

Computer-aided process engineering in developing and operating continuous processes

Salvador García Muñoz, Ph.D.



Agenda

- Formulation development
- Process development
- Process de-risking and transfer
- Process Monitoring
 - MSPC for fault detection and isolation

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Formulation development

- Mechanistic modeling at this stage requires the ability to predict the **bulk-level behavior from the particle-level information** in a multi-component mixture.
 - Mechanical behavior
 - Chemical interactions
 - This is very complex and so far non-attainable.
- **Mine the data from past experiments**

Formulation development

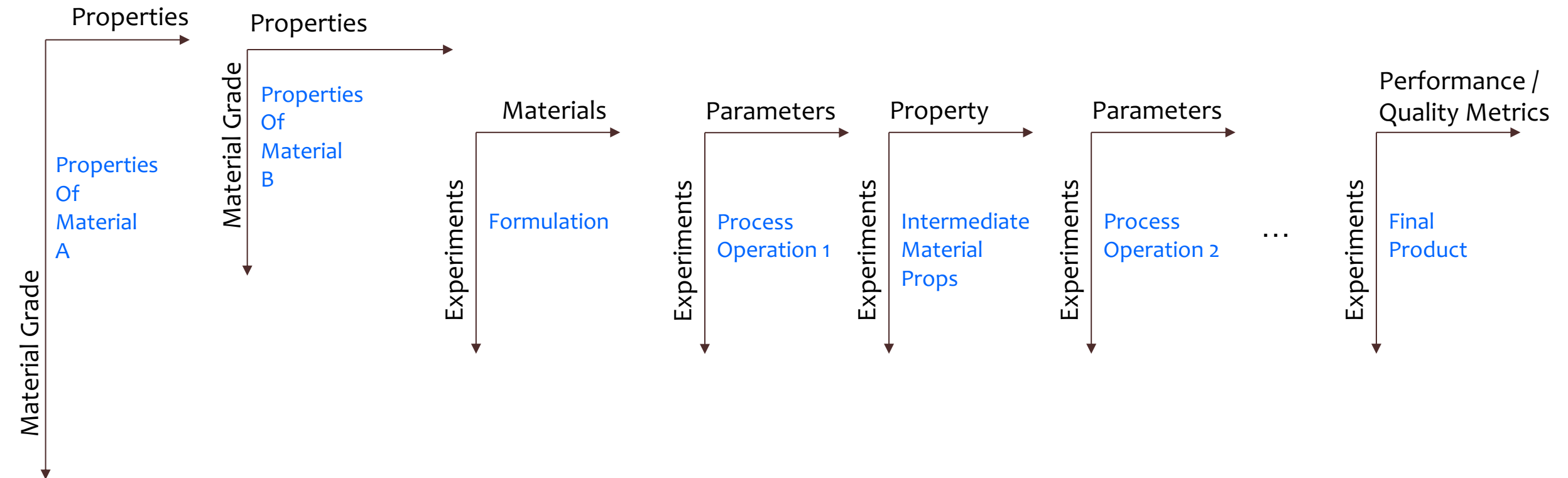
- Mining data from previous experiments.
 - Modeling data from previous products
 - In-silico formulation development
 - Surrogate selection for experimental design
 - Including material variability
 - When you have access to materials
 - When you don't

Formulation development

- Mining data from previous experiments.
 - **Modeling data from previous products**
 - In-silico formulation development
 - Surrogate selection for experimental design
 - Including material variability
 - When you have access to materials (Joe K's papers)
 - When you don't (My cloning algorithm)

