Wenhui Zhong Final Report.pdf

by Wenhui Zhong

Submission date: 31-Jul-2023 07:08AM (UTC-0700)

Submission ID: 2139535609

File name: Wenhui_Zhong_Final_Report.pdf (526.51K)

Word count: 5674

Character count: 33218



Introduction:

In today's industry, ensuring the safety, reliability, and compliance of industrial processes is of paramount importance. Reflecting on accidents in history, laws and regulations are constantly being improved. In 1992, the Occupational Safety and Health Administration (OSHA) enacted the Safe Management of Highly Hazardous Chemicals Process Regulation (29 CFR 1910.119), which is essentially a set of risk management elements known as Process Safety Management (PSM). The California Division of Occupational Safety and Health (Cal/OSHA) enacted separate PSM regulations for refineries in 2017 (8 CCR 5189.1).2 And then, to ensure that production processes involving hazardous materials follow the best, up-to-date safety practices, the PSM regulations introduce the term recognized and generally accepted good engineering practices (RAGAGEP).² RAGAGAP are not only an indispensable component of OSHA's process safety management standard (29 CFR 1910.119), but also serve as the foundation for safe and reliable inspection, maintenance, operation, and engineering activities. RAGAGEP consist of published and widely accepted codes, published consensus documents and published non-consensus documents. Firstly, widely accepted codes, such as National Fire Protection Association (NFPA) 101 life safety code, refer to the code that has been widely adopted by the federal, state or local governments.³ Therefore, any structures erected within these jurisdictions must adhere to these adopted consensus standards. Secondly, consensus documents are published by organizations that demonstrate a diverse and broadly represented committee membership. These organizations include American Society of Mechanical

Engineers (ASME), American National Standards Institute (ANSI) and so on.⁴ Thirdly, non-consensus documents are published by smaller organizations and more industry-based, such as Center for Chemical Process Safety (CCPS) guidebooks. Adhering to RAGAGEP can mitigate risks, prevent accidents, reduce downtime, and enhance operational efficiency. The following table lists some cases that did not follow RAGAGAP.⁵

Table 1 Cases of failure to study or comply with applicable codes and standards⁵

Locations	Incidents	Standards not applied
		NFPA 6543 (Standard for the
West Pharmaceutical	Explosion caused	Prevention of Fire and Dust
Services, Kinston, NC	by polyethylene (6	Explosions from the Manufacturing,
(January 29, 2003)	dead, 37 injured)	Processing, and Handling of
		Combustible Particulate Solids, 2000)
Hayes Lemmerz International, Huntington, IN	Aluminum exploded (1 dead,	NFPA 484 (Standard for Combustible Metals, Metal Powders, and Metal
(October 29, 2003)	1 seriously burned)	Dusts ,2002)
Marcus Oil and Chemical, Houston, TX (December 3,	Failed tank	ASME (Standard for pressure vessels) & NBBI (Codes for modifying pressure vessels)

The project aims to identify and implement RAGAGEP to effectively manage hazards

associated with various processes, including slitters, drying and curing operations and extrusion operations. In addition to the initial scope, the project will also expand into the realm of mechanical integrity, involving developing a common Inspection, Testing, Preventive Maintenance (ITPM) regimen for the mentioned processes based on the learnings from RAGAGEP.

Literature Review

This project will focus on the hazardous processes of slitting, drying and curing, extrusion. RAGAGAPs are the basis of construction, design, inspection, testing, and preventive maintenance. The following diagrams summarize the RAGAGAPs associated with each operation, and how they apply. Although the OSHA regulation is not RAGAGAP, it is left because it ties things together.

Slitters

A slitter machine, or simply a slitter, is an industrial device used to cut or 'slit' large rolls of material into narrower rolls. The materials can range from paper, film, foil, and various metals to rubber and plastic.⁶ In the flexible packaging industry, slitters play a crucial role in resizing large rolls of packaging material into smaller ones suitable for later-stage manufacturing processes. The main risks associated with slitters include the potential for operator injury due to the sharp blades and moving parts, as well as possible material entanglement or jamming.

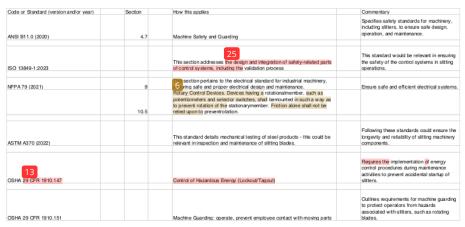


Figure 1 RAGAGAP: Slitters

Drying and curing operations

Drying and curing operations involve the removal of moisture from materials or hardening/adhesion of coatings. The primary hazards can include exposure to high temperatures, potential for fire or explosion if volatile materials are present, and exposure to harmful substances during the drying/curing process.

