

# Eli Lilly's Approach to Early Phase Chemical Reactivity Hazard Assessments

Purdue Process Safety & Assurance Center  
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*Eli Lilly and Company*

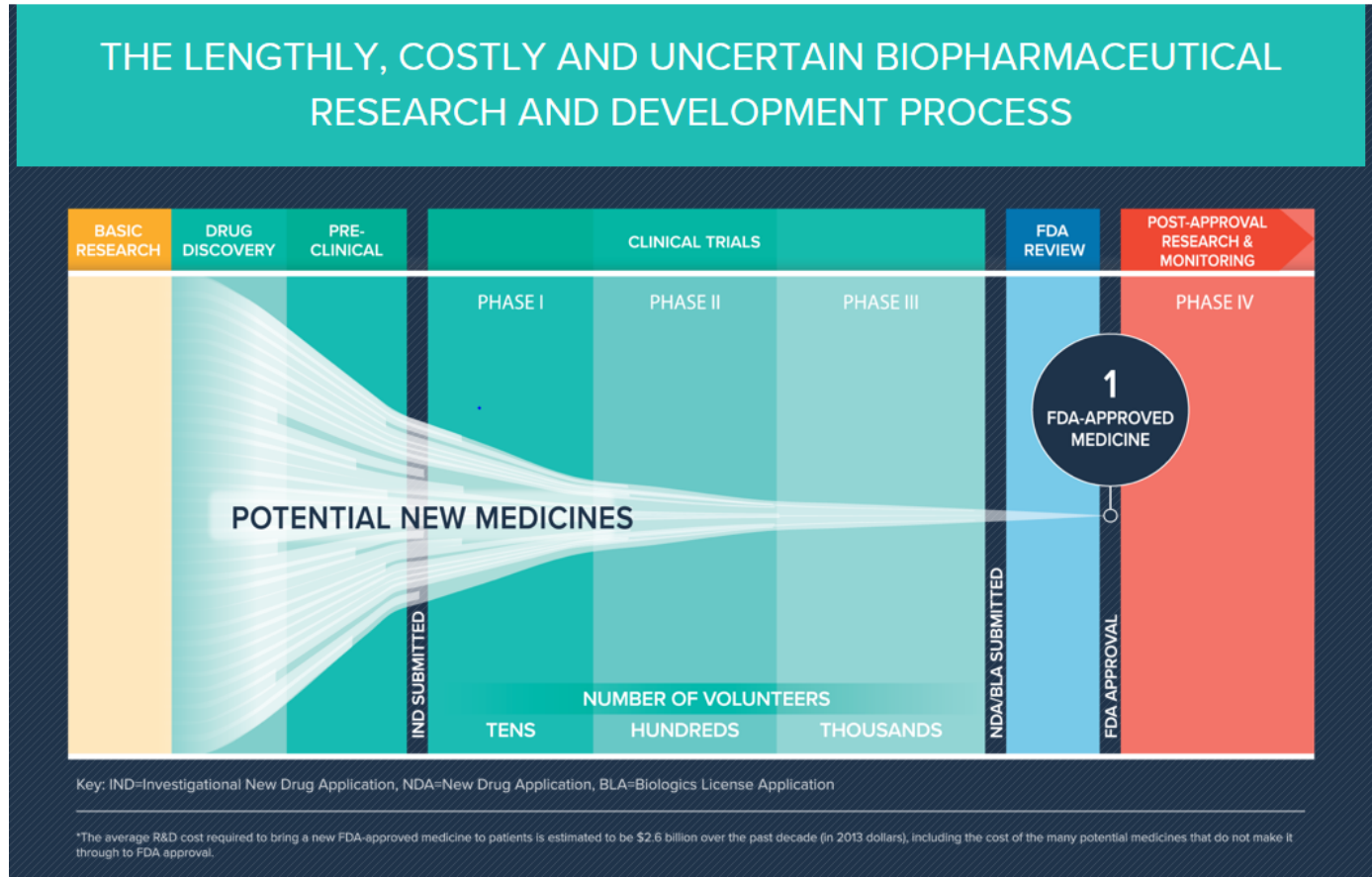
*Indianapolis, IN 46285*

# Our Fundamentals

- ◆ Our Mission: We make medicines that help people live longer, healthier, more active lives.
- ◆ Our Vision: We will make a significant contribution to humanity by improving global health in the 21st century.
- ◆ Our Values: Integrity, excellence, respect for people



