# PROCESS SAFETY AND THE PHARMACEUTICAL INDUSTRY

# SAFE BATCH SCALE-UP OF AN EXOTHERMIC GRIGNARD

**AYMAN ALLIAN** PIVOTAL COMMERCIAL SYNTHETIC



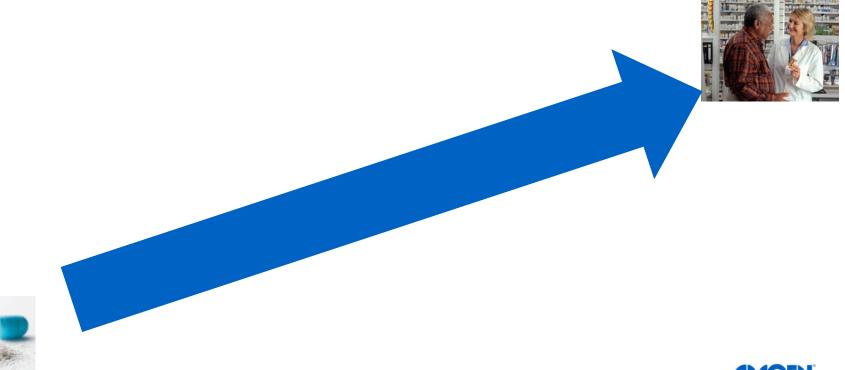
# **OUTLINES**

- Role of engineers and process chemist •
- Amgen synthetic portfolio: Opportunities and challenges in the pharma • industry
- Safety culture at Amgen •
- Safe Scale-up of an Exothermic Grignard •
  - Continous manufacturing
  - Leveraging pre-competitive space
  - Process safety for CM design





# **CHEMICAL ENGINEERING IN PHARMA: ADVANCING COMPLEX MOLECULES FROM DISCOVERY TO COMMERCIALIZATION**



# CHEMICAL ENGINEERING IN PHARMA: ADVANCING COMPLEX MOLECULES FROM DISCOVERY TO COMMERCIALIZATION





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# **ENGINEERING ROLE**



- Chemical Engineering in Pharma: Advancing complex molecules from discovery to commercialization
  - <u>Safety</u>: Process safety testing is our first line of defense against thermal hazard events such as explosions and runaway reactions
  - <u>Understand design space</u>: Generate quality product
  - <u>Consistent performance:</u> Mass Transfer, Modeling, Continuous
    Manufacturing



# **ENGINEERING ROLE**



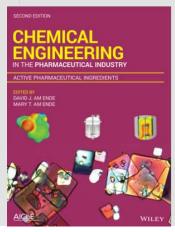
4 mL reactors

100 L reactors

1K to 10K L reactors

- Engineering: Advancing complex molecules from discovery to commercialization
- <u>Safety</u>: Process safety testing is pharma's first line of defense against thermal hazard events such as explosions and runaway reactions
- <u>Understand design space (PC driven by FMEA, criticality assessment)</u>
- <u>Consistent performance (Mass Transfer, Modeling, Continuous</u> Manufacturing) -Scale-Up of Mass Transfer-Limited Reactions: Fundamentals and a Case Study

### David J. am Ende





# **OUTLINES**

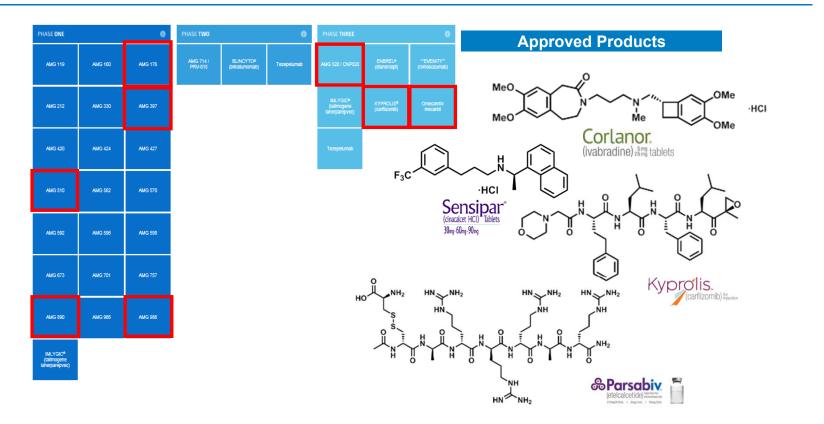
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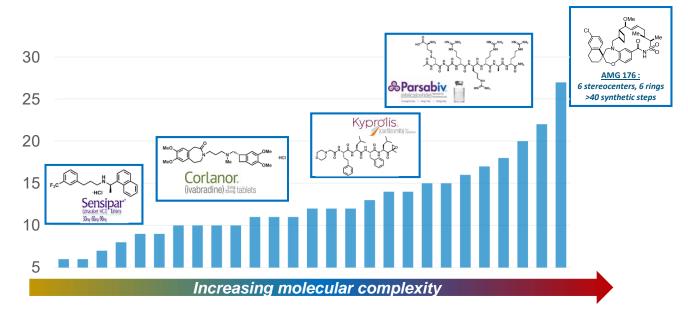