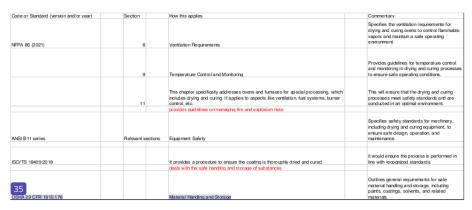


Figure 2 RAGAGAP: Drying and Curing

Extrusion operations

Extrusion is a production technique in which raw material is propelled through a custom-shaped die, thereby fabricating items with a distinct form and outline. This technique utilizes a broad range of materials, encompassing metals, plastics, ceramics,

and more.⁷ Hazards can include high temperatures, high pressure, moving machinery, and possible exposure to raw materials that could be harmful.

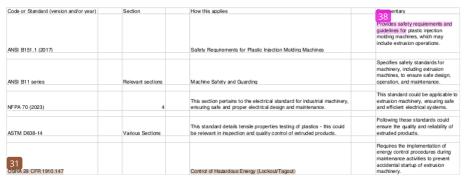


Figure 3 RAGAGAP: Extrusion

Results and Data Interpretation-Part 1-Prioritization

This part introduces a method to ensure key safety standards. First list some hazards. Then a standard is used for rating - if this standard is not complied with, what is the severity. Use the first standard as the rating basis, and then rate the other standards. Finally, the average of each standard is calculated to arrive at the priority order. The results of the three operations are listed in the figures below.

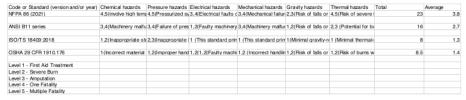


Figure 4 Prioritization of Drying and Curing

Code or Standard (version and/or year)	Chemical hazards	Pressure hazards	Electrical hazards	Mechanical hazards	Gravity hazards	Thermal hazards	Total	Average
ANSI B11.0 (2020)	1(This standard me	3(Improper machin	3,4(Improper safe	3,4(These standards	2(The standard inc	1(The standard inc	1	4 23
ISO 13849-1:2023	1(This standard pri	2(Inappropriate re	2,3(This standard	2,3 (This standard re	1 (This standard m	2(This standard re	1	1 13
NFPA 79 (2021)	2(This standard ad	2(Malfunctioning e	4,5(This standard	1,2(This standard ma	1 (This standard m	3 (This standard in	1	4 23
ASTM A370-20				1(This standard deals				6 1

Figure 5 Prioritization of Slitters

Code or Standard (version and/or year)	Chemical hazards	Pressure hazards	Electrical hazards	Mechanical hazards	Gravity hazards	Thermal hazards	Total	Average
ANSI B151.1 (2017)	1(This standard is m	2(This standard ind	1 (While this stand	3 (This standard include	2(The standard's f	2 (This standard co	11	1.8
ANSI B11 series	2(The B11 series pr	3 (The B11 series of	2(This series cover	4(The B11 series cove	3(The B11 series	3(The B11 series co	17	2.8
NFPA 70 (2023)	1(This standard mai	1 (The B11 series of	4(This is the Nation	1 (This standard main)	1(This is primarily	1 (While primarily an	9	1.5
ASTM D638-14	1(This standard, wh	1 (The B11 series of	1(This standard pri	2(This standard, which	1(This standard is	1(While primarily an	7	1.2

Figure 6 Prioritization of extrusion

Take drying and curing as an example, the processes have been evaluated against key safety standards, focusing on various hazards including chemical, pressure, electrical, mechanical, gravity, and thermal risks. This evaluation has revealed significant differences in the potential severity of these hazards under non-compliance with each standard. The highest potential risk is associated with non-compliance with NFPA 86 (2021)⁸. This standard deals with ovens and furnaces and involves high temperatures and flammable substances.8 Any mismanagement could result in severe injuries or fatalities due to fires or explosions, with severity levels ranging from 4 to 5. Furthermore, pressurized systems under this standard, if not adequately maintained or operated, can also lead to significant injury or fatalities, posing the same severity level (4 to 5). Electrical and mechanical failures under this standard could lead to similar severe consequences (severity level 3 to 4), further exacerbating the risks. Gravity hazards pose a slightly lower, yet significant risk (severity level 2 to 3), mainly due to the possibility of falls or falling objects during emergencies. Lastly, the standard presents significant thermal risks with severity levels ranging from 4 to 5, primarily due to the potential for severe burns or heat stress. The overall average severity level for this standard is 3.8, highlighting its crucial role in the drying and curing processes. ISO/TS 18409:2018, which focuses on waste management systems, generally presents lower hazard severity levels. Most notably, inappropriate storage or disposal of waste chemicals could lead to chemical spills or exposures requiring first aid, with severity levels ranging from 1 to 2. Inappropriate handling of pressurized waste systems may result in burns or injuries, warranting a severity level of 2 to 3. Given the nature of the standard, electrical, mechanical, gravity, and thermal hazards are less prevalent and typically less severe, with each posing a severity level of 1. The average severity level for this standard is 1.3, indicating a lower overall risk in comparison to NFPA 86 (2021).