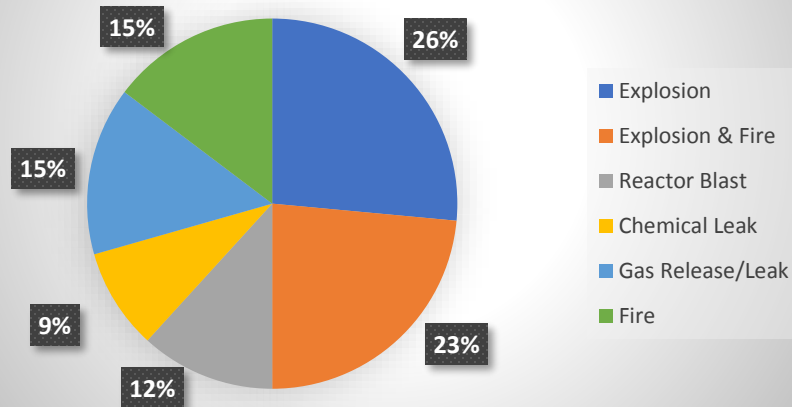
# The Biopharmaceutical Research & Development Process



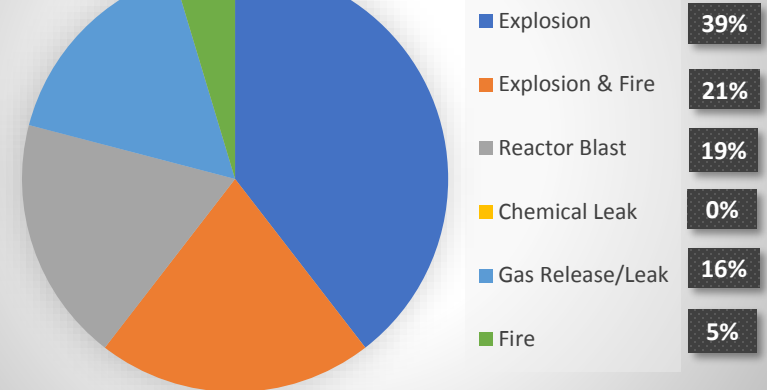
On average it takes 10 to 15 years for a medicine to make its way through the entire R&D process to approval by the U.S. Food and Drug Administration (FDA).