### **Amgen Synthetic Pipeline**



AMGEN

# Increasing molecular complexity and shortened development timelines drive the case for innovation



#### **Complexity Index factors:**

- molecular weight
- # of synthetic steps
- # stereogenic centers
- # rings



The future of the small molecule? Increased complexity and biologic pairings, says industry of May 2018 / Non Seather

The many roles of molecular complexity in drug discovery

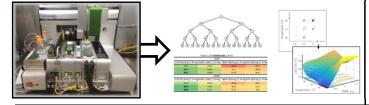
AMGEN

### Asset complexity coupled with shrinking timelines.

### Representative Platforms to Accelerate Synthetic Process Development

#### Automated Reaction Development:

- High-throughput and multi-variable reaction screening
- · Rich data sets enable development of predictive models



#### Crystallization - Solubility Modeling:

Solubility measurements and prediction streamline process design and execution to improve control strategy



### Continuous Manufacturing (CM):

 Reduced manufacturing footprint enables integration of analytics & improved processing safety & control





# **Outlines**

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# **HOW ABOUT PROCESS SAFETY?**



Moro Rock **Sequoia National** park



# SAFETY IS ABOUT PROTECTING YOUR LOVED ONES

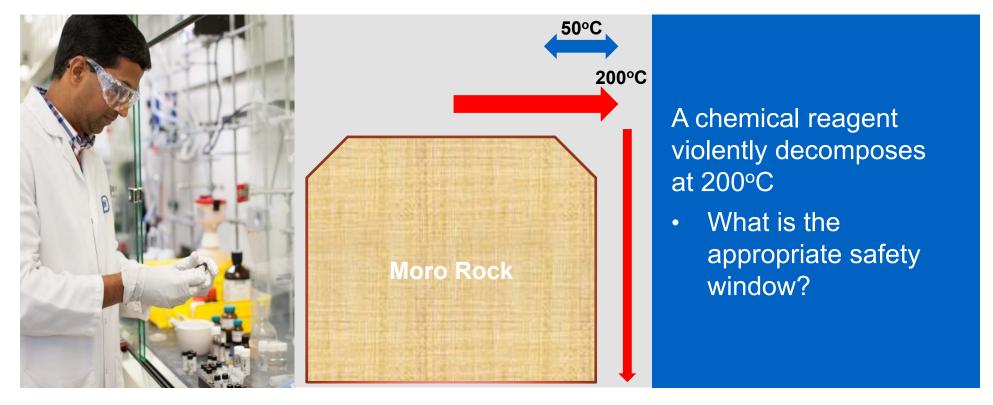
- Science tells you
  - You are 2 m from the edge
  - It is 75 m fall
- Your 9 year old son tells you, can he take just one step to get a better view.
- How close is too close?







# OUR SCIENTIST HANDLE CHEMICALS DAILY BASIS ARE THEY SAFE TO HANDLE?





# **BEIRUT EXPLOSION**



- 2700 tonnes Ammonium nitrate
- <u>Onset</u> temperature is ~200°C
- <u>Magnitude:</u> Heat of decomposition is 700 J/g
- Heat was used to selfheat, temperature will rise to 350 °C!!
- Portion of that energy will be converted to destructive pressure wave.

