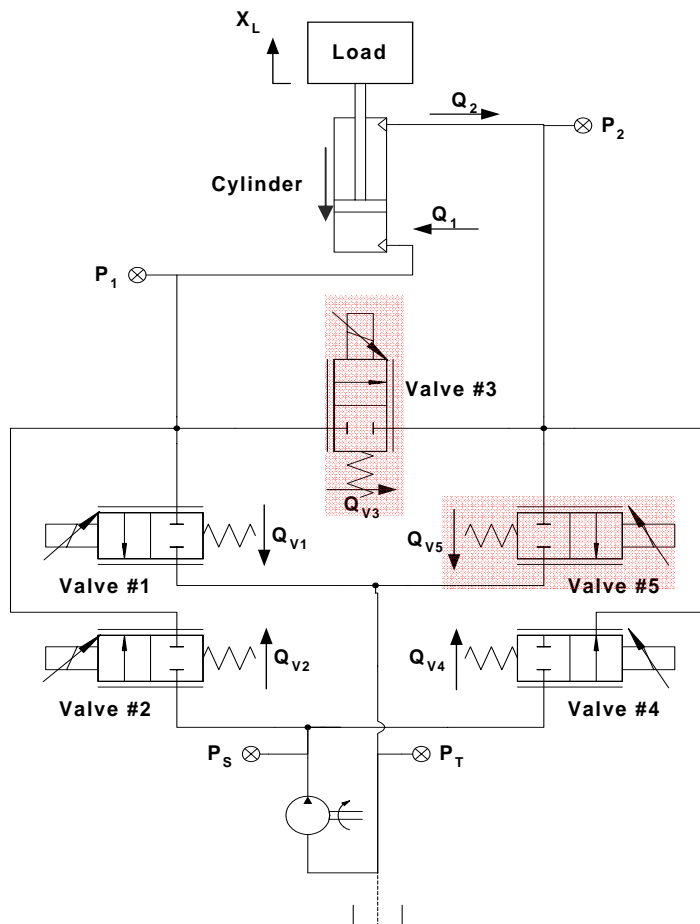
Desired Cylinder
Velocity > 0

Desired Cylinder
Force > 0

Uses Valve #2 and
Valve #5

Maintain P2 as
Low as Possible

Mode T3

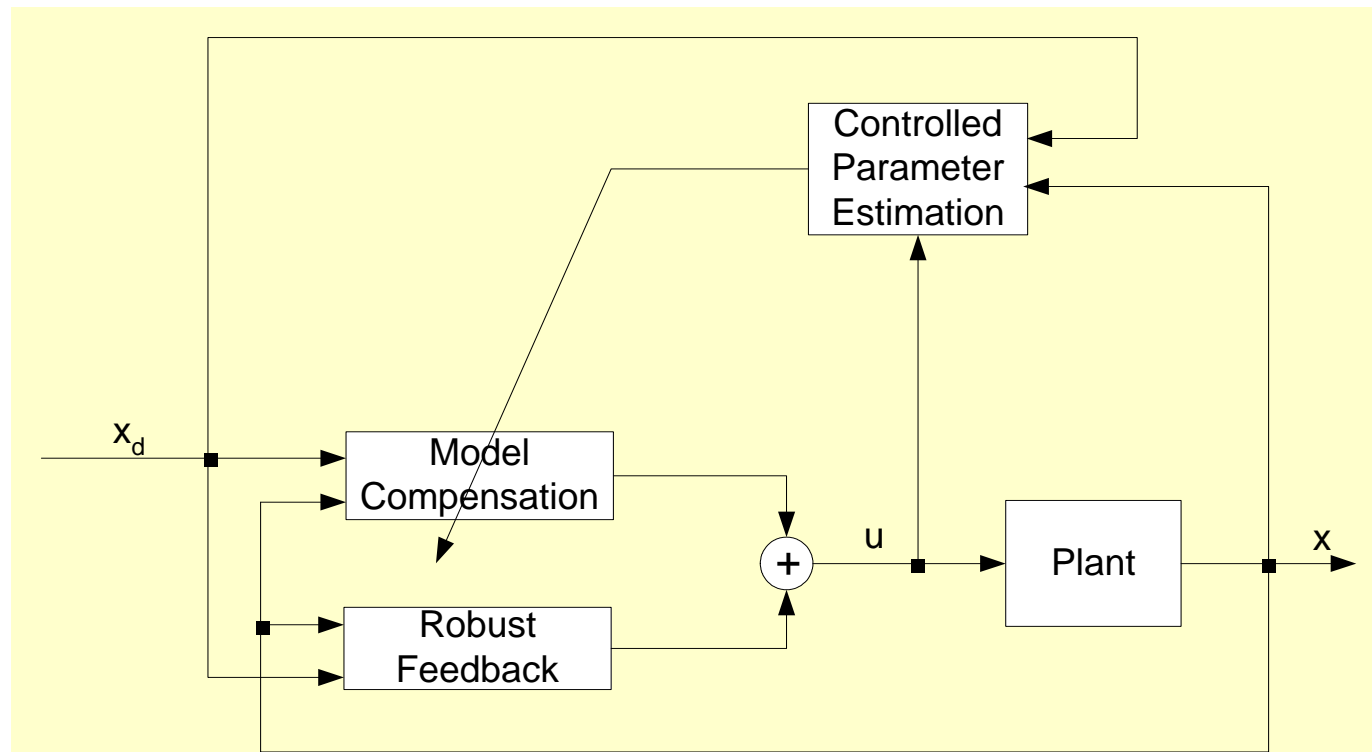


- Desired Cylinder Velocity < 0
- Desired Cylinder Force > 0
- $P_1 > P_2$
- Uses Valve #3 and Valve #5
- Maintain P_2 as Low as Possible

Valve-Level Control --- Adaptive Robust Controller

- Nonlinear model based controller design
- Compensate known nonlinearities and disturbances
- Guarantee stability and prescribed transient performance in the presence of unmodeled uncertainties and external disturbances
- Achieve asymptotic stability in the absence of disturbance

[Adaptive Robust Control Structure]



[Valve-Level Control]

- Off-side pressure regulator
 - Maintain the off-side chamber at a constant low pressure
- Working-side motion controller
 - Control the working-side pressure so that the desired trajectory is followed as close as possible
- Flow distribution
 - convert flow commands to valve voltage input signals

[Flow distribution]

< 0	> 0 $P_1 > P_2$	$Q_1 = -Q_{v3}$ $Q_2 = Q_{v5} - Q_{v3}$	P_2	T3
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$$Q_{v1} = 0$$