# Process Safety Incidents in the Pharma Industry

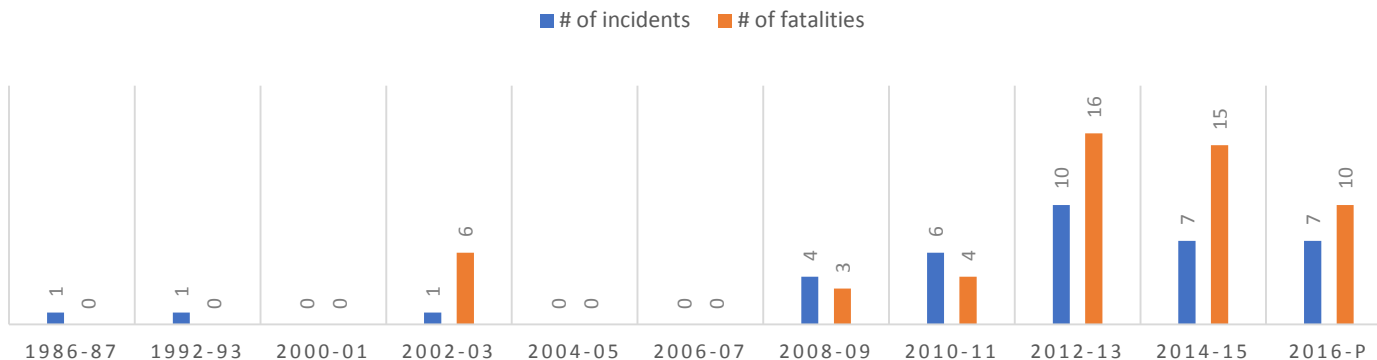
Number of incidents vs. Incident type



Number of fatalities vs. Incident type



FATALITIES & INCIDENTS VS. YEAR



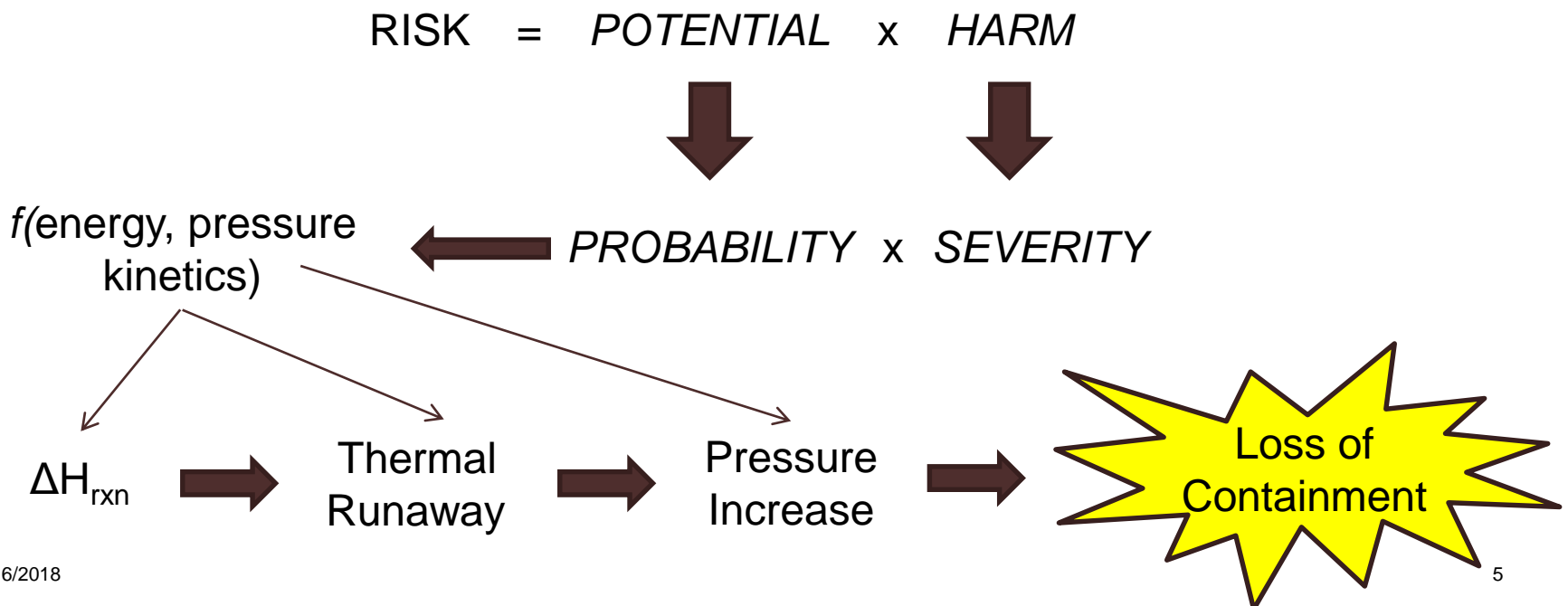
*Professor Ray Mentzer, Purdue Process Safety and Assurance Center (P2SAC)*

# Risks

- ♦ “A situation that has the potential to cause harm to human, environment, and property”

-European Federation of Chemical Engineering

-Stoessel, F. (2008). Thermal Safety of Chemical Processes.



# The concept of Reaction Scale as a Surrogate for Risk Likelihood

## Heat Balance for a Batch Reactor

Exponential

Linear

$$k_0 e^{-E/RT} \cdot C_{A0}^n (1 - X)^n \cdot V \cdot (-\Delta H_r) \leq U \cdot A \cdot (T_c - T_r)$$

Diagram illustrating the heat balance equation for a batch reactor. The equation is shown with brackets indicating the heat generation term (left) and the heat removal term (right). The heat generation term is labeled 'Exponential' and the heat removal term is labeled 'Linear'. The equation is also labeled 'Both are functions of geometry'.

