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Boiling Configurations

Boiling Applications

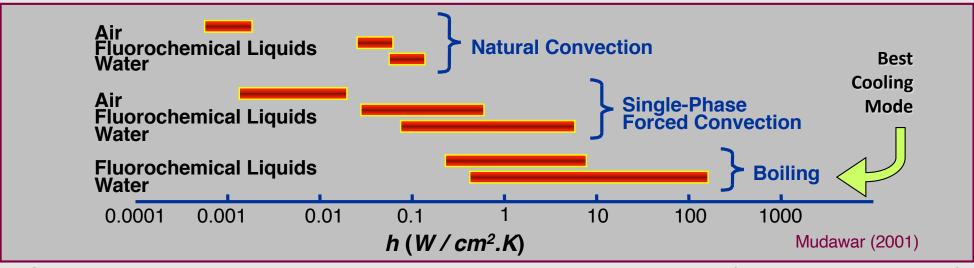
High-Flux (25 - 10³ W/cm²)

Power plant boilers
Food production
Geothermal systems
Metal production
Computer chips
Fuel cells
Spacecraft electronics

Ultra-High-Flux (10³ - 10⁵ W/cm²)

Pressurized water reactors
Particle accelerators
Laser & microwave weapons
Radar systems
Rocket nozzles

Turbine blades Afterburners



- Constant pursuit of more compact and lightweight packaging, and better performance (lower junction temperature)
 has lead to alarming increases in power density
- Because thermal management is mostly an afterthought, pushing limits of existing cooling solutions (e.g., using air-cooled heat sinks) often results in costly upper bounds to many technologies
- What is presently needed is a new class of thermal management solutions capable of dissipating very high power densities
- With this capability, these solutions will allow vast advances in performance without the need for costly changes in system packaging
- Systems utilizing liquid-to-vapor phase-change are the most effective thermal management solutions for highpower-density applications



Nucleate Boiling

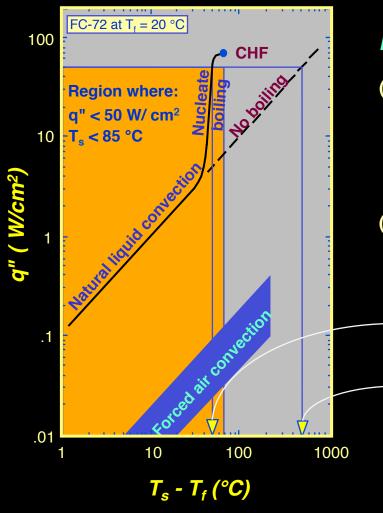


Critical Heat Flux



Film Boiling





Key Merits of Boiling:

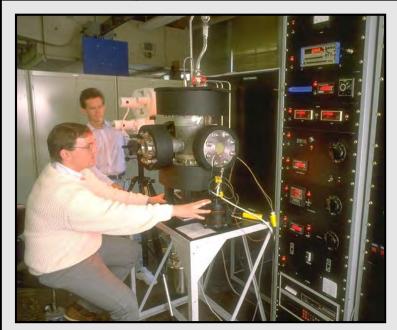
- (1) Modest changes in device temperature corresponding to broad changes in device heat flux (in nucleate boiling region)
- (2) Much lower device temperatures than with single-phase cooling. For this device:

T_s = 70 °C at 50 W/cm² with boiling

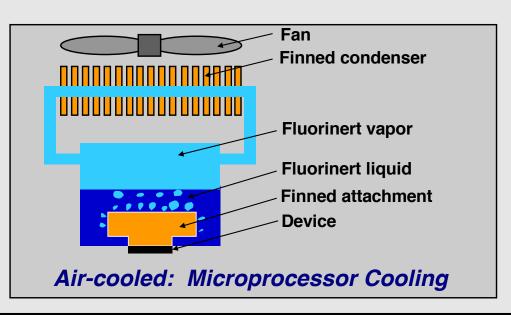
T_s = 525 °C at 50 W/cm² without boiling

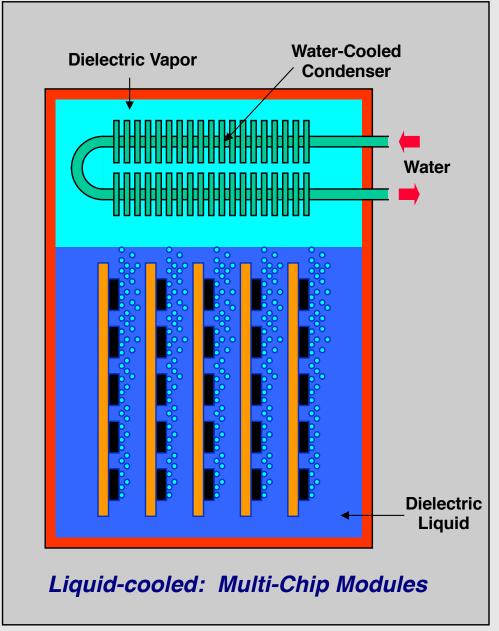


Boiling Configurations: Pool Boiling Thermosyphons







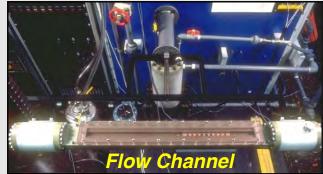


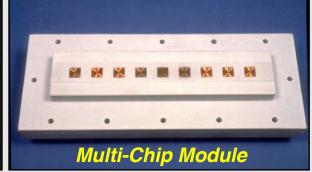


Boiling Configurations: Channel Flow



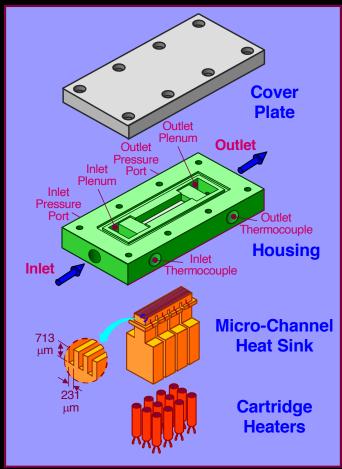








Boiling Configurations: Mini/Micro-channel Flow



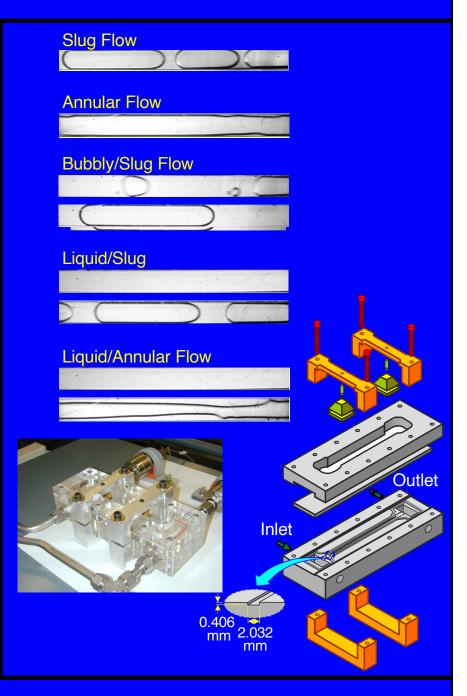






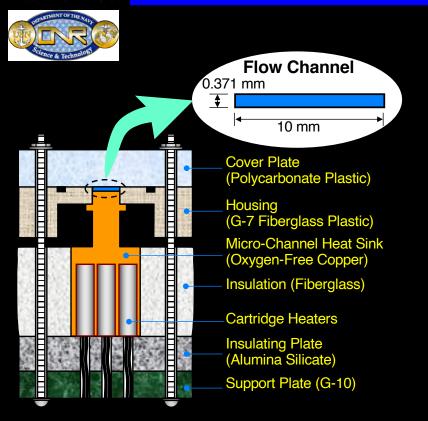


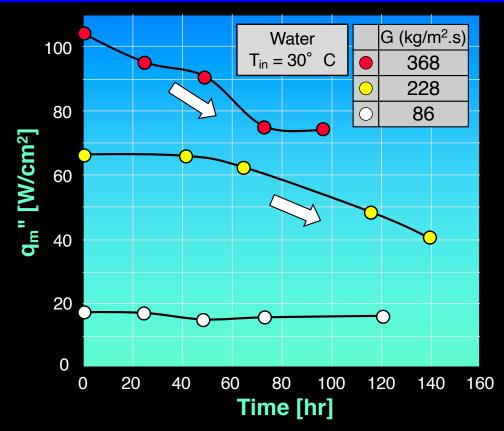


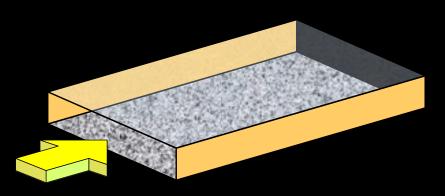


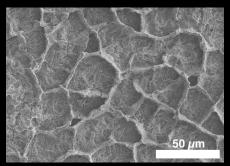


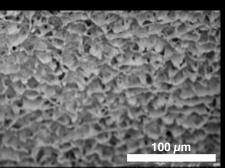
Boiling Configurations: Mini/Micro-channel Flow/Carbon Nanotubes











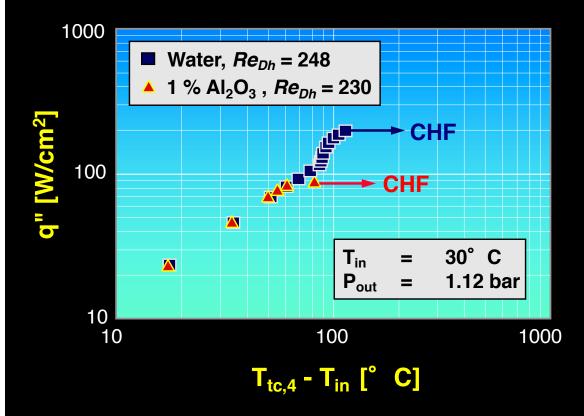
Isolated cellular formations

Dominant 'fish-scale' pattern

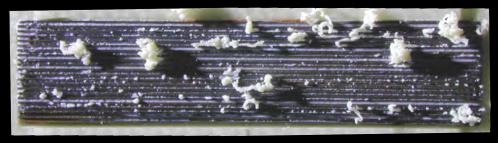
Khanikar, Mudawar & Fisher (2009)

G = 368 kg/m².s, T_{in} = 30° C, after 5 tests





- Stable flow boiling never achieved due to CHF occurrence shortly following onset of boiling
- Severe nano particle deposition inside micro-channels
- Particle clustering began forming at channel outlet, then propagated rapidly upstream
- Temperature of heat sink rose continuously after particle clogging



215 μm x 821 μm

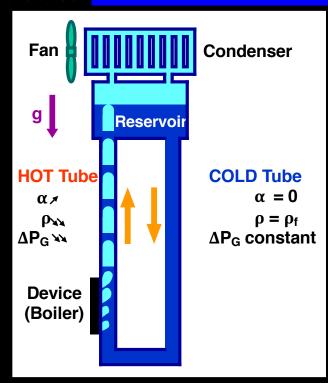
Enhancement efforts should focus on surface itself, not fluid!

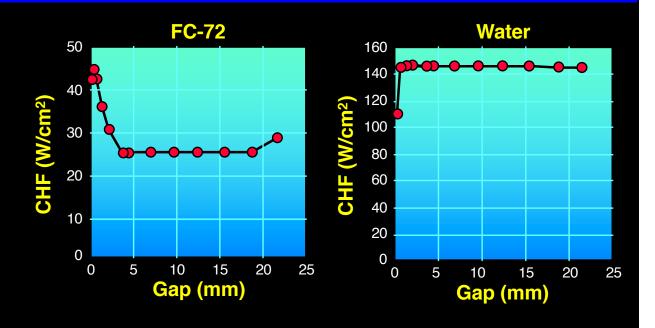


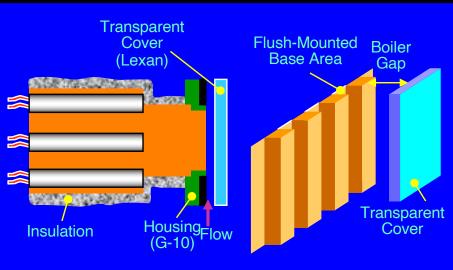
Lee & Mudawar (2006)