$$Q_{v2} = 0$$

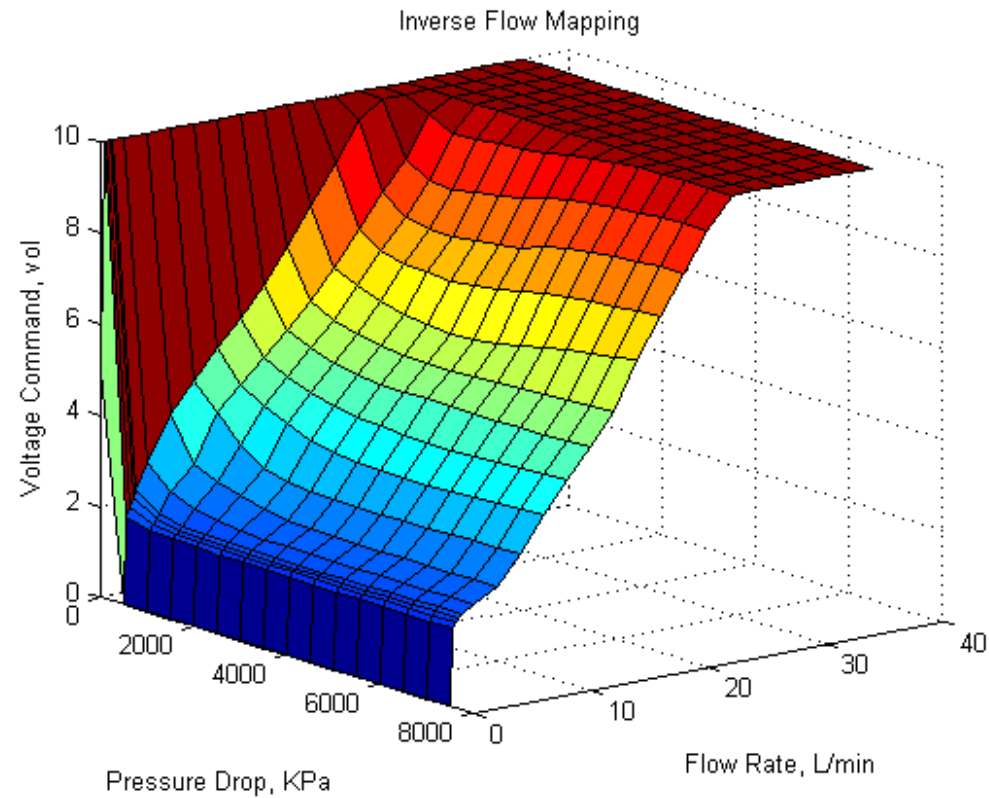
$$Q_{v4} = 0$$

$$Q_{v3} = -Q_{1md}$$

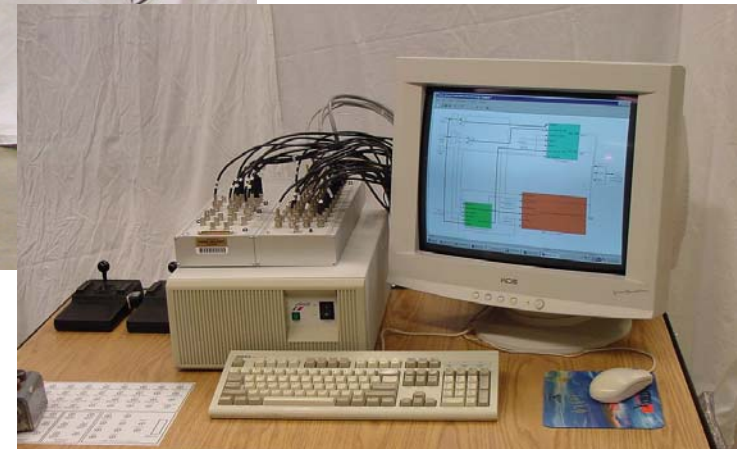
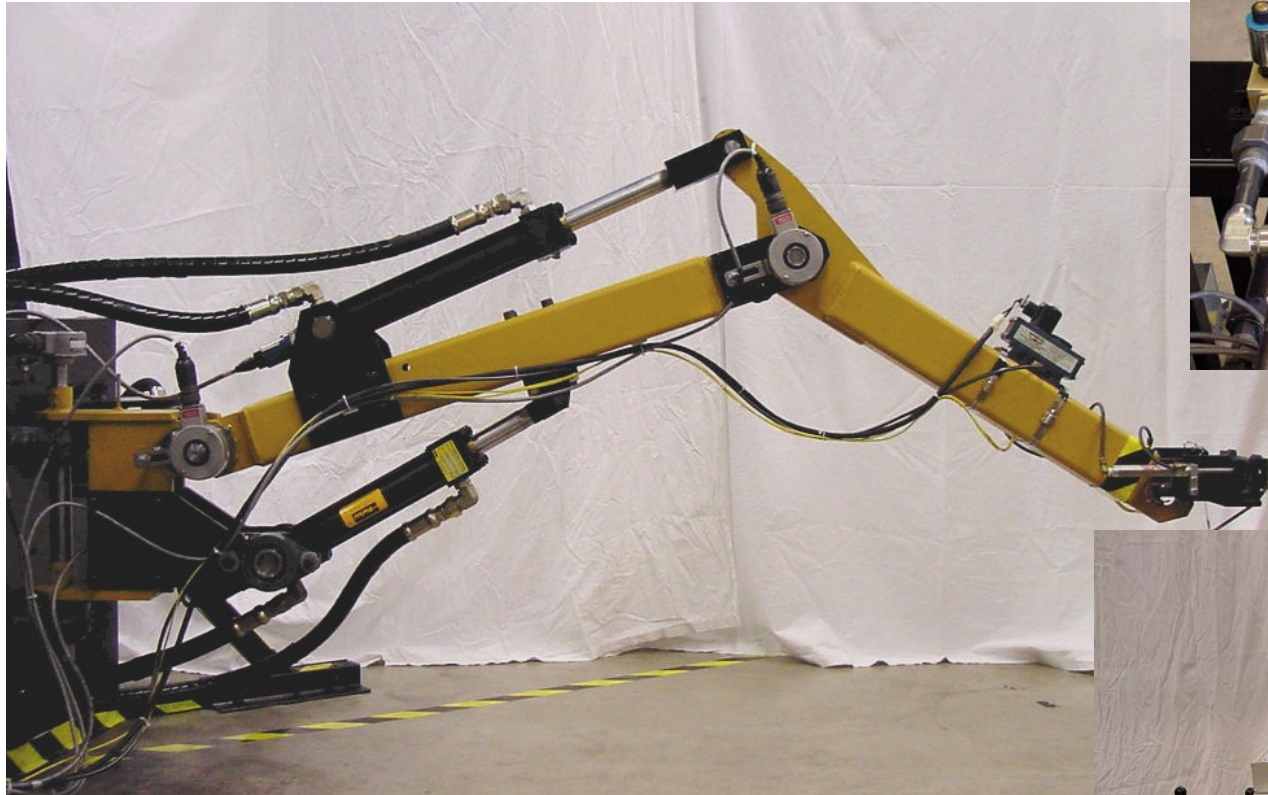
$$Q_{v5} = Q_{2md} + Q_{v3} = Q_{2md} - Q_{1md}$$

Flow distribution

- Inverse flow mapping to convert flow commands to valve voltages input signals



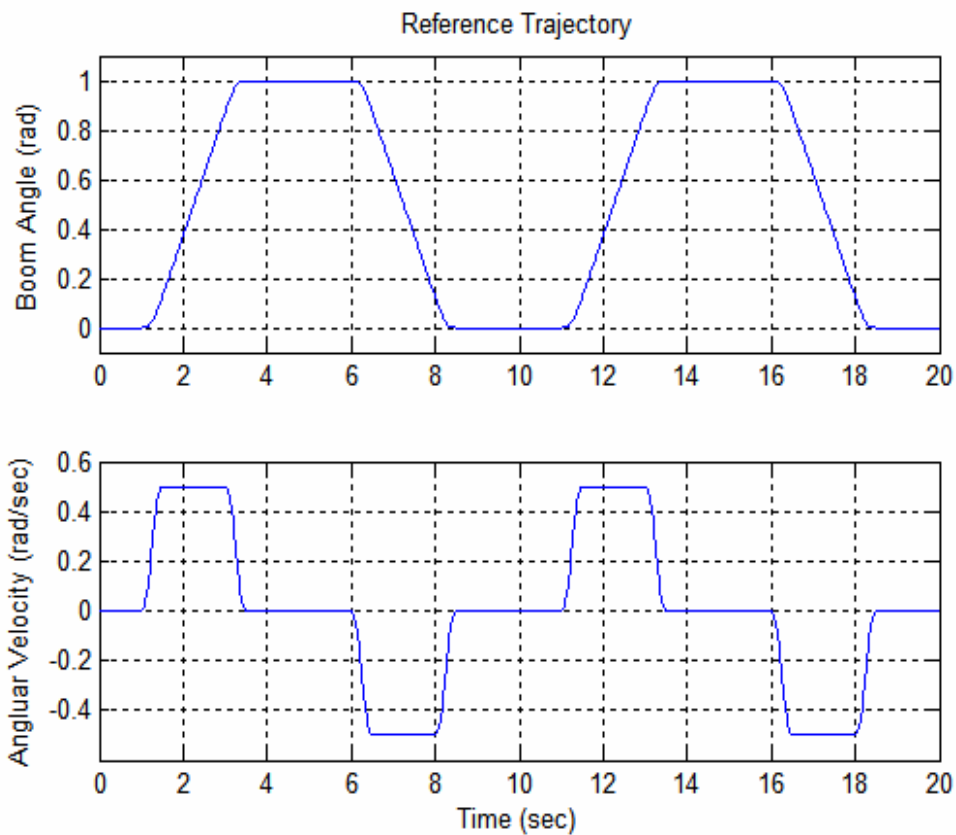
[Experimental Setup]



[Smooth Working Mode Switching]