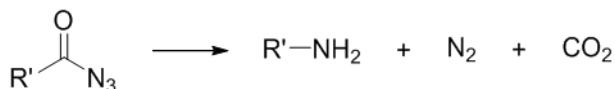
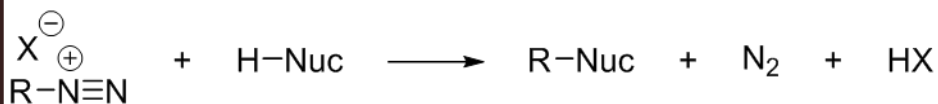
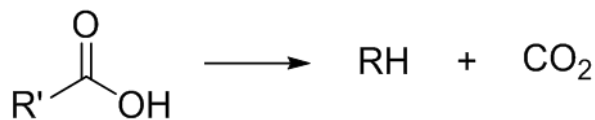
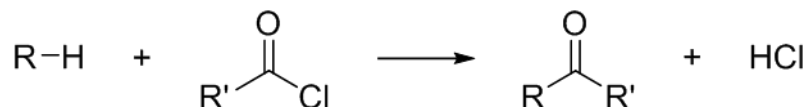
Both are functions of geometry

Scale	Reactor Volume (m <sup>3</sup> )	Exchange Area (m <sup>2</sup> )	Specific Cooling Capacity (W/kg·K)	Typical Cooling Capacity (W/kg)
Research Lab	0.0001	0.01	30	1500
Bench Scale	0.001	0.03	9	450
Pilot Plant	0.1	1	3	150
Production	1	3	0.9	45
Production	10	13.5	0.4	20

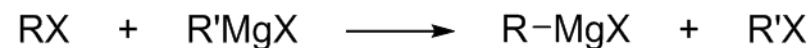
# Assessment of Reactivity Hazards – High Hazard Reactions

- ◆ Check against internal pick list of known high hazard transformations:

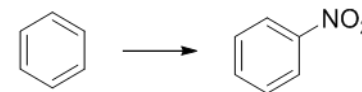
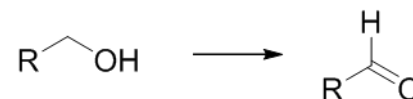
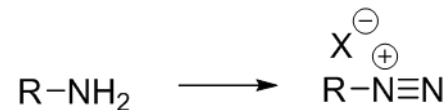
## Gas Generating Reactions