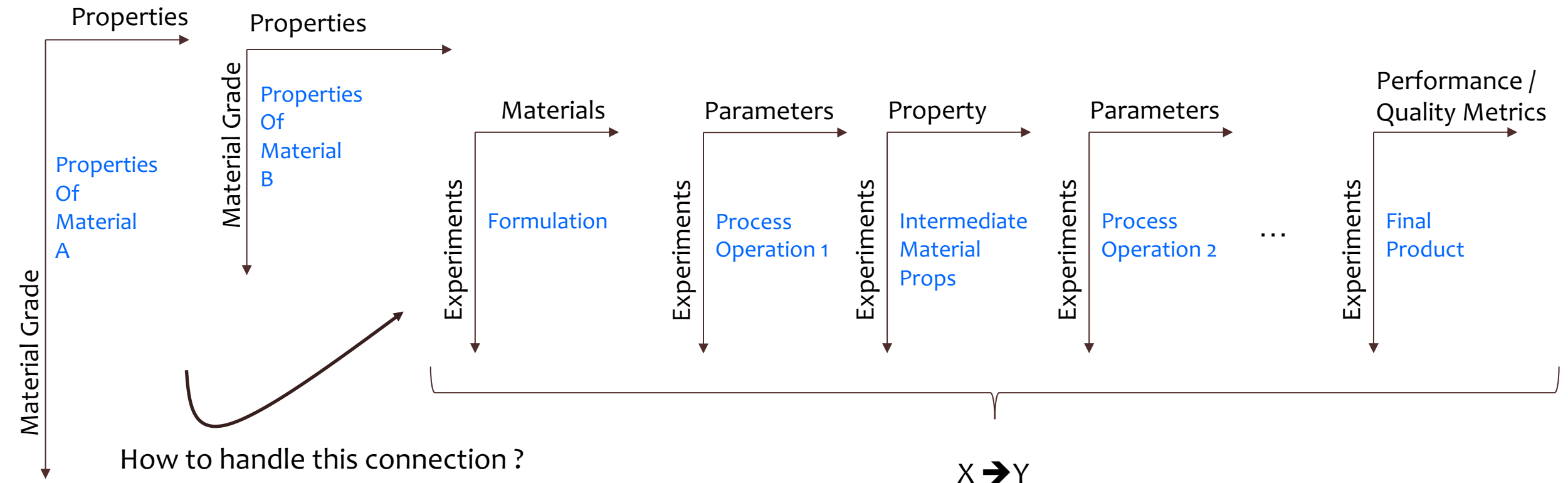
Formulation development

- Product development data is complex

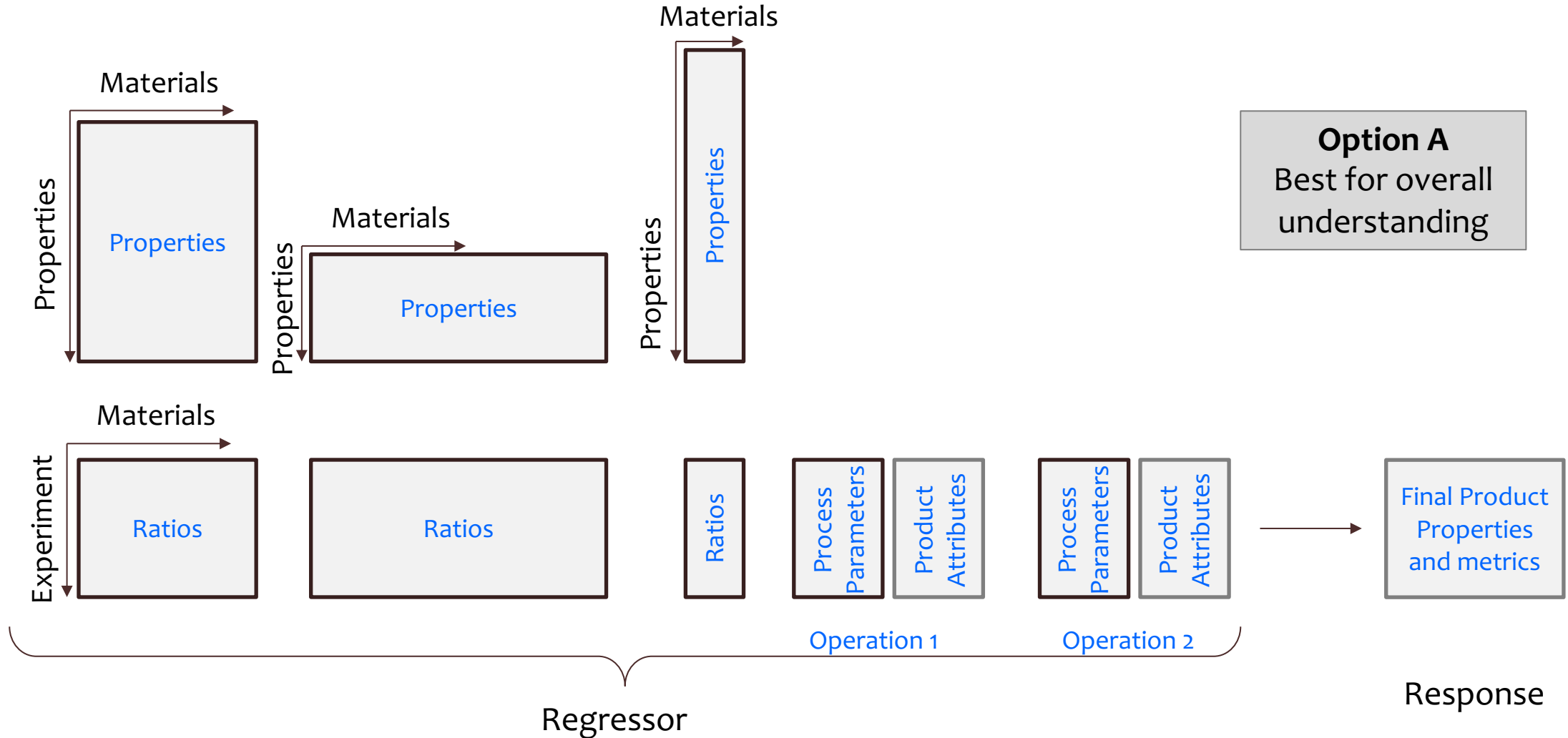


Formulation development

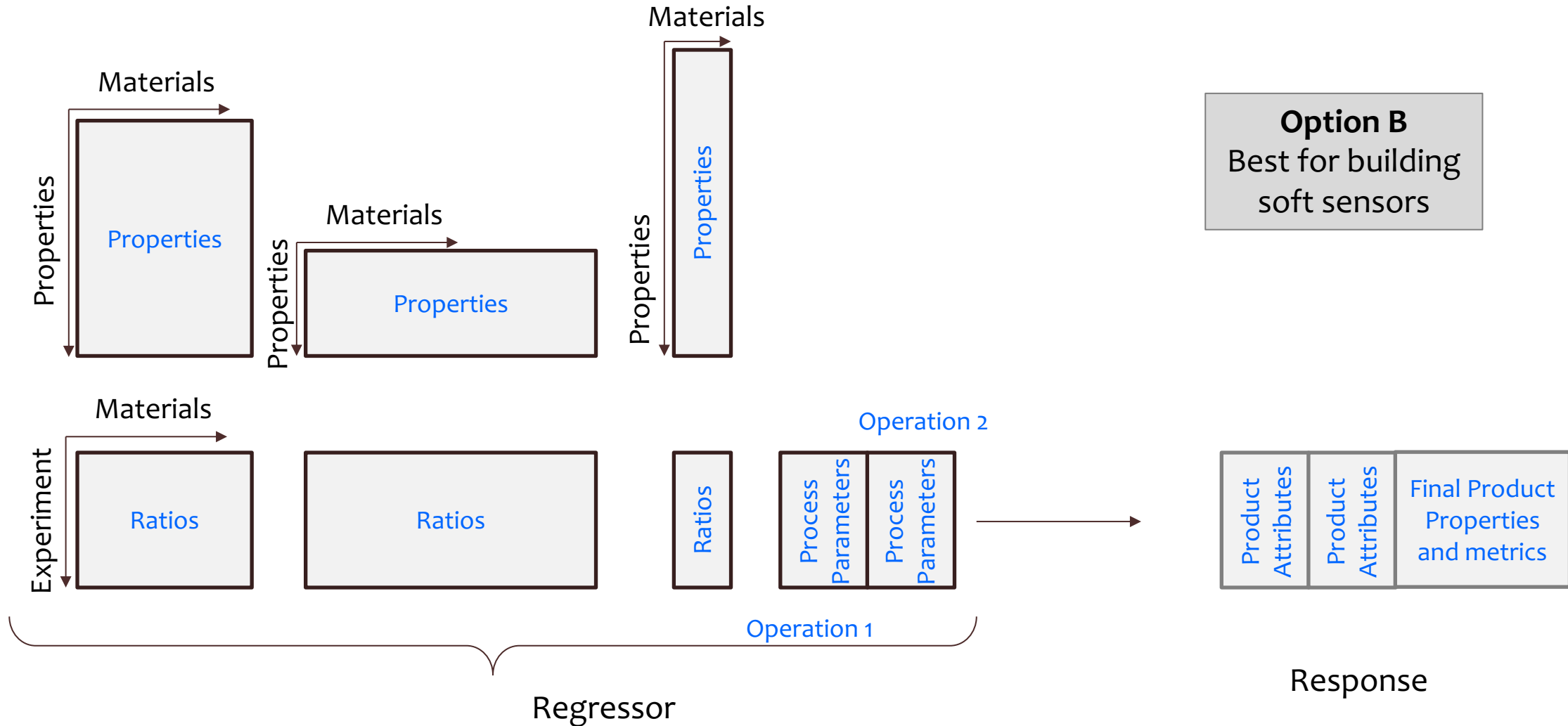
- Product development data is complex



Formulation development



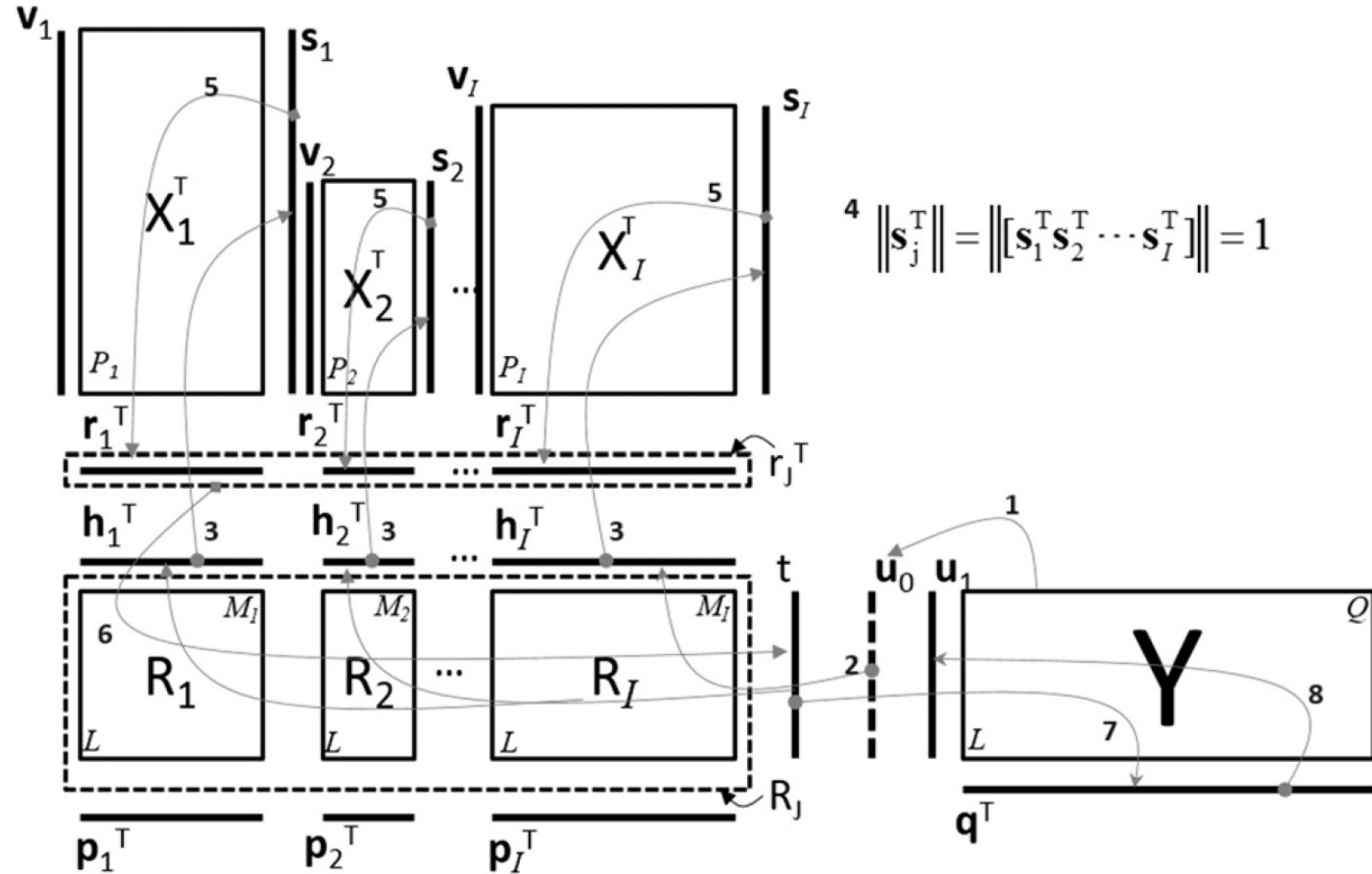
Formulation development



Formulation development

S. Garcia-Munoz / Chemometrics and Intelligent Laboratory Systems 133 (2014) 49–62

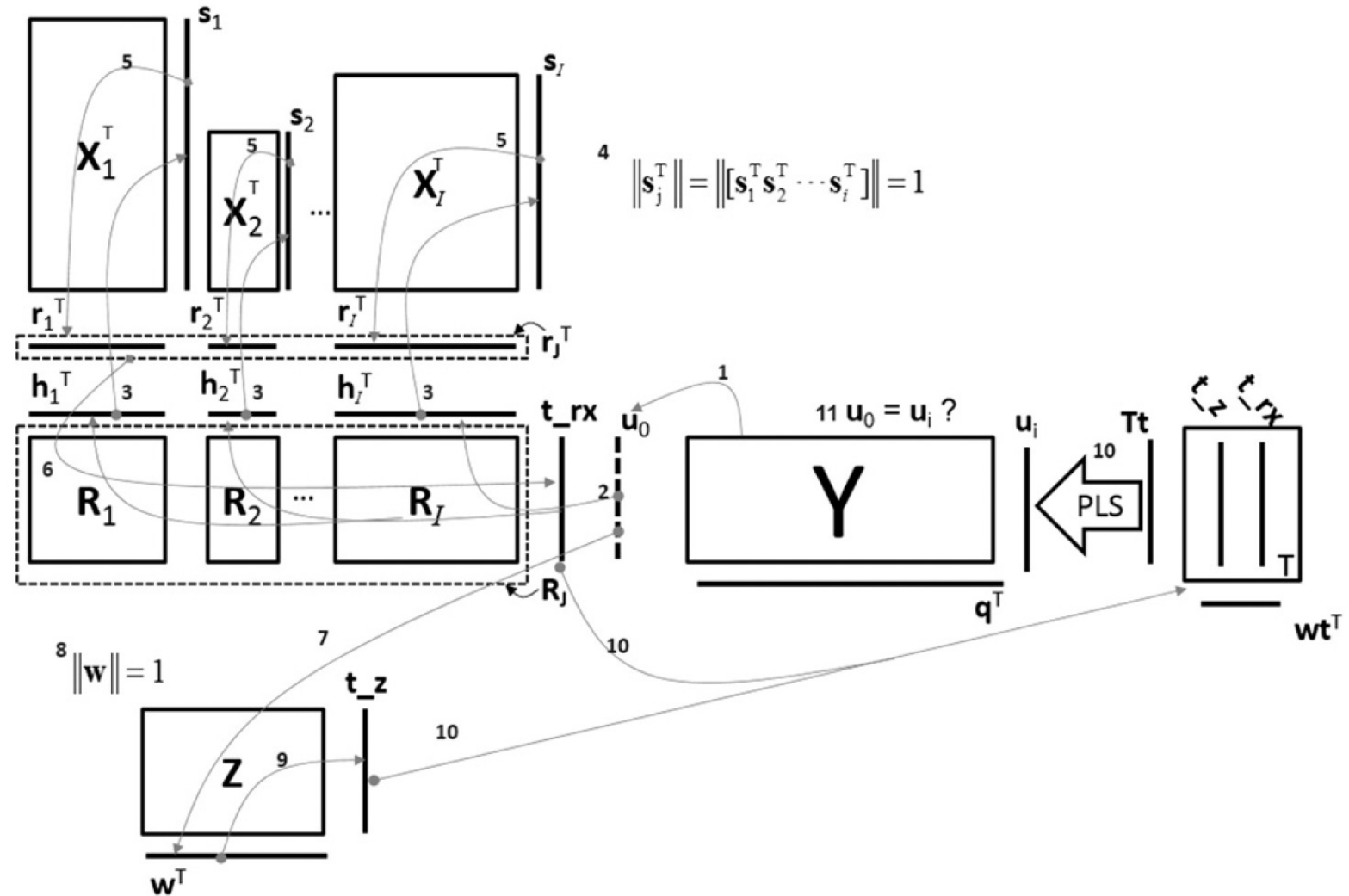
- JRPLS
designed to regress effect of materials characterized with different methods.



Formulation development

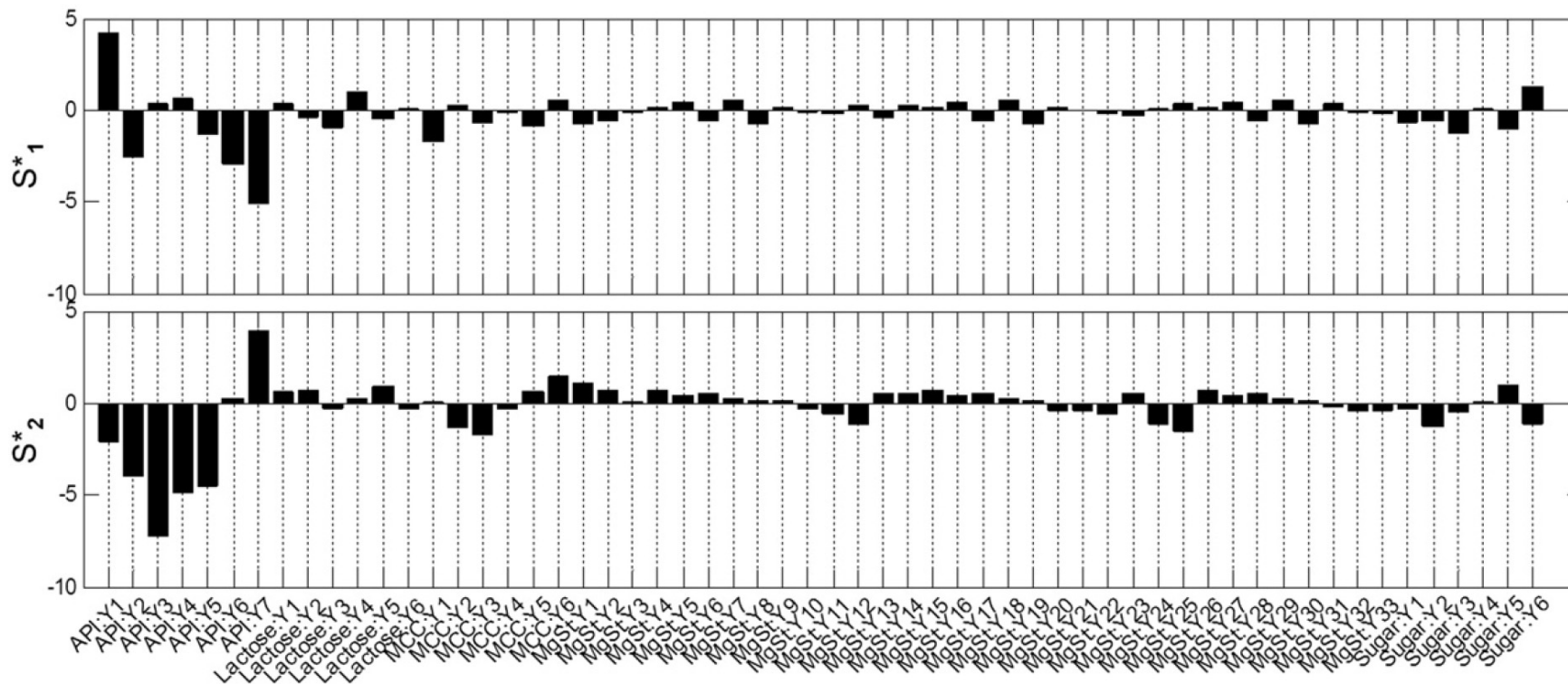
S. Garcia-Munoz / Chemometrics and Intelligent Laboratory Systems 133 (2014) 49–62

- TPLS
designed to
add process
information



Formulation development

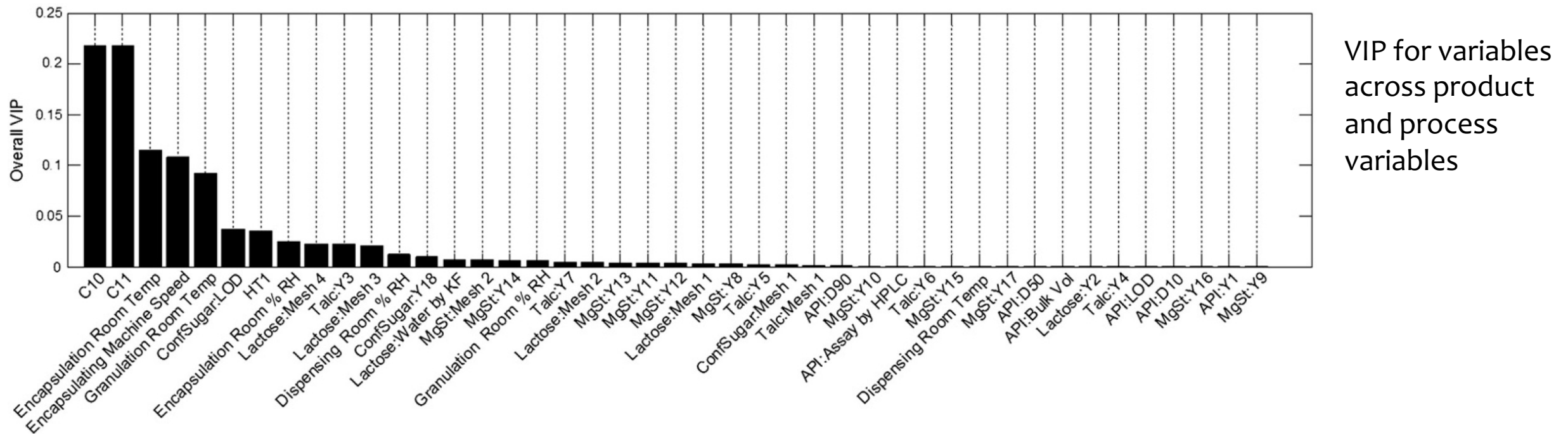
- The objective of using a TPLS or JRPLS model is **understanding**.



Loadings for
material properties
across materials

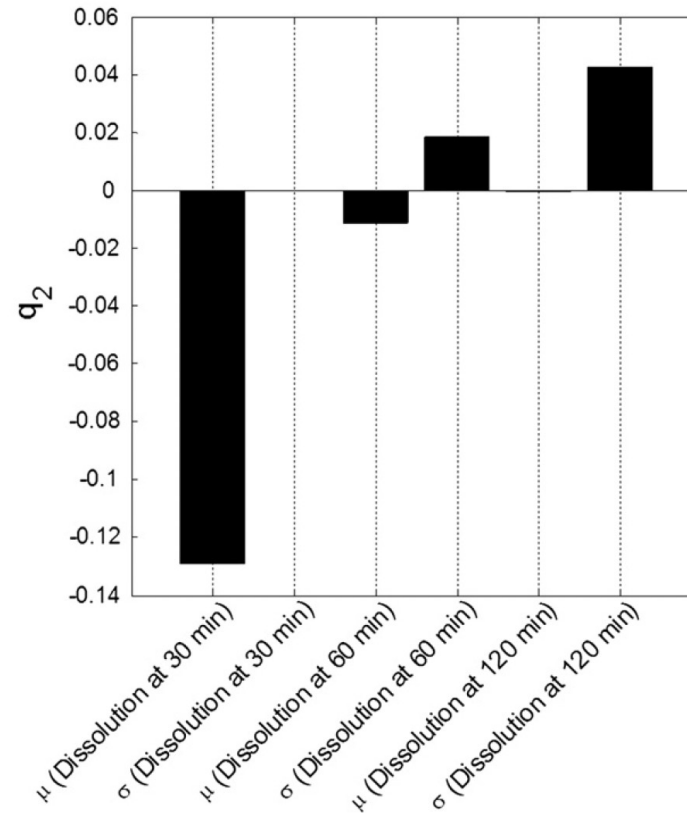
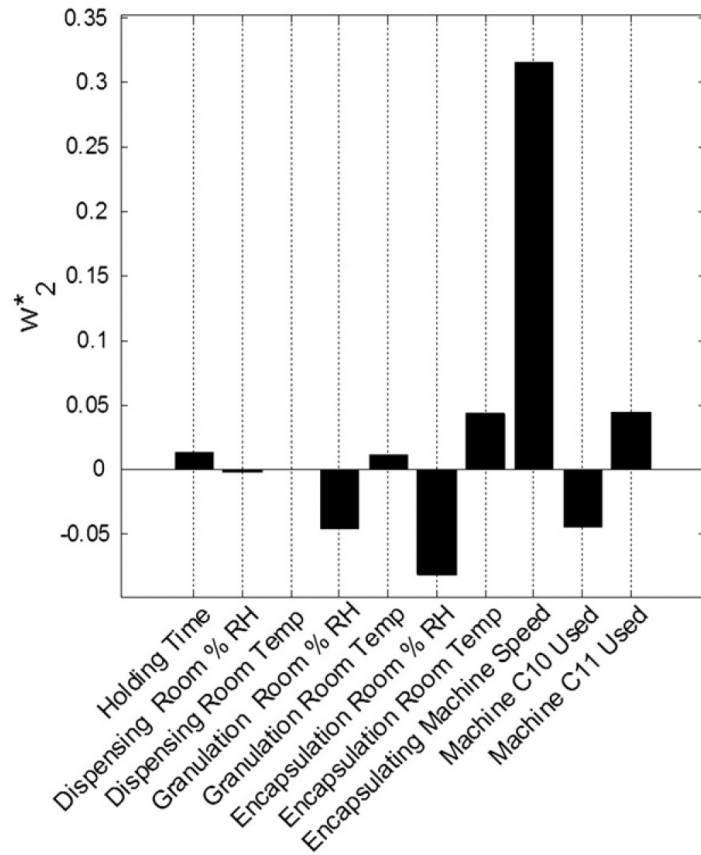
Formulation development

- The objective of using a TPLS or JRPLS model is **understanding**.



Formulation development

- The objective of using a TPLS or JRPLS model is **understanding**.