Results and Data Interpretation-Part 2-Risk Assessment

This report covers the risk assessment for the mentioned operations within the manufacturing facility. Using the Bow-Tie approach, we identify hazards, threats, mitigative measures, preventive measures, and consequences associated with each operation. Preventive and mitigative strategies are proposed, adhering to the RAGAGAP.

The bow tie methodology is a graphical risk analysis and management method, which intuitively expresses the causes of accidents and a series of possible consequences, and covers the control measures to prevent accidents and slow down or reduce accidents mitigation measures for the consequences, etc. A bow tie diagram troubleshoots a potential major incident by graphically mapping the hazards, threats, and potential adverse consequences that could lead to an incident, and most importantly, it includes all barriers and degradation controls that can reduce the risk.

Bow tie diagrams facilitate barrier management, analysis of risk reduction and

assessment of existing barriers and provide a powerful means of communicating complex systems to employees, management, regulators, the public and other stakeholders, organizational and process safety information. The elements of the bow tie are shown in Figure 7¹⁰.

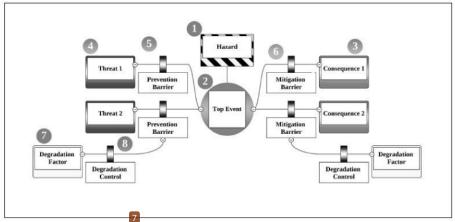


Figure 7 Standard Bow Tie Showing all the Basic Elements 10

Slitters

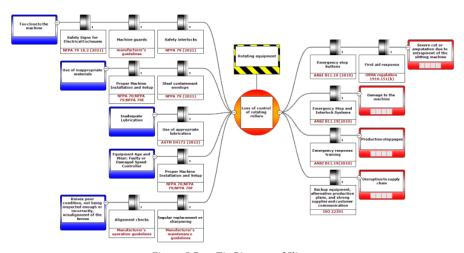


Figure 8 Bow Tie Diagram of Slitters

Figure 8 is the slitting operations' bow tie diagram. The core hazard associated with slitting operations is the loss of control of rotating rollers. Slitting operations, by nature, involve the use of these blades to cut materials, presenting inherent risks that

must be managed effectively. Threats in slitting operations can occur in several ways, primarily from the operator being too close to the machine, use of inappropriate materials, inadequate lubrication, equipment age and wear and knives' poor condition. These threats have the potential to compromise the amputation, damage to the machine, and the quality of the product.

Addressing these threats requires a comprehensive and proactive approach to maintenance and inspection. Regular replacement or sharpening of knives, thorough machine guards following the manufacturer's operation guidelines, use of appropriate lubrication with ASTM D4172¹¹ and proper machine installation and setup following NFPA 70¹² are all essential preventive measures. Each of these measures aligns with a particular threat, but together they contribute to a comprehensive preventive strategy. Similarly, the potential consequences of these threats can be mitigated with appropriate measures. Mitigative measures include emergency stop buttons, emergency response training and backup equipment, in compliance with ANSI B11.19 and ISO 22301.^{13,14}

Drying and curing operations

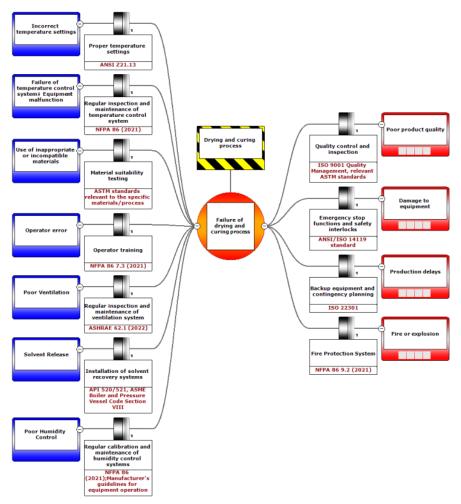


Figure 9 Bow Tie Diagram of Drying and Curing

Figure 9 is the drying and curing operations' bow tie diagram. As we delve deeper into the risk assessment of the drying and curing operations, it's essential to define the primary hazard - the failure of the drying and curing process. This could result from several potential threats, each of which has its associated preventive measures guided by RAGAGAP.

