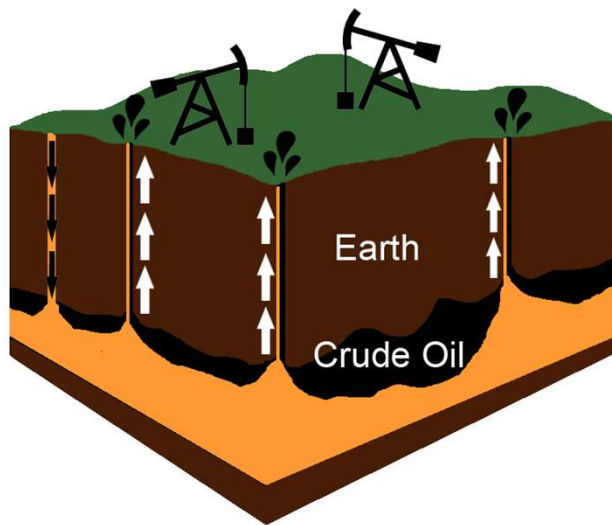
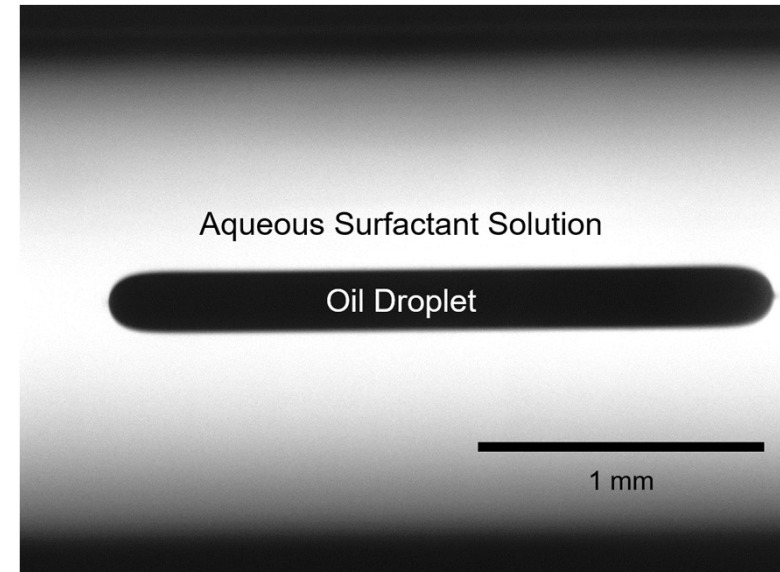
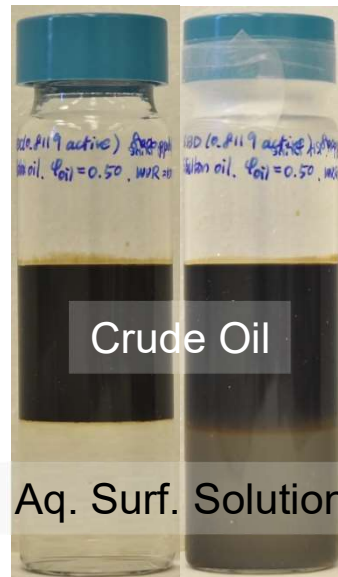


Phase Behavior and Interfacial Tension of Pre-Equilibrated Mixtures of Aqueous Solutions of a Commercial Surfactant and Crude Oil



Aq. Surfactant Solution



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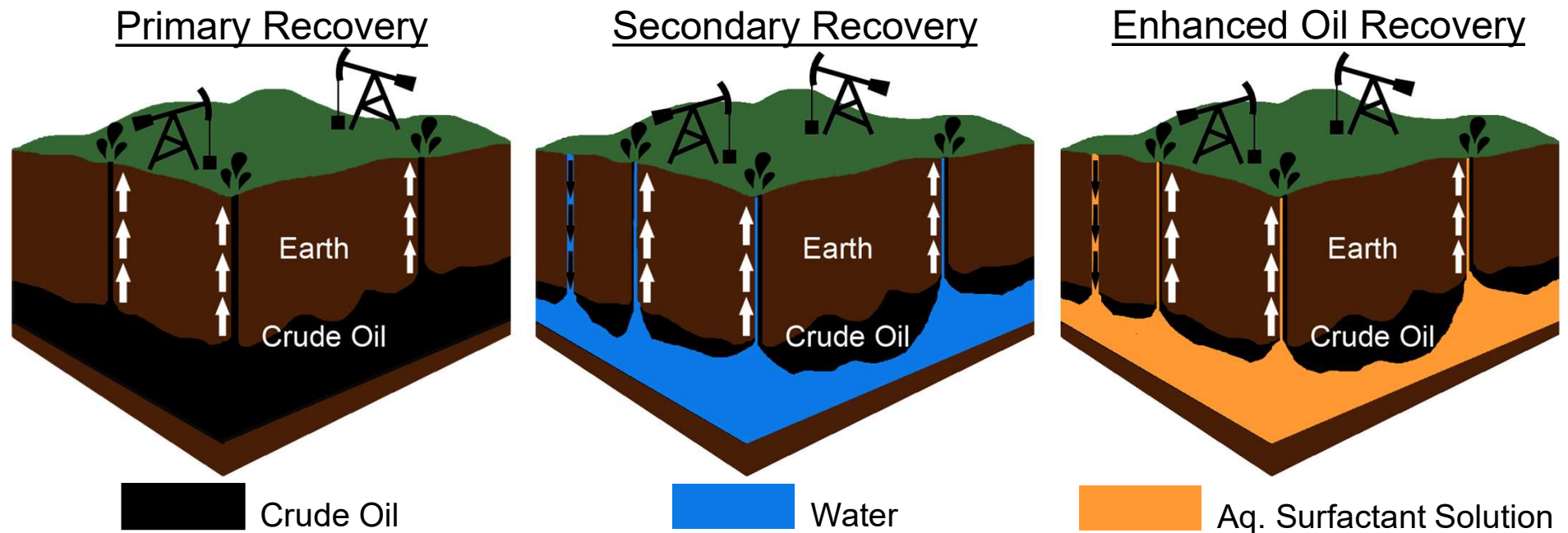


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Injection of Surfactant Solution Increases Oil Recovery



$$N_C = \frac{\mu U}{\gamma}$$

(μ : Fluid Viscosity; U : Fluid Velocity; γ : Interfacial Tension)

Injection of aqueous surfactant solutions, usually with polymer in brine, can dramatically improve the oil recovery.

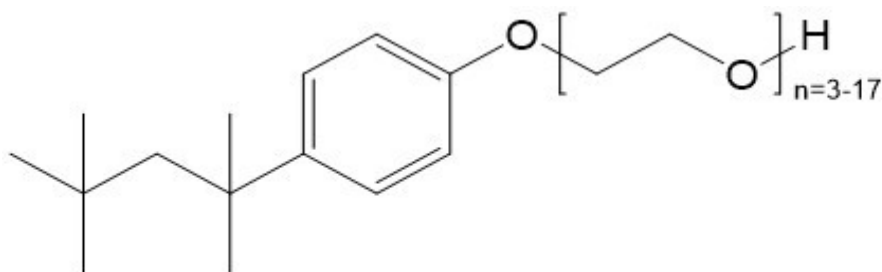
Uren, L.C.; Fahmy, E.H. *Trans. AIME* **1927**, 77, 318–335.