## Water Reactives

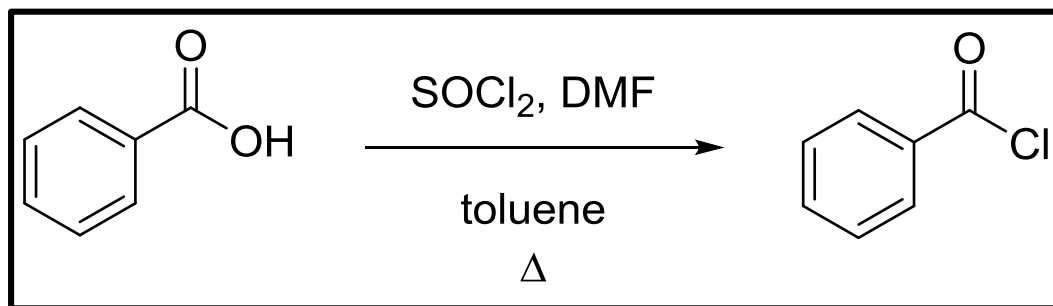


## Known High Energy Transformations

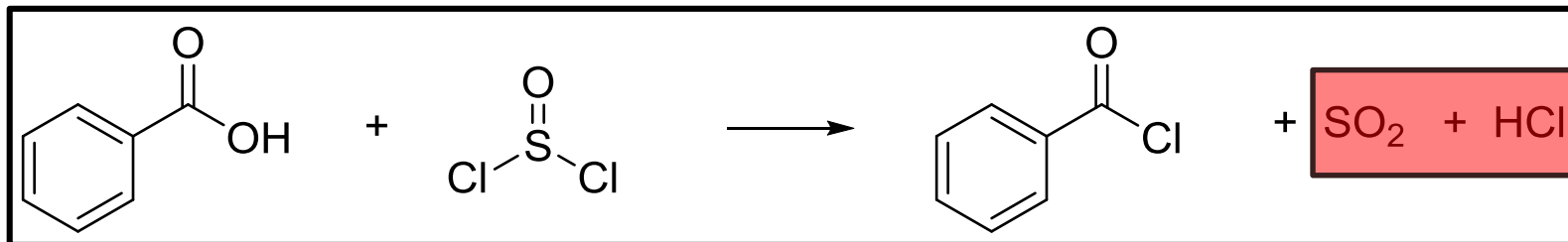


# The Importance of a Balanced Chemical Equation

- ♦ Oftentimes, when chemistry comes from the lab, the reaction scheme only focuses on what we 'want' to make:

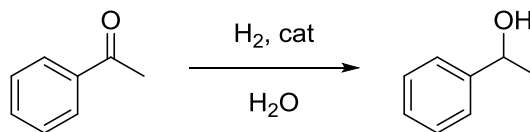


- ♦ Unbalanced chemical equation can mask certain hazards:



# Assessment of Reactivity Hazards with limited Data

*“A ketone is to be hydrogenated to the corresponding alcohol in an aqueous solution at a concentration of 0.1 M and a pressure of 2 bar in a reactor protected against overpressure by a safety valve with a set pressure of 3.2 bar.”*



- ◆ No thermal data are available
- ◆ Assess the severity that thermal risks pose for this reaction.
- ◆ What now?

# Use of tabulated Data Provides a Good, Quick entry

$$Q'_r = \frac{C \cdot (-\Delta H_r)}{\rho}$$

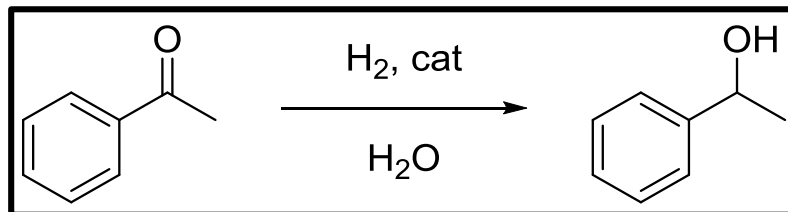
Given (0.1 M) → C

$\rho=1$  for H<sub>2</sub>O →  $\rho$

Reaction	$\Delta H_{\text{rxn}}$ (kJ/mol)
Neutralization (HCl)	-55
Neutralization (H <sub>2</sub> SO <sub>4</sub> )	-105
Sulfonation	-150
Hydrogenation (alkene)	-200
Hydrogenation (nitro)	-560
Hydrogenation (ketone)	-200
Nitration	-130

- 10-fold change in concentration leads to increase of heat release by an order of magnitude!
- If switching to nitro group hydrogenation:
  - 0.1 M sol'n => 56 kJ/kg
  - 1.0 M sol'n => 560 kJ/kg

# More 'Sophisticated' Modeling Approaches



## Group Additivity Calcs

$$\Delta H_r = -56 \frac{\text{kJ}}{\text{mol}}$$

$$Q'_r = \frac{0.1 \frac{\text{mol}}{\text{L}} \cdot \left( - \left( -56 \frac{\text{kJ}}{\text{mol}} \right) \right)}{1.00 \frac{\text{kg}}{\text{L}}} = 5.6 \frac{\text{kJ}}{\text{kg}}$$

- ◆ Benson Group Increment Theory
- ◆ *Approximations* account for atomic, bond and group contributions to  $\Delta H^\circ$

## Quantum Calcs

$$\Delta H_r = -67 \frac{\text{kJ}}{\text{mol}}$$

$$Q'_r = \frac{0.1 \frac{\text{mol}}{\text{L}} \cdot \left( - \left( -67 \frac{\text{kJ}}{\text{mol}} \right) \right)}{1.00 \frac{\text{kg}}{\text{L}}} = 6.7 \frac{\text{kJ}}{\text{kg}}$$

- ◆ Fundamental electronics calculations.
- ◆ Doesn't rely on group energies

# Assessment Criteria for Severity of a Runaway

- ♦ The severity of a runaway can be evaluated using the temperature levels attained if:
  - the desired reaction and the undesired reaction proceed under adiabatic conditions.