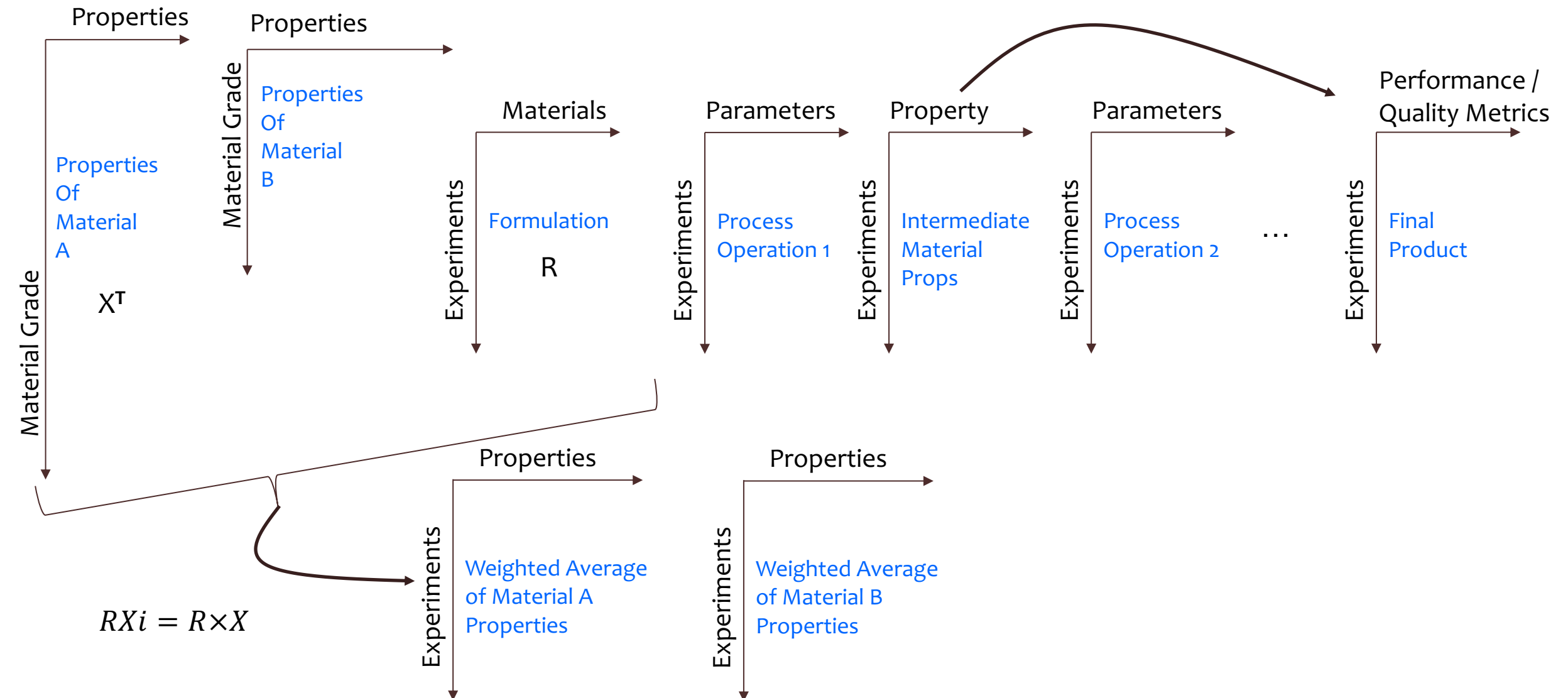


Loadings for
process and
Quality

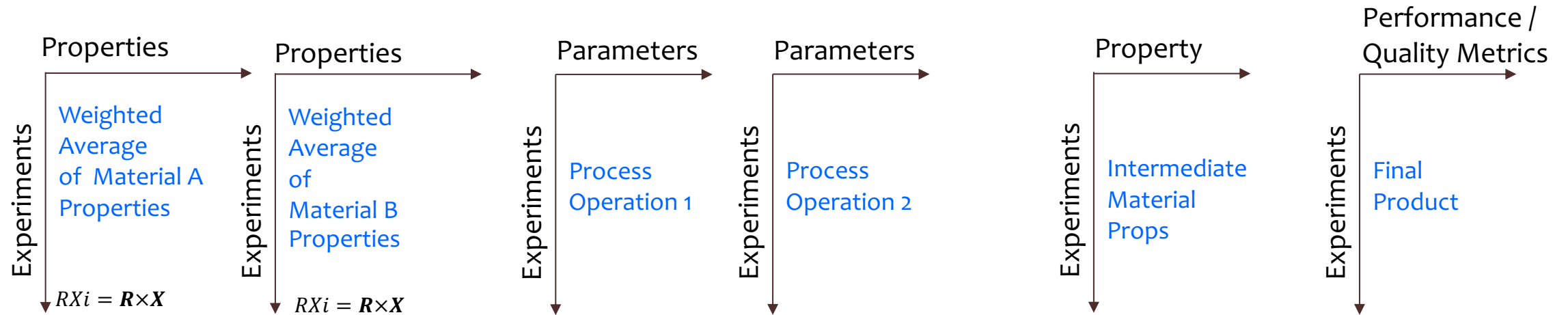
Formulation development

- A new product likely introduces a new material for which there is not experimental data yet.
- TPLS and JYPLS assign a **loading per material**.
- No material = No loading
- Without a loading we cannot predict
- Need a different approach

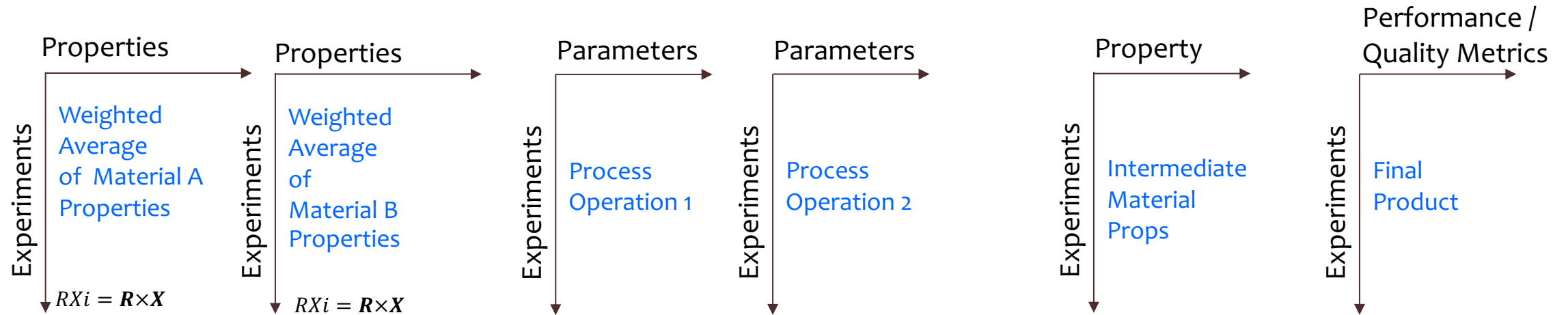
Formulation development



Formulation development

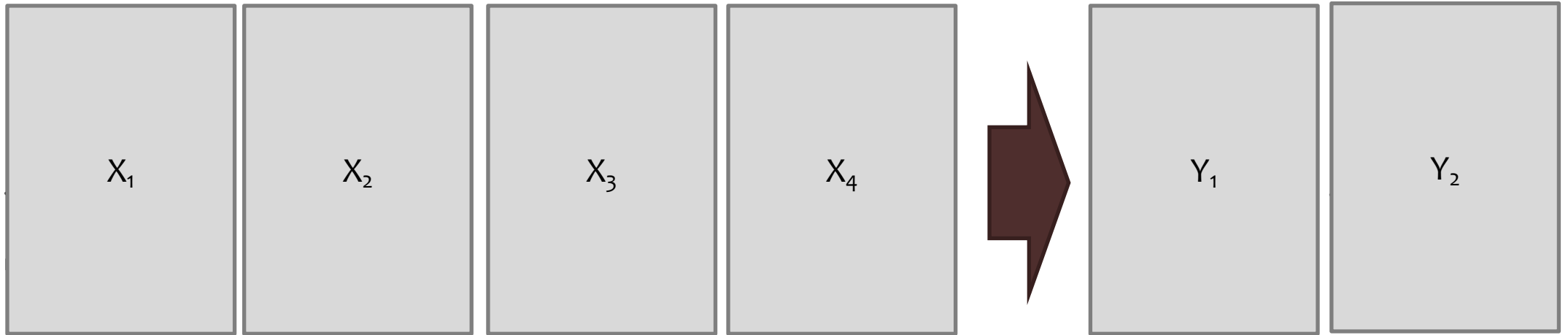


Formulation development



- This data can be regressed with a MBPLS model

Formulation development



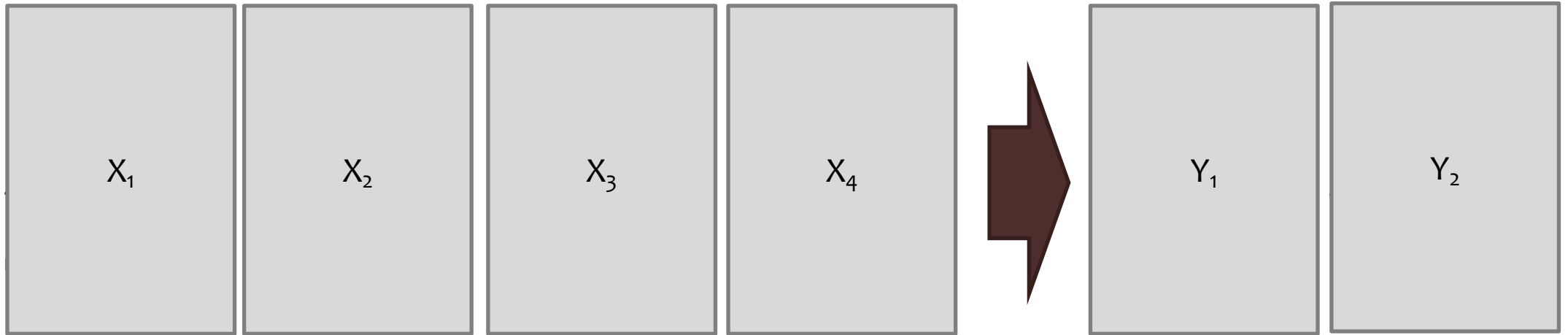
- This data can be regressed with a MBPLS model

Analysis of Multiblock and Hierarchical PCA and PLS Models - J. Chemometrics 12, 301–321 (1998)

Formulation development

- Although the MBPLS model does not explicitly model the relationships across material and product characteristics, it allows the exploration of new materials.
- Given that they are characterized with the same properties as their predecessors
- Loadings are assigned to properties not directly to materials.

Formulation development



Int. Mat. Propsi, $Y = f(RXi_1, RXi_2, \dots, RXi_m, Process_1, Process_2, \dots, Process_n, IMP_n)$

$$RXi_m = \underbrace{R_m \times X_m}$$

*This allows us to use this model
formulation to predict new
materials*

*Analysis of Multiblock and
Hierarchical PCA and PLS Models -
J. Chemometrics 12, 301–321 (1998)*

Formulation development

- Mining data from previous experiments.
 - Modeling data from previous products
 - **In-silico formulation development**
 - Surrogate selection for experimental design
 - Including material variability
 - When you have access to materials
 - When you don't

Formulation development

- Once we have a predictive model where

$$\text{Int. Mat. Prop.}, Y = f(RXi_1, RXi_2, \dots, RXi_m, Process_1, Process_2, \dots, Process_n, IMP_n)$$

$$RXi_m = R_m \times X_m$$

- The available inputs to the model are:
 - $R_m, Process_1, Process_2, \dots, Process_n$

 Choices of materials

Formulation development

- How to use such model in developing a new formulation:
 - A. Human driven trial and error: generate different choices of materials and ratios (R_i) and process conditions and examining the model predictions.
 - B. Use optimization methods.

Formulation development

- Optimization based formulation
 - Components of an optimization formulation
 1. **Objective:** Quantitative *scalar* that we seek to minimize or maximize
 2. **Degrees of freedom:** Variables that the optimizer will use to achieve its objective
 3. **Constraints:** Conditions that the optimal solution must comply with ($=, \geq$ *or* \leq *statements*)

Formulation development

- Optimization based formulation

- Illustrative Example

1. **Objective:** maximize dissolution at 30 min
2. **Degrees of freedom:** Choice of disintegrant and lubricant and percentages in formula and tablet press conditions.
3. **Constraints:**
 1. The Model [*this is what relates the df with the obj*]
 2. Min. hardness \leq Tablet hardness \leq Max. hardness
 3. Tablet Weight RSD $\leq 2\%$
 4. Formulation needs to add up to 100%

Formulation development

- Optimization based formulation
 - How do optimizers work?
 - Gradient based: will use derivatives (or approximation of the derivatives) of the objective function with respect to the degrees of freedom to find the optimal solution.
 - Blind search (popular with ML): Use of extensive sampling to search the solution space and find a better solution than the initial guess.

Formulation development

- Optimization based formulation
 - If there are multiple objectives
 - One solution is to use the sum of the weighted objectives
 - The mathematical formulation of the problem is very important
 - “Choosing materials” is much better when binary variables are involved in the formulation
 - Use realistic constraints

Formulation development

- Actual example from Computers and Chemical Engineering 60 (2014) 396– 402

$$\min \left(\sum_n (\hat{y}_i(n) - y_i^{\text{target}})^2 \right)$$

s.t.

$$\hat{\mathbf{y}}(n) = \mathbf{Q}\boldsymbol{\tau}_{\text{new}}(n)$$

$$\boldsymbol{\tau}_{\text{new}}(n) = \mathbf{W}^{*T} [\mathbf{z}^T(n) \mathbf{r} \mathbf{x} \mathbf{i}^T(n)]^T$$

$$\mathbf{r} \mathbf{x} \mathbf{i}^T(n) = [\mathbf{r} \mathbf{x} \mathbf{i}_{\text{api}}^T(n) \mathbf{r} \mathbf{x} \mathbf{i}_{\text{ex1}}^T(n) \mathbf{r} \mathbf{x} \mathbf{i}_{\text{ex2}}^T(n) \mathbf{r} \mathbf{x} \mathbf{i}_{\text{ex3}}^T(n) \mathbf{r} \mathbf{x} \mathbf{i}_{\text{ex4}}^T(n)]$$

$$\text{spe}_X(n) = \sum ([\mathbf{z}^T(n) \mathbf{r} \mathbf{x} \mathbf{i}^T(n)]^T - \mathbf{P} \boldsymbol{\tau}_{\text{new}}(n))^2$$

$$\text{Hot } T^2(n) = \sum_{a=1}^A \left(\frac{\tau_{\text{new}a}(n)}{\sigma_a} \right)^2$$

$$\text{spe}_X(n) \leq \text{spe_upper_limit}$$

$$\text{Hot } T^2(n) \leq \text{hot2_upper_limit}$$

$$z_l(n) \leq z_max_l$$

$$z_l(n) \geq z_min_l$$

$$z_l(n) = z_fixed_l$$

$$\hat{y}_i(n) \leq y_max_i$$

$$\hat{y}_i(n) \geq y_min_i$$

$$\forall j = [\text{api}, \text{ex1}, \text{ex2}, \text{ex3}, \text{ex4}]$$

$$\mathbf{r} \mathbf{x} \mathbf{i}_j(p_j, n) = \sum_{m_j} \mathbf{r}_j(m_j, n) \mathbf{x}_j(p_j, m_j)$$

$$\mathbf{r}_j(m_j, n) \leq \mathbf{r} \mathbf{b} \mathbf{i} \mathbf{n} \mathbf{a} \mathbf{r} \mathbf{y}_j(m_j, n)$$

$$\sum_{m_j} \mathbf{r}_j(m_j, n) = 1$$

$$\mathbf{mass}_j(m_j, n) = \mathbf{r}_j(m_j, n) \times \text{mass_required}_j$$

$$\sum \mathbf{mass}(m_j, n) \leq \text{mass_available}(m_j)$$

$$\sum_{m_j} \mathbf{r} \mathbf{b} \mathbf{i} \mathbf{n} \mathbf{a} \mathbf{r} \mathbf{y}_j(m_j, n) \leq \text{max_num_lots_to_blend}_j$$