Sheng, J.J. *Modern Chemical Enhanced Oil Recovery: Theory and Practice*; Gulf Professional Publishing **2010**.

Hirasaki, G.J.; Miller, C.A.; Puerto, M.C. *Soc. Pet. Eng. J.* **2011**, 16, 889–907.

Model Surfactant and Surfactant of Interest

Triton™ X-100 (TX100)



- Nonionic surfactant
- CMC = 0.24 mM (150 ppm)
- For procedural calibration

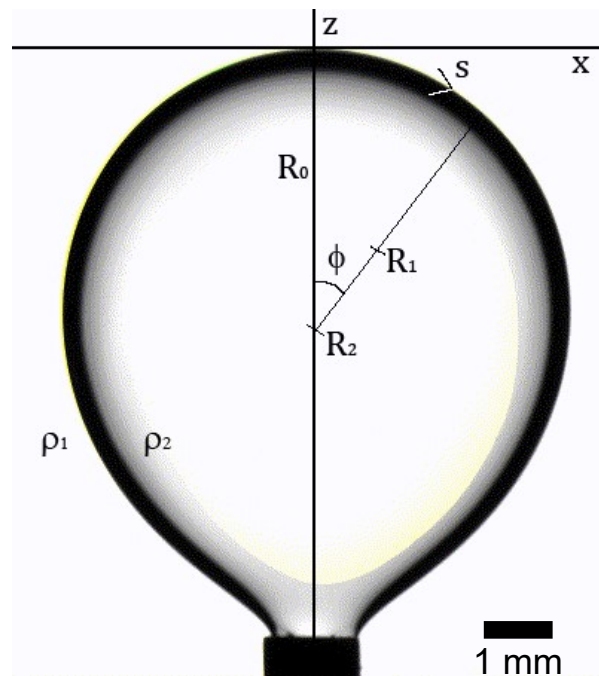
S-13D-HA



- Anionic surfactant
- 80 wt% active
- $n, m = 13$ (on average)
- PO = propylene oxide

Methods for Measuring ST and IFT

Emerging Bubble/Drop Methods (EBM/EDM)

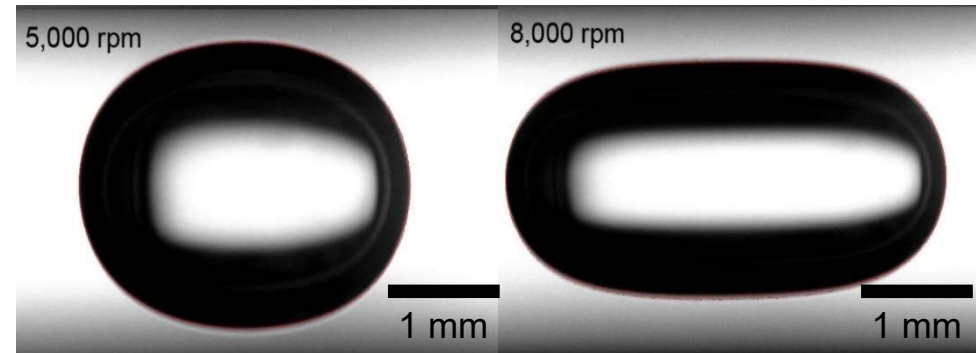


$$2H\gamma = (\Delta\rho)gz$$

H: Curvature, γ : ST or IFT, $\Delta\rho$: Density Difference

- Used for DST and DIFT ($\geq 1 \text{ mN m}^{-1}$)
- Area can be perturbed quickly by drop volume change to follow ST or IFT relaxation.

Spinning Bubble/Drop Methods (SBM/SDM)



$$\gamma \cong \frac{(\rho_1 - \rho_2)\omega^2 R^3}{4} \quad (L \geq 8R)$$

L: length of the drop, R: maximum radius of the drop

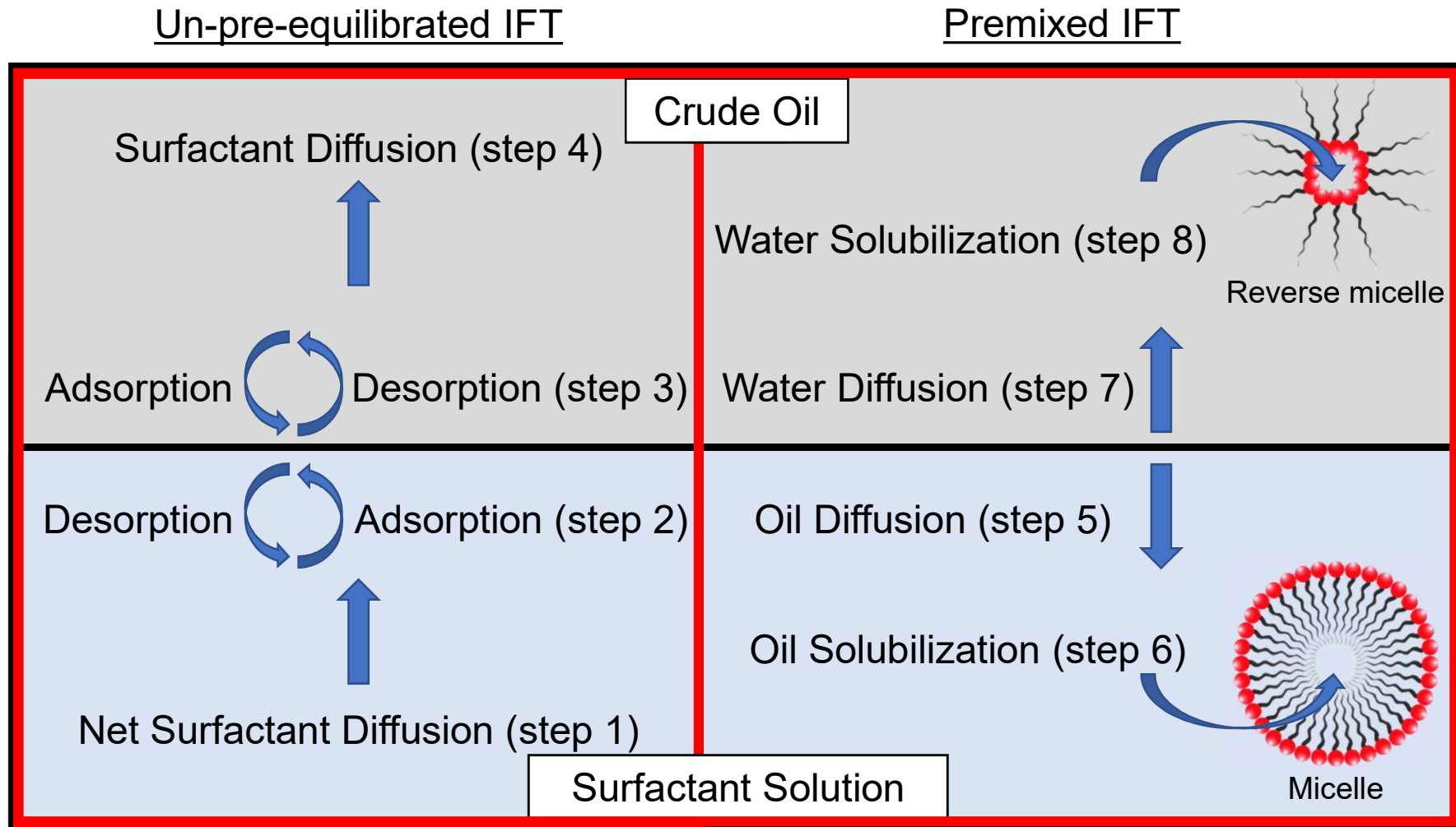
ω : Rotation Frequency, ρ : Density

- Used for both DST and DIFT ($\leq 1 \text{ mN m}^{-1}$)
- Area can be perturbed abruptly by changing rotation frequency to follow tension relaxation.