$$\Delta T_{ad} = \frac{(-\Delta H_{rxn}) \times CA_0}{\rho \times c'_p} = \frac{Q'_{rxn}}{c'_p}$$

## Assessment Criteria for Runaway Reaction Severity

Severity	$\Delta T_{ad}$ (K)	$Q'$ (kJ/kg)
High	>200	>400
Medium	50-100	100-400
Low	<50*	<100

\* and no pressure increase

Method	$Q'_r$ (kJ/kg)	$\Delta T_{ad}$ (K)
Tabular	20	~6
Group Additivity	5.6	~2
Quantum	6.7	~2

CONCENTRATION  
DEPENDENCE!!

1.0 M => 200 kJ/kg

$\Delta T_{ad} \sim 60 K$

# Differential Scanning Calorimetry (DSC)



- ◆ Good screening tool – sample 5-20mg
- ◆ No pressure measurement
- ◆ Correlation calculations allow prediction of shock sensitivity and explosion propagation (Yoshida Correlation).
- ◆ Program extensions allow easy accurate calculation of  $C_p$  and kinetics

Thermal events are visualized as

$$T_{\text{sample}} \neq T_{\text{ref}}$$

Exotherm:  $T_{\text{sample}} > T_{\text{ref}}$

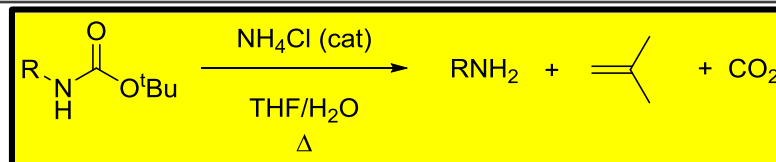
Endotherm:  $T_{\text{sample}} < T_{\text{ref}}$