Formulation development

- Examples, references

- *International Journal of Pharmaceutics* 418 (2011) 235– 242
- *Ind. Eng. Chem. Res.* 2012, 51, 12886–12900
- *Ind. Eng. Chem. Res.* 2013, 52, 5934–5942
- *Ind. Eng. Chem. Res.* 2013, 52, 8260–8271
- *Computers and Chemical Engineering* 60 (2014) 396– 402
- *Chemical Engineering Research and Design* 92 (2014) 534–544

Formulation development

- Mining data from previous experiments.
 - Modeling data from previous products
 - In-silico formulation development
 - **Surrogate selection for experimental design**
 - Including material variability
 - When you have access to materials
 - When you don't

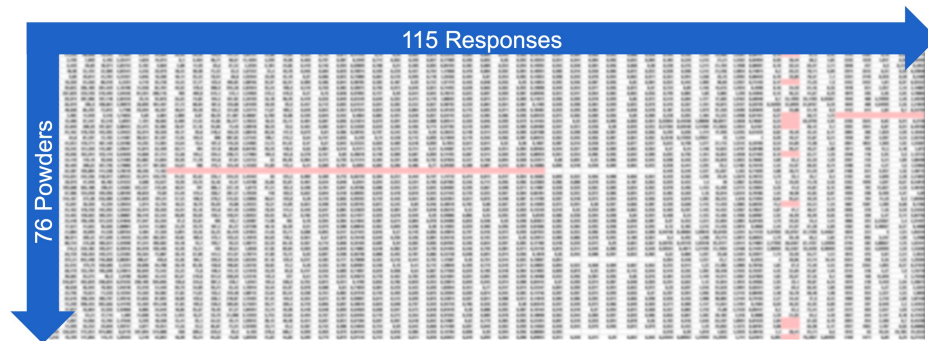
Formulation development

- **Surrogate selection:** Choose an alternative (more accessible, safe or cost effective) material that is similar to the drug to carry out development work.
- Great idea!
 - Define similar?
 - With respect to what ?
 - How similar is “similar enough” ?

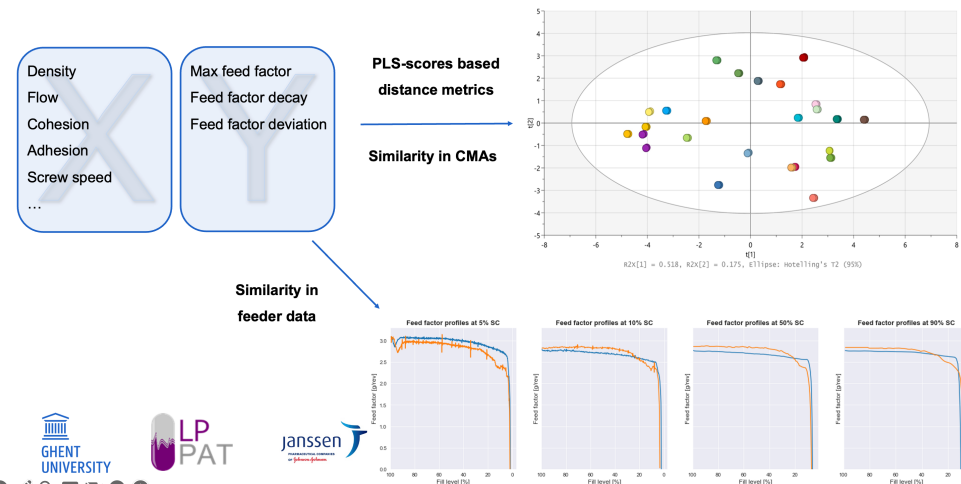
Formulation development

- All interesting questions being explored by the research group of Prof. Thomas DeBeer @Ghent University.

MATERIALS AND METHODS



MATERIALS AND METHODS



Formulation development

- Mining data from previous experiments.
 - Modeling data from previous products
 - In-silico formulation development
 - Surrogate selection for experimental design
 - Including material variability
 - When you have access to materials
 - When you don't

Formulation development

- Material variability is perhaps one of the most challenging risks to address at the R&D stage.
 - Not many lots are consumed in development
 - Vendors are getting involved and greatly helping their customers address this question.

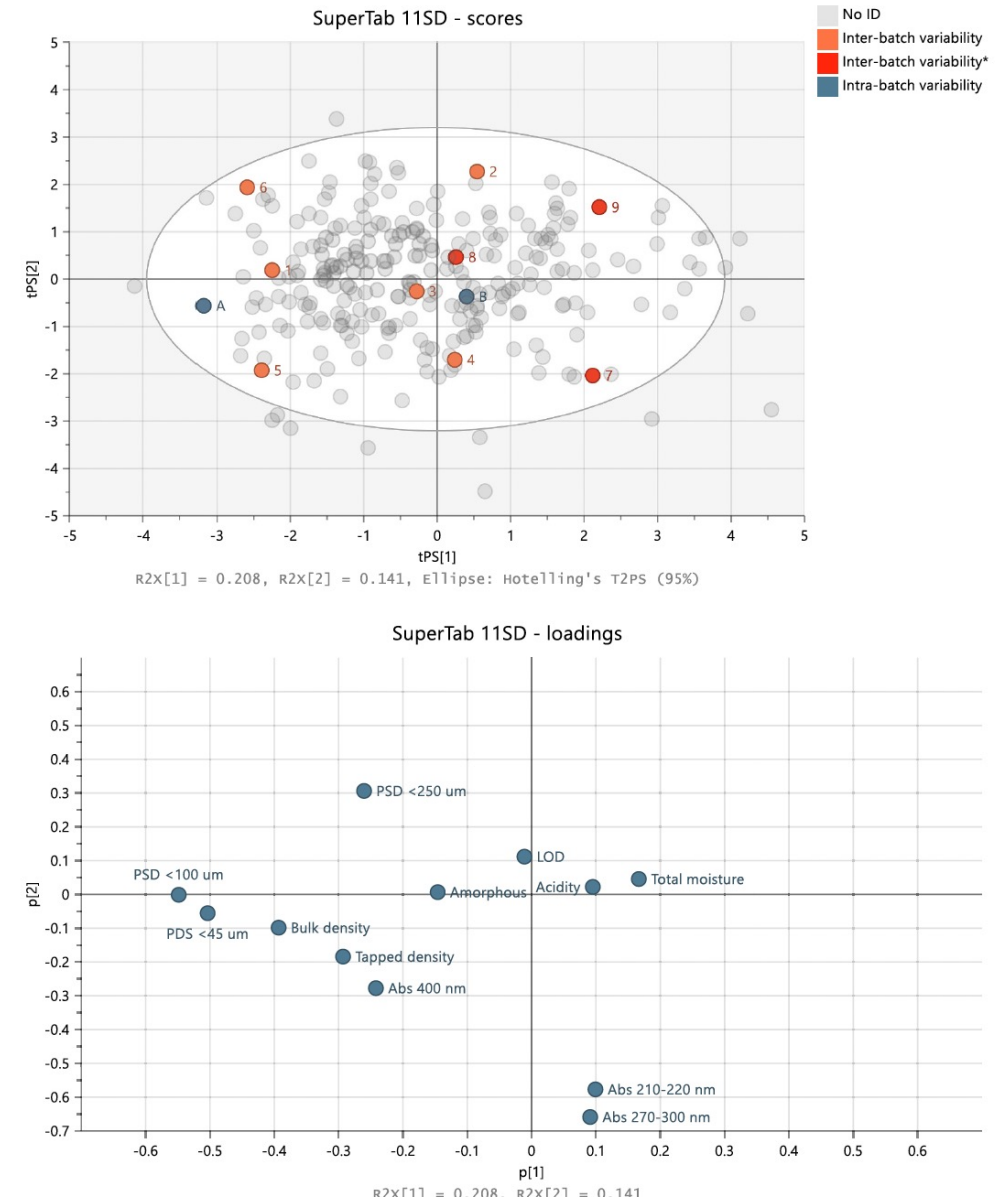
Formulation development

- Use PCA to summarize material properties.
- Use scores to help select what areas of the variation need to be explored.

Powder Technology 409 (2022) 117776

DFE Pharma

20th NPTE Conference - Tokyo 2023



Formulation development

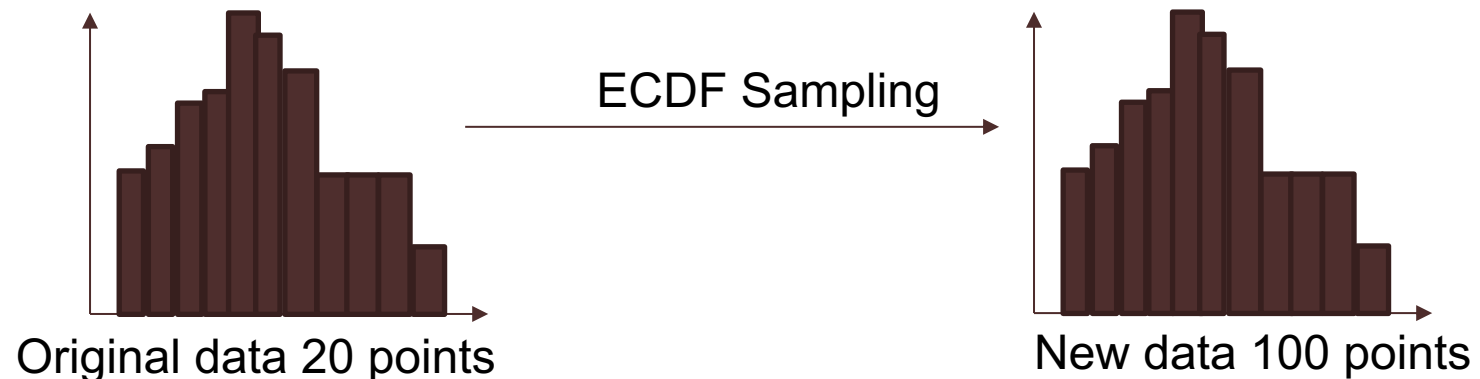
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Formulation development

- Problem: We don't have enough replicas to well represent variability.
- Objective: Create credible clones of the available data preserving the existing correlation across variables and the uncertainty distributions.

Formulation development

- Cloning data using PCA and ECDF
- The Empirical Cumulative Distribution Function can be used to draw new samples from a population while preserving the population distribution.

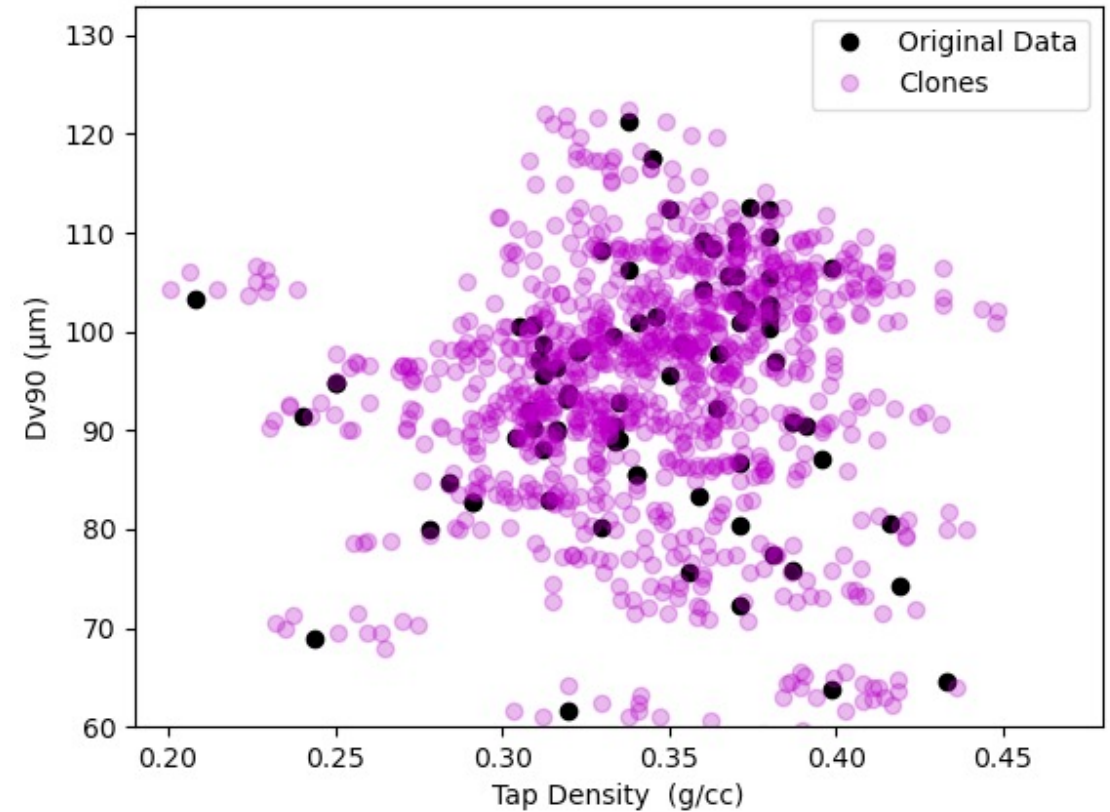
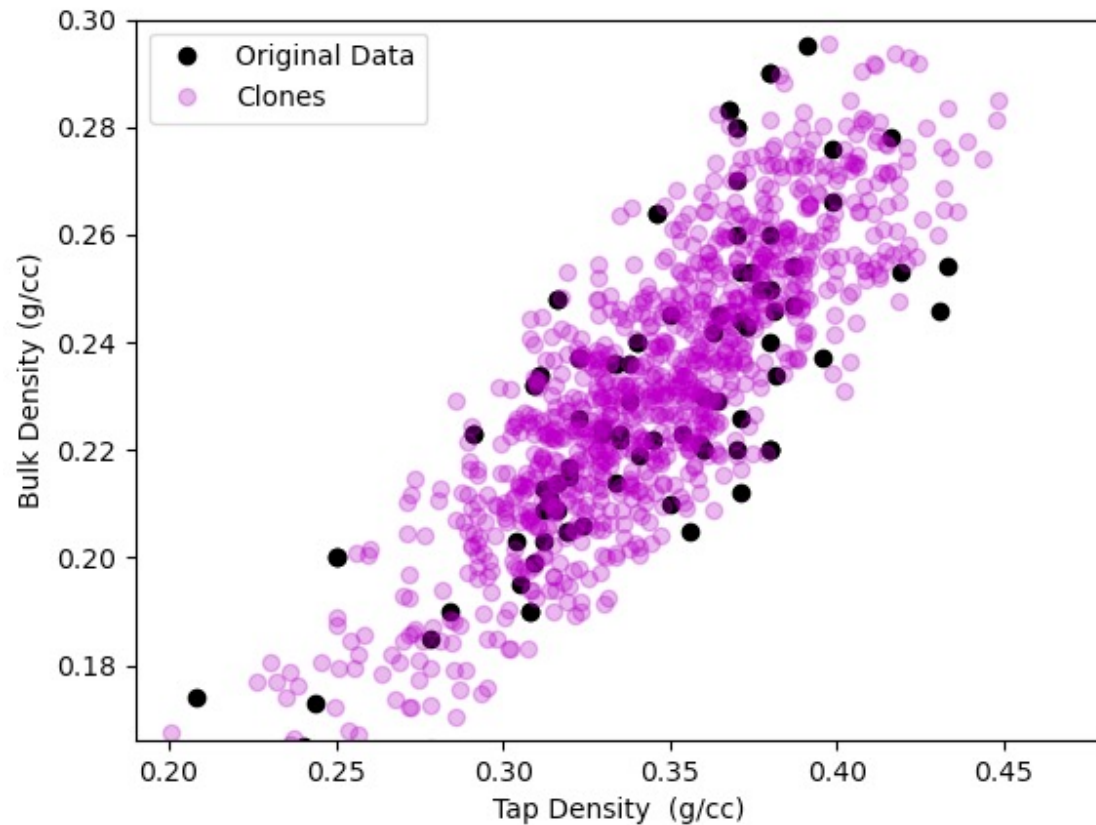


Formulation development

1. Perform PCA on X
2. Create a copy of the reconstructed portion of $\hat{X} = TP^T$
3. To each column of \hat{X} add new residuals, sampled from the population of the original residuals using ECDF.
4. Ready.