Rotenberg, Y.; Boruvka, L.; Neumann, A.W. *Journal of Colloid and Interface Science* **1983**, 93, 169-183.

Vonnegut, B. *Review of Scientific Instruments* **1942**, 13, 6-9.

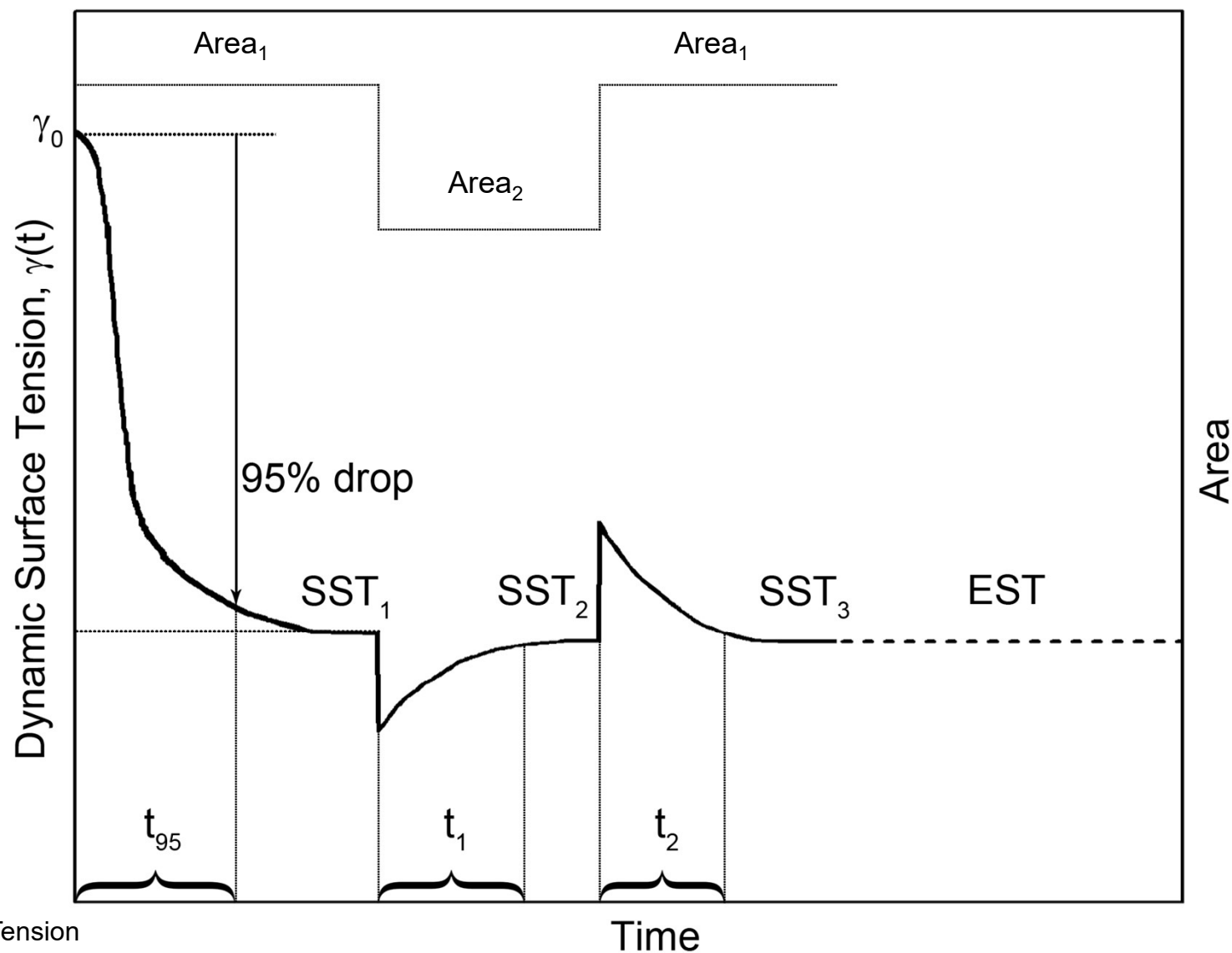
Possible Mechanisms of IFT Equilibration



IFT: Interfacial Tension

Chung, J.; Boudouris, B.W.; and Franses E.I. *Colloids Surfaces A* **2018**, 537, 163-172.