Among the most prominent threats is the incorrect temperature settings, a common yet

critical factor that can lead to the primary hazard. This threat can be prevented by proper temperature settings, guided by ANSI Z21.13¹⁵, ensuring that the process temperature is optimal and does not lead to process failure. In addition to this, there is the threat of failure of the temperature control system or equipment malfunction. Regular inspection and maintenance of the temperature control system is a preventive measure that adheres to NFPA 86 (2021), which says "the temperature indication of the excess temperature limit interlock shall be verified to be accurate".8. Moreover, the use of inappropriate or incompatible materials is a potential threat. To prevent this, material suitability testing should be carried out in accordance with relevant ASTM standards, ensuring that the materials used in the process are suitable. Operator errors also pose a threat to the drying and curing process. Therefore, operator training, as highlighted in NFPA 86 7.3 (2021), becomes a crucial preventive measure, enhancing operator skills and reducing the likelihood of human errors. Furthermore, poor ventilation and solvent release present other threats. Regular inspection and maintenance of ventilation systems, recommended by ASHRAE 62.1 (2022)¹⁶, and the installation of solvent recovery systems, in line with API 520/521 and ASME Boiler and Pressure Vessel Code Section VIII, serve as preventive measures for these respective threats. Lastly, poor humidity control is a significant threat. Preventing this requires regular calibration and maintenance of humidity control systems, adhering to NFPA 86 (2021) and the manufacturer's guidelines for equipment operation.

On the other side of the bow tie diagram, the potential consequences of process failure

are examined. Poor product quality is one such possible consequence. Quality control and inspection, in line with ISO 9001 Quality Management and relevant ASTM standards, serve as mitigative measures, ensuring that product quality is maintained even in the event of a process failure. Similarly, damage to equipment and production delays are other potential consequences. The implementation of emergency stop functions and safety interlocks, as per ANSI/ISO 14119 standard, can help mitigate equipment damage. For production delays, having backup equipment and contingency planning in accordance with ISO 22301 can minimize disruption to the overall production timeline. Lastly, a fire or explosion is a serious consequence of process failure. As a mitigative measure, a fire protection system adhering to NFPA 86 9.2 (2021) should be in place, ensuring a rapid response to any fire-related incidents, hence minimizing potential damages. NFPA 86 says "A study shall be conducted to determine the need for fixed or portable fire protection systems for ovens, furnaces, or related equipment". Therefore, these standards would provide specified "how to do it".

Extrusion operations

The extrusion process's intricacies inherently contain several threats that, if left unchecked, could culminate in the top event, the failure of the extrusion process. An overarching hazard that can drastically affect the process is the overheating of the extruder. To preemptively avoid this, interlocks for temperature control are essential, conforming to ANSI/ISO 14119 (2013) and NFPA 86 (2021) standards. Moreover, incorrect cooling rates post-extrusion could compromise the product's integrity and

potentially harm the machinery. This threat can be tackled by the use of predictive maintenance technologies as guided by ISO 17359(2018) for condition monitoring and diagnostics of machines. Other threats such as poor maintenance, incorrect installation, defective or incorrect resin, and incorrect pressure all play a role in potentially disrupting the process. Preventive measures ranging from adherence to the manufacturer's instructions and standards during installation to regular quality control checks of resin, as per relevant ASTM standards, can greatly minimize the risk posed by these threats. NFPA 79 in 4.8 mentions "The electrical equipment shall be installed and operated in accordance with the conditions outlined in the manufacturer's instructions" The criticality of correct pressure can't be undermined and should be managed through regular monitoring, control of machine pressure, and installation of pressure control and safety devices, guided by manufacturer's guidelines and ASME BPVC Section VIII.

The unfortunate realization of these threats leads to a set of consequences that can have a profound impact on the production process and safety. Equipment damage or extruder rupture can be a direct result of unmanaged threats. However, well-structured emergency response protocols in line with API Recommended Practice 520 can serve as a mitigative measure. Moreover, the increased downtime can be managed effectively through robust contingency planning and having backup equipment, aligning with ISO 22301 for business continuity management. Finally, safety incidents, especially due to high pressure, can be contained by the implementation of

a robust safety management system as prescribed by ISO 45001 for occupational health and safety management.

Results and Data Interpretation-Part 3-ITPM

RAGAGEPs serve as critical resources for Mechanical Integrity (MI) programs.