Boiling Configurations: Mini/Micro-channel Flow using Smart, Pump-Free Loop









FC-72 0.51 mm gap 50% CHF



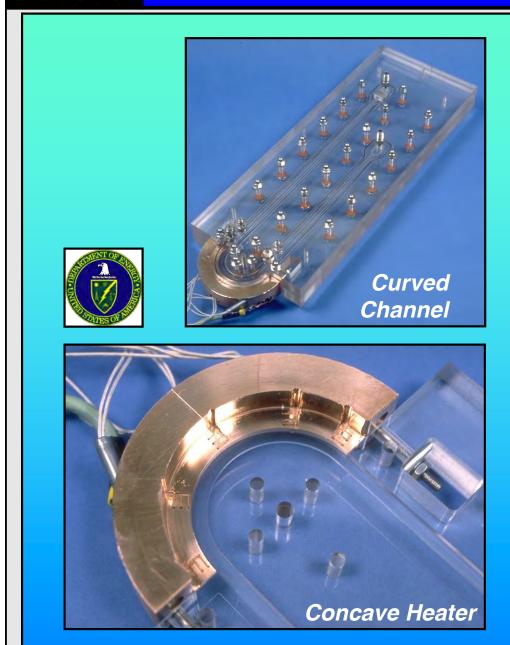
Water 0.13 mm gap 50% CHF

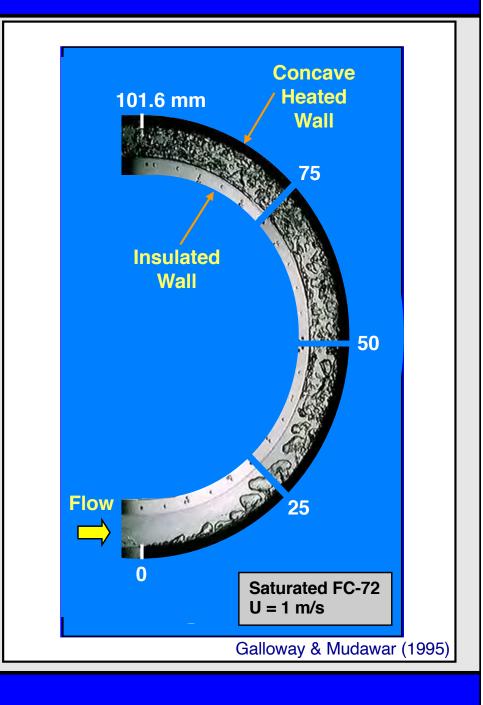


Mukherjee & Mudawar (2003)



Boiling Configurations: Curved Channel Flow

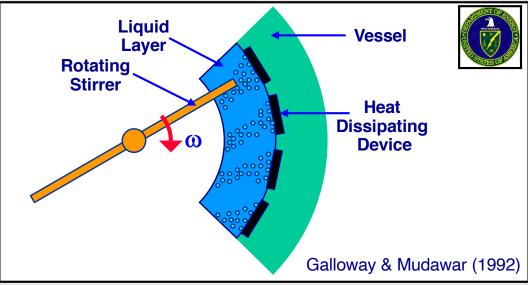






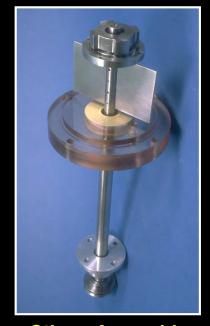
Boiling Configurations: Centrifugal Flow









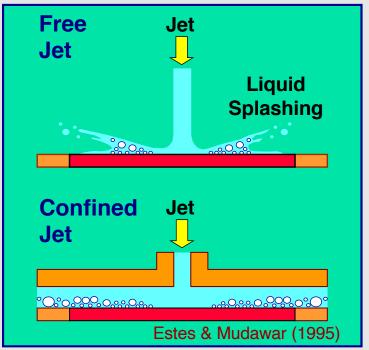


Stirrer Assembly



Boiling Configurations: Jet Impingement







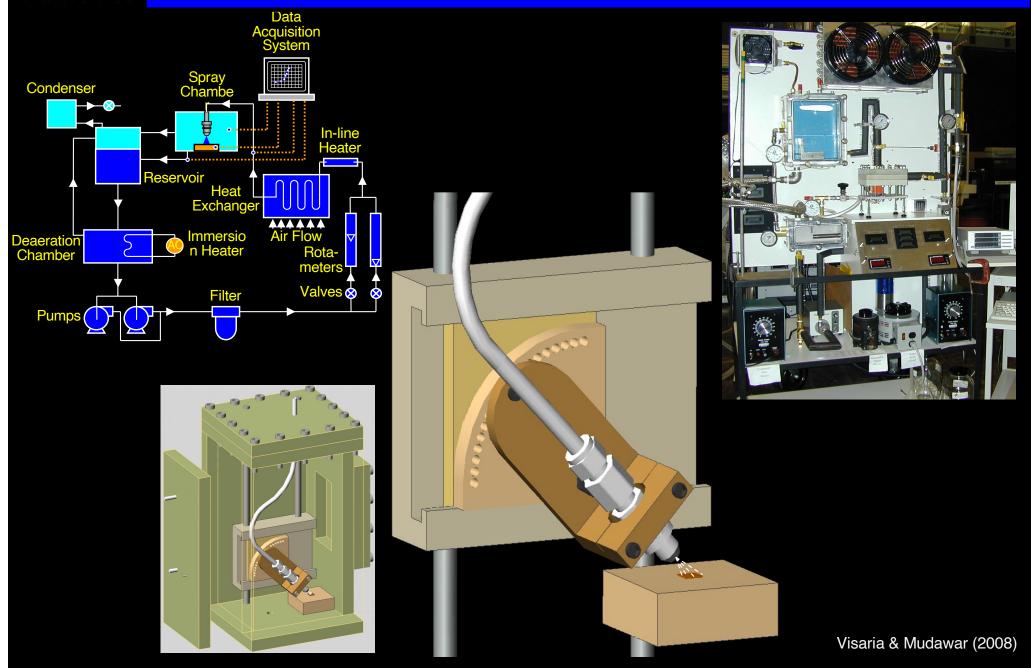
Highest CHF of 411 W/cm² achieved with subcooled flow boiling FC-72 & Surface Enhancement





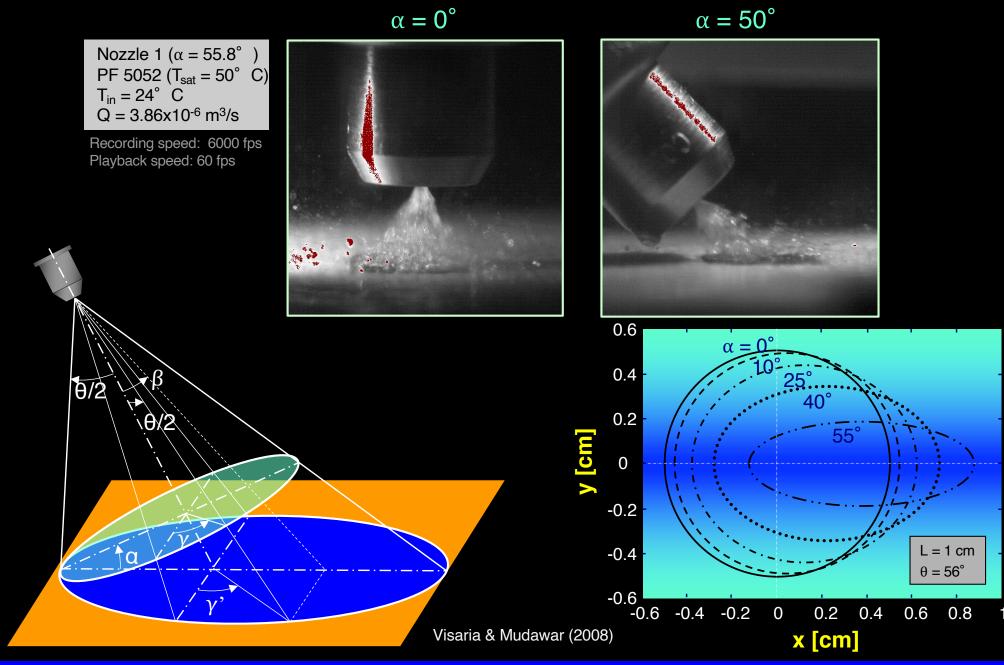


Boiling Configurations: Spray Cooling



PURDUE

Boiling Configurations: Spray Cooling



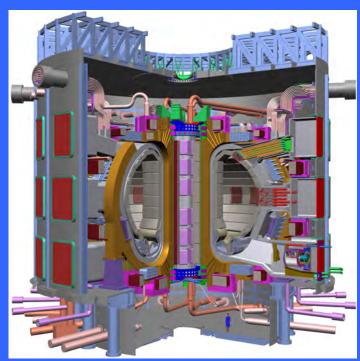


BTPFL Applications

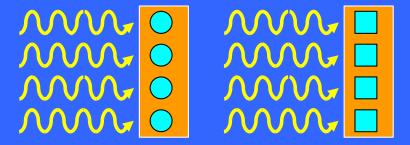


Applications: Very-High-Flux Fusion Reactors, Particle Accelerators & MHD Generators

Fusion Reactor Blanket



International Thermonuclear Experimental Reactor (ITER)

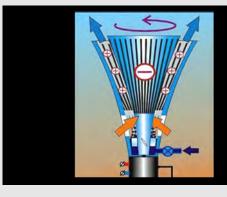


Heat flux in cooling channels can exceed 10⁴ W/cm²

- Magnetic containment of plasma in donut-shaped vacuum vessel (tokomak)
- Fusion reactor blanket extracts fusion power to generate electricity
- Highly subcooled water cooling at high pressure and high mass velocity required to guard against CHF



Particle Accelerator Target



MHD Electrode Walls



Applications: Very-High-Flux Fusion Reactors, Particle Accelerators & MHD Generators

Ultra-High-Flux Flow Boiling in Micro-Channels Low mass velocity High mass velocity High subcooling Low subcooling **Dryout DNB** Liquid film evaporation **Annular** flow **Bubbly Subcooled** flow boiling Slug flow **Saturated** boiling **Bubbly** flow Subcooled boiling Single-**Forced** Single-Forced phase convection convection phase liquid flow liquid flow heat transfer heat transfer

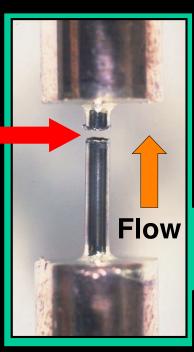
CHF = 27,600 W/cm² demonstrated experimentally

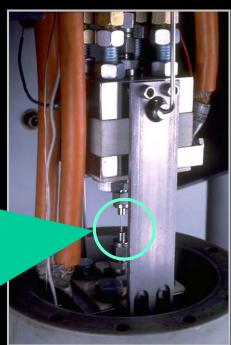




G = 120,000 kg/m².s

D = 0.406 mm





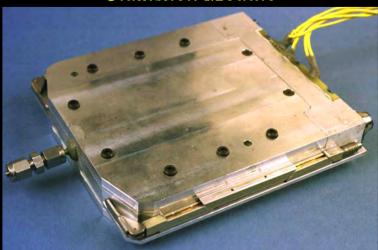
Mudawar & Bowers (1999)



Applications: Avionics

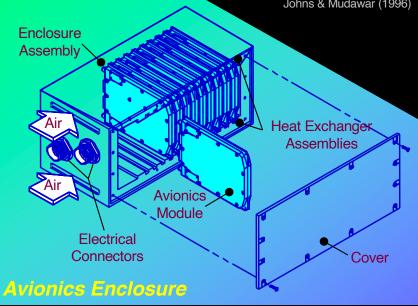
- 40 W cooling capacity for conventional 5.38 x 6.41 x 0.59 in³ edge air-cooled module
- 200 W capacity for equivalent flow-through polyalphaolafin (PAO) module



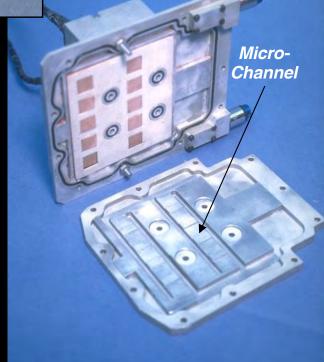


BTPFL-C2 3 kW Micro-Channel Clamshell Module







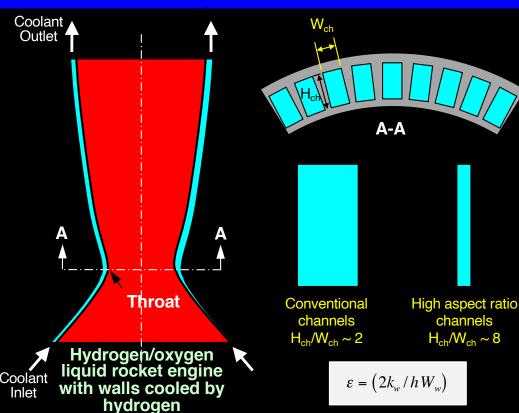




Applications: Boiling in Rocket Engines, Turbine Blades

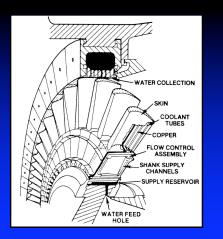
NASA rocket engine with high aspect ratio cooling channels

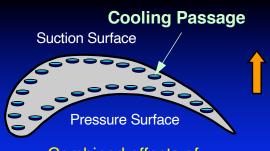




- Engine life doubled by decreasing wall temperature by 50-100° C
- Cooling performance in wall enhanced by using closely-spaced micro-channels separated by thin walls
- Depending on rocket engine type, boiling may or may not be desirable

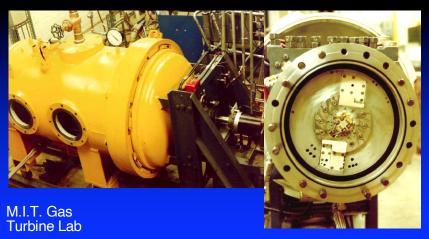






Combined effects of centrifugal and Coriolis forces help achieve 4500 W/cm² inside blade