# **HIGH-ENERGY MATERIALS IN USE AT AMGEN**

Reagent	Onset Temperature	Energy Released	
TNT	309 °C	2,510 J/g	
Propargyl Alcohol	103 °C	3,675 J/g	
HBTU	162 °C	1,004 J/g	
твти	178 °C	1,208 J/g	
HOBt.xH <sub>2</sub> O	158 °C	1,984 J/g	
Amgen T790M intermediate	158 °C	2,370 J/g	
Amgen BACE intermediate	123 °C	2,718 J/g	

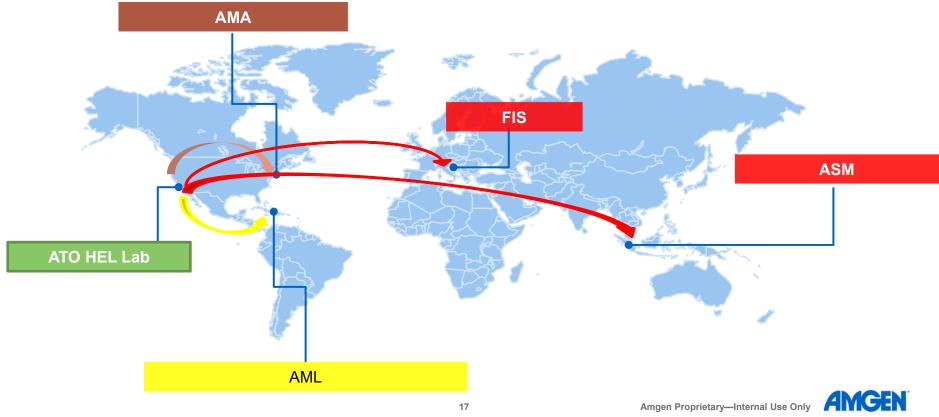
- **Reagents and** 1. intermediates that are worse than Ammonium nitrate
- Close in energy to 2. TNT
- Have lower onset 3. temperature than TNT