Various process safety reference documents and guidance 1. Organize Equipment materials rely heavily on the equipment and production Into Equipment practices detailed within RAGAGEPs, like "CCPS, "Design Gather Equipment Information codes represent . . . minimum requirements"; Guidelines for Engineering Design for Process Safety"18. MI represents the 3. Assemble ITPM Task systematic execution of tasks essential to confirm that significant equipment remains fit for its planned application 4. Select ITPM Tasks and throughout the operational lifespan.¹⁹ Besides, ITPM is at the heart of the MI program and its objective is to identify and Document the Selecte perform maintenance tasks to ensure the continued integrity of Figure 10 ITPM task selection process19 equipment. This approach provides factories with the freedom to get rid of the "after-the-fact" maintenance concept. 19 This report covers the development of ITPM tasks.

A five-step process for selecting ITPM tasks is illustrated in Figure 10 This project creates an ITPM plan according to the flow chart except the third step. Equipment classes are provided by the company. There are pressure vessels, pumps, tanks piping,

coating, switchgear, furnaces, lower flammable limit systems, gas trains and heat exchangers. Through a detailed exploration of typical failure points, required activities, intervals or frequencies, guidelines, and additional considerations, the report emphasizes the importance of stringent ITPM practices in mitigating equipment failures, enhancing safety, and improving overall productivity. Figure 11 shows a part of the ITPM plan and the complete ITPM plan is placed in the appendix.

	Equipment Class	Typical Failure Points	Required Activity	Interval or Frequency	Guidelines	
	Pressure Vessels	Discrition of pre-ssure boundary, lealage from crade	External visual inspection 2 Tokness measurement Internal inspection or alternatively on- stream inspection (as applicable)	5-year maximum 12 curroson Me or 10- year maximum 12 curroson Me or 10- year maximum 12 curroson Me or 10- year maximum, Pickness measurement suffices if	ASME Sec VIII div 1 API 610/580	
H						
Ì		inadequate lubrication, bearing failure, or wear	Visual inspection of sealing system	Each shift to weekly (depending on criticality)	ANSI/ASME 673.1	
Pumps		*Loss of, or inadequate, flow/pressure, resulting from failure of a dries component. *Loss of, or inadequate, flow/pressure, resulting from failure, corrosion, erosion, or wear of an intensi component (e.g., implet). *Damage to	Vibration analysis	*Continuous for pumps with large motions (e.g., 10,000 hp) *Weeley to quarterly (departing on criticality and horsepower)	2 510 API 674 API 675 API 676 API 681 API 682	
Ę						
	Tanks.	Corrosion; Leaks; Structural Integrity; Versilation and safety valves	Visual Inspection	Monthly	API RP 575 API 620	
Tanks	a its		Pressure testing	annually	API 650 API 653	

Figure 11 Part of ITPM Plan

Pressure Vessels, often subject to extreme conditions, are prone to distortion of pressure boundaries, leaks from cracks caused by environmental factors or stress corrosion cracking, and corrosion under insulation. The ITPM regimen for these vessels includes external visual inspection every five years maximum, thickness measurement every half corrosion life or ten years maximum, and internal inspection or on-stream inspection every half corrosion life or ten years maximum. These activities align with guidelines from the ASME Sec VIII div 1 and API 610/580. Besides, the challenges with Pumps revolve around leakage from the seal/packing assembly, failure of a drive component, and failure, corrosion, or wear of internal

components. The ITPM regimen suggests visual inspection of the sealing system, depending on the criticality, on a shift to a weekly basis, and vibration analysis, ranging from continuous for large motors to weekly to quarterly, again depending on the criticality and horsepower. The guidelines for these inspections and activities align with ANSI/ASME 673.1, ANSI/ASME 873.2, API 610, API 674, API 675, API 676, API 681, and API 682. Tanks are integral to many industrial processes and are prone to corrosion, leaks, and structural integrity issues. The ITPM regimen for Tanks includes monthly visual inspection and annual pressure testing. Corrosion can lead to leaks, loss of material strength, and eventual structural failure. Proper coatings or other anti-corrosion measures should be in place as per the guidelines laid down by API RP 575, API 620, API 650, and API 653.

Conclusion

In conclusion, prioritization of these safety standards is essential for effectively managing risks in these three processes. For drying and curing, compliance with NFPA 86 (2021) should be a priority due to its high average severity level, indicating the potential for severe consequences if not properly followed. Meanwhile, standards like ISO/TS 18409:2018, while presenting lower overall risk levels, should not be neglected as they too contribute to the overall safety of the drying and curing processes. By understanding the potential severity of hazards associated with each standard, organizations can better prioritize their safety efforts and allocate resources where they are needed most. Furthermore, the journey from identifying the potential

threats in these three processes to understanding their consequences and implementing preventive and mitigative measures is a testament to the intricate relationship between these factors. It underlines the need for rigorous safety protocols, adherence to established RAGAGAPs, and a comprehensive understanding of the process itself. By marrying these aspects, we can ensure safer, more efficient, and reliable processes. Lastly, a well-executed ITPM regimen is indispensable for industrial operations. By identifying potential failure points and implementing timely inspection, testing, and preventive maintenance activities, industries can significantly enhance the reliability, safety, and efficiency of their operations. Adherence to recognized standards such as those from ASME, API, and ANSI, among others, ensures that the ITPM practices are in line with established best practices, thus reinforcing the overall operational excellence.