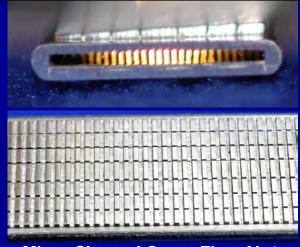






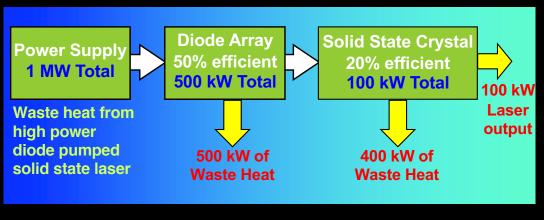


Nacke, Northcutt & Mudawar (2011)

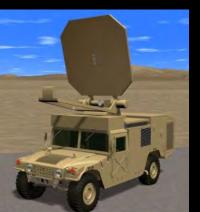


Micro-Channel Cross-Flow Air-to Fuel (JP-8) Heat Exchanger

High-Power Laser, Radar and Microwave Systems









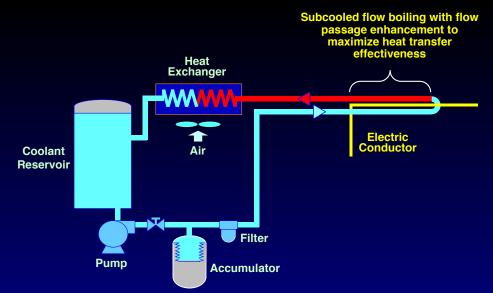


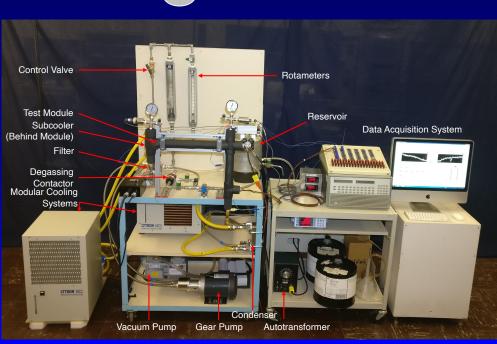


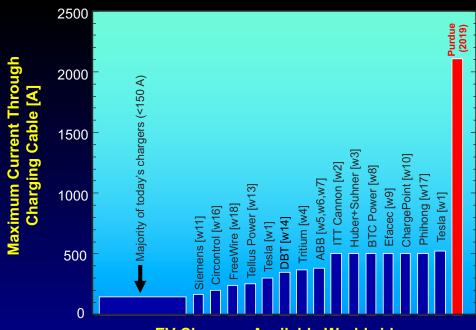
Mudawar (2001)



Applications: 5-Minute Charging of Electric Vehicles





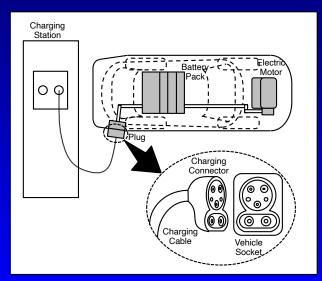


EV Chargers Available Worldwide



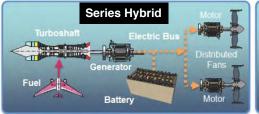


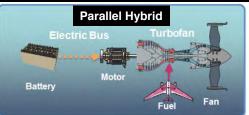


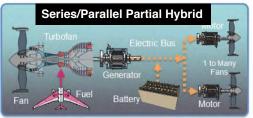


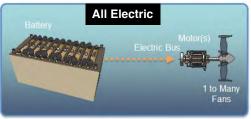


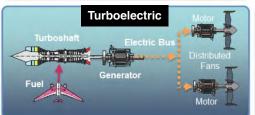
Applications: Hybrid & All-Electric Aircraft

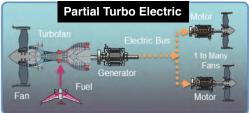












· W TherM



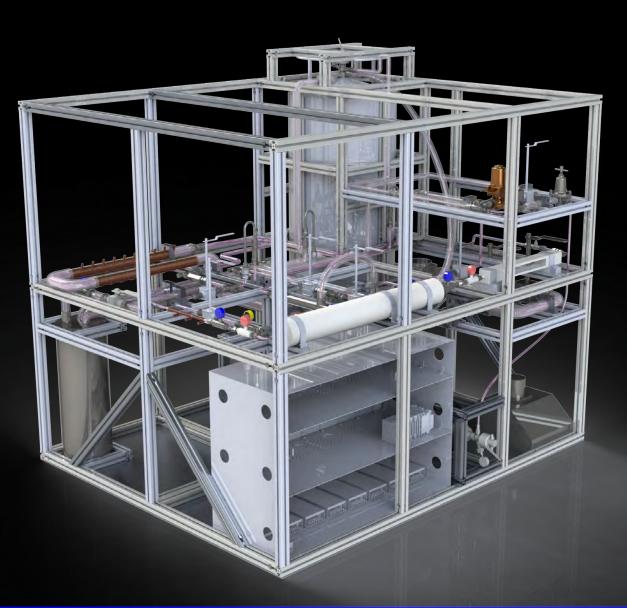
Immediate Goals: High-flux liquid cooling of

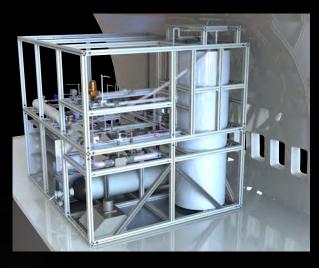
- Power electronics
- Motor
- Power transmission cable
- Other components important to industry partners

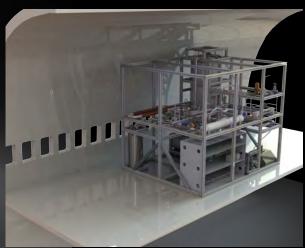








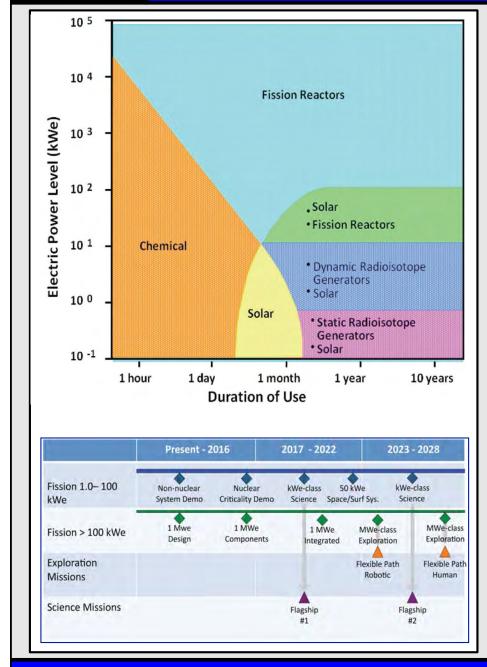






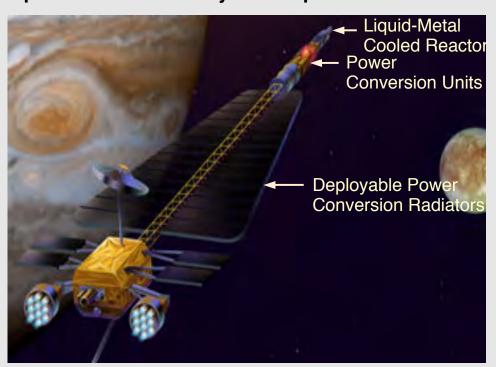
Flow Boiling & Condensation Experiment (FBCE) for the International Space Station (ISS)

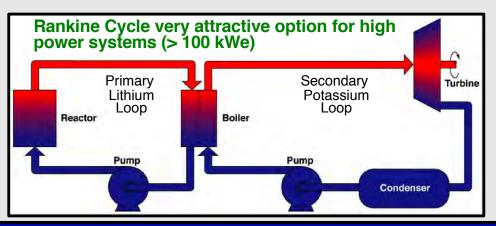
FBCE Applications: Nuclear Fission/Rankine Power Cycle for Future Space Missions



Project Prometheus:

Developing means to efficiently power advanced spacecraft for Solar System exploration

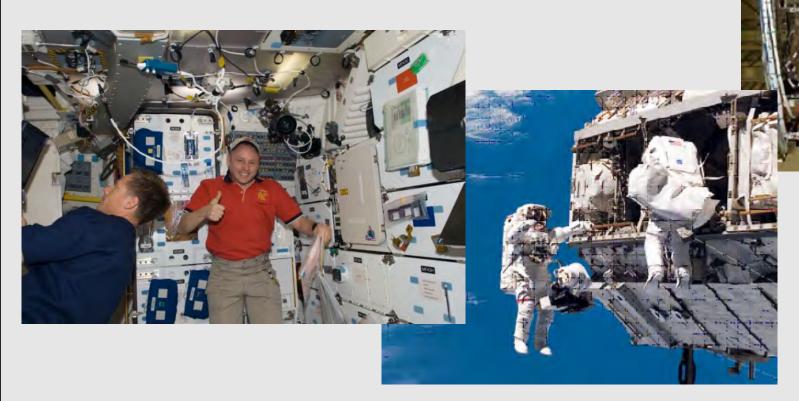






FBCE Applications: Thermal Control Systems (TCSs) & Life Support Systems for Future Space Space Missions

- Thermal management systems responsible for controlling temperature and humidity using Thermal Control System (TCS) consisting of Heat Acquisition, Heat Transport and Heat Rejection hardware
- Refrigerator/freezer components provide cooling for science experiments and food storage
- Advanced water recovery systems transfer crew and system wastewater into potable water for crew and system reuse

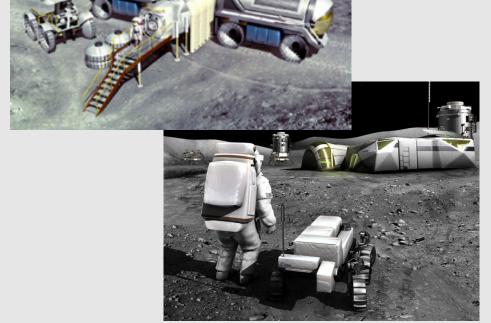


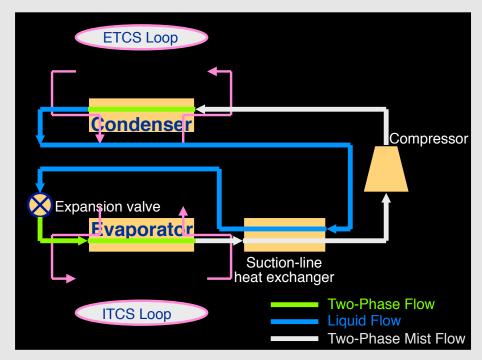


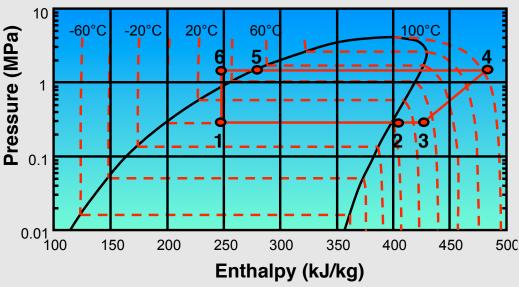
FBCE Applications: Vapor Compression Heat Pump for Future Space Vehicles Planetary Bases

NASA Johnson Space Center (JSC) Ground based Solar Heat Pump (SHP):

- Precursor to R134a vapor compression heat pump for future space vehicles and planetary bases
- Absorbs 5 to 15 kW
- Heat to evaporator provided by single-phase (liquid) Internal Thermal Control Cycle (ITCS)
- Heat from condenser by single-phase (liquid) External Thermal Control Cycle (ETCS)
- Evaporator and Condenser are SWEP Copper Brazed Plate (CBP) heat exchangers