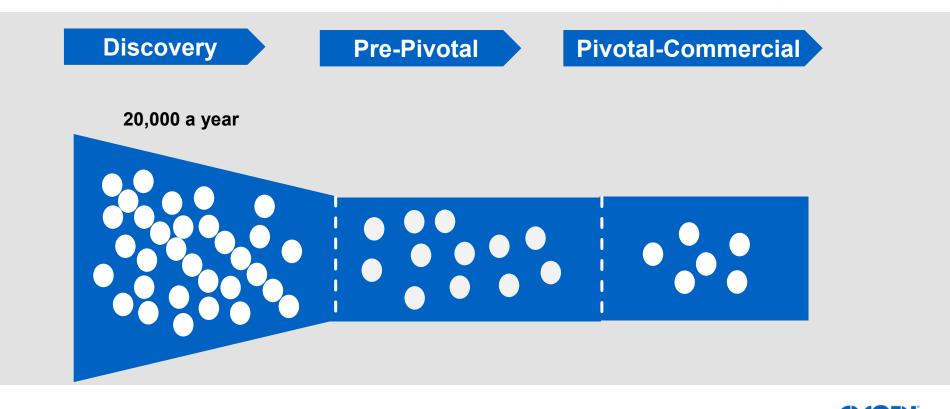
# **HAZARD EVALUATION LAB LOCATED AT ATO SUPPORT AMGEN SYNTHETIC PORTFOLIO**



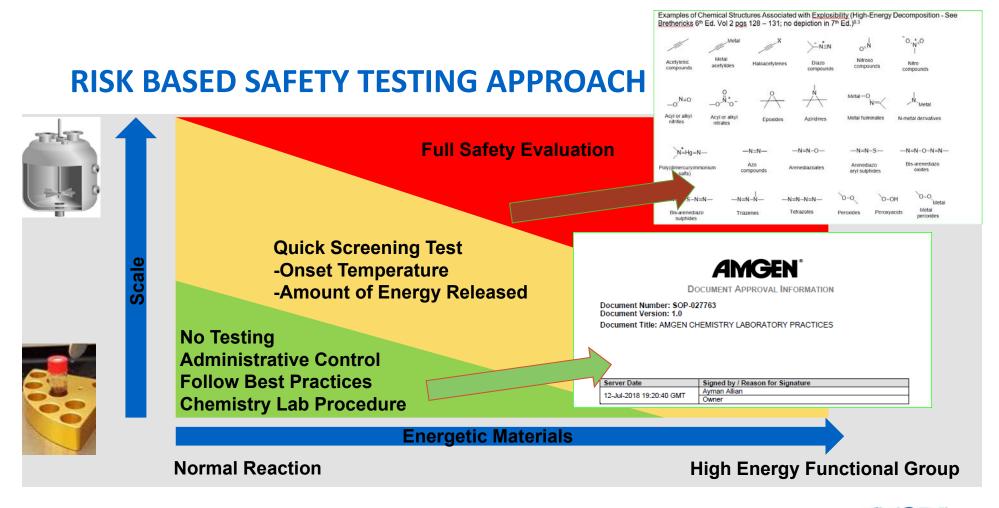


# RISK BASED APPROACH



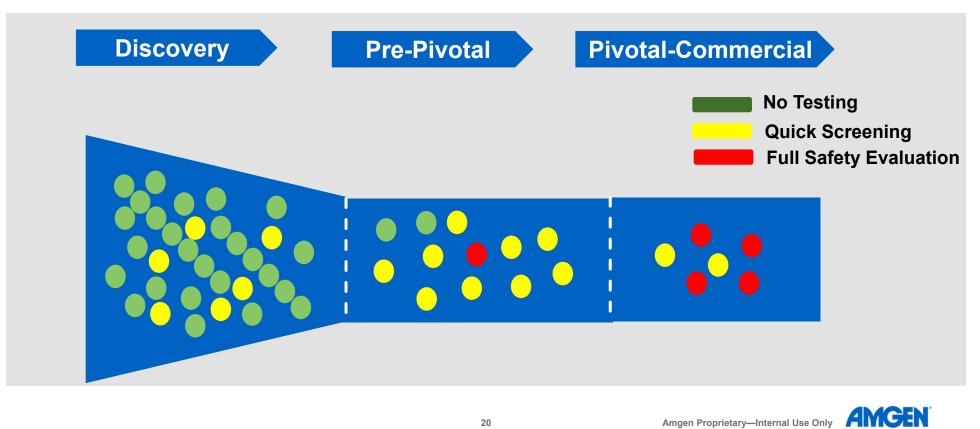






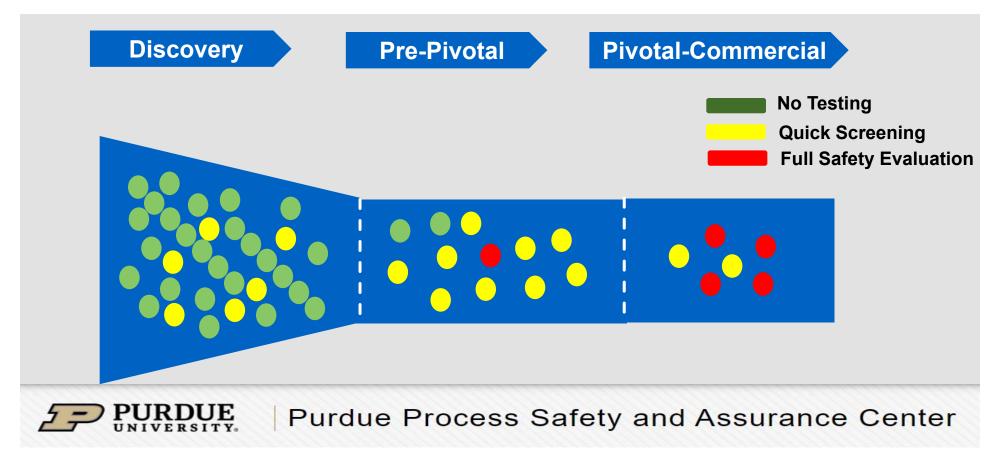


# **AFTER RISK ASSESSMENT**



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# **AFTER RISK ASSESSMENT- REVISIT OUR WORK FLOW**



### **EXTERNAL ENGAGEMENT**

# This is just one approach. How about other pharma companies? How do they handle this challenge?



# **CREATED AND LEAD A GLOBAL THERMAL HAZARD**





# AMGEN RESOURCES NEEDED TO ESTABLISH THIS TASK

- Amgen resources, we meet monthly meeting online
  - Spend 1-4 FTE hour a month for the meeting
  - Target a face-to-face meeting once a year. This year was done at Amgen ATO.





Recognition for being the most active and best attended group





# A MANUSCRIPT WAS JUST PUBLISHED

Survey 1 – Manuscript in Preparation!

Process Safety in the Pharmaceutical Companies-Part I:

Thermal Hazards Evaluation Processes and Techniques

Ayman D. Allian,\*† Nisha P. Shah,‡ Antonio Ferretti,§ Derek Brown, † Stanley P Kolis,<sup>⊥</sup> Jeffery Sperry

- Won the ACS award allowing free access for non ACS member
- One the most read/downloaded paper in OPRD



# **OUTLINES**

- Role of engineers and process chemist
- Challenges in the pharma industry
- Safety culture at Amgen
- Safe Scale-up of an Exothermic Grignard using thermal hazard testing and engineering control
  - Continous manufacturing
  - Leveraging pre-competitive space
  - Process safety for CM design