Step Forward

- Keep updating the Excel file for RAGAGAP research. Regularly updating RAGAGAP research ensures compliance with evolving industry standards and regulations, facilitates the discovery of new, more relevant standards, and ensures that risk assessments remain accurate and relevant.
- Quantitative analysis based on bow tie if necessary.
- Updating the bow tie diagrams every five years. Regularly updating bow tie diagrams ensures they accurately represent the evolving operations, facilitate

continuous learning about potential risks, and maintain their relevance for
effective communication and understanding of risks.

Reference:

- Occupational Safety and Health Administration, OSHA Instruction: PSM
 Covered Chemical Facilities National Emphasis Program, Washington, D.C.: U.S.

 Department of Labor, Directive No. CPL 03-00-021, January 17, 2017a.
- LaTourrette, T. (2022). Defining Recognized and Generally Accepted Good
 Engineering Practices for Process Safety Management.
 https://doi.org/10.7249/rra1866-1
- 3. NFPA 101: Life safety code. (2020). NATL FIRE PROTECTION ASSO.

 RAGAGEP Beyond Regulation: Good engineering practices for the design ...

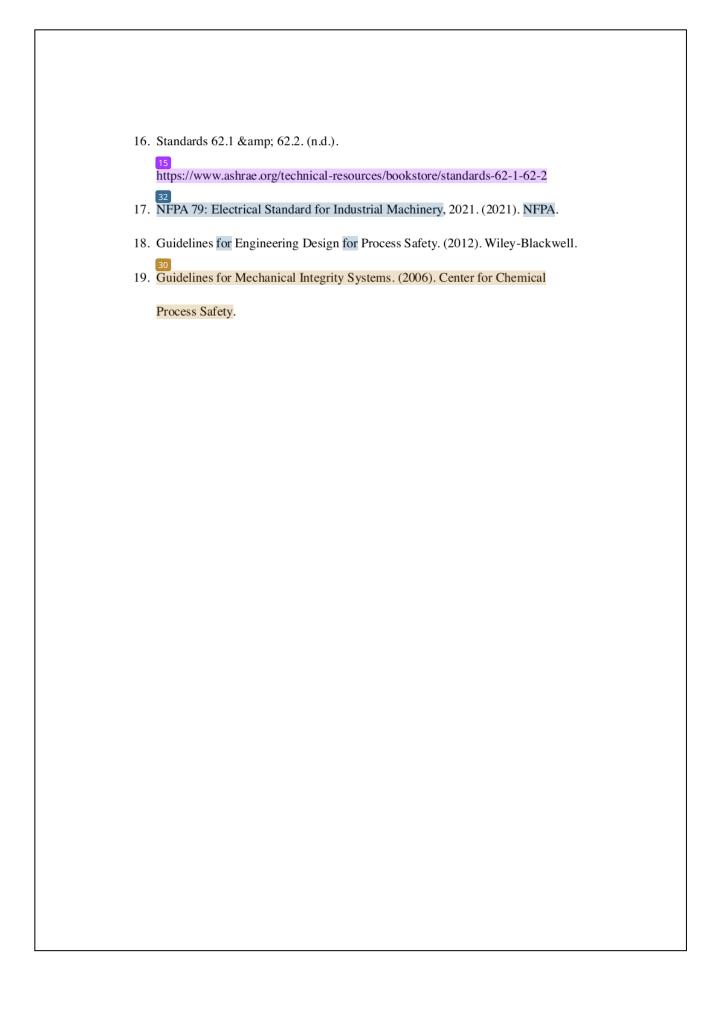
 (n.d.). https://aiche.onlinelibrary.wiley.com/doi/pdf/10.1002/prs.10211
- RAGAGEP: Codes, standards, and good engineering practice. (n.d.-b).
 http://resourcecompliance.com/wp-content/uploads/2017/09/2017-RETA-Conference-RAGAGEP.pdf
- RAGAGEP Beyond Regulation: Good engineering practices for the design ...
 14
 (n.d.-a). https://aiche.onlinelibrary.wiley.com/doi/pdf/10.1002/prs.10211
- 6. What is a slitter machine?. Thomasnet® Product Sourcing and Supplier

 Discovery Platform Find North American Manufacturers, Suppliers and

 Industrial Companies. (n.d.).