# $\Delta T_{ad}$ Estimation for Continuous Flow Thermal Deprotection

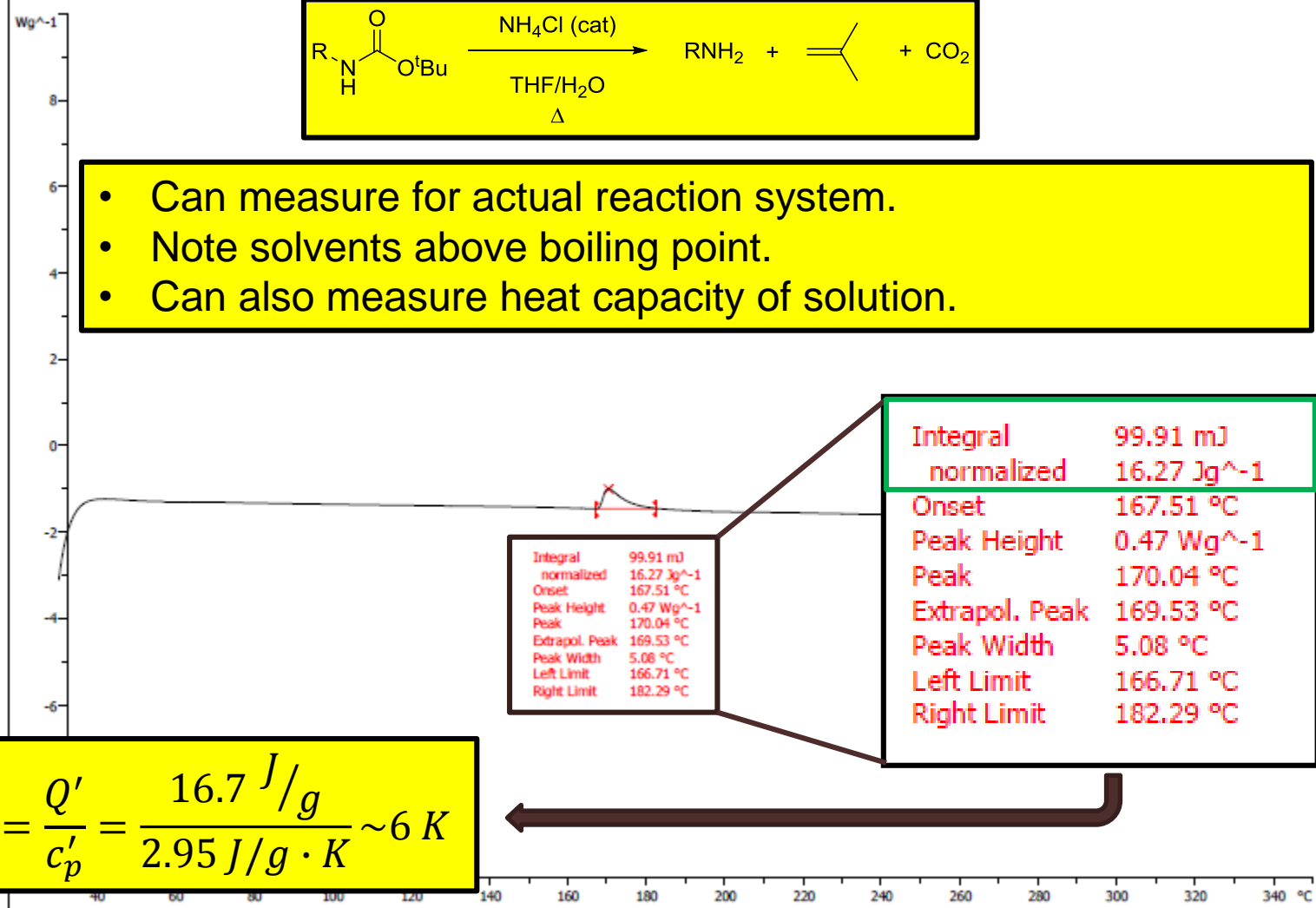
exo

135709 FeedforStep4 Lot V55-H81349-047

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- Can measure for actual reaction system.
- Note solvents above boiling point.
- Can also measure heat capacity of solution.