Area Perturbations Test The Stability of Steady-state Tension Values

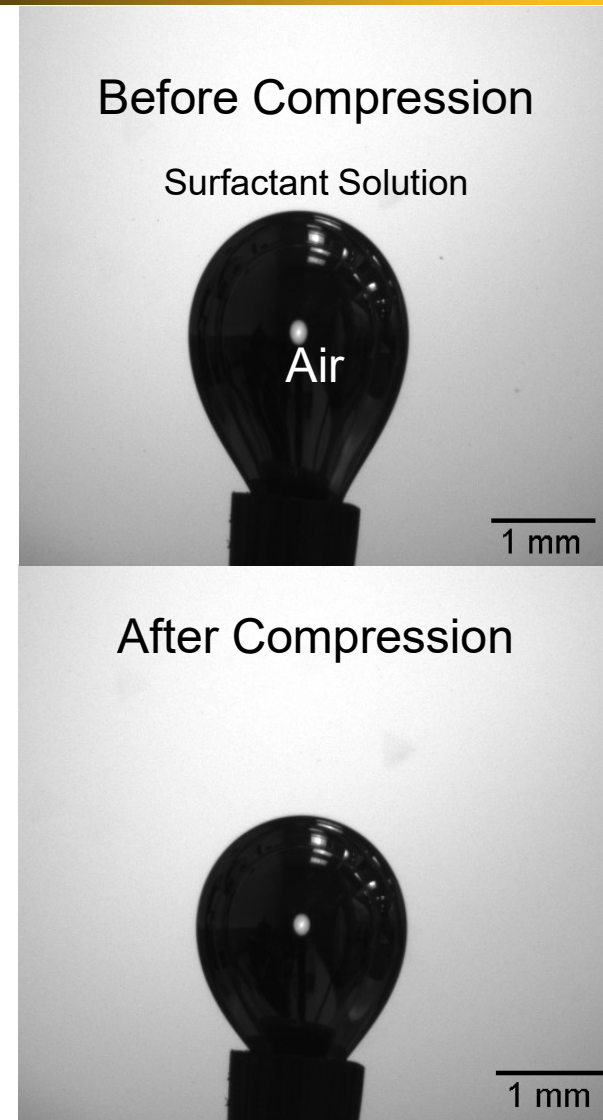
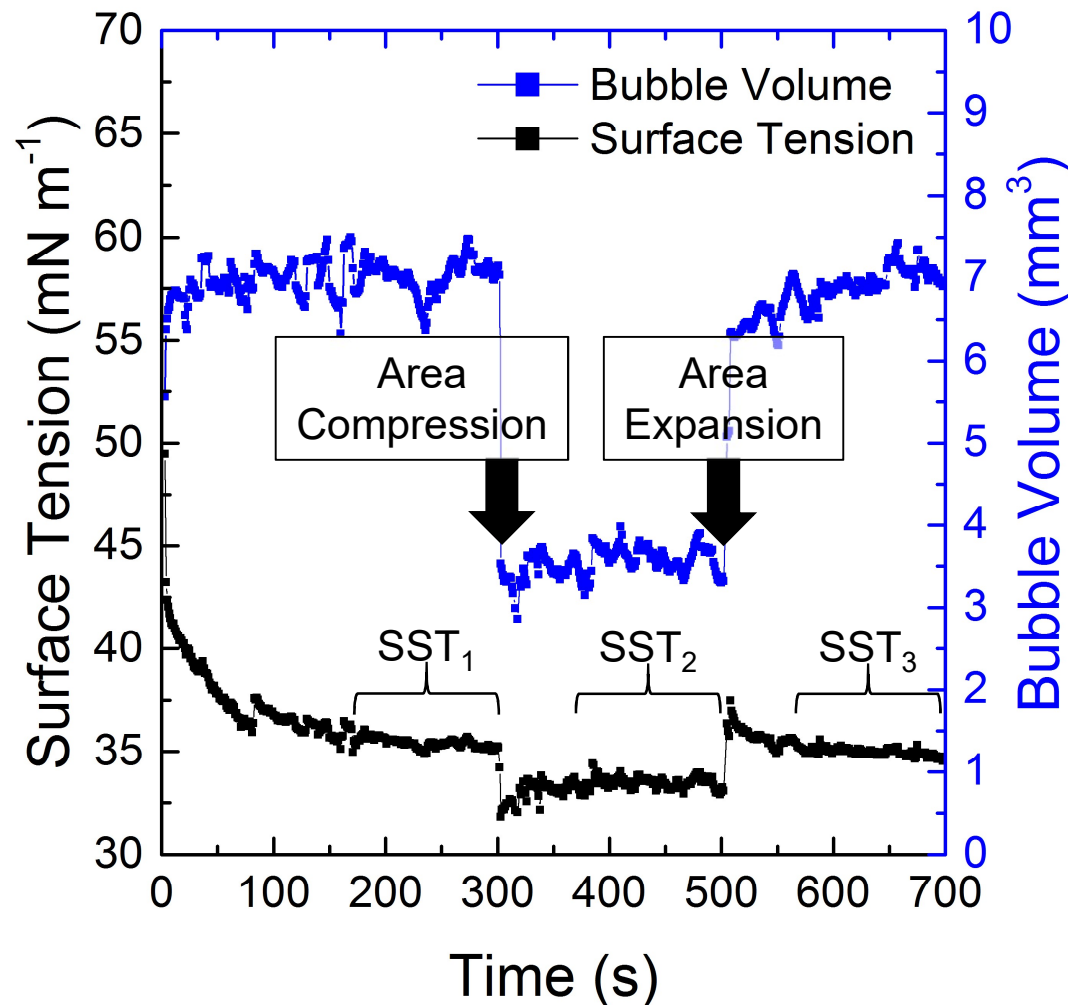


ST: Surface Tension

SST: Steady-state ST, EST: Equilibrium ST

Chung, J.; Boudouris, B.W.; and Franses E.I. *Colloids Surfaces A* **2018**, 537, 163-172.

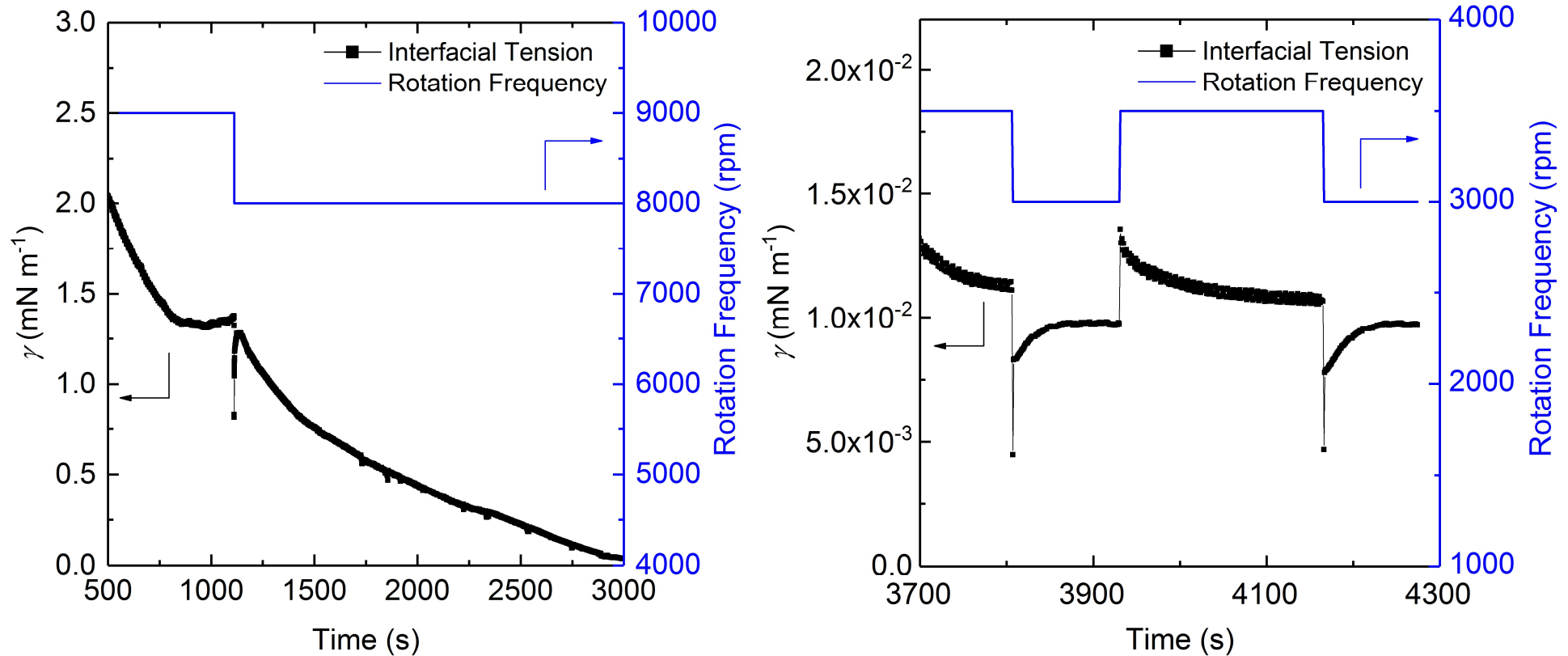
DST Data After Area Perturbations



- $SST_1 \approx SST_2 \approx SST_3 = \text{Equilibrium Surface Tension (EST)} = 35 \text{ mN} \cdot \text{m}^{-1}$