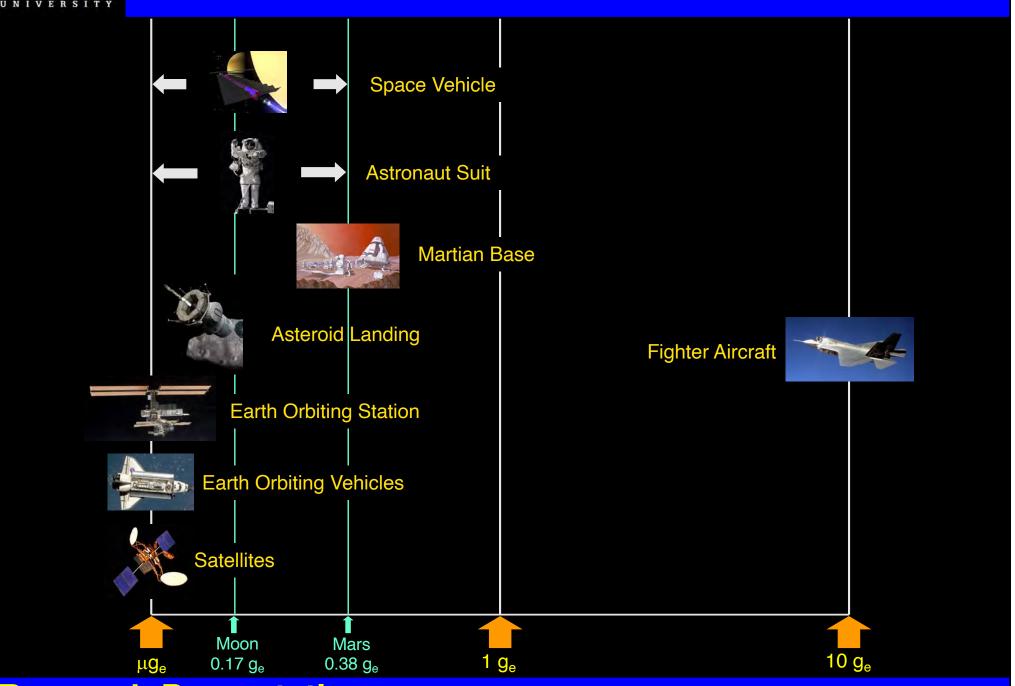








FBCE Applications: Gravity Effects on Two-phase Flow in Space Missions

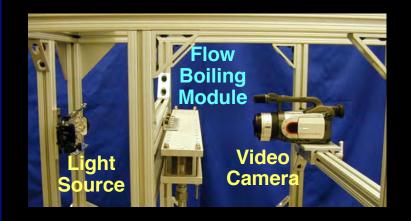


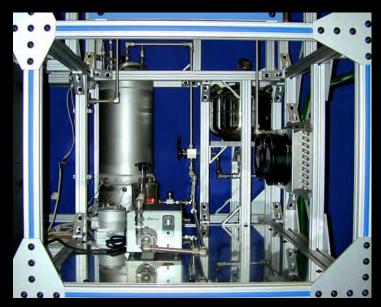






Flight Rack





Two-Phase Flow Loop

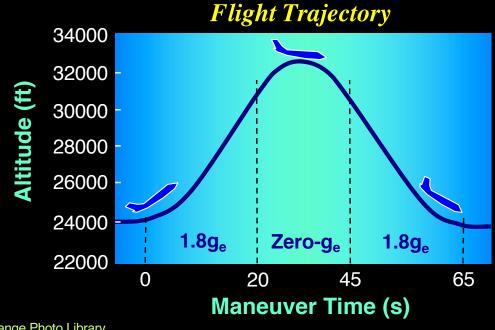




KC-135 Tests performed at NASA Glenn Research Center





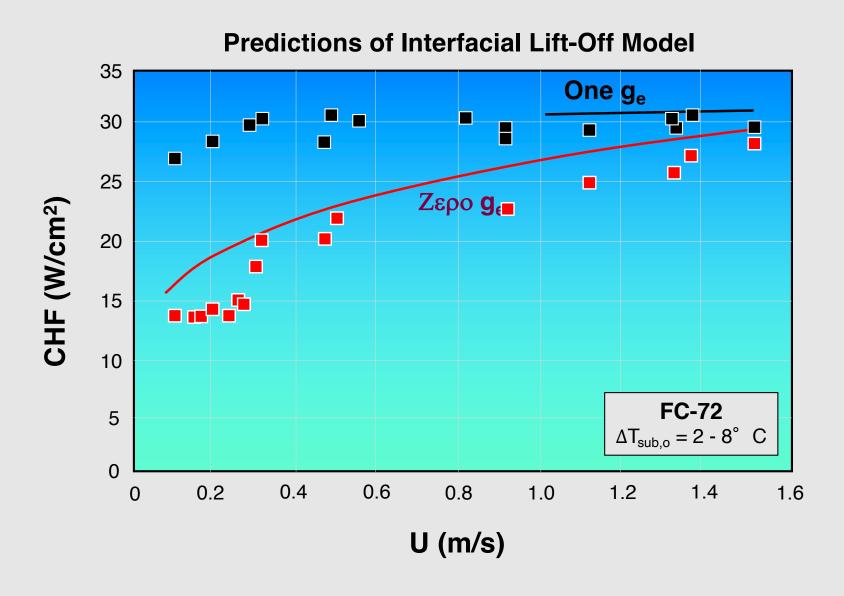


Phase Change Photo Library (Mudawar, 1984 - 2014)

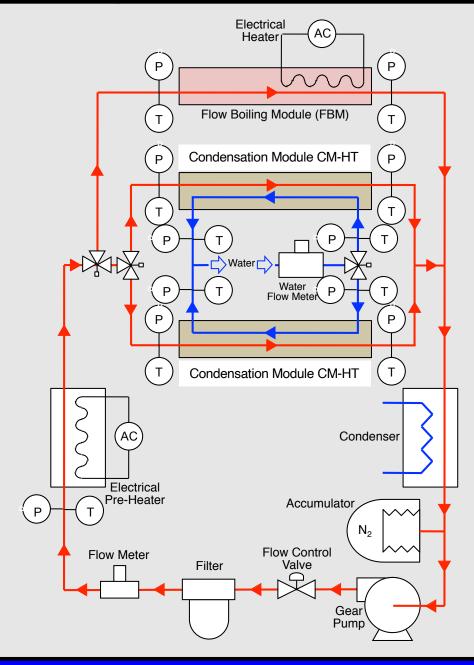












Consists of:

- nPFH sub-loop
- Water sub-loop

Contains three test modules:

- Flow Boiling Module (FBM)
- Condensation Module CM-HT for heat transfer measurements
- Condensation Module CM-FV for flow visualization

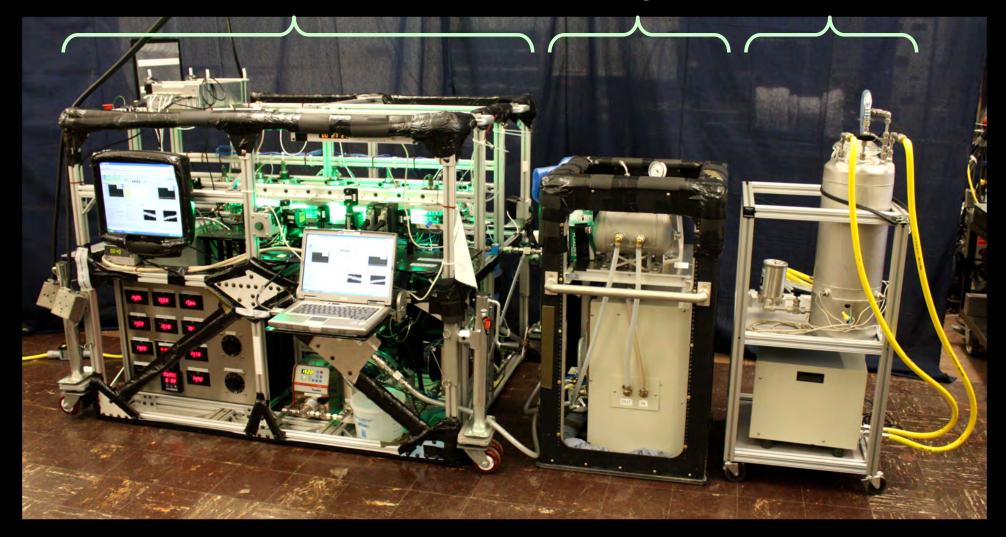


FBCE: Parabolic Flight Condensation Rig

Condensation Rig

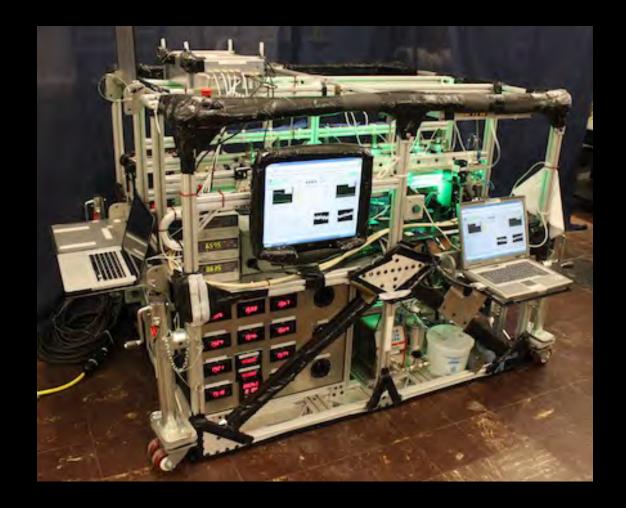
Water Conditioning Rig

Deaeration Rig



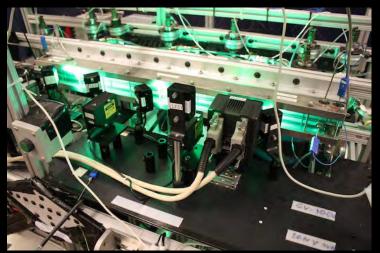








CM-HT: Condensation Module for Heat Transfer Measurements



CM-FV: Condensation Module for Flow Visualization



















Flight Campaigns:

- May 2012
- August 2012















FBCE: The Final Configuration!

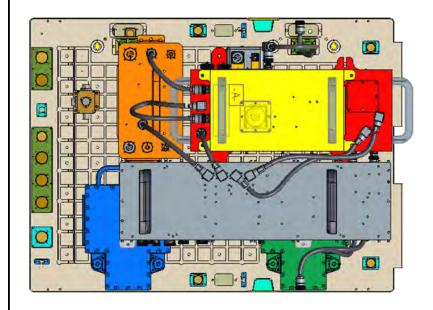


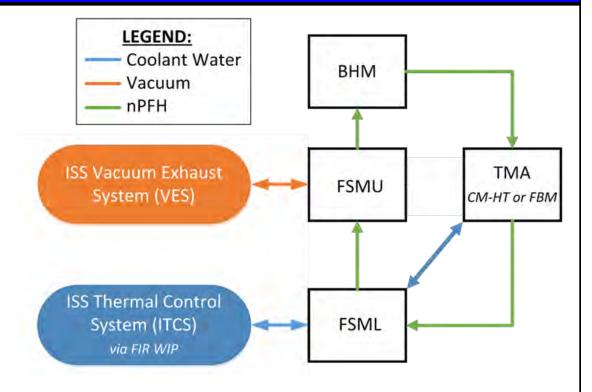




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FBCE: System Overview





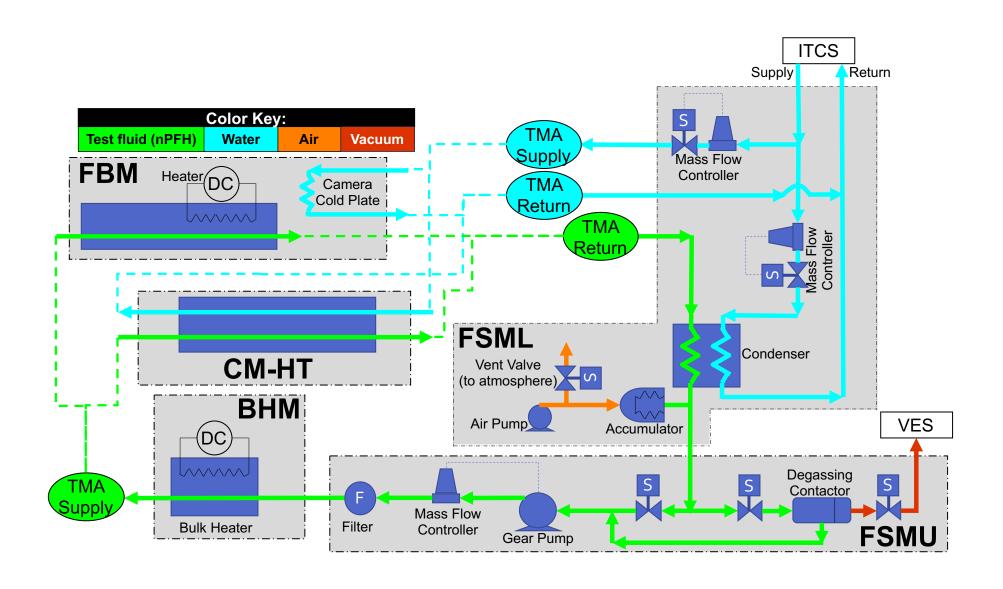
FBCE Modules:

- BHM Bulk Heater Module
- FSMU Fluids System Module Upper
- FSML Fluids System Module Lower
- RDAQM 1 Remote Data Acquisition Module 1
- RDAQM 2 Remote Data Acquisition Module 2
- ► TMA Test Module Assembly (1 of 2 installed):
 - FBM Flow Boiling Module
 - CM-HT Condensation Module Heat Transfer

FIR Provided Hardware:

- SAMS Space Acceleration Measurement System
- CCU Confocal Control Unit (on back of rack)
- IPSU-CL Imaging
 Processing Storage Unit –
 Camera Link (on back of rack)

FBCE: Fluid System Overview



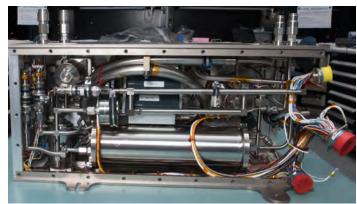


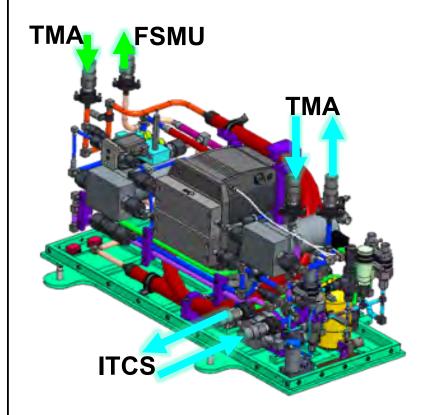
FBCE: Fluid System Module - Lower

- Provides primary cooling for the test fluid exiting the test section, and the test section itself
- System pressure set by pressurizing or venting the air-side of a bellows accumulator