Comparative Experiment



- PDC valve

Vickers KBFDG4V-5-2C50N-Z-PE7-H7-10

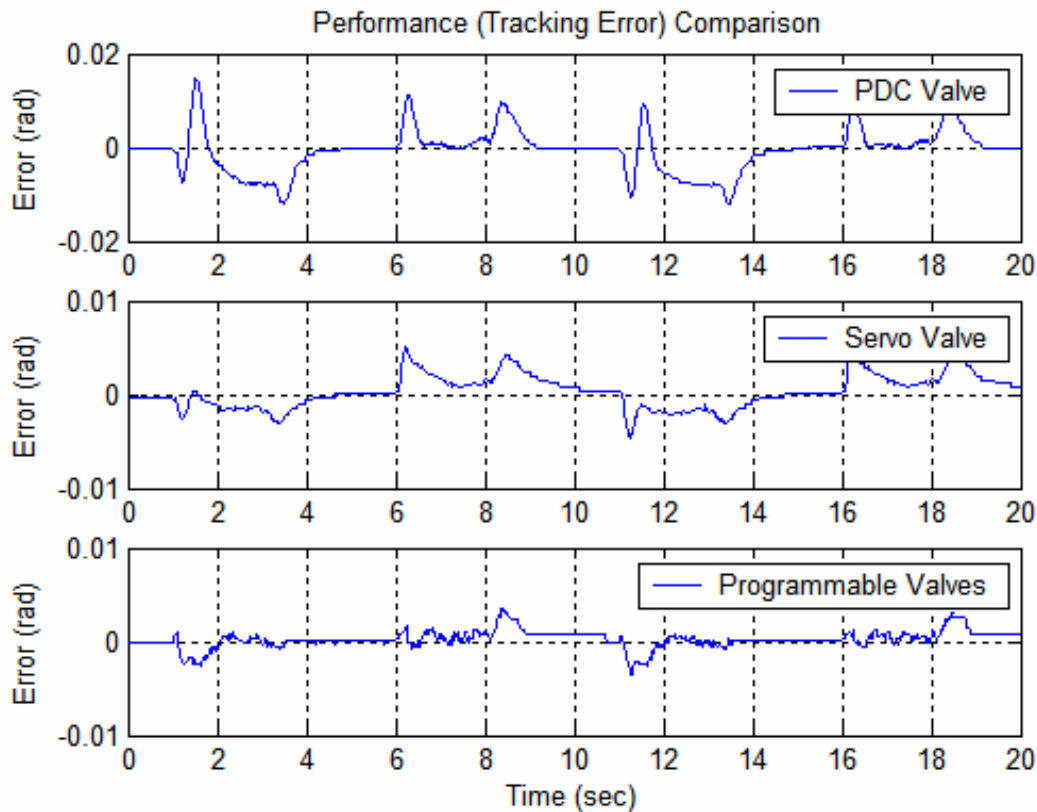
- Servo valve

Parker BD760AAAN10

- Programmable valves

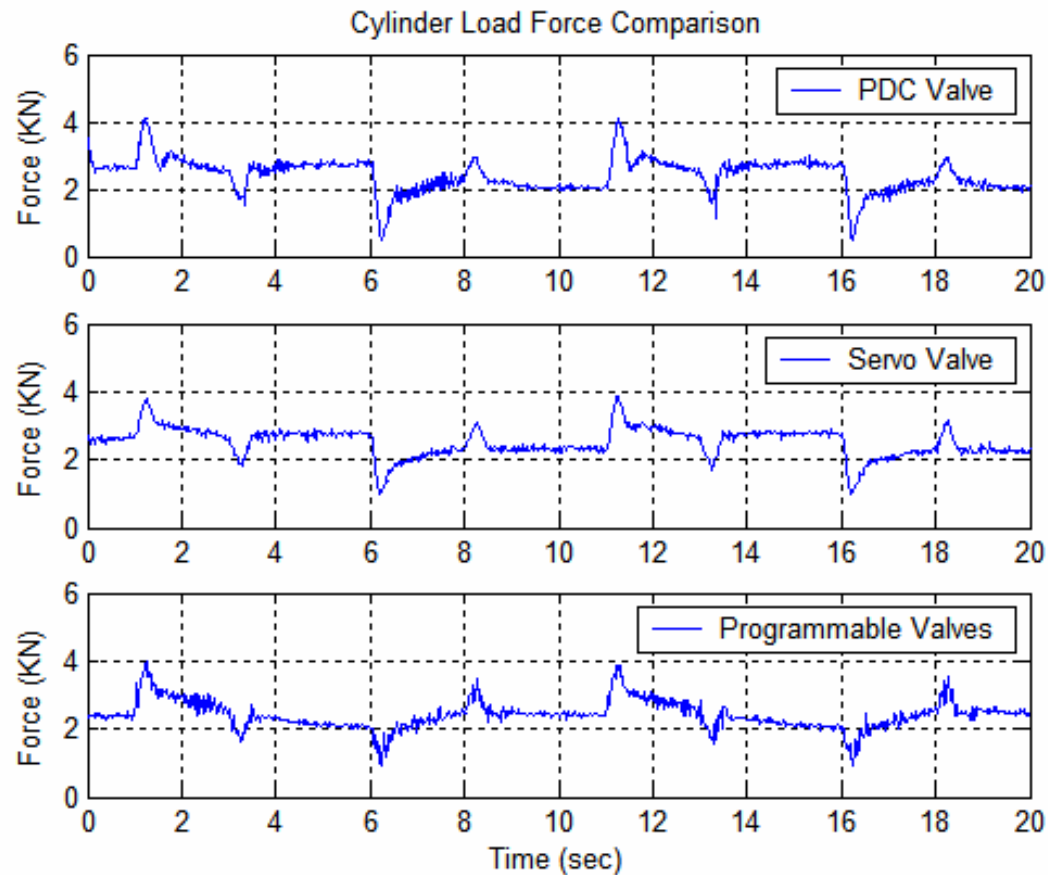
Vickers EPV10-A-8H-12D-U-10

Comparison of Performance

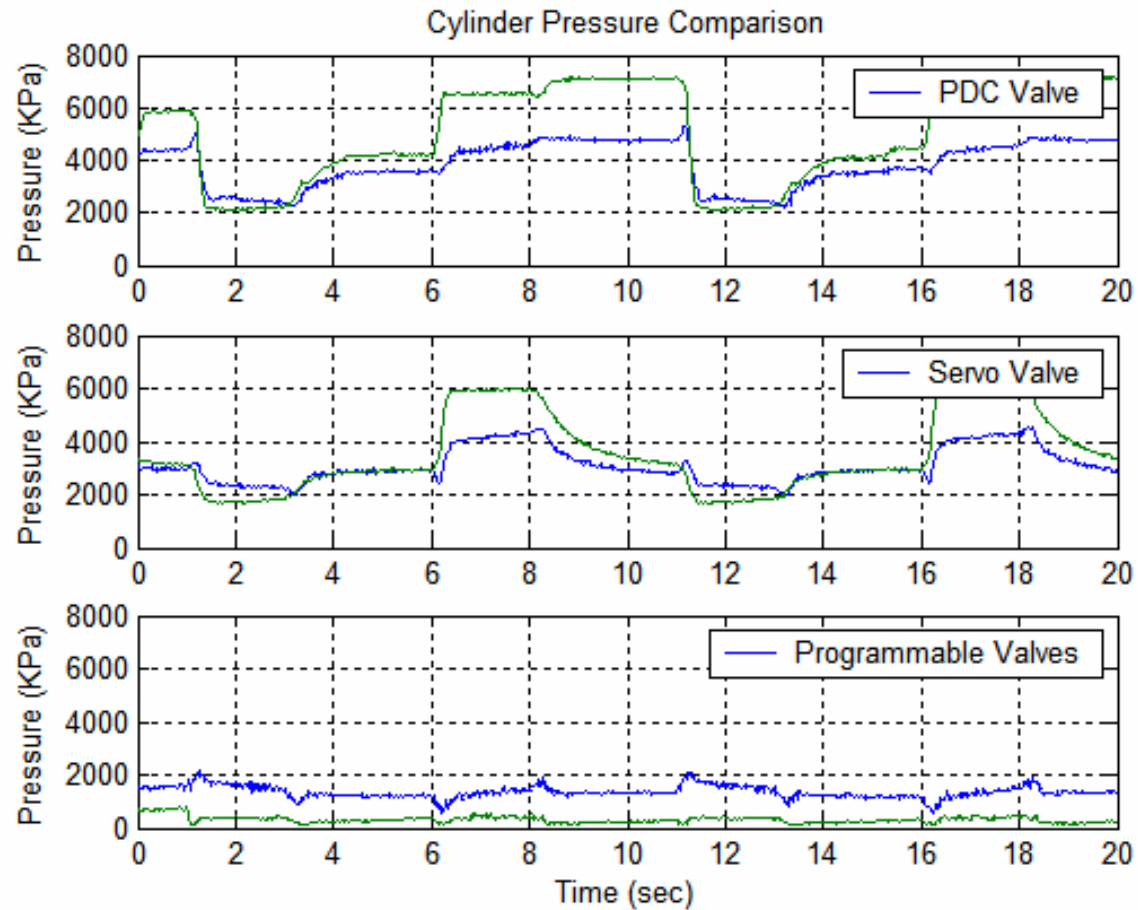


	$\ e\ _1$	$\ e\ _2$	$\ e\ _\infty$
PDC	0.0030	0.0046	0.0146
Srv	0.0014	0.0018	0.0051
Prog	0.0007	0.0010	0.0036