Formulation development

- Example



Agenda

- Formulation development
- **Process development**
- Process de-risking and transfer
- Process Monitoring
 - MSPC for fault detection and isolation

Process Development

- Computational tools:
 - Modeling of feeders
 - Modeling of mixing extent and residence time distribution (RTD)

Modeling of loss in weight feeders

- Addressed in plenty of papers in literature:
 - Yu, Y. *Theoretical modelling and experimental investigation of the performance of screw feeders*. Ph.D. Thesis, University of Wollongong, 1997.
 - Boukouvala et al., *Computers and Chemical Engineering* 42 (2012) 30–47
 - Rogers et al. *Ind. Eng. Chem. Res.* 2014, 53, 13, 5128–5147
 - Jia, J. *Pharm. Innovation* 2009, 4, 174–186.
 - Bascone, *Industrial & Engineering Chemistry Research*, 59(14), pp.6650-6661.
 - Johnson, *International Journal of Pharmaceutics*, 621, p.121776.

Modeling of loss in weight feeders

- Most recent paper from RCPE
 - Studied the process with multiple modeling approaches.

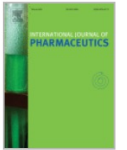
“Even a very simple model that assumes perfect mixing inside the hopper is a decent approximation of the real dynamics. This model works well for the given twin-screw feeder geometry because the agitator mixes a large portion of the material inside the feeder. Different feeder designs agitate different portions of the hold-up mass and thus have different material survival functions. The perfect mixing model is not a universal law across all feeders.”



International Journal of Pharmaceutics

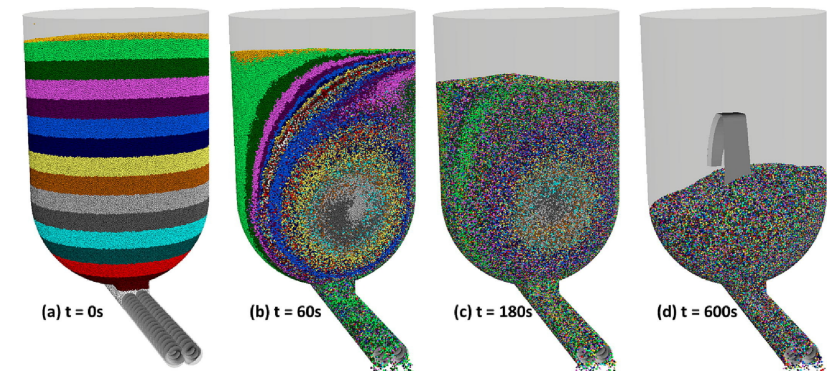
Available online 2 April 2023, 122915

In Press, Journal Pre-proof ? What's this? ➤



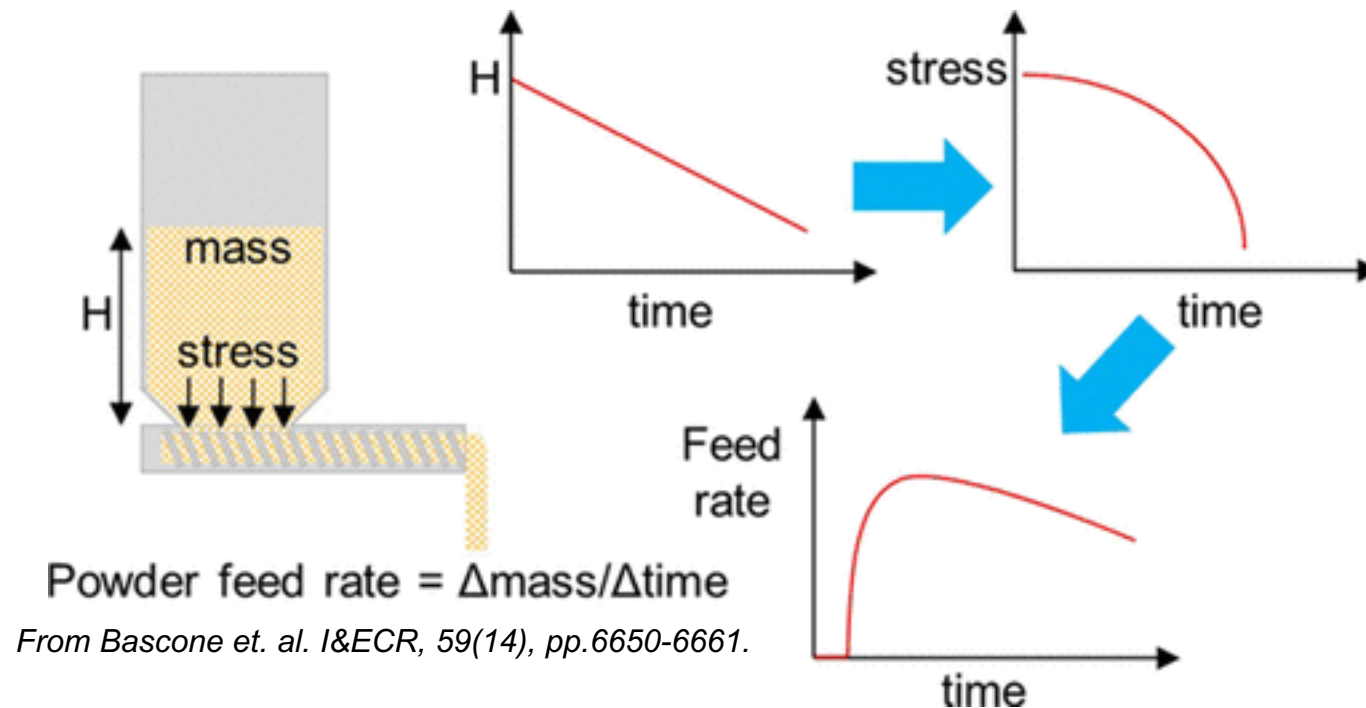
A DEM Model to Evaluate Refill Strategies of a Twin-Screw Feeder

Peter Toson^a ✉, Johannes G. Khinast^{a b} ✉



Modeling of loss in weight feeders

- Mixing behavior apart, the inherent challenge in modeling loss in weight feeders is estimating the densification of material in the base of the hopper as a function of hold up.

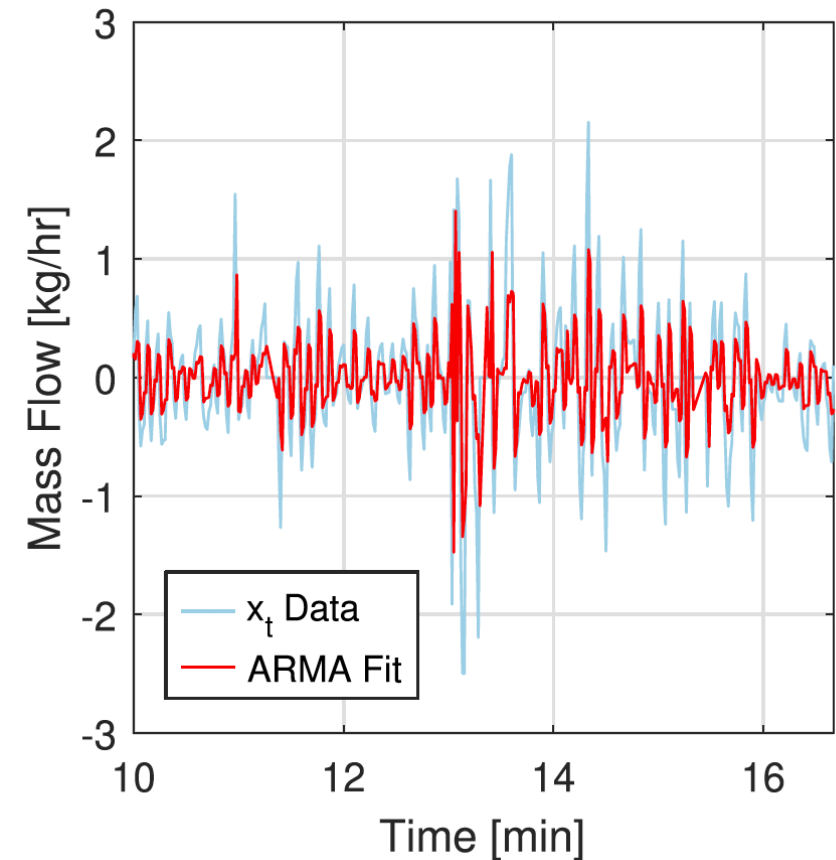


Modeling of loss in weight feeders

- Some work has been done to predict this relation through the estimation of the feed-factor from powder properties.
 - Bostijn, N.Int. J.Pharm. 2019, 557, 342–353.
 - Wang, Powder Technol. 2017,308, 135–148.

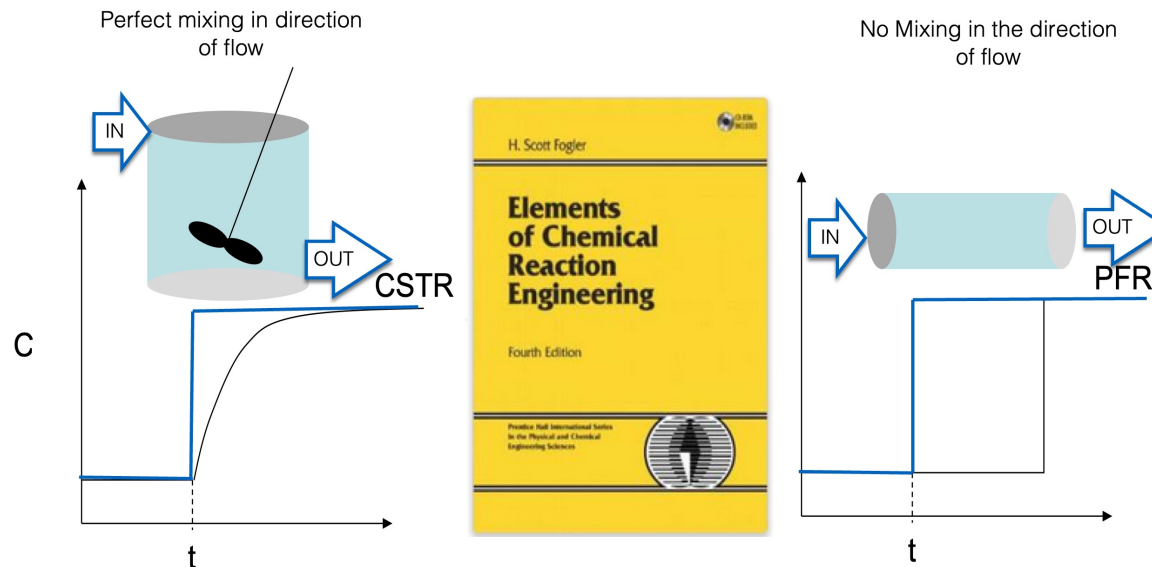
Modeling of loss in weight feeders

- Others have focused on characterizing and predicting the stochastic behavior of a feeder in gravimetric mode.
- More work is needed in this area to generate a **truly forward-predictive model** of the feeding behavior expected for a new material



Modeling the Residence Time Distribution

- Very large amount of publications in this topic.
- Application of reaction engineering concepts to determine the extent of mixing along the direction of flow of a powder.



Modeling the Residence Time Distribution

- Two modeling approaches:
 - White box model
 - Calculate the speed of transit from geometry and linear speed, which implies the knowledge of a density [difficult for powders]
 - Black box model:
 - Fit the RTD curve to time explicit functions

Modeling the Residence Time Distribution

- Two modeling approaches:

- White box model

García-Muñoz, S. AIChE Journal, 64(2), pp.511-525.

- Black box model [most recent development]:

Toson and Doshi, Processes 2019, 7, 615

$$\text{RTD}_{n,\tau}(t) = \frac{t^{n-1}}{\Gamma(n)} \cdot \left(\frac{n}{\tau}\right)^n \cdot \exp\left\{-\frac{t}{\tau}\right\}$$

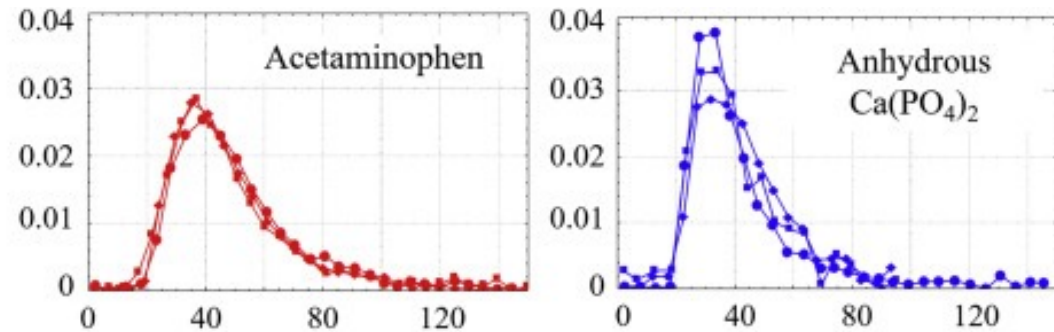
Modeling the Residence Time Distribution

- Either approach requires data!
- Two different experiments can be done

- Tracer experiment:

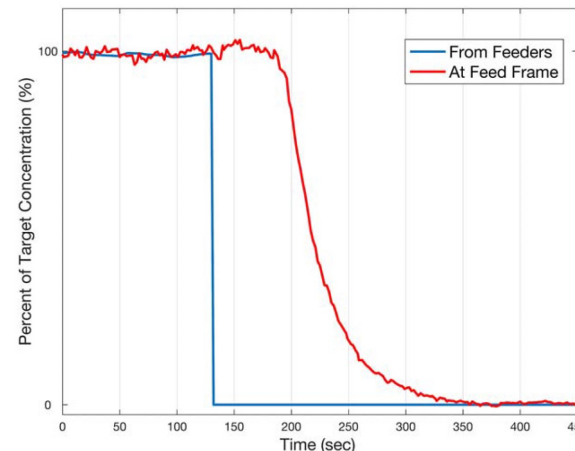
Care is needed to select the proper tracer