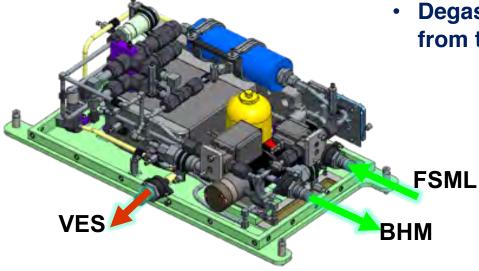


Color Key:
Test fluid (nPFH) Water Air



FBCE: Fluid System Module - Upper

- Mass flow controller drives a gear pump to provide flow throughout the closed loop system
- Multiple controls in place to prevent overpressurization
- Degassing contactor removes dissolved gases from test fluid when membrane exposed to vacuum





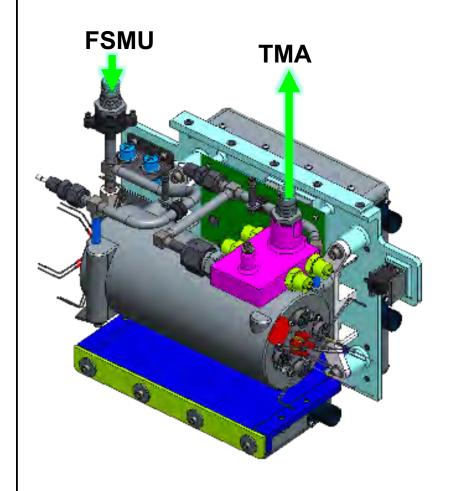
Color Key:
Test fluid (nPFH) Vacuum







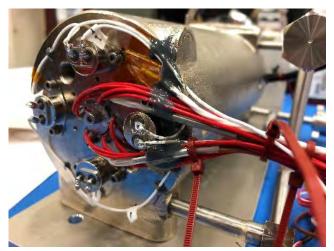
FBCE: Bulk Heater Module

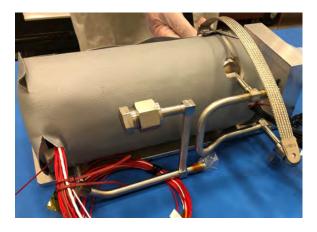


Color Key:
Test fluid (nPFH)

- Primary source of heating to condition test fluid to required test section inlet conditions
- Three 120V primary heaters and three 28V booster heaters can be operated at any time, with backup heaters available



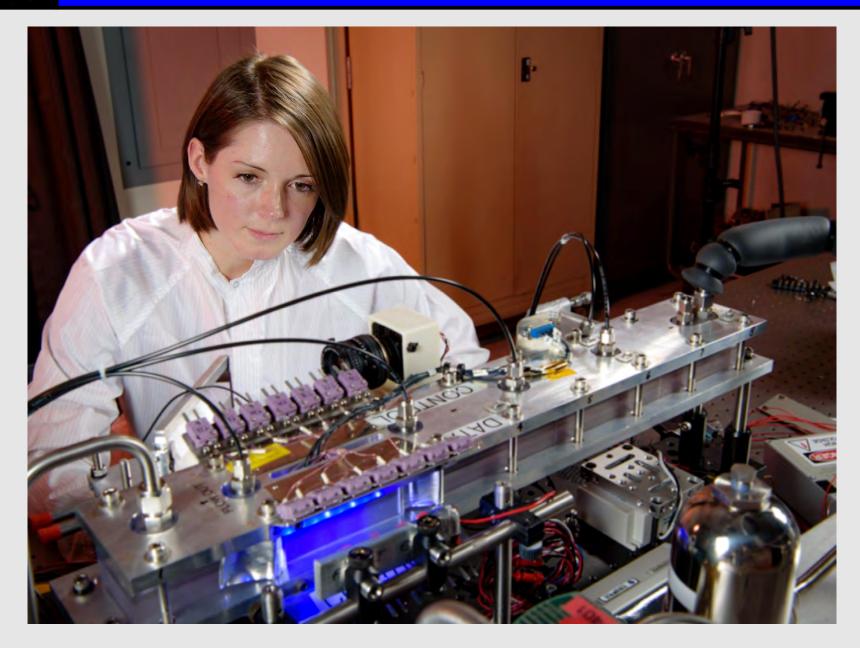








FBCE: Flow Boiling Module (FBM)





Remote Data Acquisition Module 1 (RDAQM1)





UEI Data Cubes (Thermocouple Signal Conditioning)

Remote Data Acquisition Module 2 (RDAQM2)



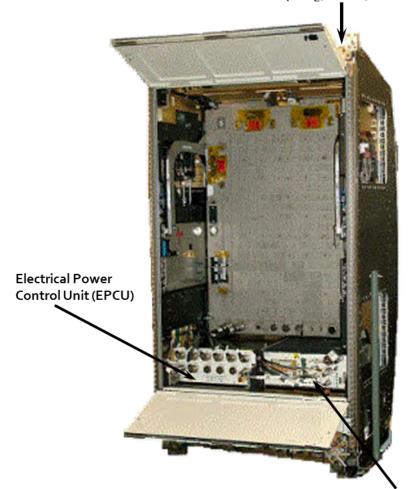


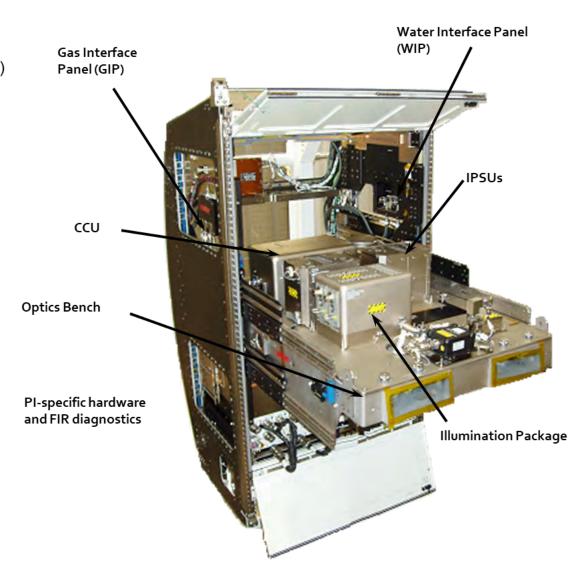
UEI Data Cube and Custom Sensor Supply Printed
Circuit Board
(Signal Conditioning and Power Distribution)

FBCE: Fluids Integrated Rack (FIR)

Environmental Control (ECS)

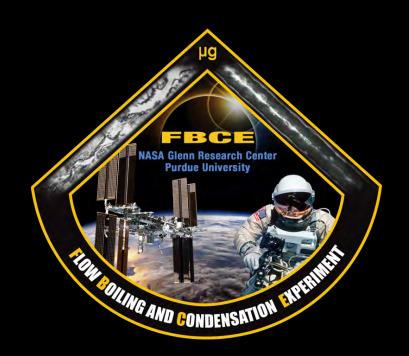
- · Air Thermal Control
- · Fire Detection & Suppression
- Water Thermal Control
- Gas Interfaces (GN₂, VES, VRS)







FBCE: Preparations for Launch











FBCE: August 10, 2021 Launch from NASA's Wallops Flight Facility in Virginia





Largest Cygnus cargo ever launched to ISS (3,723 kg)



Launch (August 10, 2021, 6:01 pm ET)



Arrival at ISS (August 12, 2021, 6:10 am ET)



Predictive Methods



Predictive Methods for Liquid-Vapor Two-Phase Systems

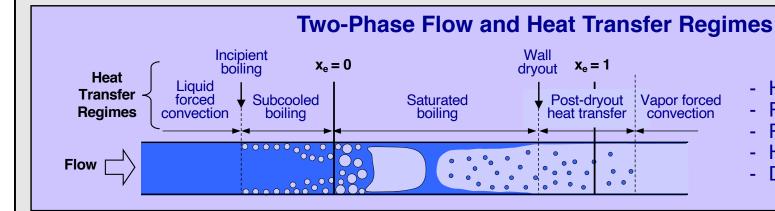
- Computational methods: computationally very intensive; predictions very sensitive to numerical and phase change model used
- Theoretical models: very few exist!
- Semi-empirical models: mechanistic models with specific constants determined from empirical data
- 'Universal' experimental correlations: based on large databases for many fluids and broad ranges of geometrical or flow parameters; few exist; most desirable in industry
- Narrow-range experimental correlations: applicable to one or very few fluids and limited ranges of geometrical or flow parameters; often extrapolated resulting in erroneous predictions
- Replication: performance based on specific fluid, geometry, and operating conditions of given device

Recent Challenges:

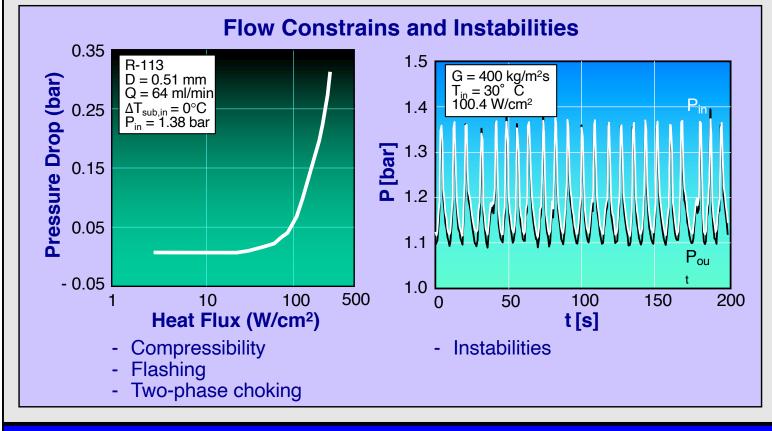
- > Reluctance to develop large, complex phase-change facilities
- > Studies focused on development of narrow-range correlations or simply data trends
- Findings very incremental
- Avoidance of mechanistic models

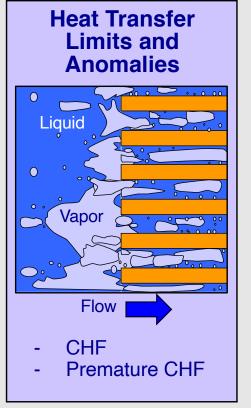


Fundamental Physics of Flow Boiling and Heat Transfer



- Heat transfer regimes
- Regime boundaries
- Pressure drop components
- Heat transfer coefficients
- Dryout versus CHF





Consolidated World Databases and Correlations for Flow Boiling Critical Heat Flux of Water in Tubes



Flow Boiling Heat Transfer Transfer Coefficient

Universal Heat Transfer Correlation for Saturated Boiling in Small Channel

Consolidated database:

10,805 saturated boiling heat transfer coefficient data points from 37 sources

FC72, R11, R113, R123, R1234yf, R1234ze, R134a, R152a, R22, R236fa, R245fa, R32, R404A, R407C, R410A, R417A, CO₂, water

 $Bo = \frac{q_H^{\prime\prime}}{G h_{fa}}$

- $-0.19 < D_h < 6.5 \text{ mm}$
- $-19 < G < 1608 \text{ kg/m}^2\text{s}$
- $57 < Re_{fo} = GD_h/\mu_f < 49,820$
- -0 < x < 1
- 0.005 < *Reduced pressure* < 0.69

$$h_{tp} = \left(h_{nb}^2 + h_{cb}^2\right)^{0.5}$$

For nucleate boiling dominant regime:

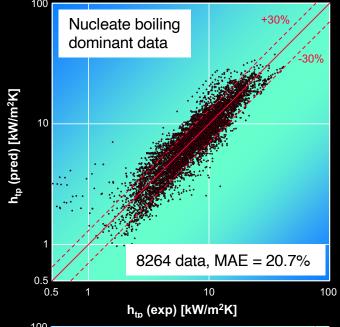
$$h_{nb} = \left[2345 \left(Bo \frac{P_H}{P_F} \right)^{0.70} P_R^{0.38} (1-x)^{-0.51} \right] \left(0.023 Re_f^{0.8} P r_f^{0.4} \frac{k_f}{D_h} \right)$$

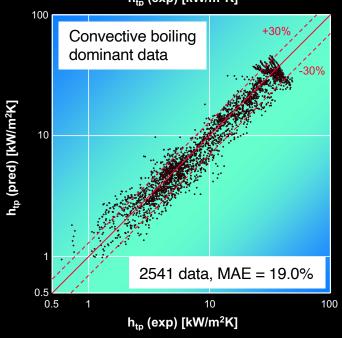
For convective boiling dominant regime:

$$h_{cb} = \left[5.2 \left(Bo \frac{P_H}{P_F} \right)^{0.08} W e_{fo}^{-0.54} + 3.5 \left(\frac{1}{X_{tt}} \right)^{0.94} \left(\frac{\rho_g}{\rho_f} \right)^{0.25} \right] \left(0.023 R e_f^{0.8} P r_f^{0.4} \frac{k_f}{D_h} \right)$$