# **CASE STUDY: GRIGNARD REACTION**

27

 Thermal hazard evaluation of every reaction before any scale up in the kilo lab

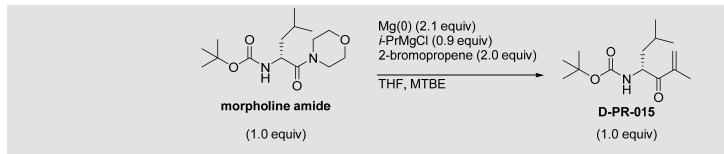








# **CHEMISTRY**



- Inherited from 3rd party through acquisition
- Grignard Reaction
- Intended for Scale up at 2 Kg scale



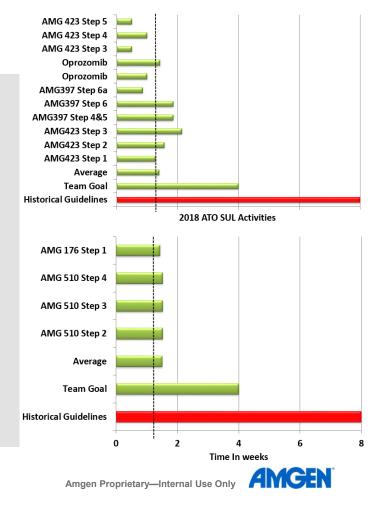


# SAFETY AND COMPLIANCE CULTURE

- Successfully executed more than 45 campaigns in the last 5 years
- No safety incident
- Two detailed GMP corporate audits in 2016 and 2019 without any critical findings

29

Still reducing turnaround by 50%



#### 2017 ATO SUL Activities

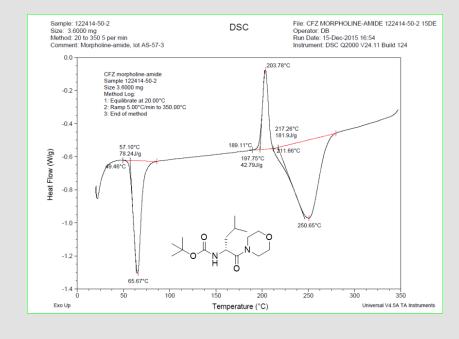
# **OUR APPROACH TO THERMAL HAZARD**

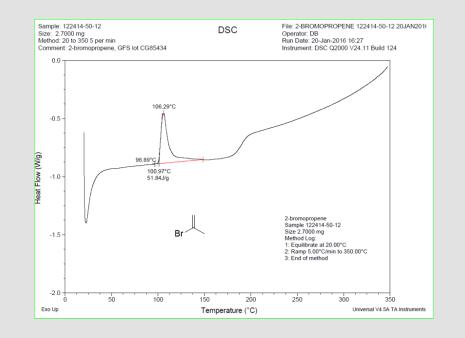
- Screen all reagents and starting material
- Screen isolated product (s)
- Screen reaction mixture (quenched solution)
- Measure Heat of reaction





# **DSC OF ISOLATED STARTING MATERIAL**

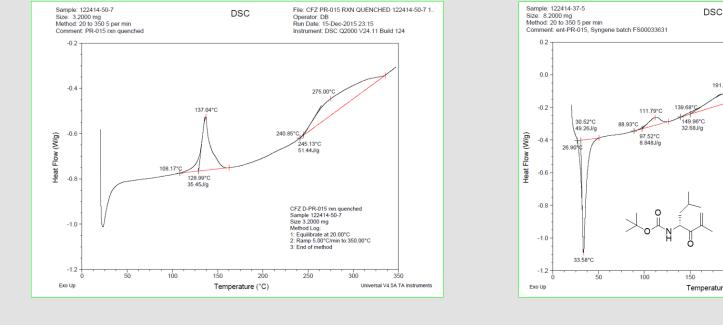


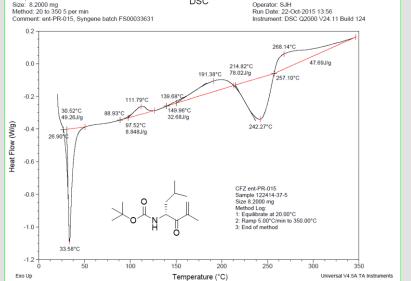




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# **DSC OF ISOLATED PRODUCT AND QUENCHED REACTION MIXTURE**



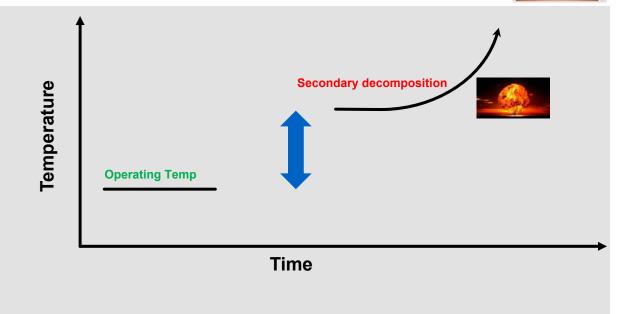




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### REACTION HAZARD CLASSIFICATION EXOTHERMIC REACTION BRING ABOUT A VIOLENT DECOMPOSITION?