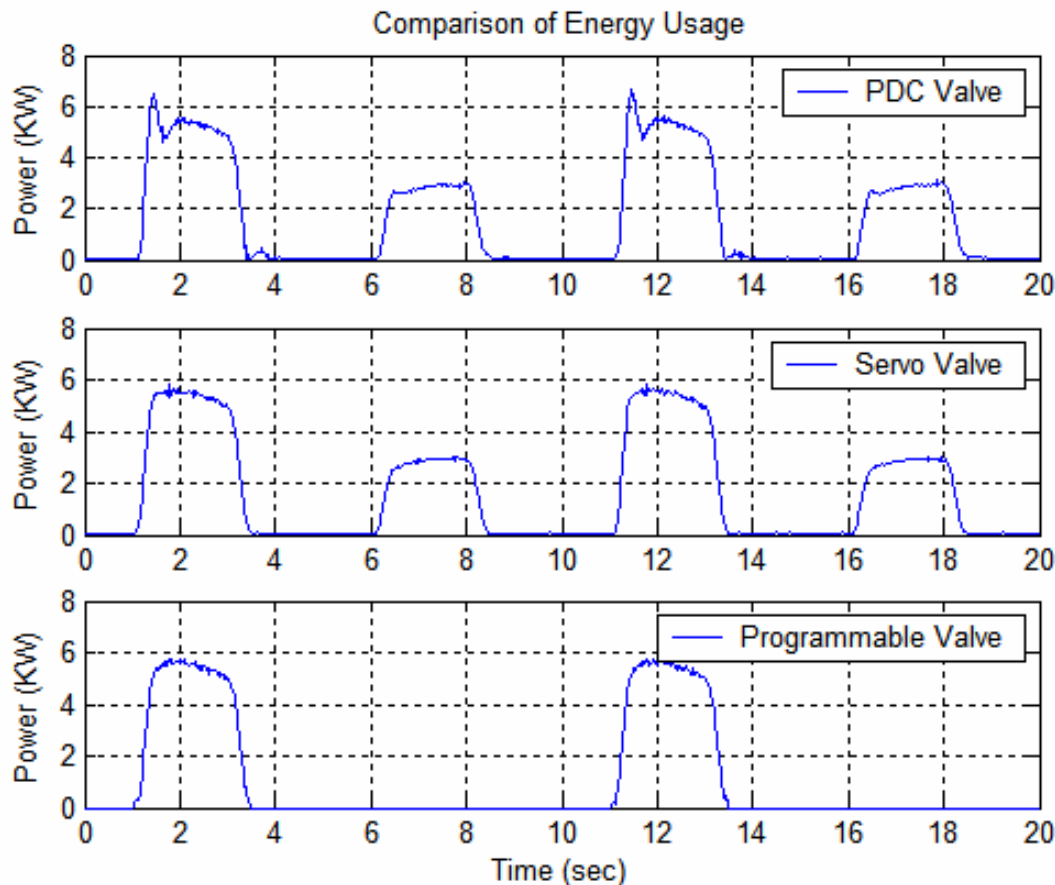
Comparison of Cylinder Force



Comparison of Cylinder Pressures



Comparison of Energy Usage, Constant Supply Pressure $P_s=1000\text{psi}$



■ 32.4 KJ

■ 32.7 KJ

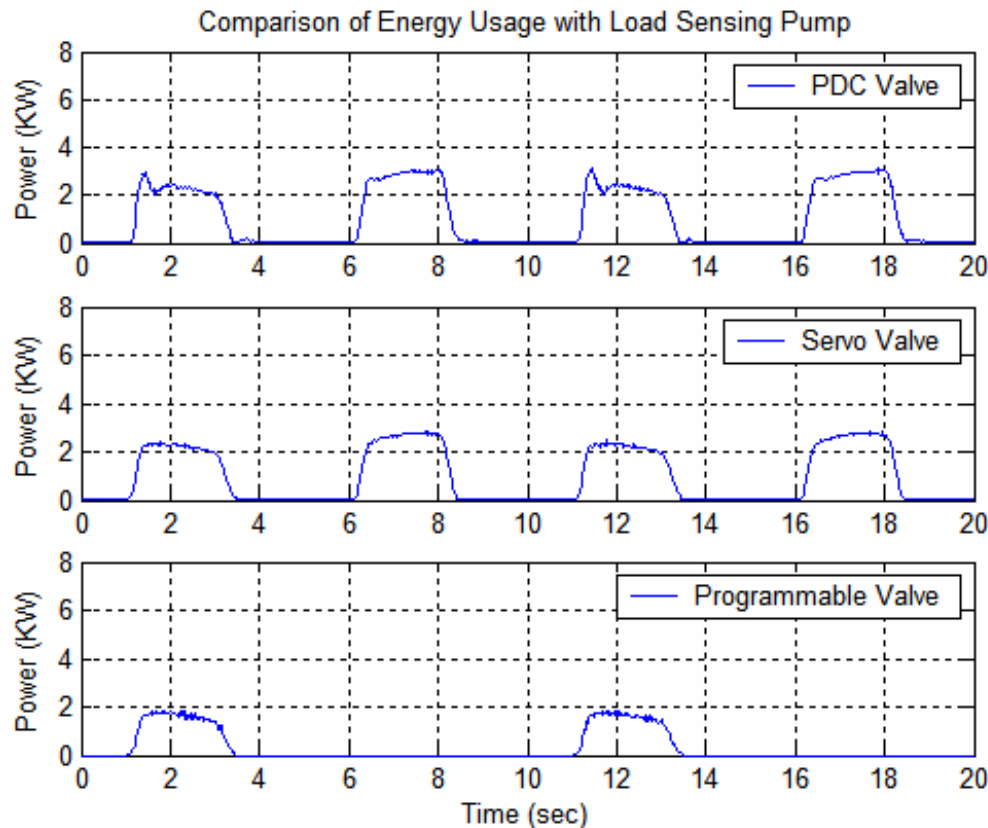
■ 21.3 KJ

34% less than PDC

35% less than Servo

Comparison of Energy Usage

$P_s = \text{Working Pressure} + 500\text{KPa}$



■ 20.9 KJ

■ 19.3KJ

■ 6.4KJ

69% less than PDC

67% less than Servo

[Outline]

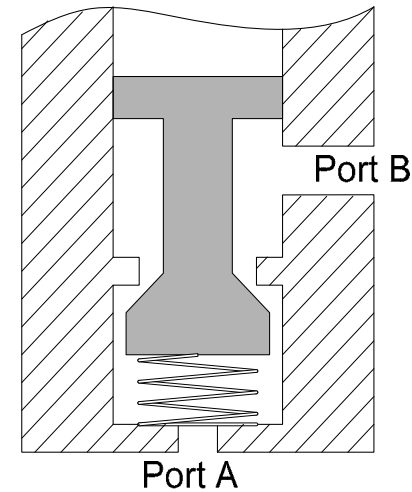
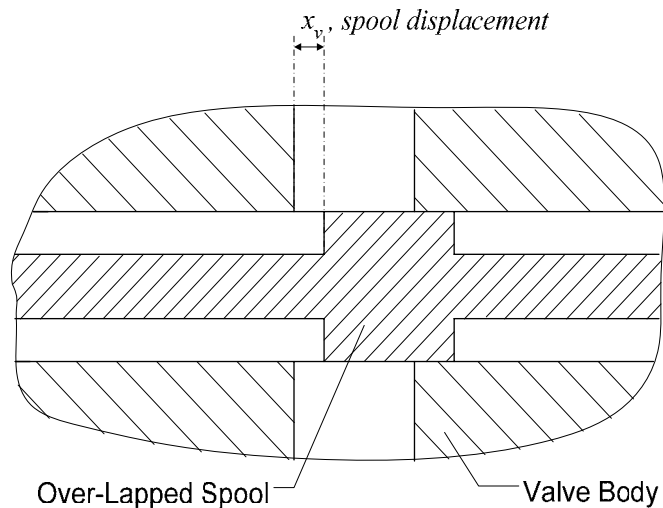
- Development of Programmable Valves
- Control of Programmable Valves
- On-board Modeling of Valve Flow Mapping
 - Problem formulation
 - Localized basis functions and smooth blending
 - On-board modeling
 - Comparative experimental results
- Programmable Valves Bypass Sandwiched Deadband Problem
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Cartridge Valve Flow Mapping

- Individually calibrated flow mapping (2002-2003)
 - Accurate
 - Off-board test, time consuming, additional calibration equipments, not suitable for industrial application
- Manufacture supplied flow mapping (2004)
 - Ready to use
 - Inaccurate, large modeling error exists, system performance compromised
- Automated on-board modeling of cartridge valve flow mapping (2004-2005)
 - Accuracy & easy implementation