Kim & Mudawar, Int. J. Heat Mass Transfer, 2013









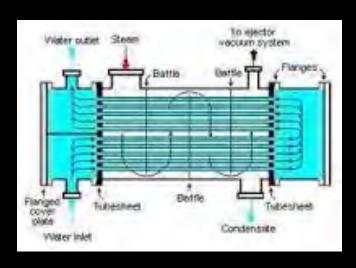
Air Cooled Condensers for Refrigerant





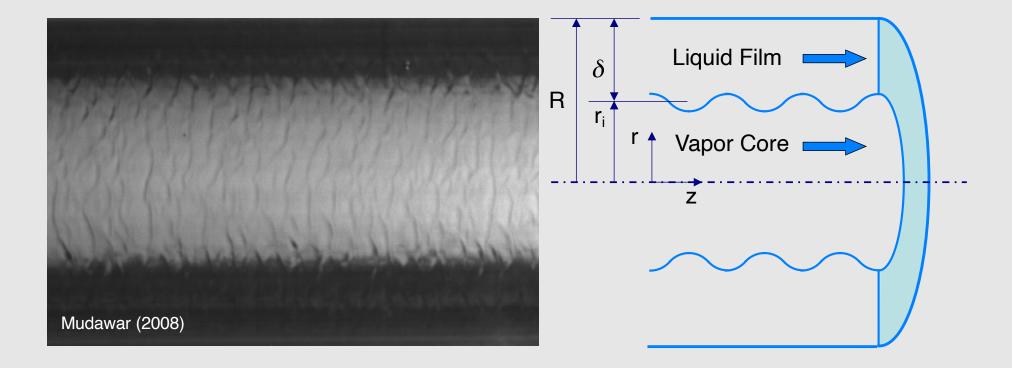


Shell-and-Tube Condensers









- Different flow regimes: pure vapor, annular, slug, bubbly and pure liquid
- Annular regime most prevalent ... separated two-phase flow consisting of thin shear-driven liquid film along tube wall and central vapor core
- Thin annular film responsible for high condensation heat transfer coefficients

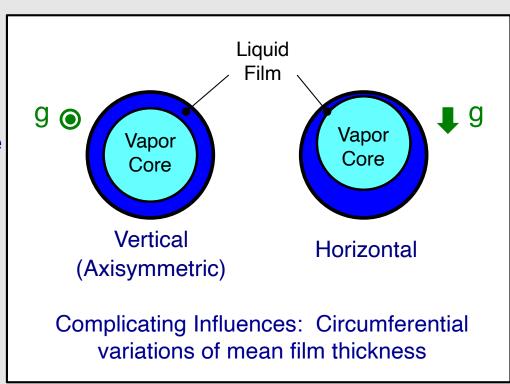


Common perception:

Separated flows presumed convenient to model because they can be represented by two predominantly single-phase flows

Complicating Influences (Fluid Physics):

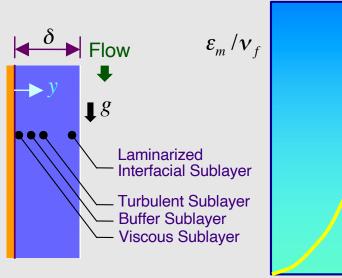
- 1. Circumferential variations of mean film thickness due to transverse body force
- 2. Complex transitional characteristics of condensation films
- 3. Turbulence dampening near film interface
- 4. Interfacial waves
- 5. Droplet entrainment and deposition

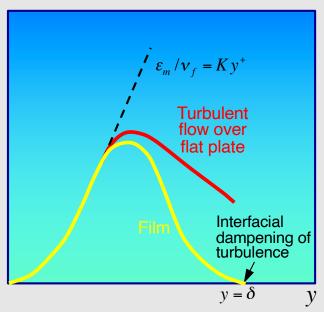


Challenges:

- 1. Develop fundamental understanding of all above
- 2. Incorporate all above influences into robust predictive model

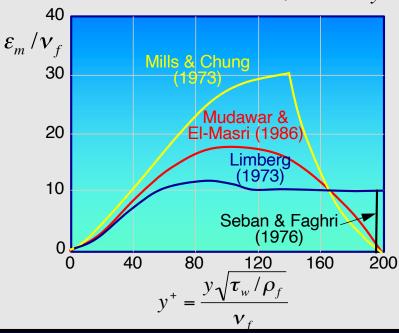
Complicating Influences: Turbulence Dampening near Film Interface

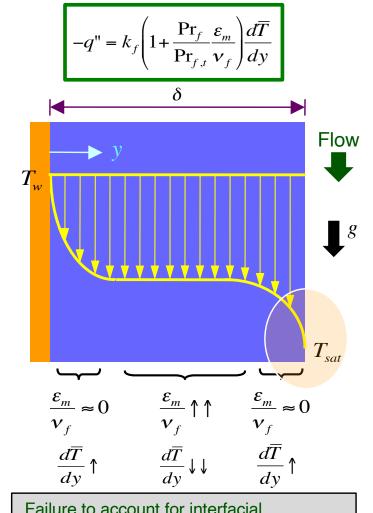




- Near-wall region: Most use Van Driest (1956) function
- Mudawar & El-Masri: Ueda et al. (1977) experimental profile in middle, and a function of Kapitza number near interface:

$$Ka = \frac{\mu^4 g}{\rho \sigma^3}$$

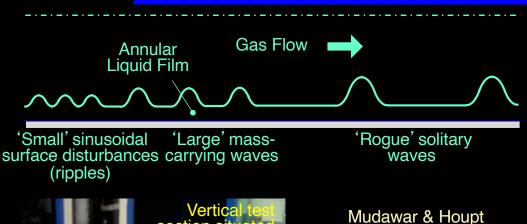


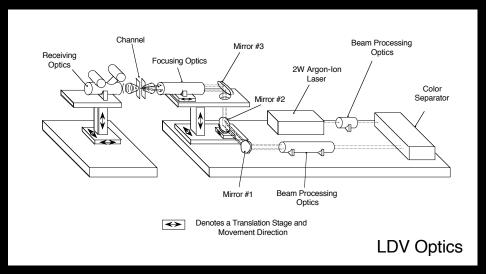


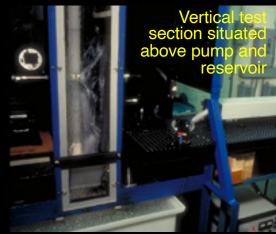
Failure to account for interfacial dampening of turbulence near the interface and large interfacial temperature gradient has been shown to produce significant errors in predicting heat transfer across films!!



Complicating Influences: Interfacial Waves

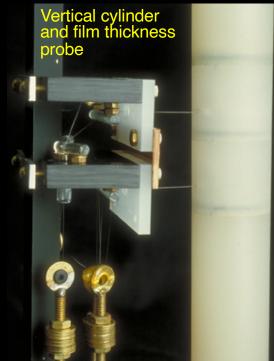






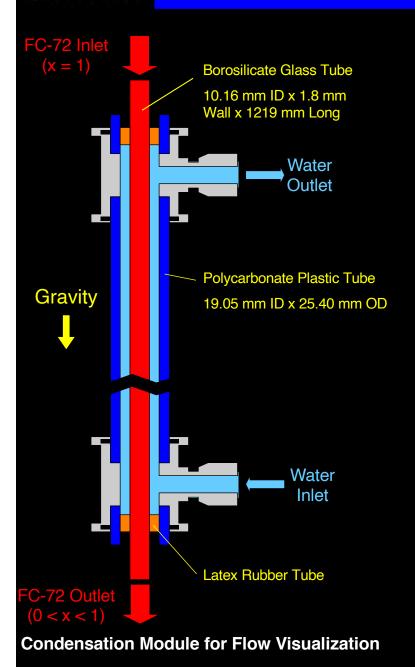
Beam crossing viewed from bottom of sampling channel

(1993a,b)



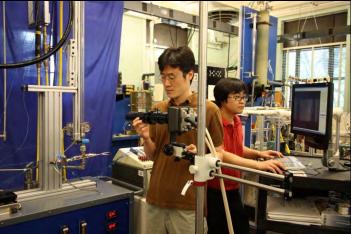


Condensation Measurements





Purdue
High Capacity
Condensation
Facility



High-Speed Video Motion Analysis System:

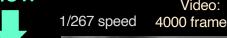
- •Photron FASTCAM-Ultima camera with shutter speeds up to 1/120,000 s
- •Infinity K-2 high magnification lenses
- •PerkinElmer Xenon source fitted with Olympus fiber optic cable

Condensation Measurements - Large Tubes

Flow

$m_{FC-72} = 19.5 - 19.6 \text{ g/s}$





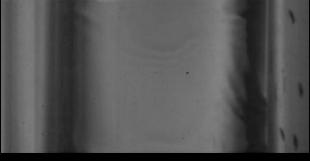
Video: 4000 frames/s



Video: 4000 frames/s

1/133 speed

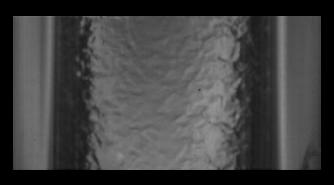
Inlet



Purdue High Capacity **Condensation Facility**

Middle





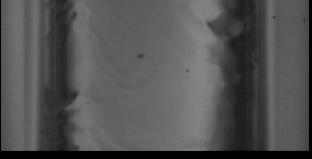
For $Re_{f,FC-72,exit} < 200$

- Smooth Laminar in inlet
- Wavy Laminar in middle and outlet

For $Re_{f.FC-72.exit} > 200$

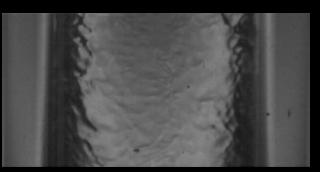
- Flow appears to turn turbulent
- Wave structure more complex





$$Re_{f, FC-72, exit} = 179 - 181$$

 $q_{out}[W] = 77.5 - 78.3$



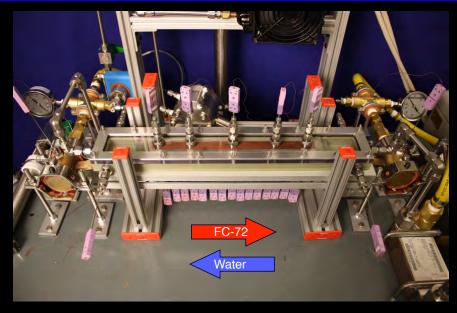
 $Re_{f, FC-72, exit} = 927 - 960$ = 392 - 406q_{out} [W]



Flow

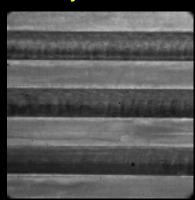
Condensation Measurements - Small Channels





Annular

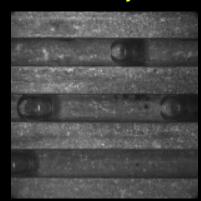
Wavy-Annular



Slug



Bubbly



Purdue
Small Channel
Condensation Facility

Regime	FC-72 (g/s)	Water (g/s)	Video Rate
Annular	1.51	5.06	1/66.6
Wavy-Annular 1.51	2.97	1/66.4	
Slug	0.55	2.97	1/66.4
Bubbly	0.55	5.06	1/66.4



In Pursuit of More Efficient, Renewable and Cleaner Energy ...

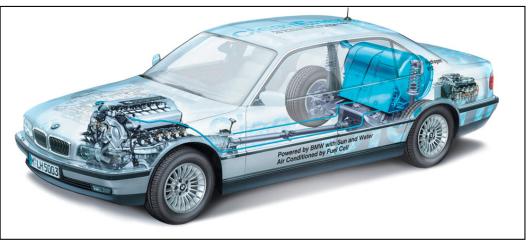
- 1. Hydrogen Fuel Cells
- 2. Hybrid Vehicles
- 3. Solar Receivers
- 4. Intelligent Heat Treating of Metal Alloys

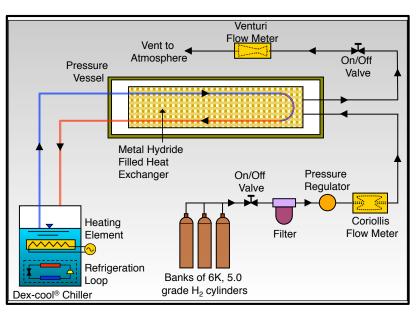


1. Heat Exchanger for Hydrogen Storage Fuel Cell Systems



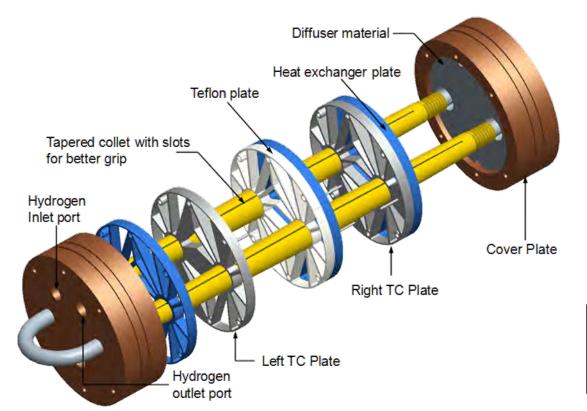
- Developed for high-pressure metal hydride (e.g., Ti_{1.1}CrMn) storage systems
- Used to remove large amount of heat dissipated from hydriding reaction when H₂ is charged into storage vessel