IFT Relaxation After Area Perturbations

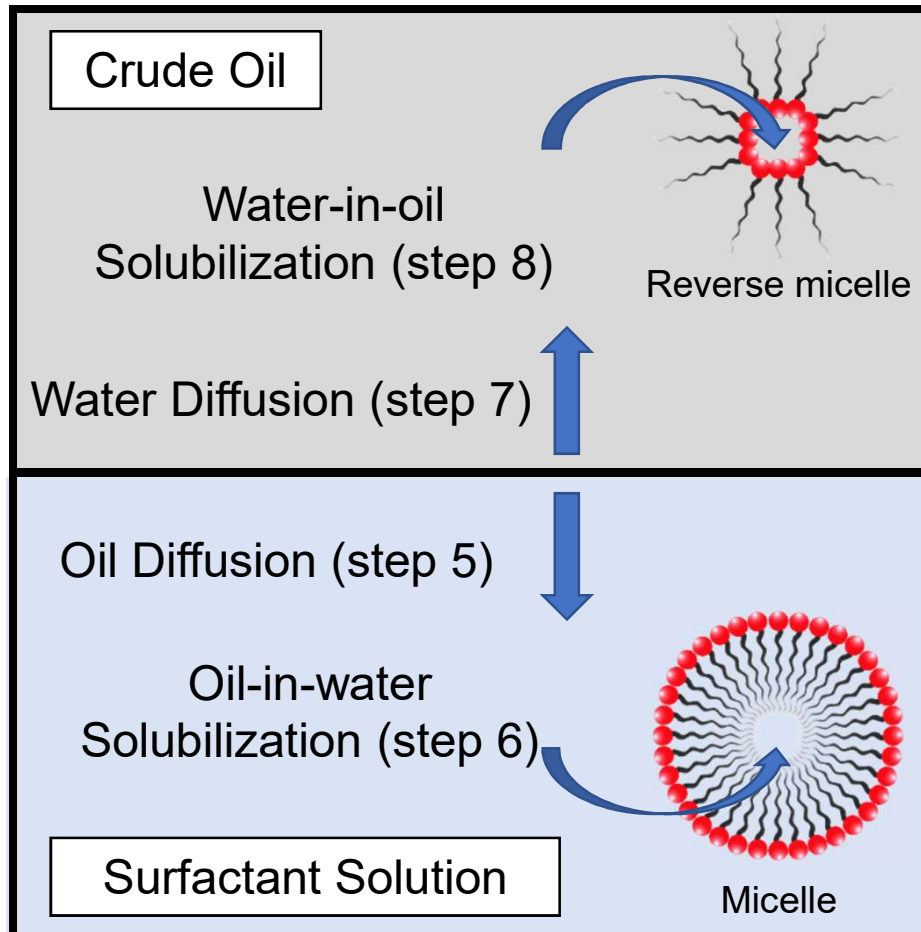
S13D 20 ppm in Brine Against Crude Oil (SDM)



- Area perturbation tests are important for testing the stability of the steady-state IFTs.
- Adsorbed surfactant layer on the interfaces are inferred to be monolayer.