From Escotet-Espinosa et.al., Powder Tech. (342),15,744-763,2019



- Step experiment:

Cost effective and informative



From Garcia-Munoz et al., AIChE J. (64),2,516,2018

Modeling the Residence Time Distribution

- The RTD model can then produce a funnel plot

- Most Funnel plots are built as a function of fed **concentration disturbances**.
- Behavior not 100% symmetric when using a white box model.
- Behavior is 100% symmetrical with black box models

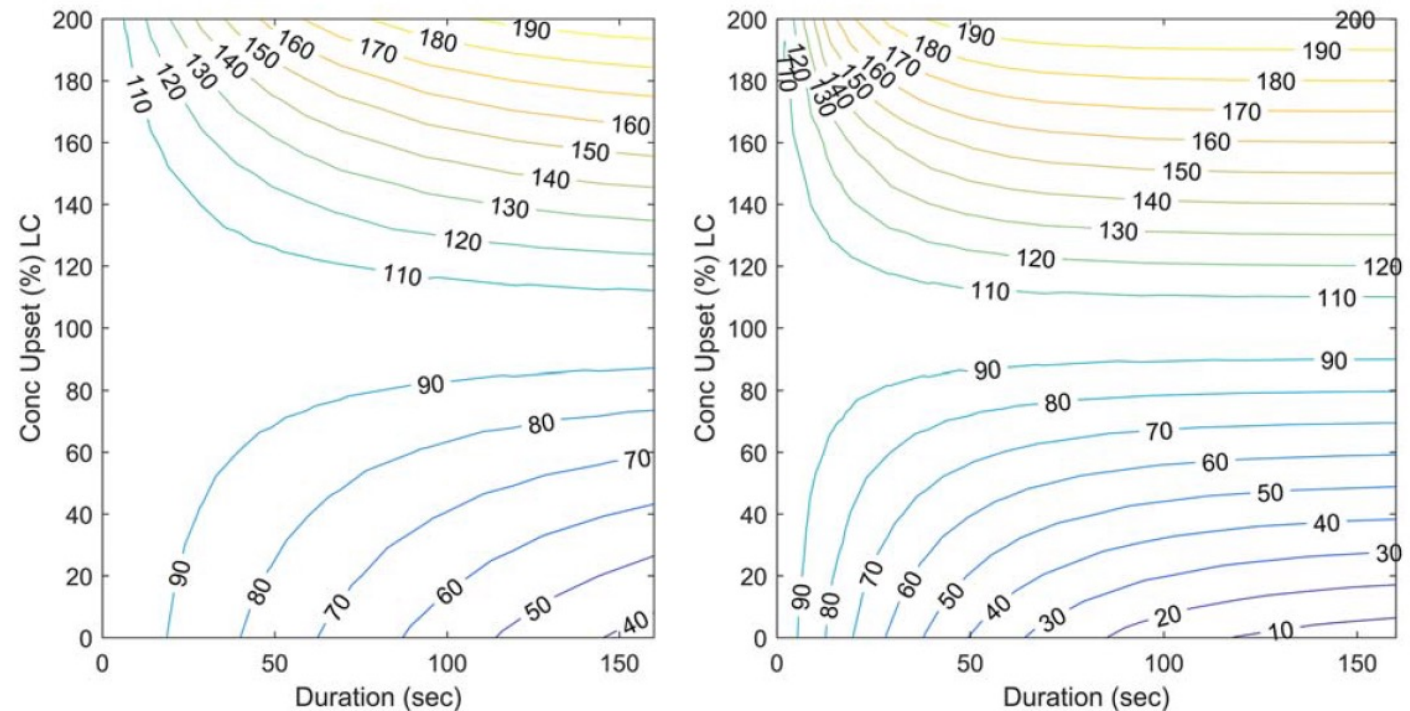
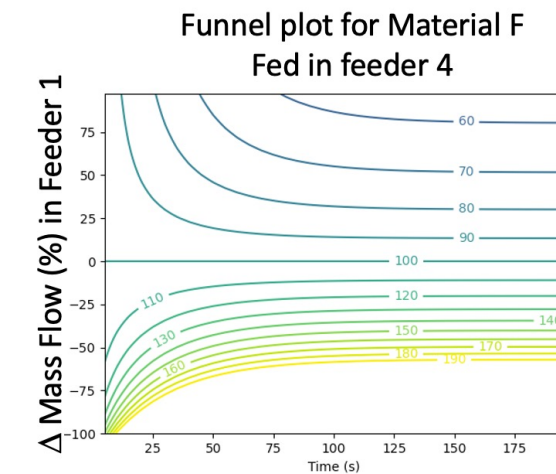
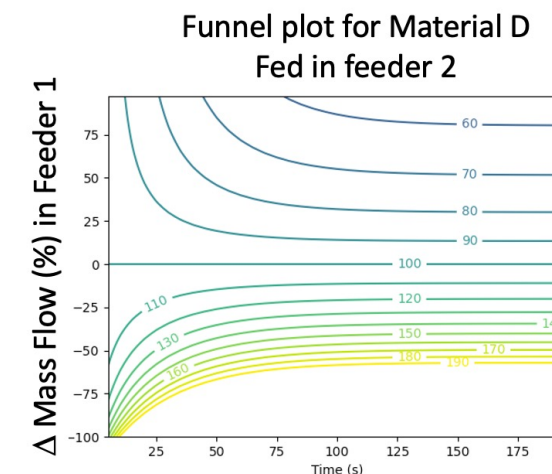
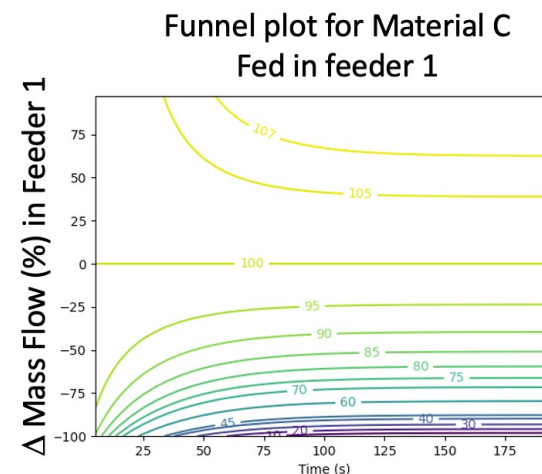
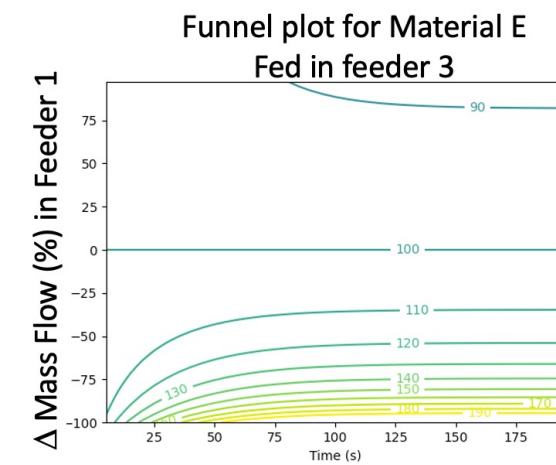
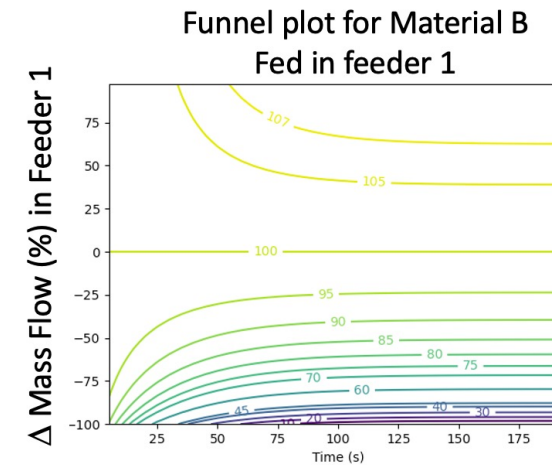
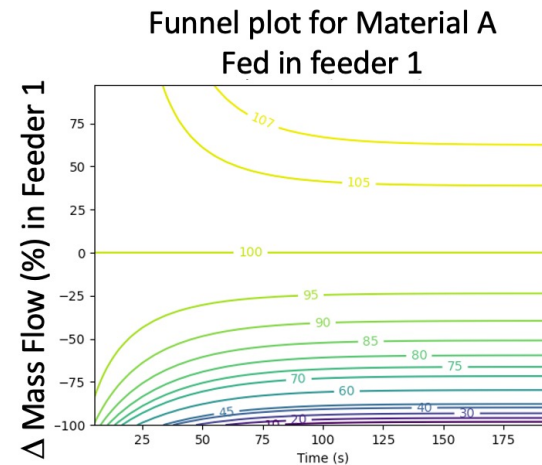


Figure 13. Two funnel plots, for low throughput (left) and high throughput (right).

Modeling the Residence Time Distribution

- Funnel plots as a function of mass flow disturbance

- FP are non-linear.
- and dependent on relative mass-flows from one feeder to the other.
- Feeder with greatest mass-flow has largest effect.
- Example assumes all other feeders are kept at target.



Modeling the Residence Time Distribution

- Uses:
 - Disturbance detection and control.
 - Genealogy tracking for incoming material.

Agenda

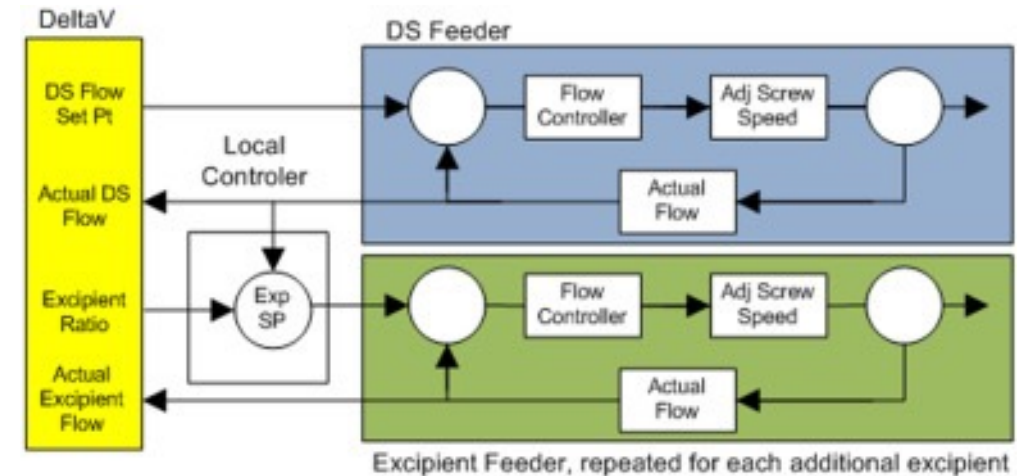
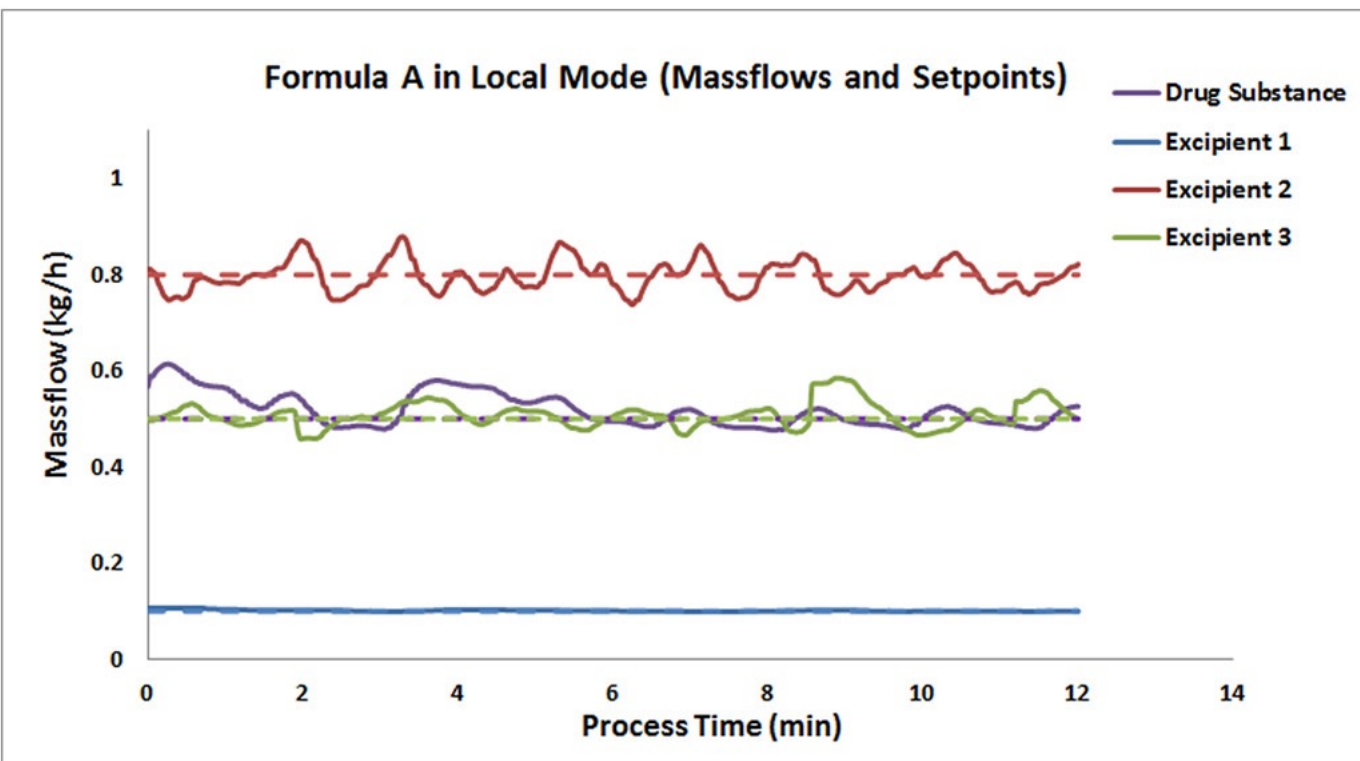
- Formulation development
- Process development
- **Process de-risking and transfer**
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 - MSPC for fault detection and isolation

Process de-risk and transfer

- Areas of risk are very few:
 - Main potential source of disturbances is the dispensing of materials [feeder performance]
- Mitigation strategies
 - Use ratio control
 - Quantitation of disturbance effects