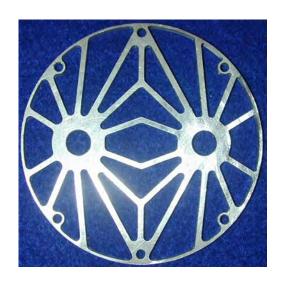






1. Thermally-Optimized Heat Exchanger





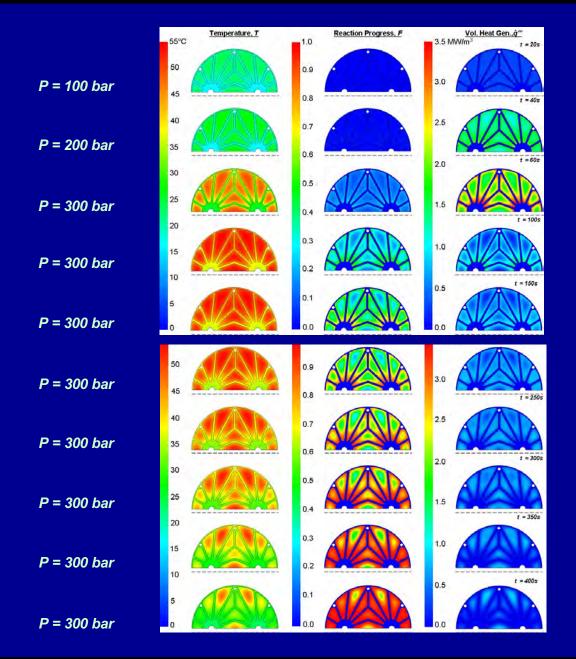
US Patent 8,636,836 B2 January 28, 2014

Assembled Heat Exchanger





1. Transient Contours of Temperature, Fraction of Reaction Completion and Volumetric Heat Generation Rate during Hydriding

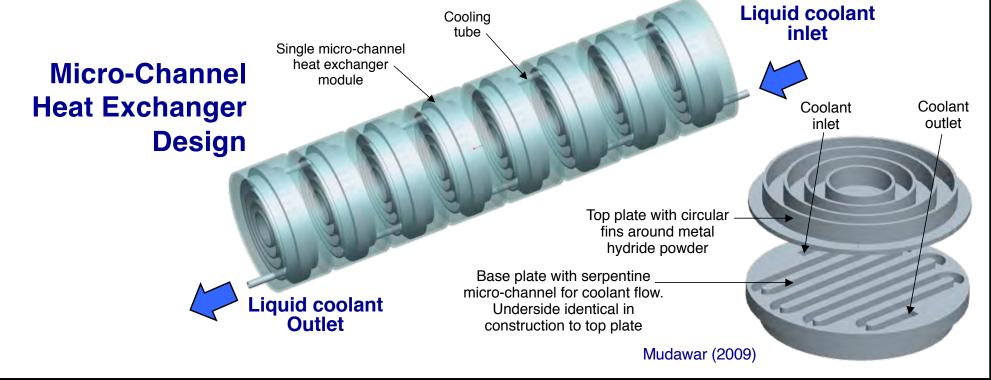


1. Coiled and Micro-Channel Heat Exchangers



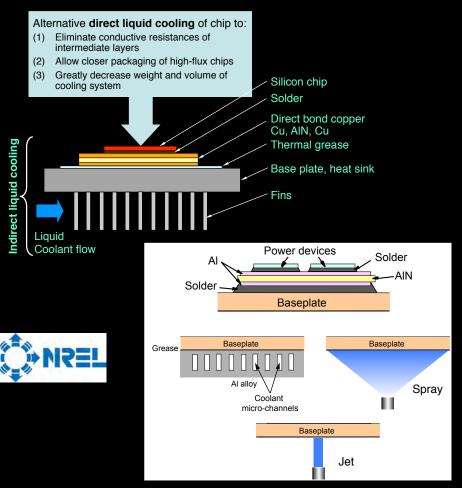
Coiled Heat Exchanger Design

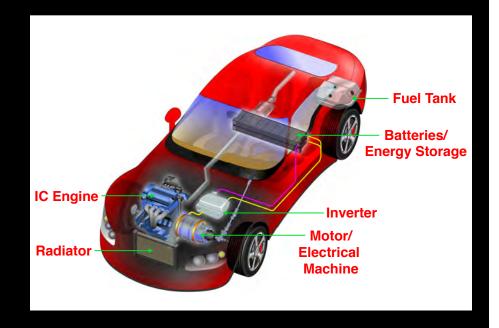
> US Patent 8,778,063 B2 July 15, 2014



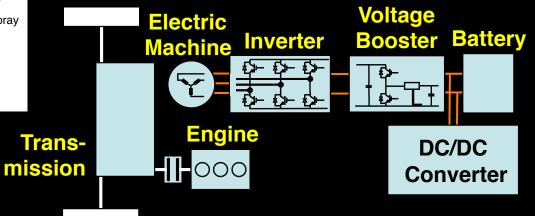


2. Hybrid Vehicle Power Electronics



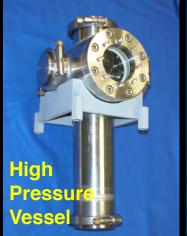


- Goal: dissipate over 250 W/cm² while maintaining device temperature below 125° C for silicon devices
- Two-phase cooling options: R134a loop that taps into vehicle's refrigeration loop, or separate HFE 7100 cooling loop





2. NREL Hybrid Vehicle Power Electronics Thermal Test Laboratory







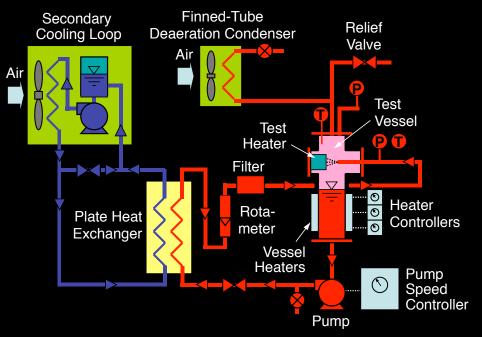




Mudawar, Bharathan, Kelly & Narumanchi (2009)







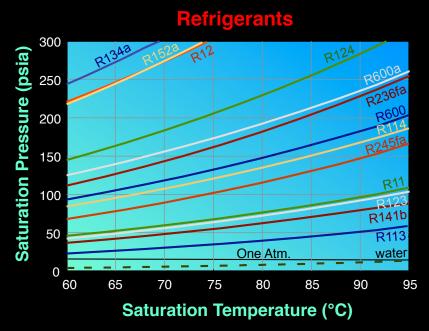




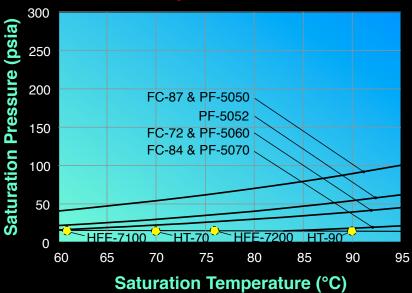
Power Supply and Instrumentation Rack



2. Coolant/Refrigerant Thermal/Environmental Study



Liquid Coolants



Refrigerants

Chlorofluorocarbons (CFCs) (*e.g.*, R11, R12, R113 and R114) composed of chlorine, fluorine and carbon; they are nontoxic and inert, but highly ozone-depleting and contribute to global warming.

Hydrochlorofluorocarbons (HCFCs) (e.g., R123, R124 and R141b) constitute a more recent alternative to CFCs, given their somewhat similar inertness and cooling characteristics but less than 10% of the ozone-depleting effects of CFCs.

Hydrofluorocarbons (HFCs) (e.g., R134a and R143a) provide essentially zero ozone depletion and reduced global warming effects; R134a has good ratings in most performance categories.

Liquid Coolants

3M perfluorocarbons (PFCs) (*e.g.*, Fluorinerts FC-72, FC-87 and FC-84, and Performance Fluids PF-5050, PF-5052, PF-5060 and PF-5070) have *average* environmental ratings because of their relatively high GWP

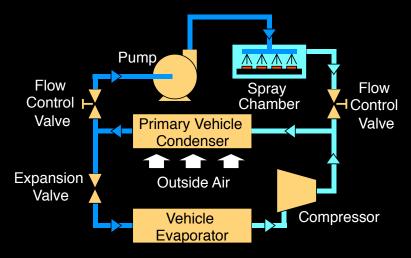
3M HFCs (*e.g.*, Novec fluids HFE-7100 and HFE-7200). HFE-7100 has *good* ratings in all performance categories but HFE-7200 carries a low LEL. HFE-7100 has a freezing point of -135° C, which is well below any expected automobile application range of temperatures.

Most promising: R134a and HFE-7100

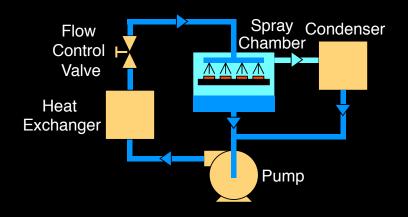


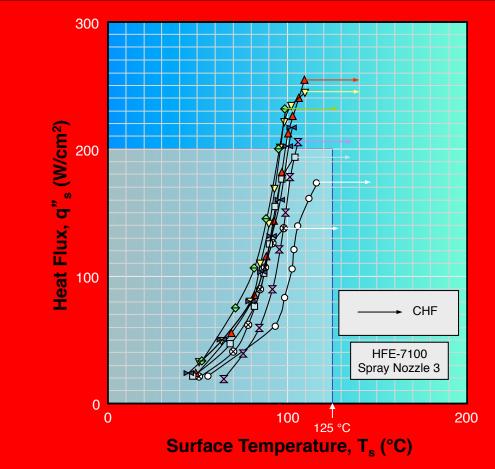
2. Cooling Loop Options for Hybrid Vehicle Power Electronics

Modified R134a Air-Conditioning Refrigeration Loop



Separate Cooling Loop with Appropriate Coolant



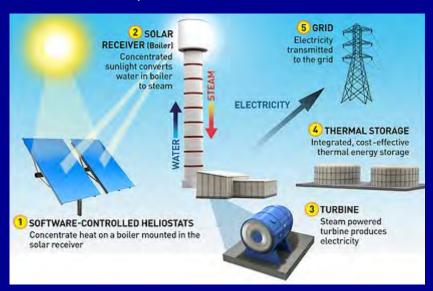


- R134a can yield high CHF values, but cannot maintain low device temperatures.
- HFE-7100 can yield CHF values in excess of 200 W/cm² at surface temperatures below 125° C.
- Two-phase HFE-7100 spray cooling is effective at meeting thermal management requirements of hybrid vehicle electronics.

3. Solar Receiver Steam Generator

Ivanpah Solar Power Facility

- World's largest solar thermal project
- California Mojave Desert
- 3,600 acres (3 units)
- 370 MW power output
- 173,500 heliostats
- Serves 140,000 homes



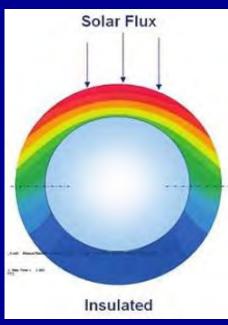
- Evaporator heats subcooled water to boiling temperature to produce steamwater mixture at high pressure and temperature
- Heat flux one-sided and much higher than in fossil boilers





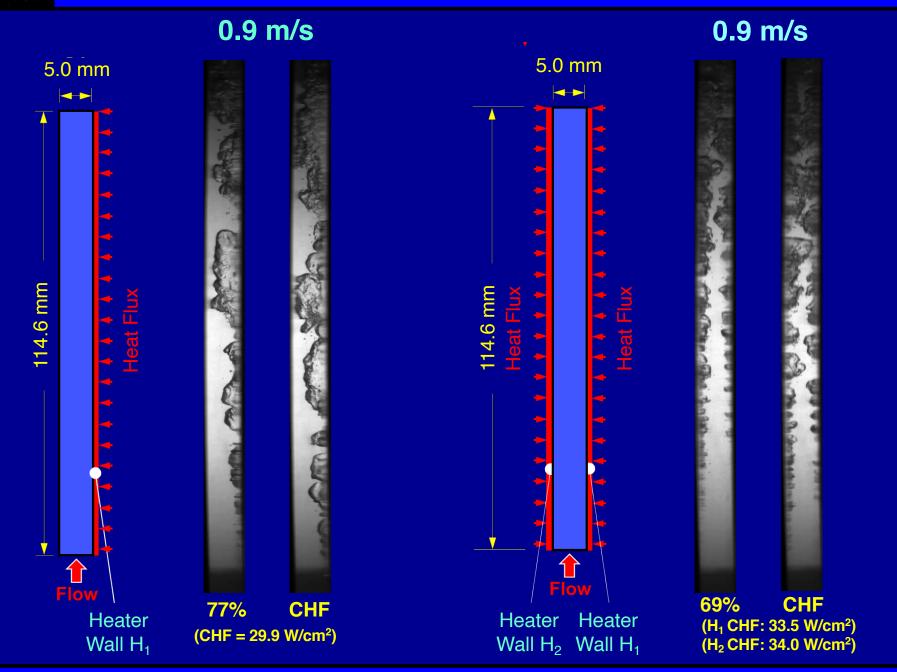
120' Solar Receiver Steam Generator

339' Tall Tower



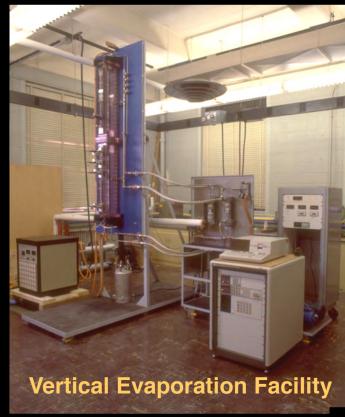


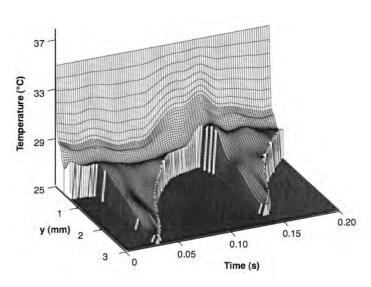
3. Single-Sided versus Double-Sided Heating