Modeling of Cartridge Valve Flow Mapping

$$Q(u, \Delta P) = C_d A_v(x_v(u, \Delta P)) \sqrt{\frac{2}{\rho}} \sqrt{\Delta P}$$



$$Q = k_q u \sqrt{\Delta P}$$

Unknown nonlinear function $Q(u, \Delta P)$

On-board Modeling of Cartridge Valve Flow Mapping --- Observer Approach

Flow Rate Observer based on Cylinder Pressure Dynamics

$$\frac{V_1(x)}{\beta_e} \dot{P}_1 = -A_1 \dot{x} + Q_1(u_1, \Delta P_1)$$

$$Q_{vi} = f(u_{vi}, \Delta P_{vi})$$

Known Control
Signal

Measurable

[On-board Modeling of Cartridge Valve Flow Mapping]

$$\underline{Q}(u, \Delta P) = \bar{Q}(u, \Delta P) + \Delta, \quad \bar{Q} = \varphi_N^T(u, \Delta P) \cdot w_N$$

- Huge number of basis functions and weighting factors
- Limited experimental data
- Dynamic flow rate unavailable

Cylinder Dynamics Based Estimation

Cylinder dynamics: $\frac{V_1(x)}{\beta_e} \dot{P}_1 = -A_1 \dot{x} + Q_1(u_1, \Delta P_1)$

Define $\theta_{\beta_e} = \frac{1}{\beta_e}$

$$\longrightarrow A_1 \dot{x} = -V_1(x) \dot{P}_1 \cdot \theta_{\beta_e} + \varphi_N(u_1, \Delta P_1)^T \cdot \theta + \Delta$$

Defining $\varphi_{new}^T = [-V_1(x) \dot{P}_1 \quad \varphi_N(u_1, \Delta P_1)^T]$ $\theta_{new}^T = [\theta_{\beta_e} \quad \tilde{\theta}^T]$

$$\longrightarrow A_1 \dot{x} = \varphi_{new}^T \cdot \theta_{new} + \Delta$$

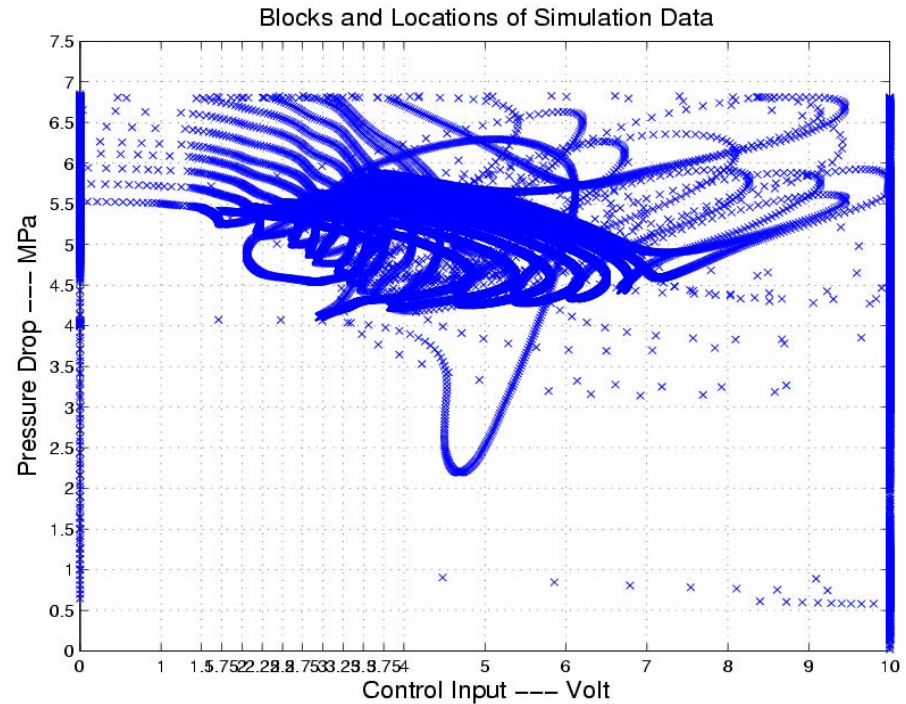
Why localized estimation?

$$[Q] = \Phi \cdot \theta + [\Delta]$$

$$\hat{\theta} = \Phi^+ \cdot [Q]$$

$$\tilde{\theta} = \Phi^+ [\Delta] = (\Phi^T \Phi)^{-1} \Phi^T [\Delta]$$

Invertibility



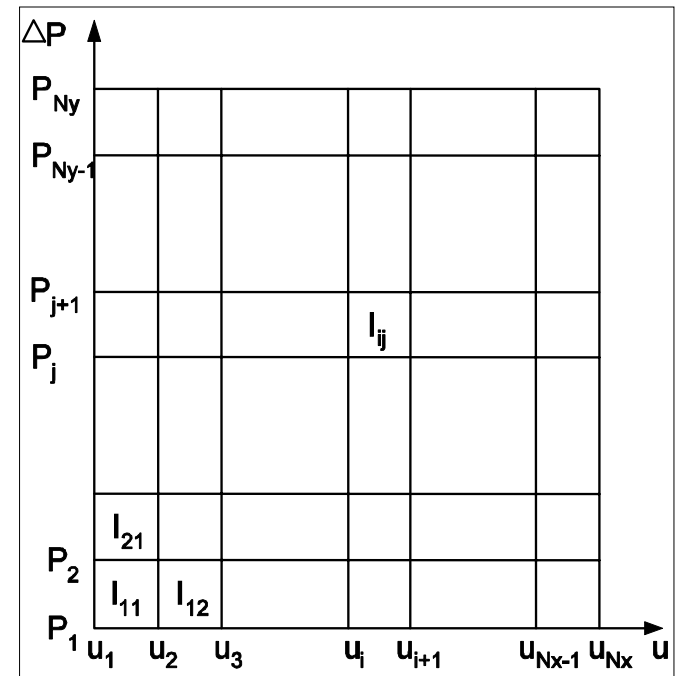
Localized Basis

$$Q(u, \Delta P)|_{(u, \Delta P) \in I_{ij}} = Q(\bar{u}_i, \Delta \bar{P}_j) + \frac{\partial Q}{\partial u}|_{(\bar{u}_i, \Delta \bar{P}_j)} \tilde{u} + \frac{\partial Q}{\partial \Delta P}|_{(\bar{u}_i, \Delta \bar{P}_j)} \tilde{P} + \frac{1}{2} \frac{\partial^2 Q}{\partial u^2}|_{(\bar{u}_i, \Delta \bar{P}_j)} \tilde{u}^2 + \frac{1}{2} \frac{\partial^2 Q}{\partial \Delta P^2}|_{(\bar{u}_i, \Delta \bar{P}_j)} \tilde{P}^2 + \frac{1}{2} \frac{\partial^2 Q}{\partial u \partial \Delta P}|_{(\bar{u}_i, \Delta \bar{P}_j)} \tilde{u} \tilde{P} + \Delta$$

$$\varphi_{ij}^T = \begin{cases} [1, \tilde{u}, \tilde{P}, \tilde{u}^2, \tilde{P}^2, \tilde{u}\tilde{P}] & (u, \Delta P) \in I_{ij} \\ [0, 0, 0, 0, 0, 0] & \text{otherwise.} \end{cases}$$

$$\bar{Q}(u, \Delta P)|_{(u, \Delta P) \in I_{ij}} = \varphi_{ij}^T \cdot \theta_{ij}$$

$$\bar{Q}(u, \Delta P) = \sum_{j=1}^{N_y} \sum_{i=1}^{N_x} \varphi_{ij}^T \cdot \theta_{ij}$$



Localized Estimation

$$[Q(u, \Delta P)]|_{(u, \Delta P) \in I_{ij}} = \Phi_{ij} \cdot \theta_{ij} + [\Delta]$$

$\Phi_{ij}^T \Phi_{ij}$ is invertible

$\Phi_{ij}^T \Phi_{ij}$ is not invertible

$$\hat{\theta}_{ij} = (\Phi_{ij}^T \Phi_{ij})^{-1} \Phi_{ij}^T \cdot [Q(u, \Delta P)]|_{(u, \Delta P) \in I_{ij}}$$

Extrapolation

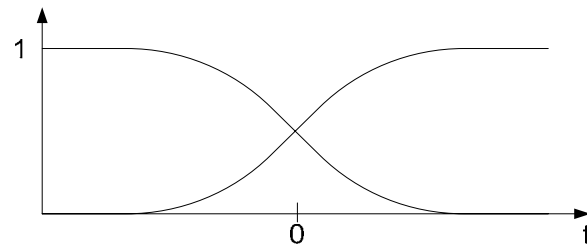
- PE condition is easily satisfied in small local region rather than globally
- Estimation error can be controlled by checking the condition number instead of invertibility
- Discontinuity may happen at the block borders

Smooth Blending

$$P^+ f(t) = \beta(t)[\beta(t)f(t) + \beta(-t)f(-t)]$$

$$P^- f(t) = \beta(-t)[\beta(-t)f(t) - \beta(t)f(-t)]$$

$$\beta(t) = \begin{cases} 0 & \text{if } t < -1 \\ 1 & \text{if } t > 1 \end{cases} \quad \text{and } \beta^2(t) + \beta^2(-t) = 1 \quad \forall t \in [-1, 1]$$




Theorem 1: (Coifman and Meyer) The operators P^+ and P^- are orthogonal projectors respectively on W^+ and W^- . The spaces W^+ and W^- are orthogonal and $P^+ + P^- = \text{Identity}$.

