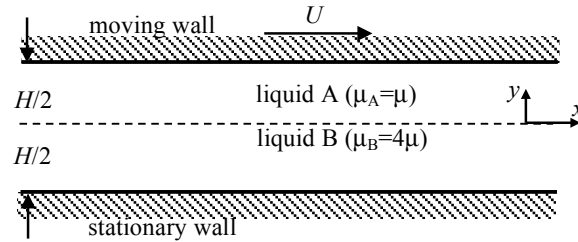


Two immiscible viscous liquids are introduced into a Couette flow device so that they form two layers of equal height as shown:



The dynamic viscosity, μ , of liquid A is one quarter that of liquid B. The upper plate is moved at a constant velocity, U , while the bottom plate remains stationary.

- Determine the velocity of the interface between the two liquids.
- Determine the “apparent viscosity” of the mixture as seen by an experimenter who believes that only one liquid is in the device.

SOLUTION:

Make several assumptions regarding the flow in each region:

- planar flow $\Rightarrow \frac{\partial}{\partial z}(\dots) = 0, u_z = 0$
- steady flow $\Rightarrow \frac{\partial}{\partial t}(\dots) = 0$
- fully-developed flow in the x -direction $\Rightarrow \frac{\partial u_x}{\partial x} = \frac{\partial u_y}{\partial x} = 0$
- no pressure gradient in the x -direction $\Rightarrow \frac{\partial p}{\partial x} = 0$
- no body forces $\Rightarrow g_x = g_y = g_z = 0$

First examine the continuity equation.

$$\underbrace{\frac{\partial u_x}{\partial x}}_{=0(\#3)} + \frac{\partial u_y}{\partial y} = 0 \Rightarrow \frac{\partial u_y}{\partial y} = 0$$

This result combined with assumptions 1 and 3 indicate that $u_y = \text{constant}$. Since there is no flow through the walls, $u_y = 0$ everywhere (call this condition #6).

Simplify the Navier-Stokes equation in the x -direction.

$$\rho \left[\underbrace{\frac{\partial u_x}{\partial t}}_{=0(\#2)} + u_x \underbrace{\frac{\partial u_x}{\partial x}}_{=0(\#3)} + \underbrace{u_y}_{=0(\#6)} \frac{\partial u_x}{\partial y} \right] = - \underbrace{\frac{\partial p}{\partial x}}_{=0(\#4)} + \mu \left(\underbrace{\frac{\partial^2 u_x}{\partial x^2}}_{=0(\#3)} + \frac{\partial^2 u_x}{\partial y^2} \right) + \rho \underbrace{g_x}_{=0(\#5)}$$

$$\frac{d^2 u_x}{dy^2} = 0 \quad (\text{Note that } u_x = u_x(y) \text{ from assumptions 1, 2, and 3.}) \quad (1)$$

Integrating twice with respect to y gives:

$$\frac{du_x}{dy} = c_1 \quad (2)$$

$$u_x = c_1 y + c_2 \quad (3)$$

Note that Eqs. (1) - (3) are valid for both fluids (A and B).

Now apply boundary conditions for each fluid.

Fluid B:

$$\text{no-slip at } y = 0 \quad \Rightarrow \quad u_{xB}(y=0) = V_i \Rightarrow c_{2B} = V_i \quad (\text{where } V_i \text{ is the interface velocity})$$

$$\text{no-slip at } y = -H/2 \quad \Rightarrow \quad u_{xB}(y = -\frac{H}{2}) = 0 \Rightarrow c_{1B} = \frac{2V_i}{H}$$

$$\therefore u_{xB} = V_i \left[2 \left(\frac{y}{H} \right) + 1 \right] \quad (4)$$

Fluid A:

$$\text{no-slip at } y = 0 \quad \Rightarrow \quad u_{xA}(y=0) = V_i \Rightarrow c_{2A} = V_i \quad (\text{where } V_i \text{ is the interface velocity})$$

$$\text{no-slip at } y = H/2 \quad \Rightarrow \quad u_{xA}(y = \frac{H}{2}) = U \Rightarrow c_{1A} = \frac{2(U - V_i)}{H}$$

$$\therefore u_{xA} = 2(U - V_i) \left(\frac{y}{H} \right) + V_i \quad (5)$$

Also note that the shear stress is continuous at the interface.

$$\begin{aligned} \mu_A \frac{du_{xA}}{dy} \Big|_{y=0} &= \mu_B \frac{du_{xB}}{dy} \Big|_{y=0} \\ \mu \frac{2(U - V_i)}{H} &= 4\mu \frac{2V_i}{H} \\ \boxed{\therefore V_i = \frac{1}{5}U} \end{aligned} \quad (6)$$

To determine the “apparent viscosity”, μ^* , note that if there was only a single fluid between the two plates with viscosity, μ^* , the shear stress exerted by the upper plate would be:

$$\tau = \mu^* \left(\frac{U}{H} \right) \quad (7)$$

With the two fluids, the shear stress exerted by the upper plate on fluid A is:

$$\tau = \mu \frac{2(U - V_i)}{H} = \mu \frac{2(U - \frac{1}{5}U)}{H} = \frac{8}{5}\mu \left(\frac{U}{H} \right) \quad (8)$$

Equating Eqns. (7) and (8) shows that the apparent viscosity is:

$$\boxed{\mu^* = \frac{8}{5}\mu} \quad (9)$$