 $https://www.thomasnet.com/articles/machinery-tools-supplies/what-is-a-slitter-m\\ achine/#:~:text=A\%20slitter\%20machine\%2C\%20commonly\%20called,unwoun\\ d\%20material\%20into\%20various\%20widths.$

7. Everything you need to know about extrusion processes - studentlesson. Student Lesson. (2023, July 8). https://studentlesson.com/extrusion-processes-definition-applications-function-pr ocess-materials-equipment-types-working-principle-advantages-and-disadvantage NFPA 86: Standard for ovens and furnaces. (2015). National Fire Protection Association. 9. ISO/TS 18409:2018. ISO. (2021, November 2). https://www.iso.org/standard/66733.html 10. Bow ties in risk management a concept book for process safety. (2018). Wiley. 11. ASTM D4172. ASTM D4172: Standard Test Method for Wear Preventive Characteristics of Lubricating Fluid (Four-Ball Method). (n.d.). https://global.ihs.com/doc_detail.cfm?item_s_key=00018375 12. NFPA 70: National Electrical Code 2023. (2022). National Fire Protection Association. 13. ANSI B11.19-2019. ANSI Webstore. (n.d.). https://webstore.ansi.org/standards/amt/ansib11192019 14. ISO 22301:2019. ISO. (2019, October 30). https://www.iso.org/standard/75106.html 15. Energy code ace - home page. (n.d.). https://energycodeace.com/site/custom/public/reference-ace-2019/index.html#!D ocuments/gloss_ansiz2113.htm



Appendix

ITPM Plan						
Equipment Class	Typical Failure Points	Required Activity	Interval or Frequency	Guidelines	4 Comments	
Pressure Vesse ls	"bularizard presure boundary leukagation makks (e.g., Indigae, endormentalyinduced, direas comolen cracking countecnacking, or tries in presure boundary Commission of presure boundary, including comolen index insulations, including comolen index insulation of grounding, and eccessive, comolenal directors in the proper similarization of grounding and eccessive comolenal directors in the proper similarization of grounding systems.	Diamet visual impection 2 This result resourcement Internal impection or alternal wely construent impection (as applicable)	5-y-pointer. 1/2 derman Heier 10-year mastrum, Februa measurement auf om if	ASMESecVII dv I AR 610/580	Completed during maline manuful by operature, deficiencies are decurrented but surveillement that does not libertify a defail enty or not decurrented. Yourself impaction and thickness measurement	
Purqu	"Leaves go from the seed packing seasonth ly as a neath of overpressurfusion of the seasonthing management and control of the control of the seasonthing of the control of the seasonthing of the control	1 Itsus respection of seeing system	Tax shift to seekly (depending on critically)	2 CNE 6721 2 CNE 6722 10 UN 674 AR 675		
	Hernal component (e.g., the elect "Durnage to pump cashightom bose or broken Hernal component (e.g., the elect "Durnage to seek/packing and/or associated egi/prent/caused by economive vibration"	Vibration amalysis	Continuous for pumps with large motions (e.g., 10,000 hp). Weekly to quarterly (depending on critically and home power)	API 676 API 681 API 682		
Tarrios	Corosion: Leaks; Strudural Integrity, Ventilation and safety valves	Wasel Impaction	Monthly	AM F8P 575 AM 620 AM 620	Corronion can lead to leake, loss of make fall strength, and wvertable shuctural failure. Emake proper coalings or other arti- corronion measure are in place.	
	1	Pressure testing	ernasty	AFI 653	SATIONAL PROGRAMO WE FLY SEAL.	
Piping	Leskage from cracks (e.g., biligue), environmentally intiused, alreas corresion cracking, quantic cracking), internal or external corresion, corresion under insulation, excessive vibration	External visual inspection	Ordinal Inferval value is in API 570	ASME 031.3		
	imsupported or bound piping, permerent detortion, piping component not meeting pressure rating.	Thickness messure ment inspect on	Lesser of default interval values in API 570 or half-life based on measured wall thickness and calculated corresion rates			
Coating	Ositing Diagnostation and Presting, Cornosion under Insulation Coating Admission Pallane, Coating Mickinson Incomistancy, Overopossure to UV or Overricois	Visual Impection	Sent-annually or as required	NFPA33 Spray Application NFPA34 Coating & Disping	Early detection of costing damage can prevent corrosion and structural damage to the bark best.	
		Ulrasonic Testing	Typically every 5 years, but can vary depending on environment, tark use, and local segulation			
	"Failure to provide electrical power to safety- critical devices (e.g. controls) as a result of failure of bathe it es, correction, transfer as fich, and/or discrima switern	Wasel Inspection	Monthly to quarterly (outdoor installations) "Quarterly to sentamusely () roton installation; Annually to 2 years, depending on criticality. History, and starter size			
Seel to Ingener	Protected updates source or electrical abook to personnel as a result of sabort in davis or connection, income of overcommit protection device (e.g., incomed fuel), or operating equipment with satisface load (e.g., the operating temperature is 1.00.	Calibration and testing of protective relays: tripping of breakers; and testing insulation resistance of controls, meters, and protective devices	Ortusey to J. years, depending on critically in stay, and senter size 3 to 6 years, depending on conditions	NEPA TOES		
Fumaces	Tube splures, tube buiging and distortions, corep damage, steam leale, process fluid leaks, refractory/rature, structural support belure	inspection of heater or turnace firebox and tubes	Scheduled by user, usually inconjunction with planned unit shutdown or when an imminent feature condition is visible	NFPASS Overs & Pursuoss		
LFL Systems	Sensor Accuracy, Sensor Lifesport, System Asertic, Power Supply; Physical Dismage	Calibration and Bump Testing Sensor Replacement	Bump testing should be done daily before each use, and call bratton should be performed every 6 months. Typically 2-3 years.		Calibration ensures the accuracy of the device, which is crucial for safety.	
Gas Trains	Control Yell ve Palure, Pressure Regulator Palure; Safety Dovkar (n.g., Plante Safeguard, Safety Stub-off Yellow): Palure, Safe or Gasalet Palure; Piter Blockage; Improper Combustion;	Visual Impaction Punctional testing	ercettly ercenty	NPA 06	Control valve failure could lead to improper fuel supply, redficiert combustion; or a safety instend.	
Heat Exchangers	Fouling or Scaling: Corresion; Leake; Gasket Palure; Mechanical or Structural Palitire	Visual inspection Efficiency monitoring	ernally continually	ASVE Sec VIII dv I	Fouling or tool ingreduces heat transfer efficiency and increases energy consumption.	