Examination of Premixed Systems

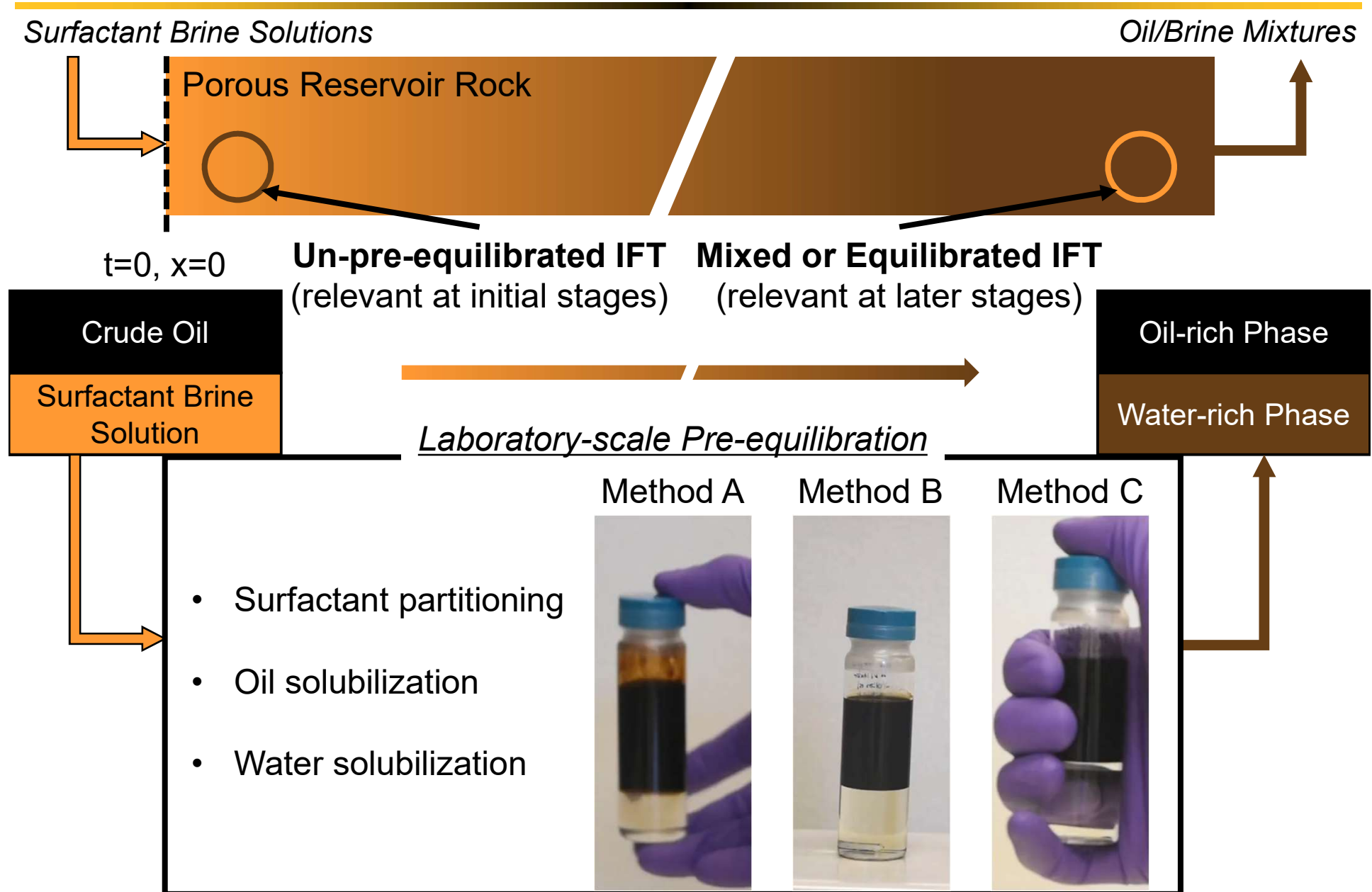
Pre-equilibrated IFT



Additional Issues for the Premixed Systems

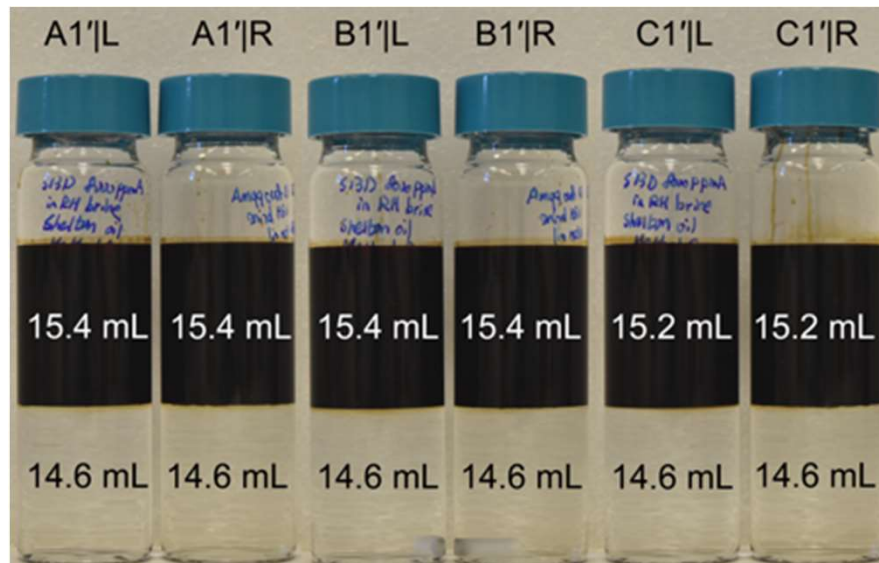
1. Partitioning of components in each phase
 - Quantification of surfactant
 - Volume ratio of each phase
2. Solubilization of components into micelles
 - Distinguish solubilization/dissolution from emulsification
3. Effect of surfactant components
4. Effect of surfactant structures

Laboratory-scale Pre-equilibration

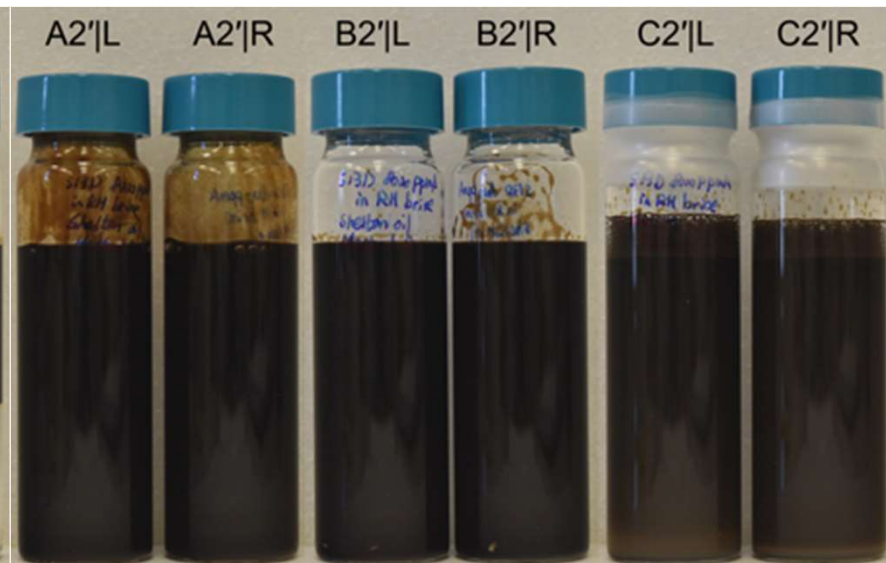


Pre-equilibration Results for Brine Systems

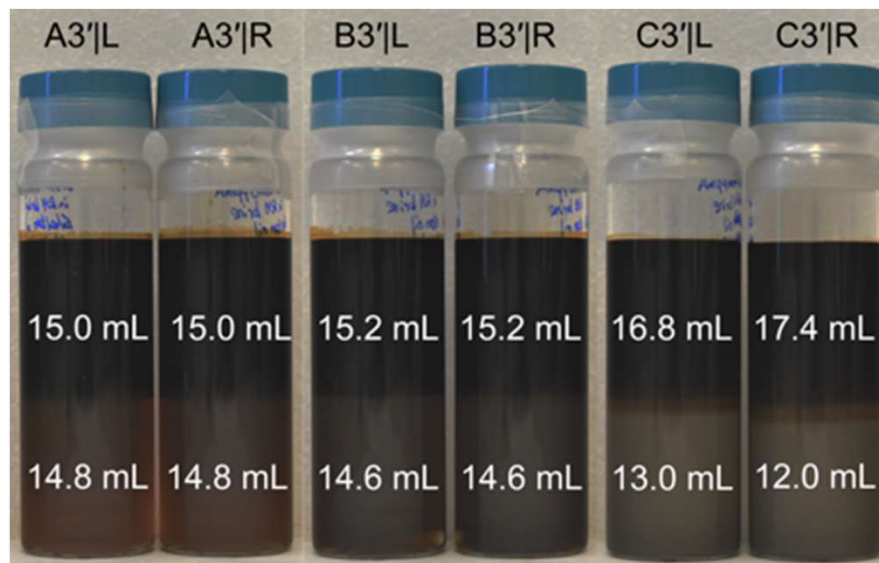
Just Layered



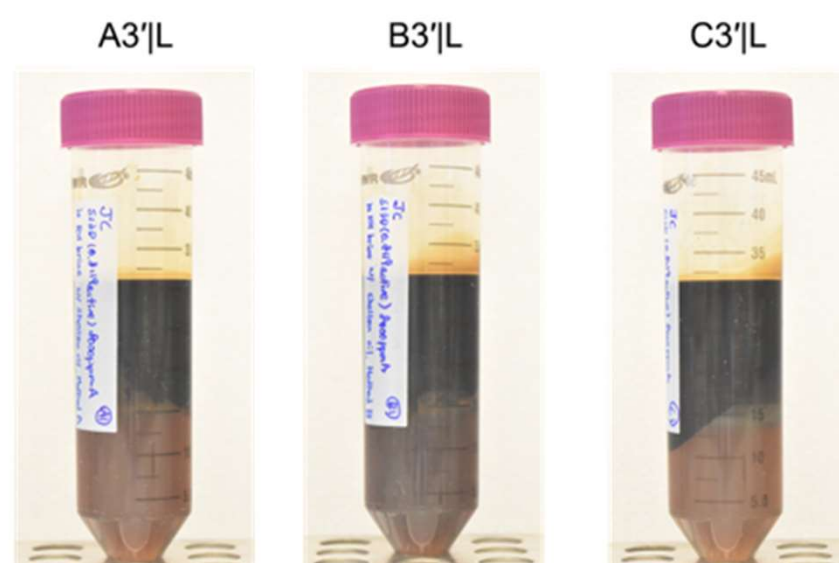
10 s after mixing



200 h after mixing



After centrifugation



Shaking by Hand Provides Mixtures Closer to the Equilibrium


Mixing Method	Surfactant Concentration In the Bottom Layer (ppm)	$\frac{C_{T,o}}{C_{T,w}}$	EIFT	
			Before Mixing ($\times 10^{-3} \text{ mN}\cdot\text{m}^{-1}$)	After Mixing ($\times 10^{-3} \text{ mN}\cdot\text{m}^{-1}$)
(A) Mild Mixing	$8,000 \pm 100$	(< 0.009)	14 ± 1	16 ± 1
(B) Magnetic Stirring	$7,900 \pm 100$	(< 0.021)	14 ± 1	37 ± 2
(C) Shaking by Hand	$4,300 \pm 100$	1.07	14 ± 1	387 ± 7

- Only two phases were observed for all mixtures.
- Method C produced mixtures closest to the phase equilibrium.
- EIFT varies significantly among three mixing methods. EIFT was higher for Method B than for Method A, and much higher for Method C.