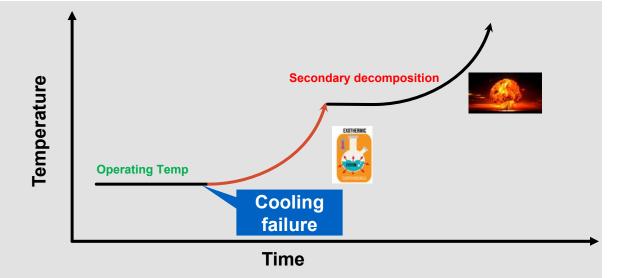


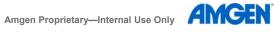
200 cm



# EXOTHERMIC REACTION BRING ABOUT A VIOLENT DECOMPOSITION

- Operating with a good safety window
- Cooling failure for an exothermic reaction



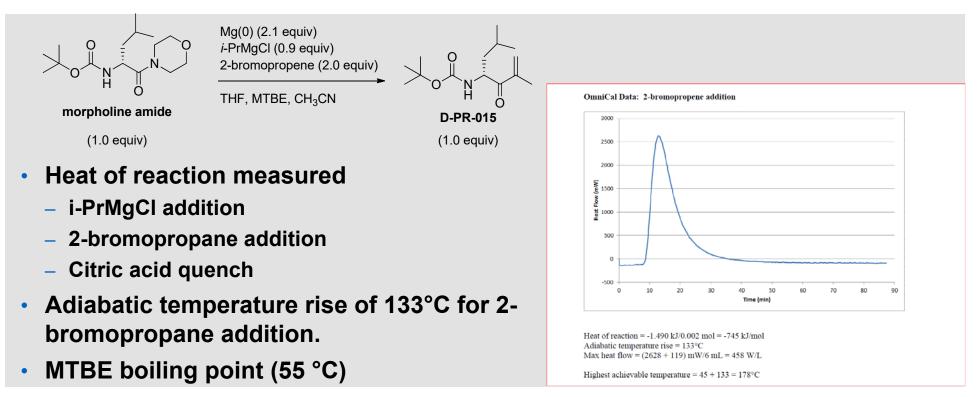




# **EXOTHERMIC REACTION BRING ABOUT A VIOLENT DECOMPOSITION**

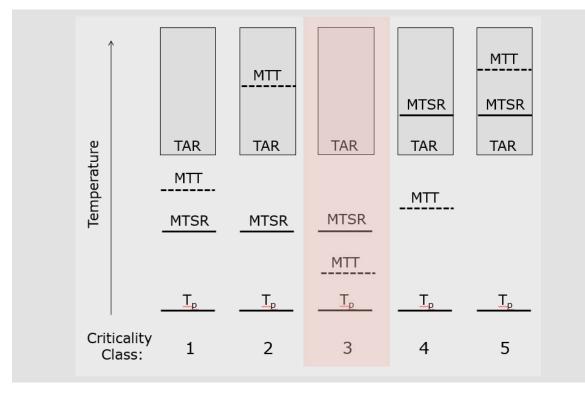
 Operating with a good safety Secondary decomposition Temperature Cooling failure for an exothermic • reaction EXOTHERMIC Ozonolysis 216°C • **Operating Temp** Cooling failure Time - 445 kJ/mol 2 L Outlet Valv 1 L Outlet V Drainar -110 kJ/mol Figure 2. Calculation of Enthalpy of Reaction for Isobutylene Ozonolysis

# THERMAL HAZARD EVALUATION





## **STOESSEL CRITICALITY CLASS OF CHEMICAL REACTIONS**



- Class 1 are safest
- Class 3 can very dangerous if significant amount of solvent is boiled
- Class 4 and 5 are potentially very hazardous.

