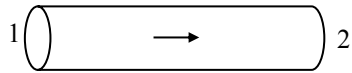


The average flow speed in a constant-diameter section of the Alaskan pipeline is 8.27 ft/s. At the inlet, the pressure is 1200 psig and the elevation is 150 ft; at the outlet, the pressure is 50 psig and the elevation is 375 ft. Calculate the head loss in this section of pipeline.

SOLUTION:



Apply the Extended Bernoulli's Equation from 1 to 2.

$$\left(\frac{p}{\rho g} + \alpha \frac{\bar{v}^2}{2g} + z \right)_2 = \left(\frac{p}{\rho g} + \alpha \frac{\bar{v}^2}{2g} + z \right)_1 - H_{L,1 \rightarrow 2} + H_{S,1 \rightarrow 2} \quad (1)$$

where

$$\frac{p_2 - p_1}{\rho g} = \frac{(50 - 1200) \frac{\text{lb}_f}{\text{in}^2} \cdot 144 \frac{\text{in}^2}{\text{ft}^2}}{\underbrace{(0.9)}_{=\text{SG}_{\text{oil}}} \left(1.94 \frac{\text{slug}}{\text{ft}^3} \right) \left(32.2 \frac{\text{ft}}{\text{s}^2} \right)} = -2940 \text{ ft} \quad (2)$$

$$\left(\alpha \frac{\bar{v}^2}{2g} \right)_2 = \left(\alpha \frac{\bar{v}^2}{2g} \right)_1 \quad (\text{since the flow is fully developed and mass is conserved}) \quad (3)$$

$$z_2 - z_1 = (375 - 150) \text{ ft} = 225 \text{ ft} \quad (4)$$

$$H_{L,1 \rightarrow 2} = ? \quad (\text{This is what we're trying to find.}) \quad (5)$$

$$H_{S,1 \rightarrow 2} = 0 \quad (\text{There is no shaft work between points 1 and 2.}) \quad (6)$$

Substitute and solve for H_L .

$$H_{L,1 \rightarrow 2} = - \left(\frac{p_2 - p_1}{\rho g} \right) - (z_2 - z_1) \quad (7)$$

$$\therefore H_{L,1 \rightarrow 2} = 2940 - 225 \text{ ft} = 2720 \text{ ft} \quad (8)$$