Automated On-board Modelling of Valve Flow Mapping

$$A_1 \dot{x} = \varphi_{new}^T \cdot \theta_{new} + \Delta$$

$$\theta_{new}^T = [\theta_{\beta_e} \quad \tilde{\theta}^T]$$

$$\varphi_{new}^T = [-V_1(x)\dot{P}_1 \quad \varphi_N(u_1, \Delta P_1)^T]$$

$$H_f(s) = \frac{\omega_n^2}{s^2 + 2\zeta\omega_n s + \omega_n^2}$$


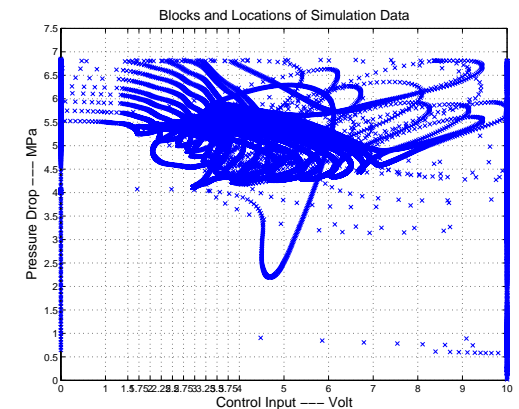
$$A_1 \dot{x}_f = \varphi_{newf}^T \cdot \theta_{new} + \Delta_f$$

[On-line Estimation]

On-line, Swiped sinusoidal trajectory, 0.1Hz~0.5Hz over 80sec.

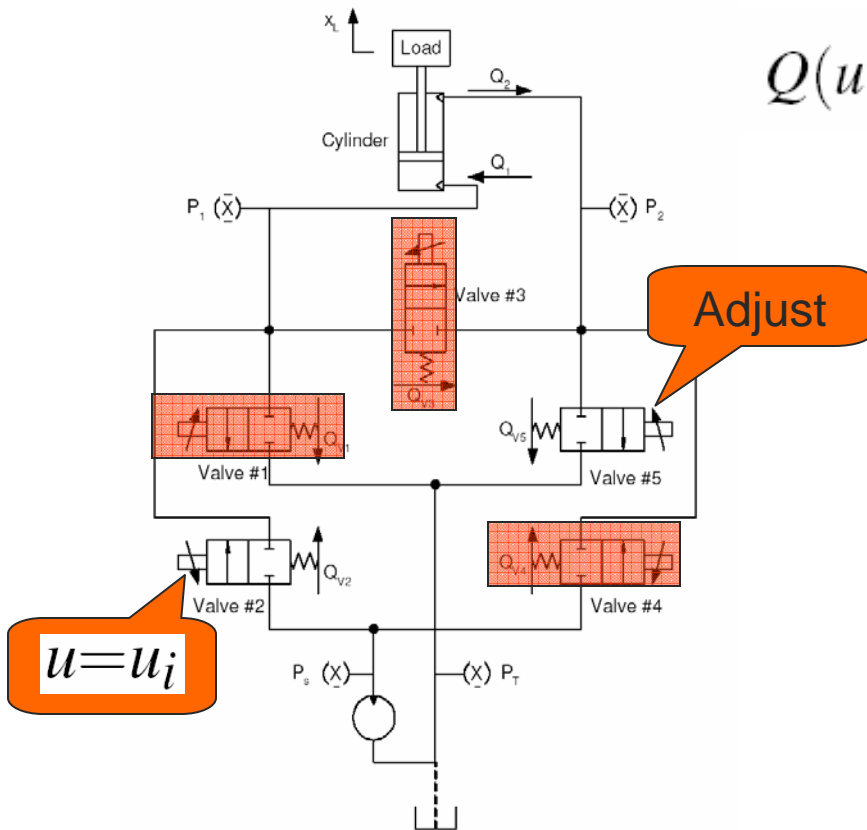
TABLE I
ESTIMATED FLOW MAPPING VS. TRUE VALUE

	4v	5v	6v	7v
4.5MPa	7.33	12.02	17.79	22.96
	8.00	11.83	17.57	22.60
5MPa	8.20	12.44	17.37	22.62
	8.00	12.22	17.18	21.95
5.5MPa	7.98	12.02	NA	NA
	7.97	12.00	16.39	20.61