Process de-risk and transfer

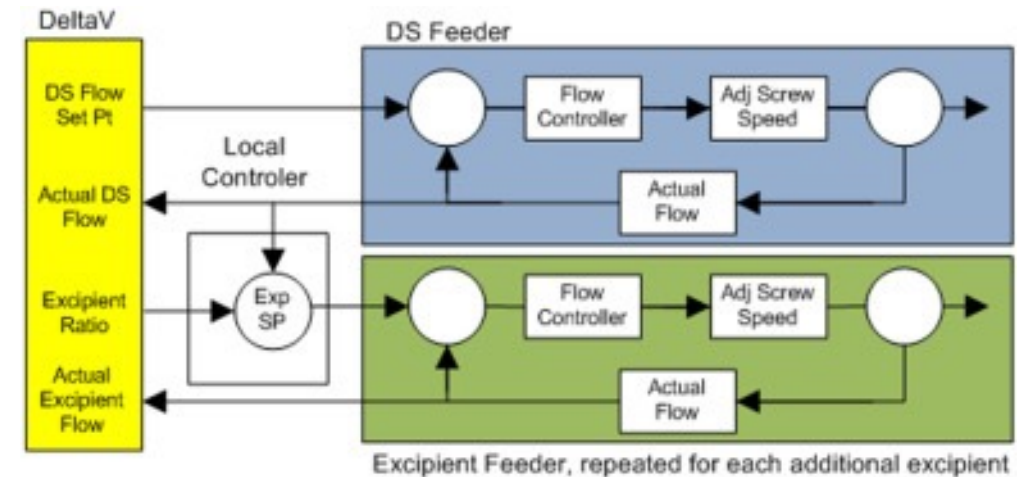
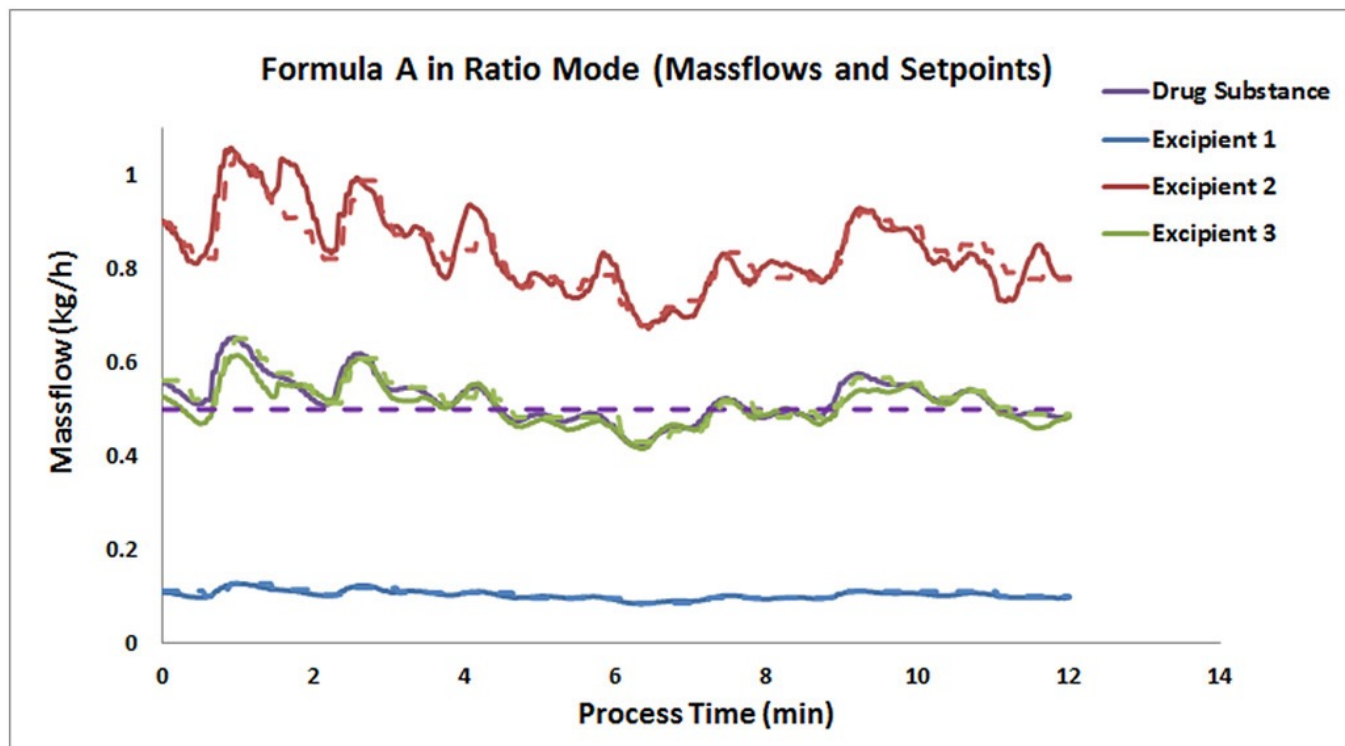
- Ratio-control ensures concentration at the cost of small variation in mass-flow.



From Hanson, Powder Tech.(331),15,236-243,2018

Process de-risk and transfer

- Ratio-control ensures concentration at the cost of small variation in mass-flow.



From Hanson, Powder Tech.(331),15,236-243,2018

Process de-risk and transfer

- Quantitation of disturbance effects
 - Parse though data acquired during development and clinical manufacture.
 - Characterize all [even small] disturbances from set-point.
 - Place disturbances in funnel plot.

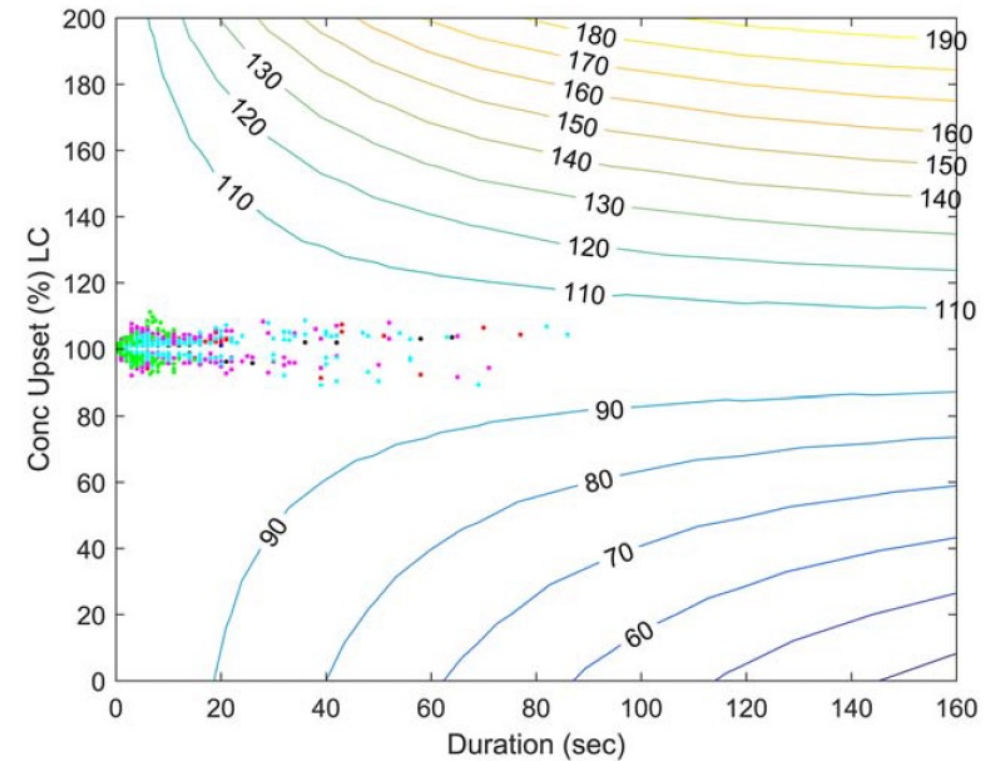


Figure 14. Funnel plot overlay with all events (i.e., disturbances) from historical data supporting process development.

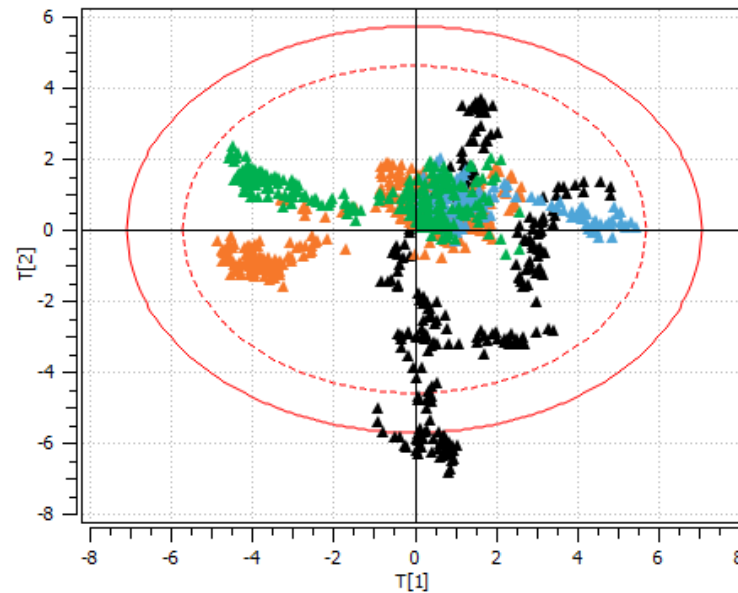
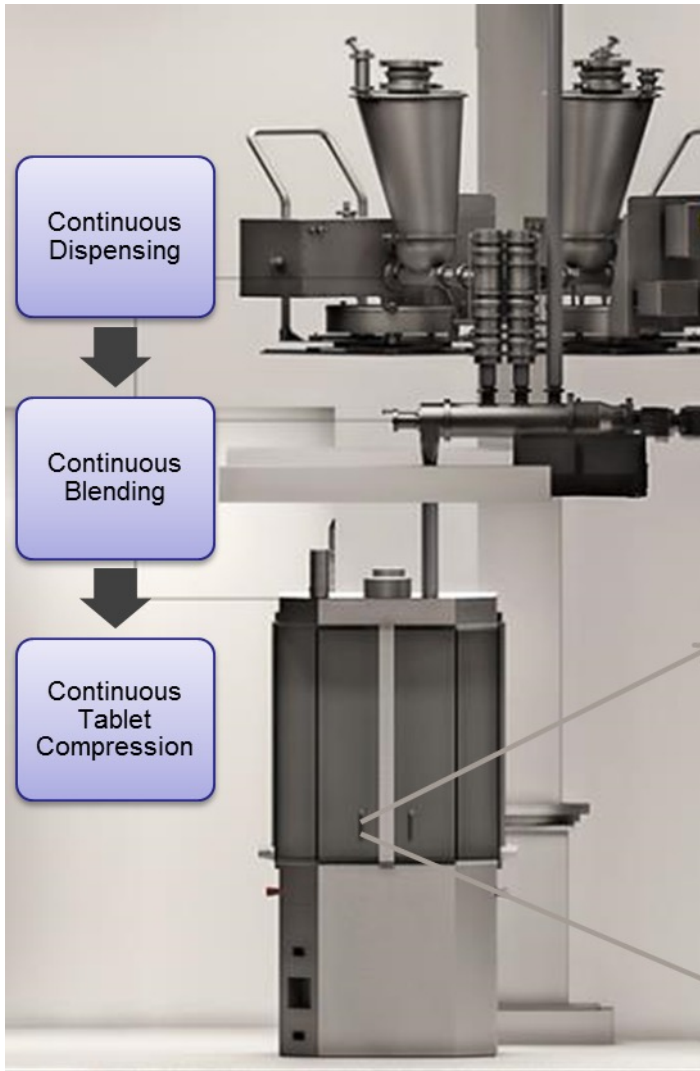
Agenda

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- **Process Monitoring**
 - **MSPC for fault detection and isolation**

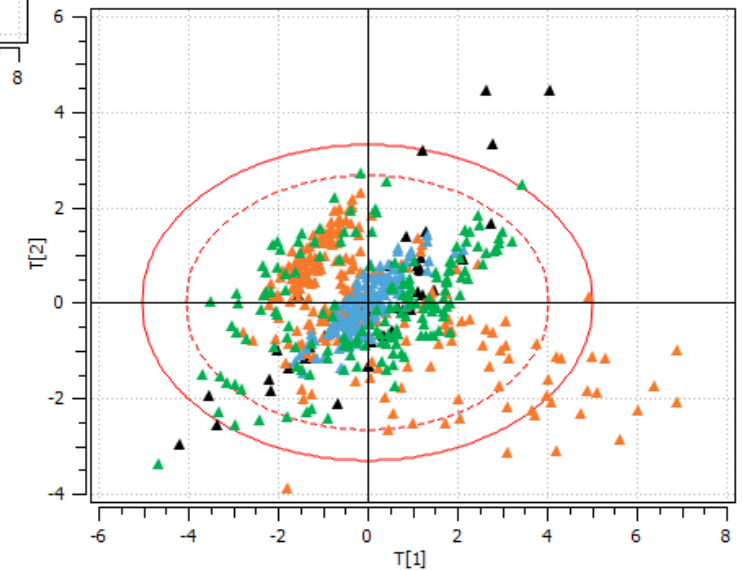
Process Monitoring - MSPC

- Multivariate Statistical Process Control (MSPC) is an established method for monitoring and fault detection.
- Established in 1994.
- Plenty of software available commercially.
- Mostly implemented in bio-pharmaceutical processing.

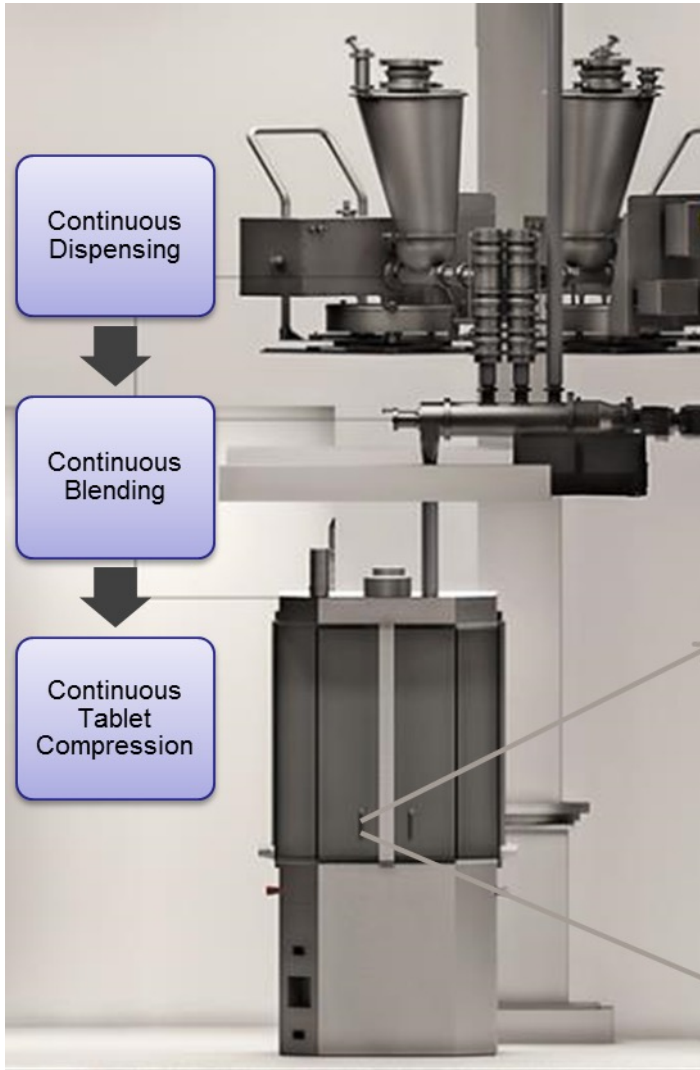
Process Monitoring - MSPC



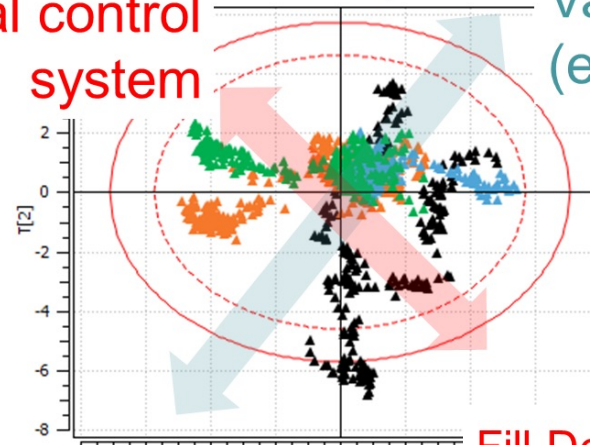
Model built with data from 6 different molecules