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#### **CONSEQUENCES OF THE HIGH EXOTHERMIC REACTION**

- Mitigate the risk by physically breaking the charge into 7 charges of 0.2 to 0.3 equivalents each.
- Literature showed that despite slow addition of reagent, accidents happened because of lack of understanding of the reaction initiation time.
  - There is a need to confirm reaction progress during scale up to ensure safety.
- FTIR was used as FIO





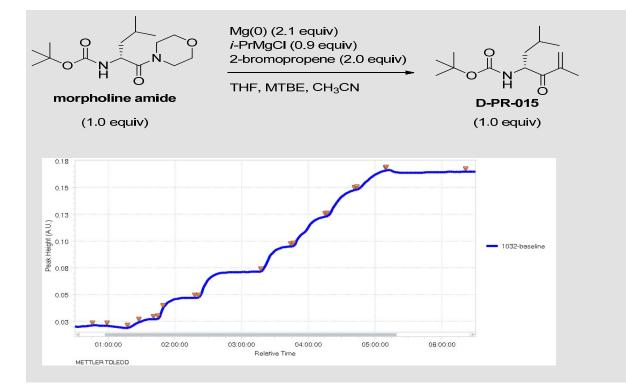
## **DEPLOYMENT OF IN-SITU IR IN THE GMP FACILITY**



Using FTIR to ensure no buildup of energetic intermediates



# **IN SITU FTIR SPECTRA EXAMPLE**



- Campaign utilized insitu IR spectroscopic data to study these intermediates.
- IR profile consistent with HPLC measurement



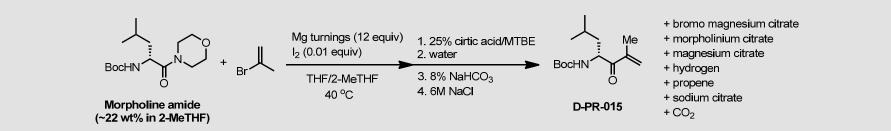


### **CONCLUSION PART1**

- Successful scale up of energetic reaction using thermal hazard evaluation and engineering control
- During the run every 0.2 equivalent caused about 5°C rise
  - Batch sheet ask for 40± 5°C, and add over no less than 10 min
  - Reality
    - Cool the batch to ~37°C, after each addition reactor warmed up to 43°C
    - Took 20 min for each addition
- From bench to scale up initiation, 3 weeks
  - Thermal hazard evaluation
  - Equipment readiness and batch sheet writing
  - Raw material ordering



### **SECOND GENERATION CHEMISTRY**



- No longer using i-PrMgCl as a reagent
- Switch to THF/2-MeTHF solvent from MTBE



### **OUR APPROACH TO THERMAL HAZARD**

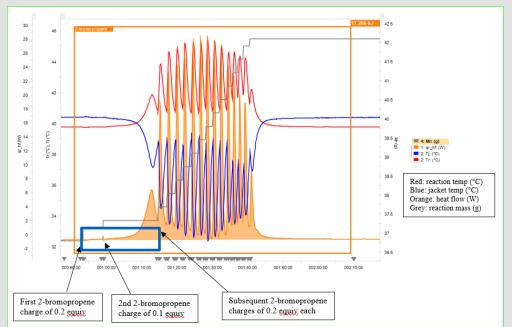
- Changes warranted thermal hazard reevaluation
- Screen all reagents and starting material
- Screen isolated product (s)
- Screen reaction mixture (quenched solution)
- Measure Heat of reaction





## **THERMAL HAZARD EVALUAITON**

- Adiabatic temperature rise of 203°C.
- Heat flow of 705 W/L
- RC1 equipped with huge thermal sink and have high surface-to-volume ratio
  - Still every 0.2 equivalent resulted in 5°C rise.
- Note initiation time





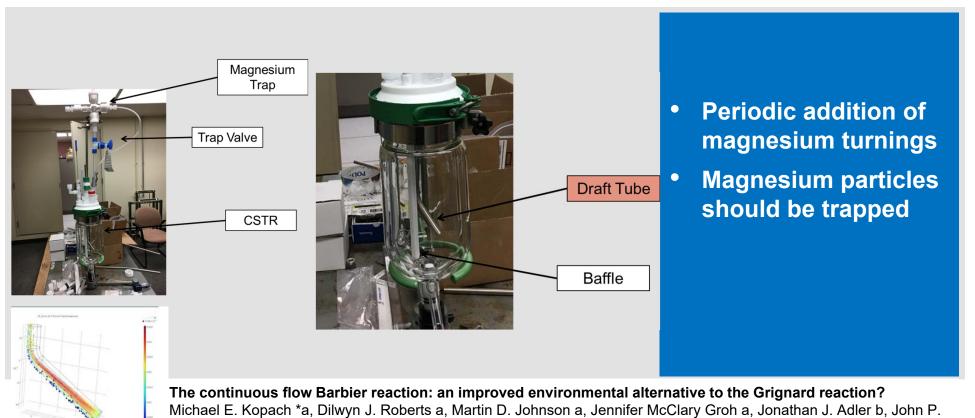
#### **HEAT OF REACTION CONSEQUENCES AT SCALE**

- Even breaking up charges will cause significant temperature rise
- Even if product demand increases, reaction must be done in small reactors to keep high surface to volume ratio
- Emergence of continuous processing.