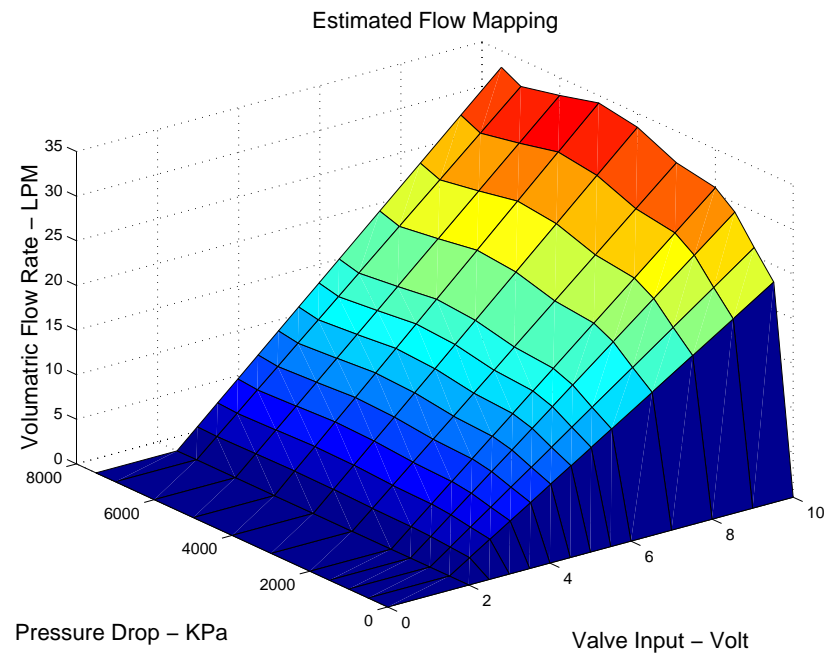


Estimated
Calibrated

Off-line Estimation

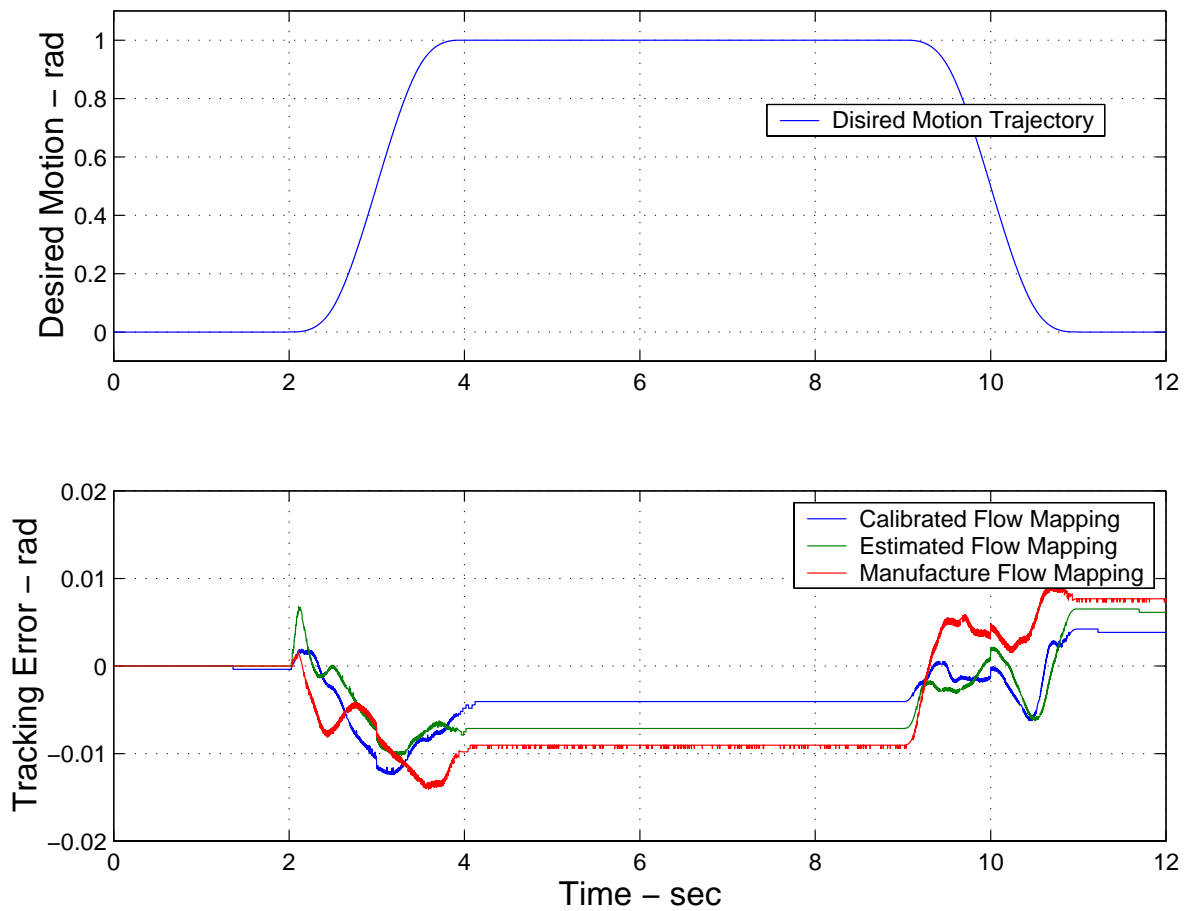


$$Q(u, \Delta P)|_{u=u_i} = Q_i(\Delta P), \quad i = 1, 2, \dots, Nx$$



Comparison of Different Flow Mappings

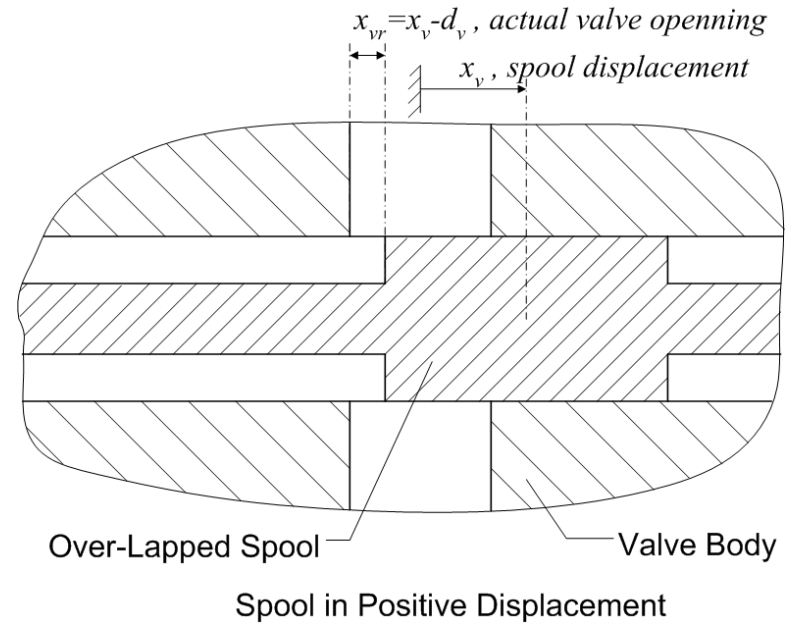
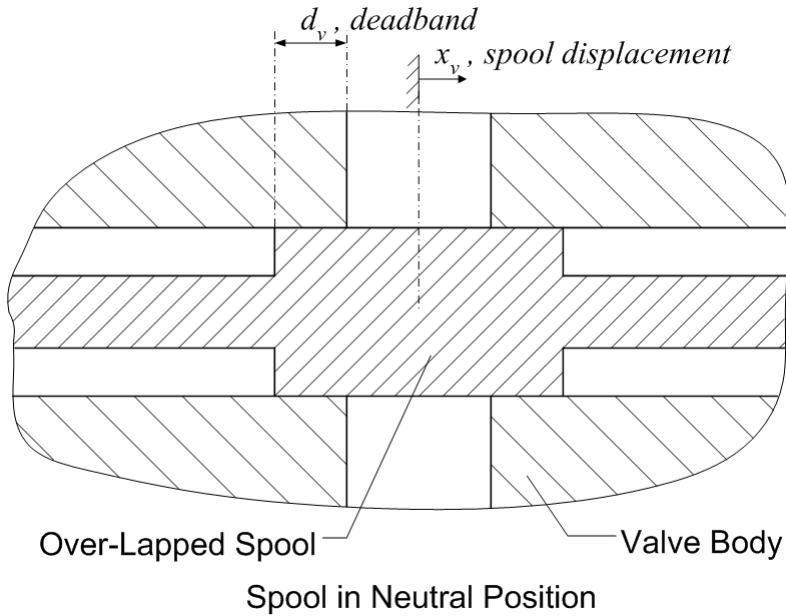
Comparative Tracking Results with Different Flow Mappings



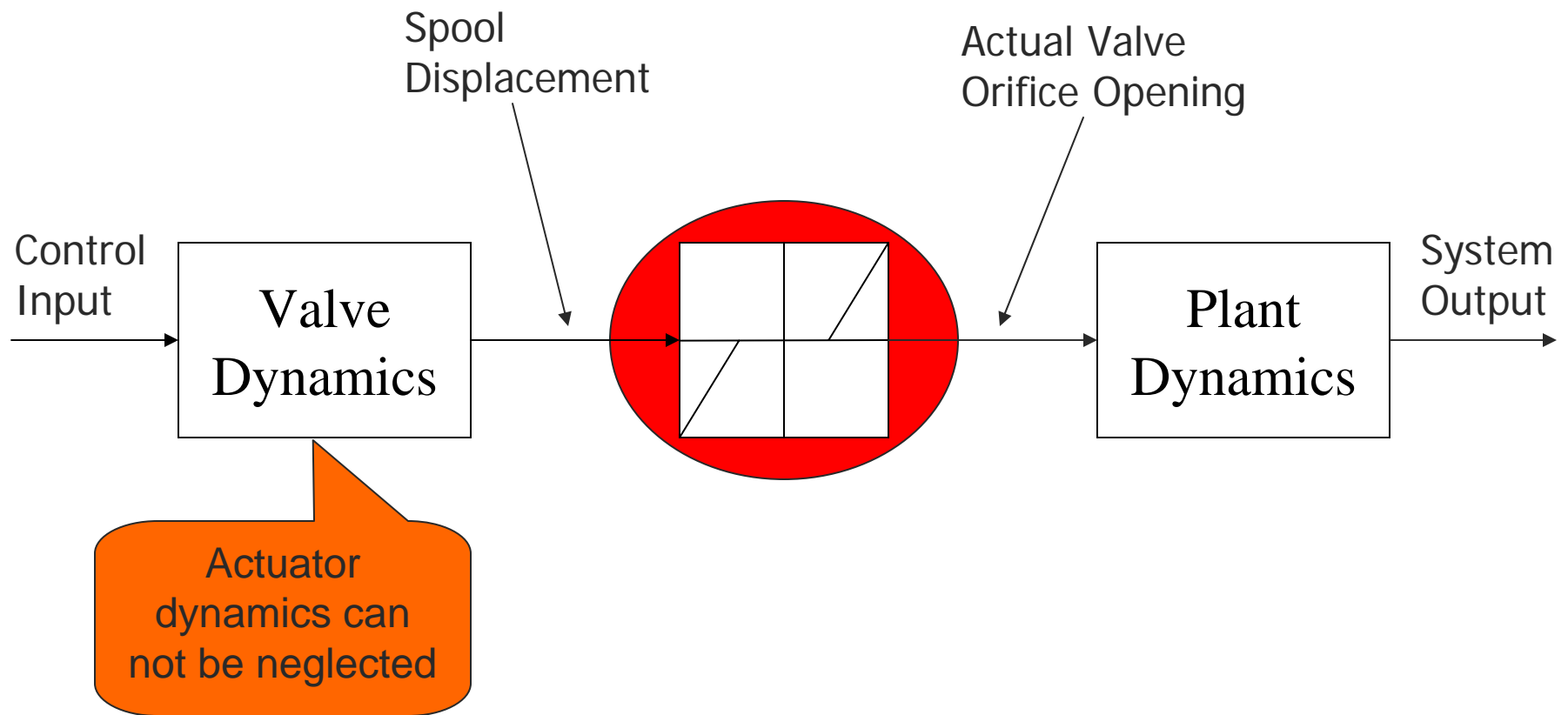
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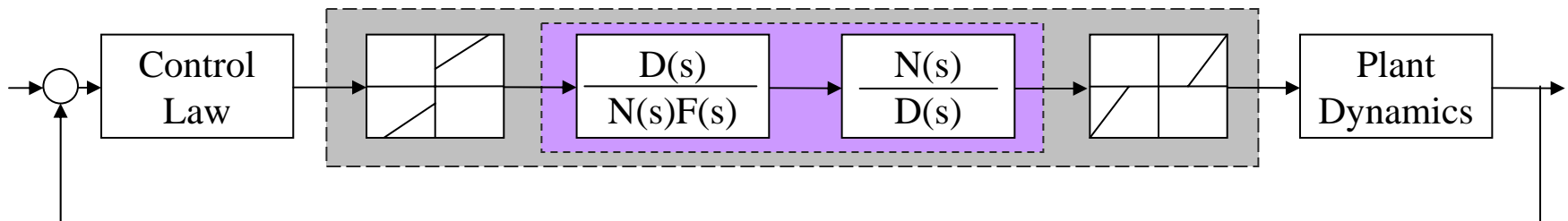
EH system controlled by a closed-center valve