Process Monitoring - MSPC



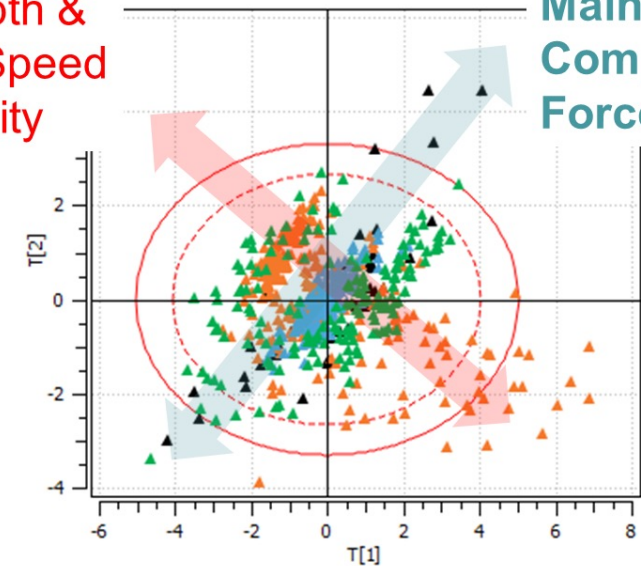
Variability in
internal control
system



Mass Flow
Variability
(e.g. Start up)

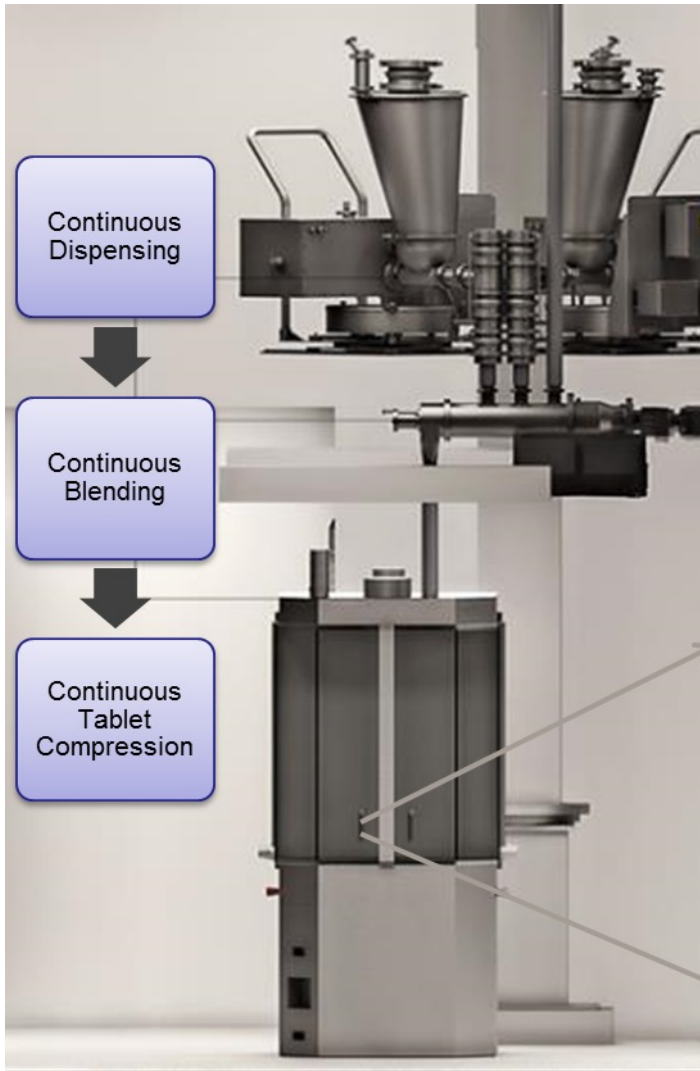
Model built with data from 6
different molecules

Fill Depth &
Rotor Speed
Variability



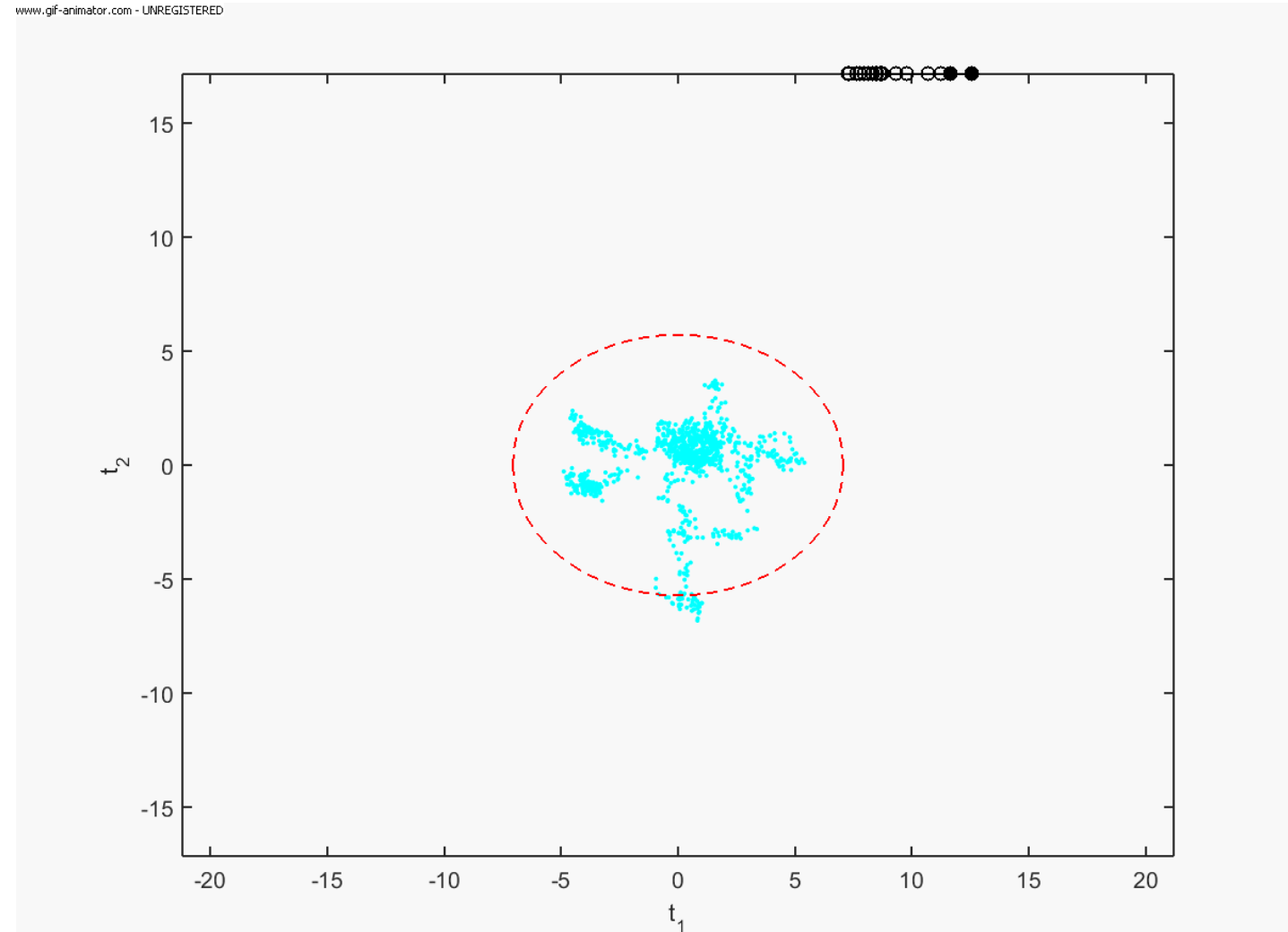
Main & Pre-
Compression
Force Variability

Process Monitoring - MSPC

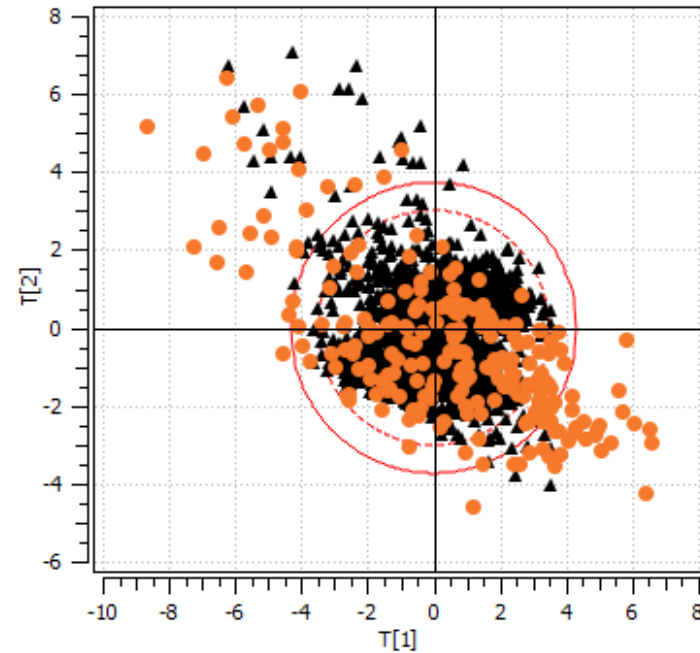
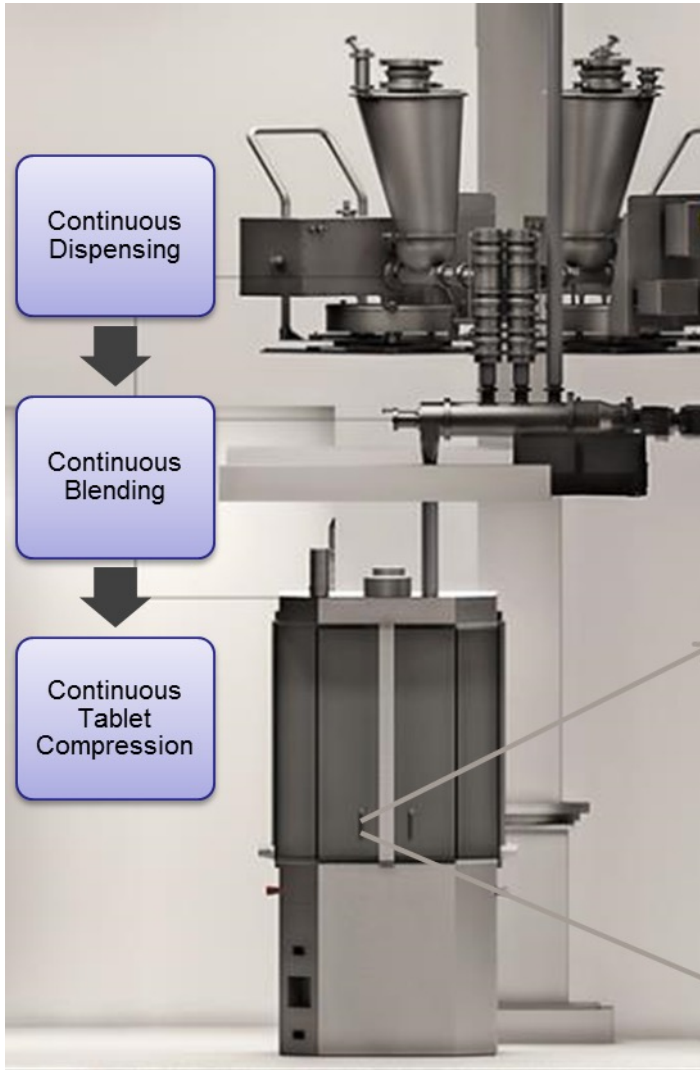


Monitoring the Startup of the Feeders

Model built with data from 6 different molecules

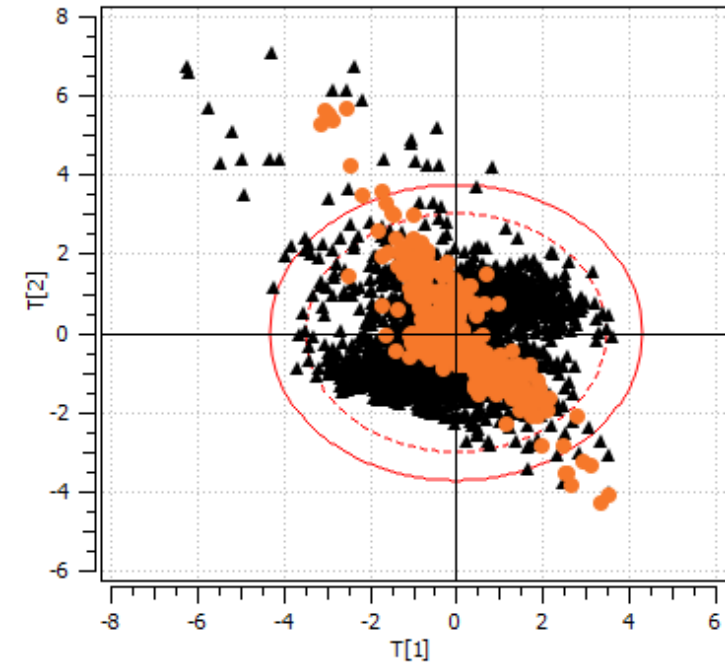


Process Monitoring - MSPC



Same API
different formula

Model built with data from 6
different molecules



Different API and
different formula

Process Monitoring - MSPC

- Details that need close attention.
 - Management of lags
 - Variables are sampled throughout the train and the interactions are not instantaneous (hence RTD)
 - A lagged model runs at the slowest dynamics
 - No time to react
 - A non-lagged model requires more latent variables

Process Monitoring - MSPC

- Very interesting new method:

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A novel dynamic PCA algorithm for dynamic data modeling and process monitoring

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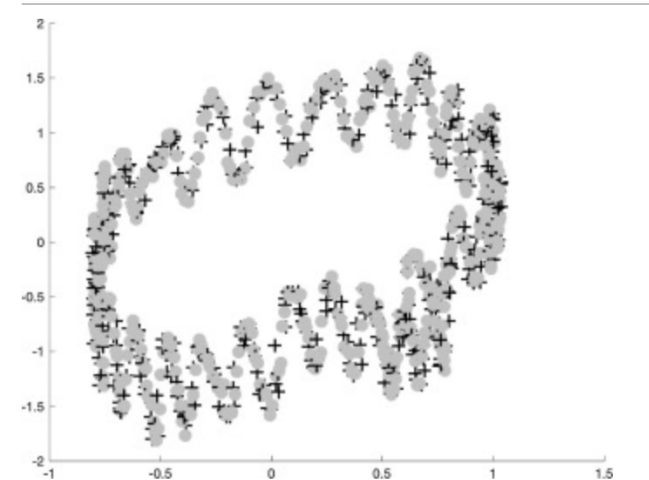


Dynamic latent variable analytics for process operations and control

Yining Dong^{a,b}, S. Joe Qin^{a,b,c}  

Process Monitoring

- DiPCA aims to capture latent-spaces that are auto-regressive.
 - **Explicit modeling of lags**
- Model semi-oscillatory behavior



Final Remarks

- The systems engineering community has and continues to develop useful computational approaches that can be exploited to accelerate product development and de-risk process operations.
- Continuous manufacturing is very amenable to the implementation of these tools.

Thank you

- Let's talk!

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