Wenhui Zhong Final Report.pdf

ORIGINA	ALITY REPORT				
2 SIMILA	5% ARITY INDEX	11% INTERNET SOURCES	19% PUBLICATIONS	6% STUDENT PAPE	RS
PRIMAR	RY SOURCES				
1		Equipment-Spec ement", Wiley, 20			8%
2	"Equipm Wiley, 2	nent-Specific Int 006	egrity Manage	ment",	3%
3	Good er	S. Blair. "RAGAG ngineering pract on of plants", Pr	cices for the de	sign and	1 %
4	epdf.pu Internet Sour				1 %
5	WWW.ra Internet Sour				1 %
6	edoc.pu Internet Sour				1 %
7		nergy Institute. ement", Wiley, 20		isk	1 %

8	Submitted to University of Sydney Student Paper	1 %
9	inspectioneering.com Internet Source	1 %
10	www.nfpa.org Internet Source	1 %
11	Submitted to New York Institute of Technology Student Paper	<1 %
12	integrativewellnessandmovement.com Internet Source	<1 %
13	www.osha.gov Internet Source	<1 %
14	www.globalscientificjournal.com Internet Source	<1 %
15	www.researchgate.net Internet Source	<1 %
16	Submitted to Purdue University Student Paper	<1%
17	Submitted to Indiana State University Student Paper	<1%
18	kupasmotor.wordpress.com Internet Source	<1%

A. Kayode Coker. "Process Safety and Energy <1% 19 Management in Petroleum Refinery", Wiley, 2023 Publication Submitted to UC, Boulder <1% 20 Student Paper egatlib.egat.co.th 21 Internet Source Submitted to Colorado State University, 22 **Global Campus** Student Paper Submitted to Technological Institute of the <1% 23 **Philippines** Student Paper az.b-ok.cc <1% 24 Internet Source docplayer.net <1% 25 Internet Source chemical-facility-security-news.blogspot.com <1% 26 Internet Source vpn.cchealth.org Internet Source www.csb.gov 28 Internet Source

29	Publication	<1%
30	Johansen, Inger Lise, and Marvin Rausand. "Barrier management in the offshore oil and gas industry", Journal of Loss Prevention in the Process Industries, 2015. Publication	<1%
31	recert.gsfc.nasa.gov Internet Source	<1%
32	niordc.ir Internet Source	<1%
33	Chai, X "Determination of the solubility of inorganic salts by headspacegas chromatography", Journal of Chromatography A, 20030509 Publication	<1%
34	ia600907.us.archive.org	<1%
35	riceequipment.com Internet Source	<1%
36	tvsfpe.org Internet Source	<1%
37	www.mdpi.com Internet Source	<1%



"Handbook of Loss Prevention Engineering", Wiley, 2013

<1 %

Publication

Exclude quotes Off Exclude matches Off

Exclude bibliography Off