Effect of the WOR or Oil Volume Fraction (ϕ) To Phase Behavior

S13D 1 % in brine with crude oil

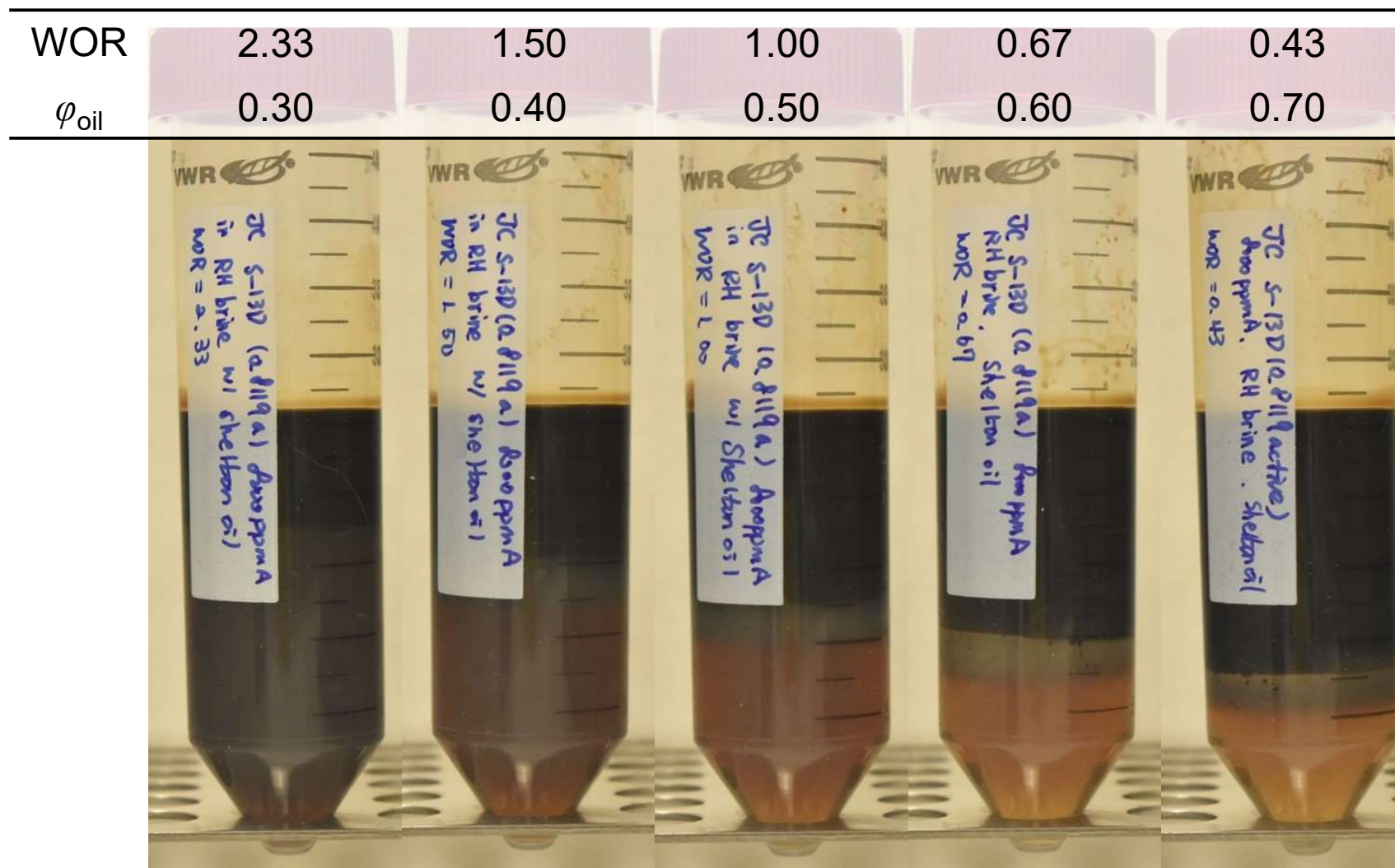
WOR	2.33	1.50	1.00	0.67	0.43
ϕ_{oil}	0.30	0.40	0.50	0.60	0.70



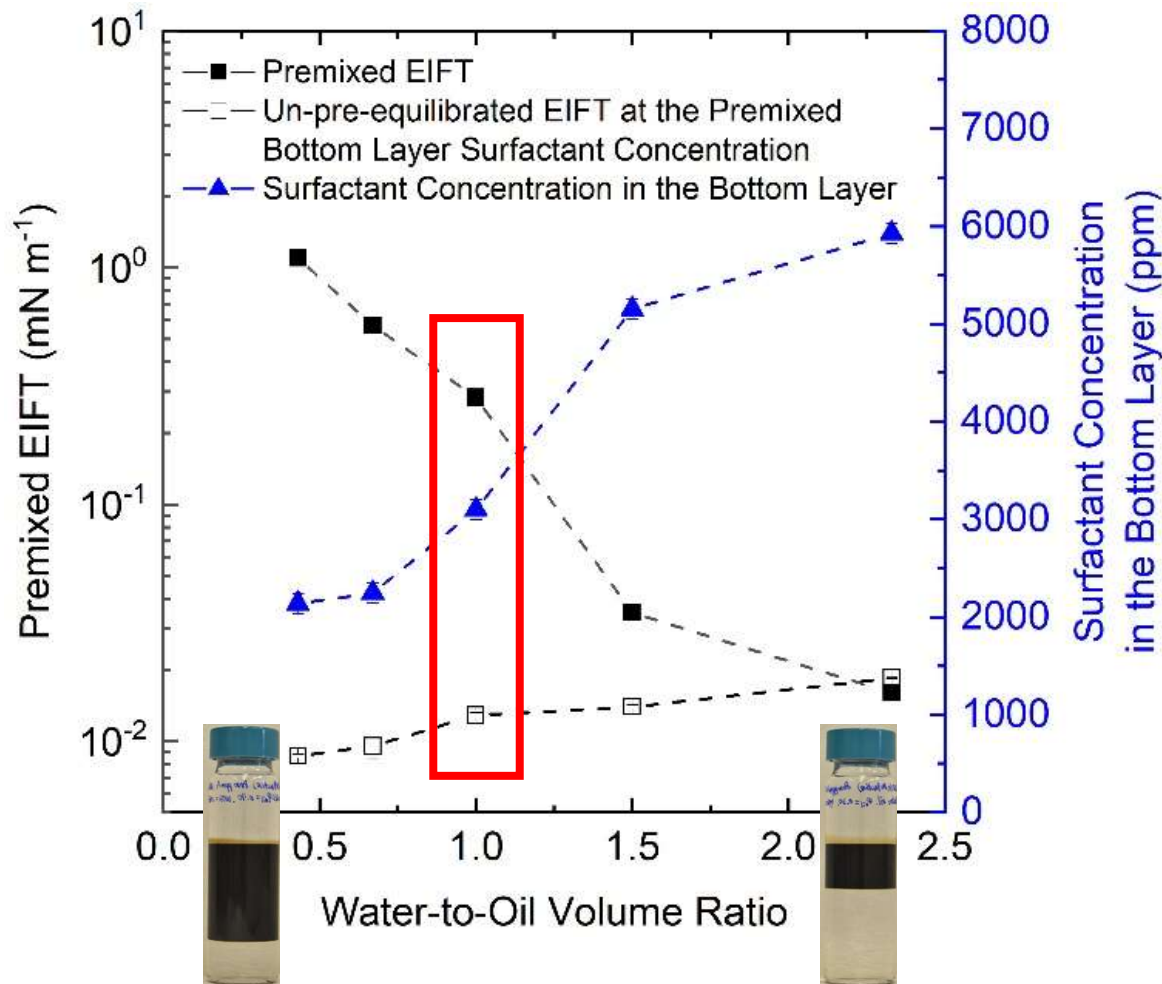
The image shows five vials containing a mixture of S13D 1% in brine with crude oil. The vials are labeled with their respective oil volume fraction (ϕ_{oil}) and water-to-oil ratio (WOR). The vials show a dark oil phase at the bottom and a lighter brine phase at the top. The interface between the two phases is visible, showing some emulsification. The vials are labeled with their respective ϕ_{oil} and WOR values.