The Evolving State of Continuous Processing in Pharmaceutical API Manufacturing: A Survey of Pharmaceutical Companies and Contract Manufacturing Organizations

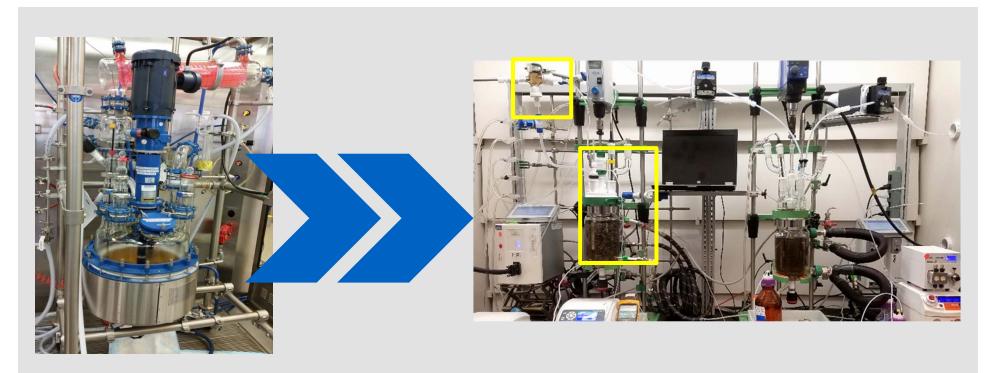
J. Christopher McWilliams\*, Ayman D. Allian, Suzanne M. Opalka, Scott A. May, Michel Journet, and Timothy M. Braden

#### **ADOPTING LILLY PLATFORM**



Schafer b, Michael E. Kobierski a and William G. Trankle a

### **FROM PLANT TO HOOD**





#### **PLANT IN THE HOOD**



CSTR1

CSTR2

flow direction

- 1 L reactor
- No solids were observed in the trap
- High throughput
  - 143 g/h (3.6 kg/day)
- Other safety concerns
  - $T_{r1} T_{j1} = 35-40 \ ^{\circ}C$

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### **CONCLUSION PART2**

- Successful scale up of a very energetic reaction using continuous manufacturing
- Leveraging precompetitive collaboration and adopting Lilly's platform
- At 1-L scale, temperature across the jacket is about 40°C
- GMP proof of concept was successful



### ACKNOWLEDGEMENTS

#### Pivotal Scale up, Thermal Hazard

#### and Engineering

- Derek Brown
- John Huckins
- Kyle Nichols
- Holden Kessler
- Matthew Eitner
- Elçin lçten-Gençer

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- Matthew Beaver
- Andrew Parsons
- Jo Anna Robinson
- Albert Shi
- Sheng Cui

#### <u>DSTE</u>

Seth Huggins

#### <u>AS</u>

- Ning Yang
- Akhil Agarwal (co-op)
- Charles Cheng
- Alicia Zeng

#### <u>MIT</u>

- Gerard Mendez
- Prof. Richard Braatz

#### **Management**

- Roger Hart
- Cenk Undey
- Rohini Deshpande





# Thank you



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#### Celebration of Dr Wilfried Hoffmann, online, 17 December at 9AM Eastern

#### Marking Wilfried's official retirement at end 2020

Scale-up Systems

- Following career of almost 40 years in process safety at Parke Davis, Warner Lambert, Pfizer and Scale-up Systems
- Purchased the first RC-1 in Germany (!); former chairman of the Mettler RXE Forum
- Has made extensive use of RC1 data, MTSR, TMR and the criticality classes outlined by Prof Stoessel when using predictive modeling alongside experimental data in process thermal safety
- Flash talks by Wilfried and collaborators including Flavien Susanne (Sanofi), Yossi Mendel (Teva) and Joe Hannon (Scale-up Systems), with open mic at the end
- Register at <u>https://dcresources.scale-up.com/?id=6427</u>



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