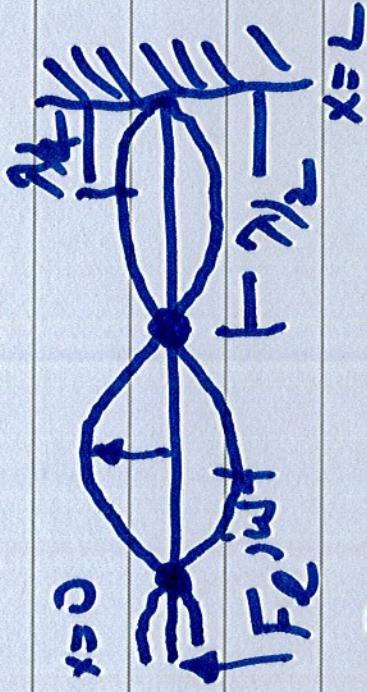


2.9.8c



Eqn 2.9.7

$$y(x,t) = \frac{F_e}{kL} \frac{\sin(k(L-x)) \cos(\omega t)}{\cos(kL)}$$

$$k = \frac{\omega}{c}$$

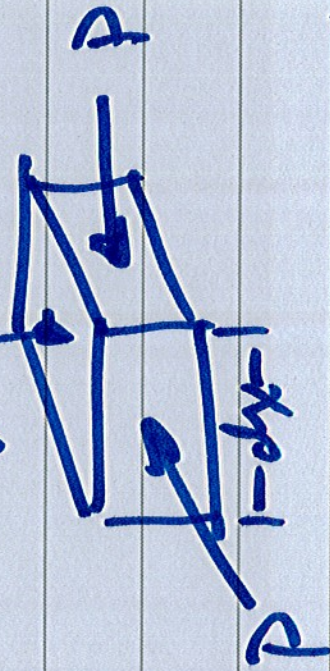
"envelope" $t=0$ & $t = \frac{T}{2}$ 1 \quad -1(a) $\frac{-i F_e \cos(kL)}{kL}$ (b) plot $|y|$ at $x=0$ vs freq $\frac{1}{k}$

plot max disp. amp
 plot the input mechanical impedance

3.2 Derivation of The Wave Eqn

3.2.1 Pressure - Velocity (I)

(i) Equi of state



Ambient Pressure

$$P_0 \approx 1 \times 10^5 \text{ Pa}$$

Ambient Air density

$$\rho_0 \approx 1.2 \text{ kg/m}^3$$

for an ideal gas

- pressure is a function of density
(and density is a function of
particle velocity)

pressure change from $P_0 \rightarrow P$
or density $\rho_0 \rightarrow \rho$

Taylor's series

$$P = P_0 + \left(\frac{dP}{d\rho}\right) (\rho - \rho_0) + \frac{1}{2} \left(\frac{d^2P}{d\rho^2}\right) (\rho - \rho_0)^2 + \dots$$

linear acoustics

- 2nd order terms ignored
- small fluctuations compared to ambient

4

Bulk modulus

$$(P - P_0) = \rho_0 \left(\frac{dP}{d\rho} \right) \left(\frac{\rho - \rho_0}{\rho_0} \right)$$

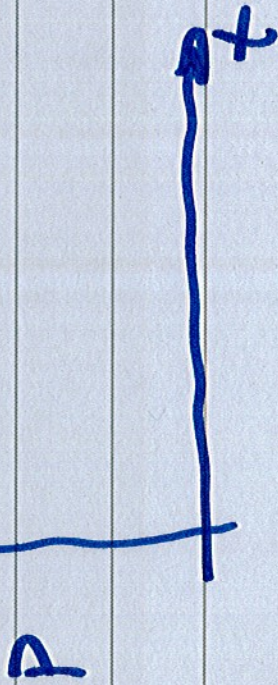
- condensation
 - non-dimensional
 density change