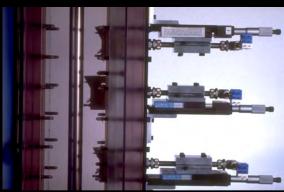
3. Measurement of Effects of Waves on Wavy Heated Liquid Layers



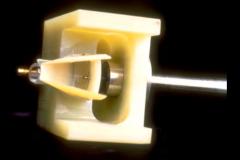


Temperature fluctuations across wavy, turbulent water film falling on vertical heated cylinder at Re = 5700 (Lyu & Mudawar, 1991) Thermocouple Knife-edge for Measurement of Temperature Profile across Wavy Liquid Layer





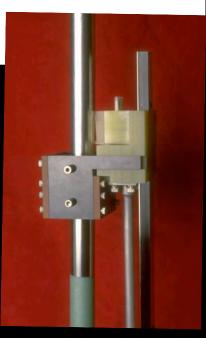
Translation stages for liquid layer probes



Scoop for measurement of mean liquid layer temperature

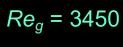
Probe for simultaneous measurement:

- Temperature profile across liquid layer
- Liquid layer thickness
- Interfacial wave speed





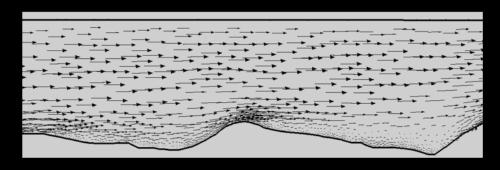
3. Computed Nitrogen Velocity Vector and Contour Plots along Stationary Wavy Interface

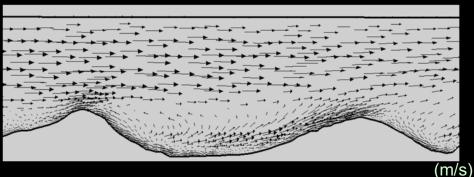


→ 24 m/s

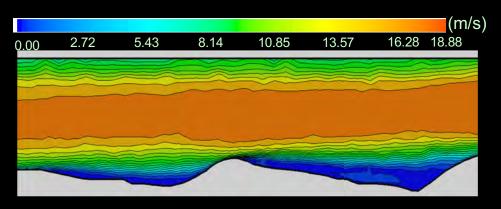
 $Re_g = 6100$

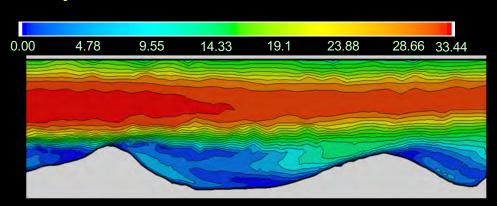
→ 40 m/s





Nitrogen velocity vector plots at z = 0





Nitrogen velocity contour plot at z = 0

FLUENT, k - ω model



4. Intelligent Heat Treating of Aluminum Alloy Parts

Enormous Energy Consumption

Poor Productivity

High Scrap Rate

High Water Consumption

High Emissions & Greenhouse Gases



Up to 50% of Cost of Aluminum Production associated with Post-Processing of Poorly Produced Parts



U.S. Aluminum Industry Profile

Energy Consumption: 200,000 Trillion BTU 23.0 B lbs Annual Production Volume Generates \$65 Billion (plus \$87 B indirect) 155,000 Employees (plus 517,000 Indirect)

Source: Aluminum Assoc.

Large Residual Stresses

Warping

Cracking

Soft Spots

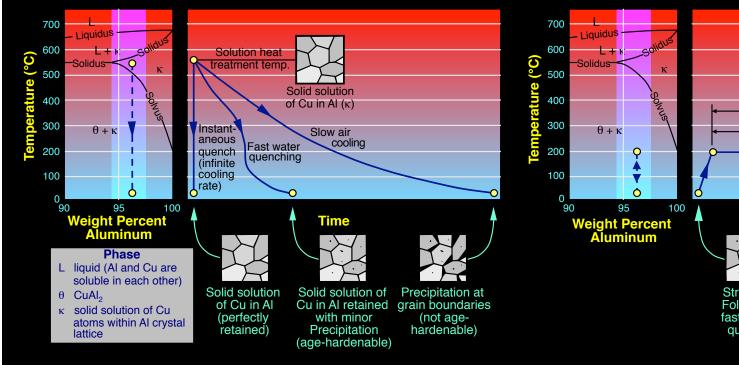
Poor Corrosion Resistance

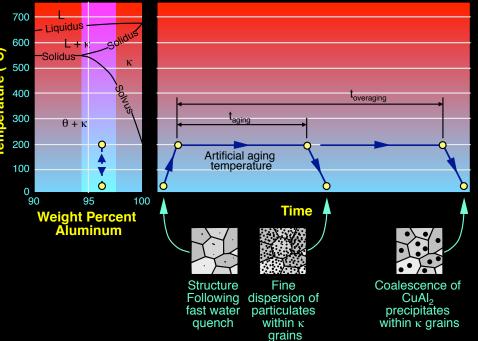
Poor Hardness

Poor Strength



4. Microstructural Development of Aluminum Alloy during Quenching Phase of Heat Treating

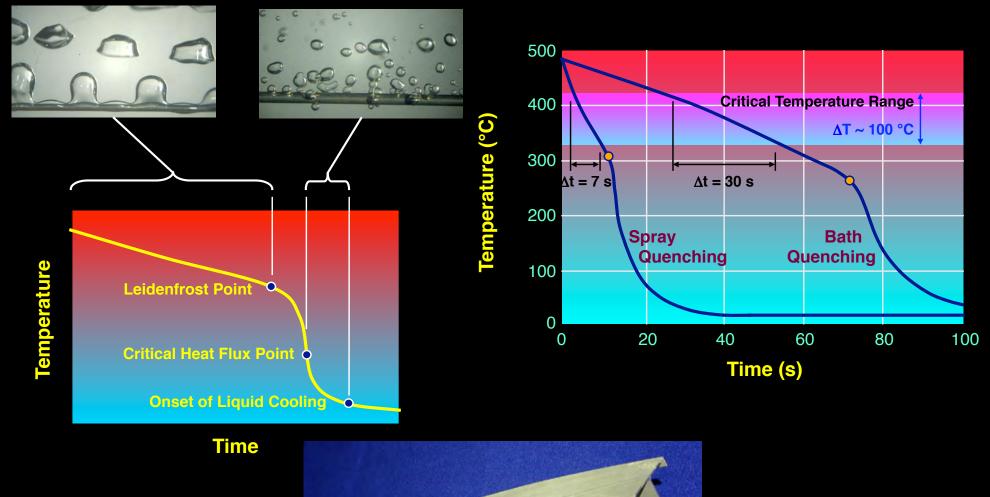




Heat treating of Al-Cu (4.4 wt %) alloy (Hall & Mudawar, 1996)



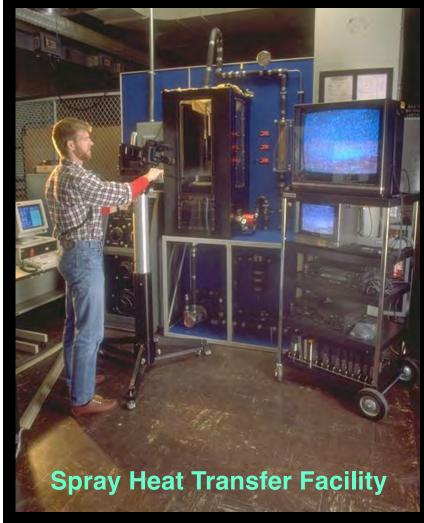
4. Cooling Curve for Liquid Bath Quenching versus Spray Quenching



Distortion induced by Poor Quenching



4. Fundamental Physics of Spray Cooling





Mudawar & Valentine (1989)





Surface Analysis Facility



Krüss Tensiometer

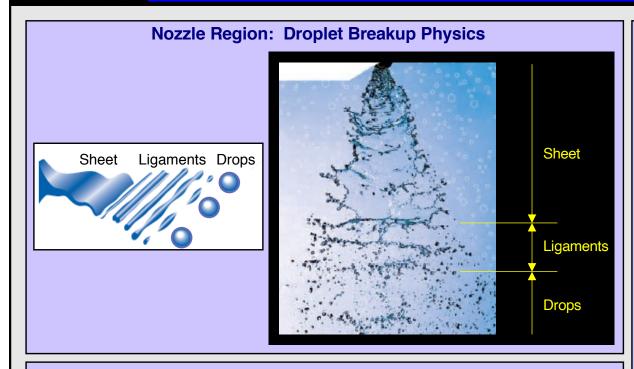


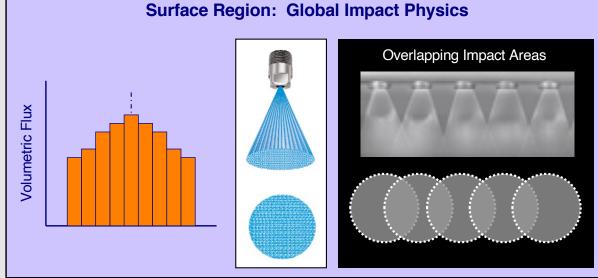


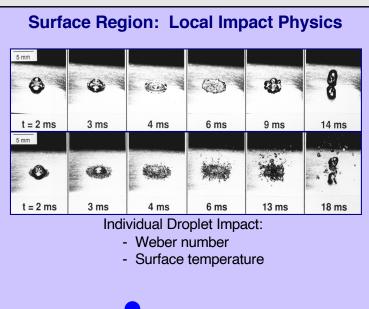


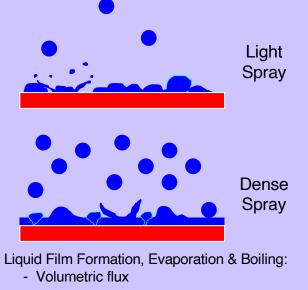


4. Fundamental Physics of Spray Cooling







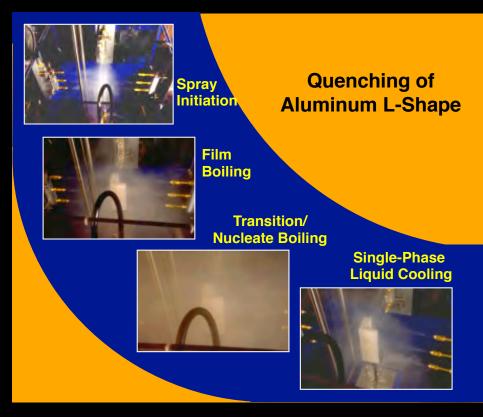




4. Purdue Quenching Facility



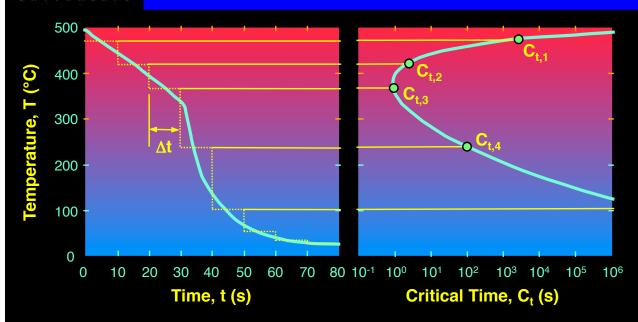






PURDUE

4. Determination of Quench Factor and Hardness



Quench factor:
$$\tau = \int_{t_1}^{t_2} \frac{dt}{C_t} \cong \frac{\Delta t_1}{C_{t,1}} + \frac{\Delta t_2}{C_{t,2}} + \dots + \frac{\Delta t_n}{C_{t,n}} = \sum_{i=1}^n \frac{\Delta t_i}{C_{t,i}}$$
 where $C_t = -k_1 k_2 \exp\left(\frac{k_3 k_4^2}{RT(k_4 - T)^2}\right) \exp\left(\frac{k_5}{RT}\right)$, T in Kelvins

Hardness: $H = H_{\min} + (H_{\max} - H_{\min}) \exp(k_1 \tau)$

- Rockwell B hardness (average of three measurements near thermocouple plane rounded to nearest 0.5 HRB, all three measurements were within ±1 HRB)
- H Rockwell B hardness contours *predicted* using quench factor technique with *predicted* temperature-time history)