[What is sandwiched deadband]

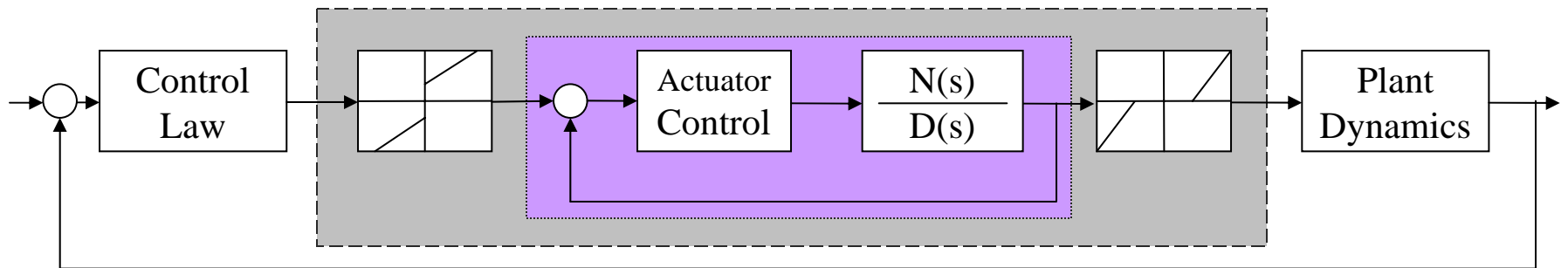


SD is hard to deal with --- Feedforward Compensation



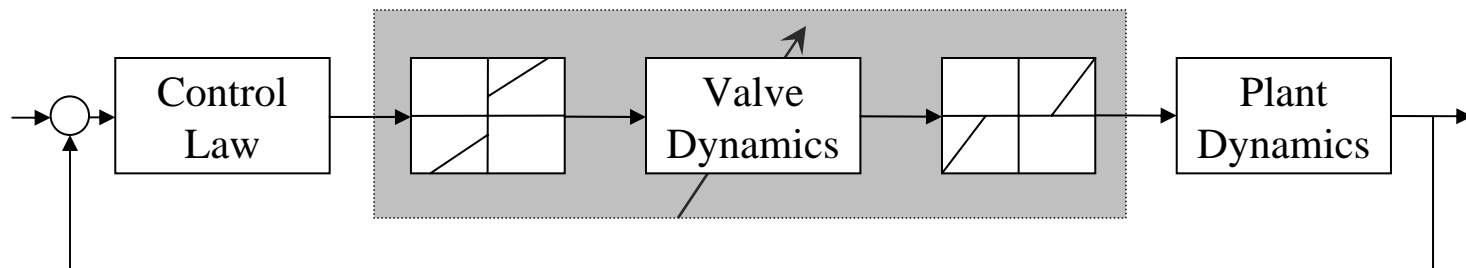
- Use feed-forward controller to increase the actuator dynamics so that it is sufficiently high to be neglected
- Used the inverse deadband function to compensate the nonlinear deadband
- **Depends on the accuracy of the valve dynamics, can only achieve limited improvements in practice due to the unavoidable uncertainties in the valve model**

SD is hard to deal with --- Feedback Compensation



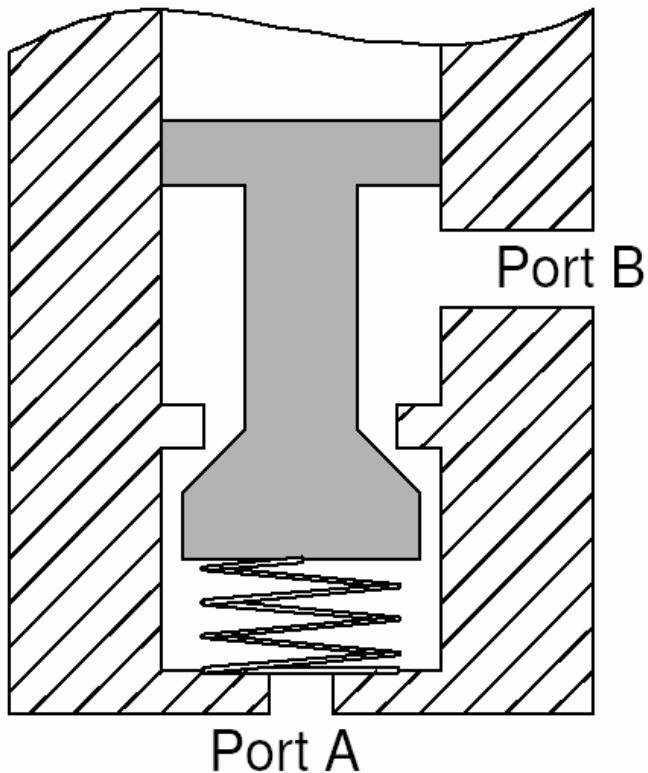
- Use local high gain feedback control to attenuate the deadband
- Require actuator output/state feedback. Significantly increases system cost.
- Sometimes actuator output/state signals are too noisy to help increasing the bandwidth significantly.

SD simple solution --- Direct Compensation



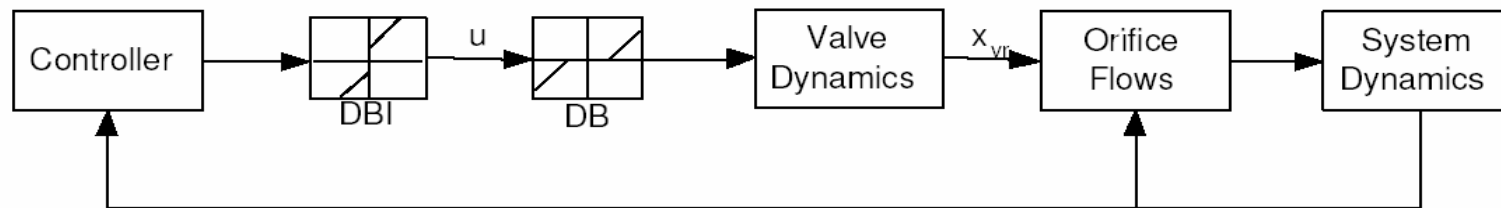
- Simply neglect valve (spool) dynamics
- Economical, easy to implement
- Limit cycle may happen if closed loop bandwidth is not low enough
- Closed loop system is usually conservative, i.e., bandwidth is limited quite low in order to safely neglect valve dynamics

Deadband of poppet-type cartridge valves



- The input signal has to be large enough to overcome the spring force and static friction.

Deadband Compensation of Poppet Valve



- Input deadband is easier to compensate
- Cartridge valve dynamics is much more faster than PDC valves.

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[Conclusions]

- Eliminate the mechanical linkage between the meter-in and meter-out orifices and enable accurately using the cross port regeneration flow for a controlled motion.
- Energy saving can be achieved without sacrificing precision motion performance.
- The two-level control system successfully control the system to achieve the dual objectives.
- Sandwiched deadband in EH systems can be bypassed by the programmable valves.
- Promising alternatives of conventional four-way valves in precision motion control.

[Acknowledgement]

- Formal Students:

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Chris Deboer

- Past Caterpillar Collaborators:

John Litherland
Doug Koehler
J. Ardema

Acknowledgements

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Regular Grant CMS-0220179

Purdue Electro-Hydraulic Research Center

Valve Donations by:



References

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