sound
 pressure

$$P - P_0 = P \quad \rho > \rho_0 \quad s > 0 \quad \text{compressed}$$

$$\rho < \rho_0 \quad s < 0 \quad \text{expanded}$$

ρ_0 ~~reference~~



$$P - P_0 = P \quad \text{reference}$$

Bulk modulus

$$P = \beta_0 \left(\frac{dP}{d\beta} \right) s$$

$\beta = \text{adiabatic}$

$$P = \beta s \quad (1)$$

stress = modulus \times strain

6
what is β for adiabatic compression

Two states P, P_0 T, T_0

From thermo

$$\left(\frac{P}{P_0}\right) = \left(\frac{T}{T_0}\right)^\gamma$$

$\gamma =$ ratio of specific heats

$$= 1.4$$

$$\beta = P_0 \left(\frac{dT}{dP}\right)_{P_0} = \gamma P_0$$

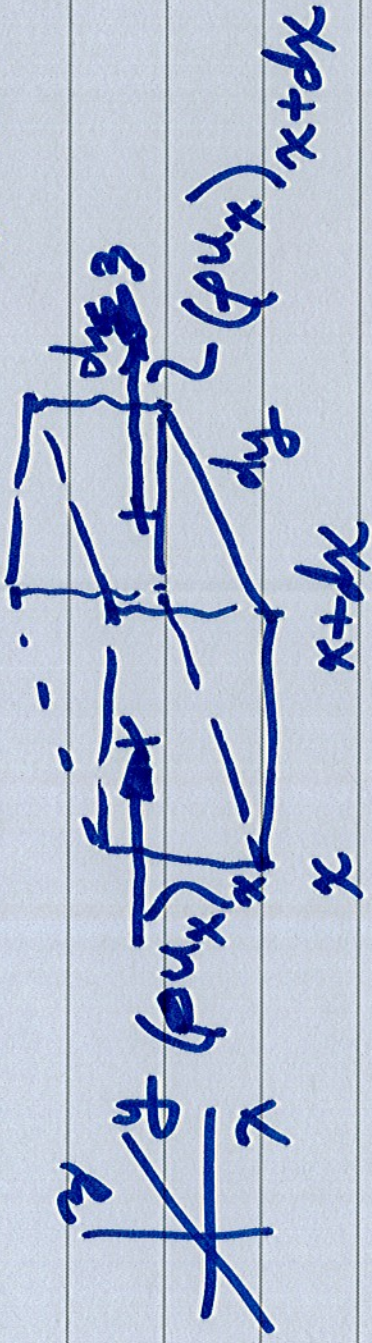
for adiabatic compression

$$= \frac{1.4 \times 10^5}{\underline{\quad}}$$

$P = \beta S^2$ relate to velocity

(iii) Continuity Eqn (conservation of mass)

control volume that is fixed in space



start with

1-D

-motion in x-direction

Rate at which mass flows in

$$(a) \quad (\rho u_x)_x dy dz \quad \text{kg/s}$$

Rate at which mass flows out

$$(b) \quad \underbrace{(\rho u_x)_{x+dx}}_{\text{kg/s}}$$

$$= \left[(\rho u_x)_x + \frac{\partial(\rho u_x)}{\partial x} dx + \dots \right] dy dz$$

net rate of mass inflow

$$(a) - (b) = - \frac{\partial(\rho u_x)}{\partial x} \Big|_x dx dy dz$$

Rate of change of mass in the control volume

$$\frac{\partial \rho}{\partial t} dx dy dz \quad \text{kg/s}$$

$$\frac{\partial}{\partial t} dx dy dz = - \frac{\partial(\rho u_x)}{\partial x} \Big|_x dx dy dz$$

$$\frac{\partial \rho}{\partial t} + \frac{\partial(\rho u_x)}{\partial x} = 0 \quad \text{conservative of mass}$$

both f & u_x are functions of x

$$\frac{\partial f}{\partial t} + u_x \frac{\partial f}{\partial x} + f \frac{\partial u_x}{\partial x} = 0$$

$$s = \frac{f - f_0}{f_0} \quad f = s f_0 + f_0 = f_0 (s + 1)$$

$$f_0 \frac{\partial (s + 1)}{\partial t} + f_0 u_x \frac{\partial (s + 1)}{\partial x} + f_0 (s + 1) \frac{\partial u_x}{\partial x} = 0$$

$$f_0 \frac{\partial s}{\partial t} + f_0 u_x \frac{\partial s}{\partial x} + f_0 (s + 1) \frac{\partial u_x}{\partial x} = 0$$

assume that the products $\frac{\partial s}{\partial x}$ of small quantities are negligible (linear acoustics)

$$\rho \frac{\partial s}{\partial t} + \rho \frac{\partial u_x}{\partial x} = 0$$

$$\left[\frac{\partial s}{\partial t} + \frac{\partial u_x}{\partial x} = 0 \right]$$

2-D

$$\left[\frac{\partial s}{\partial t} + \nabla \cdot \bar{u} = 0 \right]$$

3-D

(2)

$\nabla \cdot \bar{u}$ divergence of the
particle velocity

$\nabla \cdot \bar{u}$ is +ve \nearrow is -ve \searrow

$$\bar{u} = u_x \bar{i} + u_y \bar{j} + u_z \bar{k}$$

$$\nabla \cdot \bar{u} = \frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} + \frac{\partial u_z}{\partial z}$$

Combine (1) + (2)

$$\frac{\partial \rho}{\partial t} + \nabla \cdot \bar{u} = 0$$

Linearized continuity eqn

note correction

- relates ρ to particle velocity