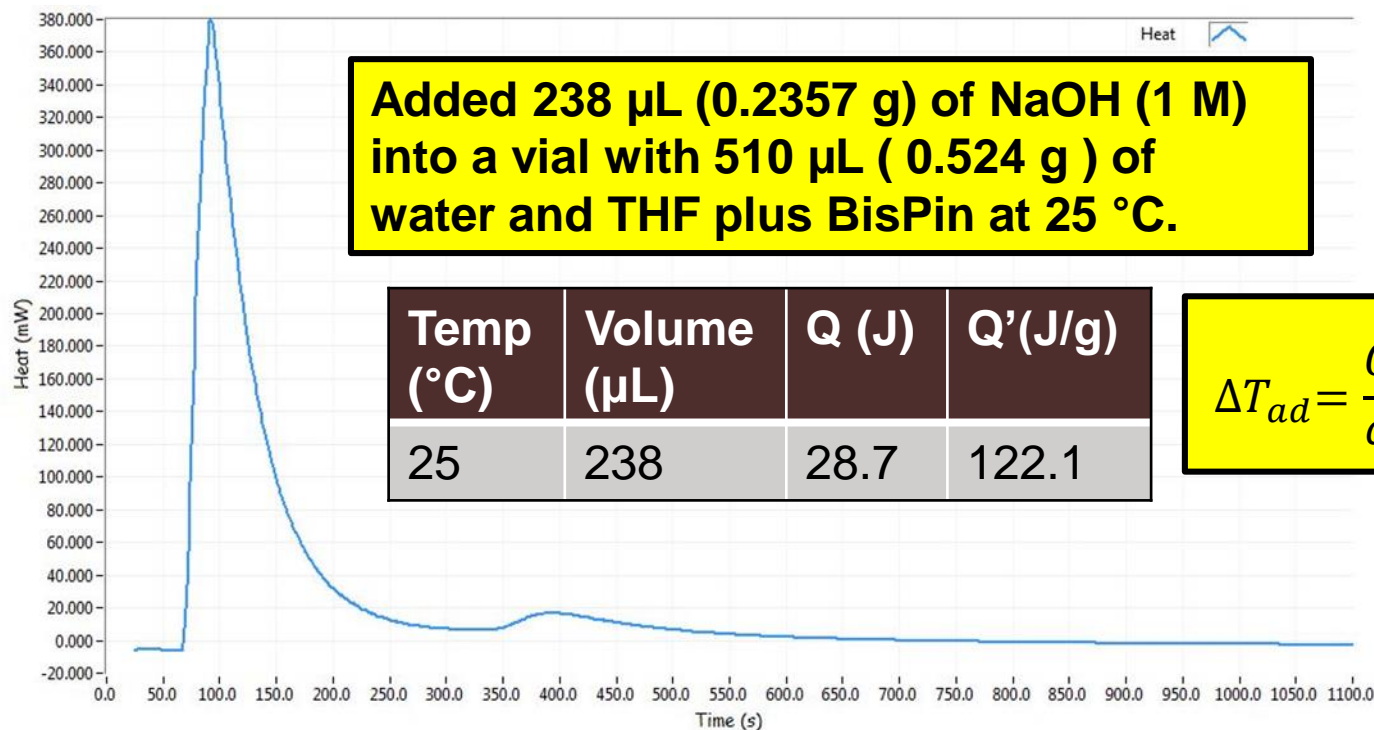
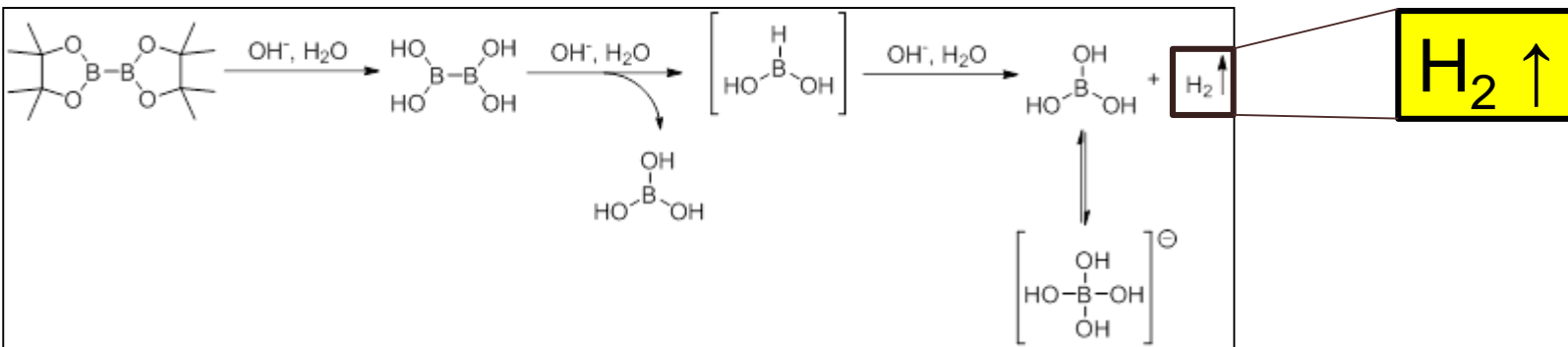
$$\Delta T_{ad} = \frac{Q'}{c_p'} = \frac{16.7 \text{ J/g}}{2.95 \text{ J/g} \cdot \text{K}} \sim 6 \text{ K}$$

# Micro Reaction Calorimeter



- ◆ Early Phase Screening Tool
- ◆ Variety of Data
  - Heat of Reaction/Mixing
  - Titration of reagents
  - Heat Capacity Determination
- ◆ Small sample size (3 mL total volume)
- ◆ Automated Dosing
- ◆ Solids addition

# Use of microcalorimeter to estimate adiabatic temperature rise



*Jeremy Merritt*  
*Odilon Campos*

# Reacting to Early Phase Risk Assessments

- ◆ Use scale as a measure of likelihood =>
  - Larger scale (volume) indicates increased risk
  - Policy to evaluate all reactions run in lab hood if >5L scale (>2 L scale if identified high hazard transformation).
- ◆ Leverage modeling data as much as possible early on; confirm with screening experimentation in medium/high severity situations.
- ◆ Don't be afraid to call a safety timeout.

# Lilly's Thermal Hazard Lab Vision our 'Why'

Proactively identify and eliminate/mitigate  
Thermal Hazard Risks to Lilly's:

Process Safety is fundamentally 'Respect  
for People' in action.

Through 'inherently safer' intermediate and  
process design