Effect of the WOR or Oil Volume Fraction (ϕ) on Phase Behavior After Centrifugation

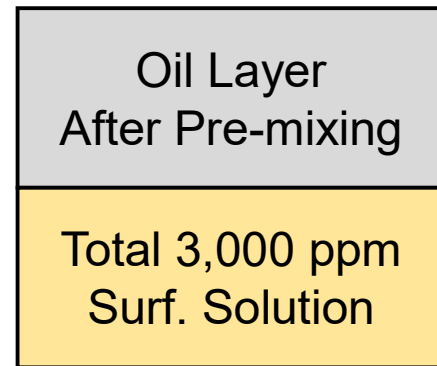
S13D 1 % in brine with crude oil



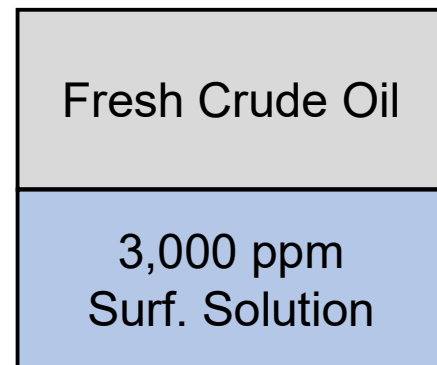
Effect of WOR on Phase Behavior and EIFT



Premixed mixture

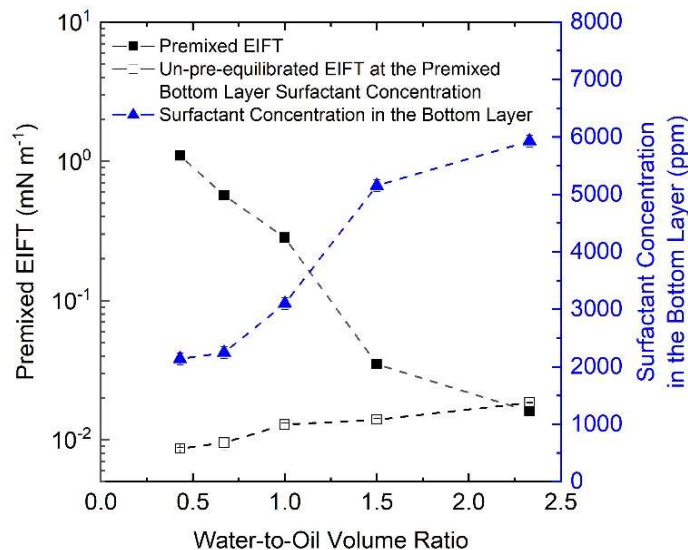
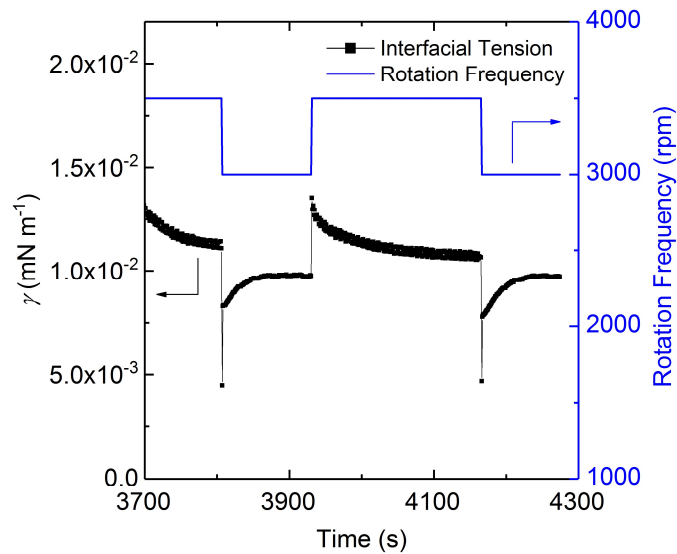


Un-premixed mixture



- As the WOR decrease, or as ϕ increase, more surfactant partitions into the oil phase.
- Partitioning of various surfactant components is inferred to be preferential.

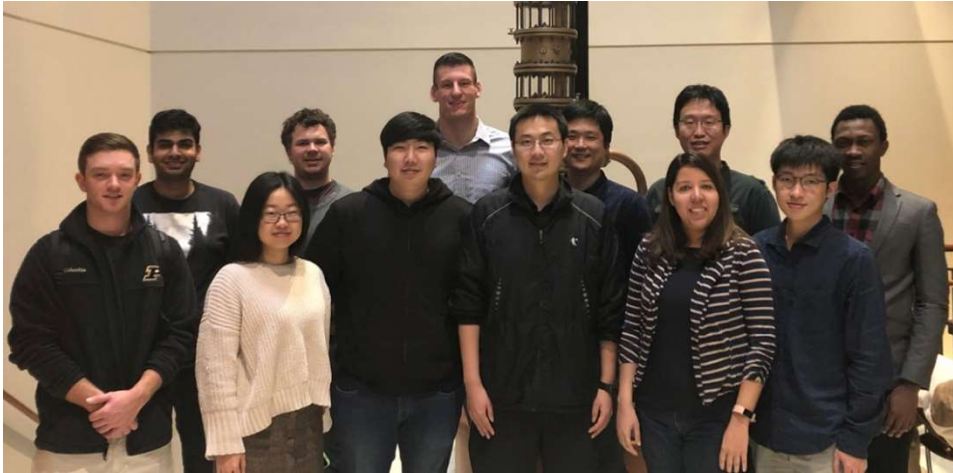
Conclusions



- Area perturbation tests stability of the steady-state tension values so that reliable equilibrium tension values can be established.
- Adsorbed surfactant layer on the interfaces are inferred to be monolayer based on the tension relaxation behavior after each area perturbation.
- Premixed EIFTs can be different from un-pre-equilibrated EIFTs. Such differences are due to preferential surfactant component partitioning in oil for multicomponent surfactants.
- No single EIFT value can fully characterize the performance of a surfactant formulation for surfactant water flooding. Therefore, One should determine how EIFT may vary with the WOR in order to infer or predict the performance of a surfactant formulation in a surfactant water flooding applications.

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